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TABLES OF THE PROPERTIES OF STEAM

AND OTHER VAPORS

AND

TEMPERATURE-ENTROPY TABLE

BY

CECIL H. PEABODY

PROPERSOR OF NAVAL METITIFICATION AND MARKET REGISTERS OF TRUBBLES ASSESSMENT OF TRUBBLES OF TRUBBLES

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PREFACE.

THE Tables of the Properties of Steam were calculated twenty years ago to accompany the author's Thermodynamics of the Steam Engine; since that time important experimental investigations have been made by Callendar, Barnes, Knoblauch and Thomas. The tables have been recomputed, introducing this information and with certain changes which will be found to facilitate their use. All the tables for saturated steam have columns of entropy due to vaporization; and the table in metric units has been made into a conversion table by aid of which properties can be found in either metric or English units or a combination of the two systems may be used. Quinn, R. D.

The development of the steam-turbine has given prominence to adiabatic computations for steam and has emphasized the facts that the usual methods are tedious and cannot be worked inversely. To meet this difficulty various diagrams have been devised, all of which have certain inconveniences; if they have a convenient scale, they are so large as to be awkward to carry or to use; all have important problems represented by curves which render interpolation troublesome.

To facilitate the solution of all adiabatic problems (and many others) a Temperature-Entropy Table has been constructed for saturated and superheated steam. For engineering purposes the answers for such problems may be read directly from the table; greater refinement can be had by interpolation when that is thought desirable. That part of the table which refers to saturated steam may be relied upon to give the nearest unit in the last place of significant figures; the degree of accuracy to be attributed to the several properties of saturated steam can be determined from the statements of experimental data and derivation of formulæ given in the Introduction. The properties of superheated steam are given with as much accuracy as conditions warrant. This part of the table offers solutions of problems that cannot be readily obtained otherwise.

Original data are given in the Introduction so far as possible, and computations and transformations of equations are set down at length

so that each one may decide for himself what degree of accuracy he shall attribute to the properties and methods presented.

The actual work of recomputing the Tables of Properties of Steam and of constructing the Temperature-Entropy Table has been done by Mr. Harold A. Everett, S.B., who has also read the proofs. How much that means can be appreciated by those familiar with such undertakings. C. H. P.

SEPTEMBER, 1907.

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PROPERTIES OF STEAM AND OTHER VAPORS.

INTRODUCTION.

For engineering purposes steam is generated in a boiler which is partially filled with water, and arranged to receive heat from the fire in the furnace.

The ebullition is usually energetic, and more or less water is mingled with the steam; but if there is a fair allowance of steam space over the water, and if proper arrangements are provided for withdrawing the steam, it will be found when tested to contain a small amount of water, usually between half a per cent and a per cent and a half. Steam which contains a considerable percentage of water is passed through a separator which removes almost all of it. Such steam is considered to be approximately dry.

If the steam is quite free from water it is said to be dry and saturated; steam from a boiler with a large steam space and which is making steam very slowly is nearly if not quite dry.

Steam which is withdrawn from the boiler may be heated to a higher temperature than that found in the boiler, and is then said to be superheated.

Saturated Steam. — Our knowledge of the properties of saturated steam and other vapors is due mainly to the experiments of Regnault,* who determined the relations of the temperature and pressure, the total heat of vaporization, and the heat of the liquid for many volatile liquids. Since his time, Rowland's determination of the mechanical equivalent of heat has given a more exact determination of the specific heat of water at low temperatures, and recently Dr. Barnes has given a very precise determination of that property for water. Again, certain work by Knoblauch, Linde and Klebe, has given us a good knowledge of the properties of superheated steam which can be extended to give the specific volumes of saturated steam over a considerable range of temperature; in the proper place a comparison will be made with the usual theoretical computations for volumes.

^{*} Mémoires de l' Institut de France, etc., tome xxvi.

Pressure of Saturated Steam. — As a conclusion from all the end on the tension of saturated steam, Regnault * gives the following the steam of the s

PRESSURE
MM. OF MERCURY.
0.32
1.29
4.60
23.55
91.98
288.50
760.00
2030.0
4651.6
9426.
17390.
0.91
54.91

From these data he calculated, by the aid of seven-place : the following formulæ, which give the pressure in millimetres for any temperature in degrees Centigrade:—

A. For steam from
$$-32^{\circ}$$
 to 0° C,
 $p = a + b\alpha^{n}$.
 $a = -0.08038$.
 $\log b = 9.6024724 - 10$.
 $\log \alpha = 0.033398$.
 $n = 32^{\circ} - t$.

B. For steam from 0° to 100° C,
$$\log p = a - b\alpha^n + c\beta^n$$
.
 $a = 4.7384380$.
 $\log b = 0.6116485$.
 $\log c = 8.1340339 - 10$.
 $\log \alpha = 9.9967249 - 10$.
 $\log \beta = 0.006865036$.

^{*} Memoires de l' Insitut de France, etc., tome xxi.

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ercury

iments

ata: --

D.

tables of the pressures of saturated steam for temperatur to 100° C. The formula D was calculated from the da for the temperatures -20° , $+40^{\circ}$, 100° , 160° , and 22° intended to represent the whole range of experiments. B instead of formula C, he calculated the pressures set dov for temperatures from 100° C. to 220° C. In the calc constants and in their application to computations of pretemperatures, there is an inevitable loss of accuracy so the not agree satisfactorily with the original data.

By aid of the formulæ A and B, Regnault calculated

Equations for the Pressure of Steam at Paris. — In view statements, it appeared desirable to re-calculate the cons tions B and C, with a degree of accuracy that should exc as to the reliability of the results. Accordingly, the loga were taken from Vega's ten-place table, and then the re calculations were carried on with natural numbers, ch pendent methods, with the following results: -

For steam from o° to 100° C, $\log p = a - b\alpha^n + c\beta^n.$ a = 4.7393622142. $\log b = 0.6117400190.$ $\log c = 8.1320378383 - 10.$ $\log \alpha = 9.996725532820 - 1$ $\log \beta = 0.006864675924$. n=t.

C. For steam from 100° to 220° C,

For steam from - 20° to 220° (

 $\log p = a - b\alpha^n - c\beta^n.$ a = 6.2640348. $\log b = 0.1397743.$ $\log c = 0.6924351.$

 $\log \alpha = 9.994049292 - 10.$ $\log \beta = 9.998343862 - 10.$

n = t + 20.

 $\log p = a - b\alpha^n + c\beta^n.$ a = 5.4583895. $\log b = 0.4121470.$ $\log c = 7.7448901 - 10.$ $\log \alpha = 9.997412127 - 10.$ $\log \beta = 0.007590697.$ n = t - 100

C. For steam from 100° to 220° C,
$$\log p = a - b\alpha^n + c\beta^n$$
.

 $a = 5.4574301234$.

 $\log b = 0.4119787931$.

 $\log c = 7.7417476470 - 10$.

 $\log \alpha = 9.99741106346 - 10$.

 $\log \beta = 0.007642489113$.

 $n = t - 100$.

To show the degree of accuracy attained, the following tables are given:—

Equation B.

CALCULATED
37199097
96369346
46014587
88081365

Equation C.

t.	p.	LOG p FROM TABLE OF LOGARITHMS.	LOG p CALCULATED BY EQUATION.
100	760.00	2.8808135923	
130	2030.0	3.3074960379	3.307496036
160	4651.6	3.6676023618	3.667602359
190	9426	3.9743274354	3.974327428
220	17390	4. 2402995820	4.240299575

The results from Equation C are quite satisfactory; for the errors come in the ninth place of decimals, and one place of decimals is unavoidably lost in the application of the formula. Equation B was calculated after Equation C and the numerical work was not carried to so large a number of decimal places. For the calculation of tables, the constants are carried to seven places of significant figures only; this gives six significant figures in the result, of which five are recorded in the tables.

Pressure of Steam at Latitude 45°. — French System. — It is customary to reduce all measurements to the latitude of 45°, and to sea-level. The standard thermometer should then have its boiling and freezing points

determined under, or reduced to such conditions. The value of g, the acceleration due to gravity, is, at Paris, latitude 48° 50′ 14″ and 60 metres above sea-level, 9.809218 metres; and at 45°, and at sea-level, it is 9.806056 metres. Consequently, 760 mm. of mercury at 45° gives a pressure equal to that of 759.755 mm. at Paris; and this corresponds to a temperature of 99°.991 C.

In other words, the thermometer which is standard at 45° has each degree 0.99991 of the length of the degree of a thermometer standard at Paris.

To reduce Equation B to 45° latitude, we have

$$\log p = a + \log \frac{980.9218}{980.6056} - b\alpha^{0.99991t} + c\beta^{0.99991t};$$

and for Equation C,

$$\log p = a + \log \frac{980.9218}{980.6056} - b\alpha^{(0.99991t_100)} + c\beta^{(0.99991t_100)}$$

$$= a + \log \frac{980.9218}{980.6056} - b\alpha^{-0.009} \alpha^{0.99991} (t_{-100}) + c\beta^{-0.009} \beta^{0.99991(t_{-100})}.$$

The resulting equations which were used in calculating Table III are

$$\log p = a_1 - b\alpha_1^n + c\beta_1^n.$$

$$a_1 = 4.739502.$$

$$\log b = 0.6117400.$$

$$\log c = 8.13204 - 10.$$

$$\log \alpha_1 = 9.996725828 - 10.$$

$$\log \beta_1 = 0.0068641$$
.

$$n = t$$
.

C. For steam from 100° to 220° C. at 45° latitude,

$$\log p = a_1 - b_1 \alpha_1^n + c_1 \beta_1^n.$$

$$a_1 = 5.457570.$$

$$\log b_1 = 0.4120021.$$

$$\log c_1 = 7.74168 - 10.$$

$$\log \alpha_1 = 9.997411296 - 10.$$

$$\log \beta_1 = 0.0076418.$$

$$n=t-100.$$

Pressure of Steam at Latitude 45°. — English System. — To reduce the equations for the pressure of steam, so that they will give the pressures in pounds on the square inch for degrees Fahrenheit, there are required the comparison of measures of length, and of weight, the comparison of the scales of the thermometers, and the specific gravity of mercury.

Professor Rogers * gives for the length of the metre, 39.3702 inches.

Professor Miller † gives for the weight of one kilogram, 2.20462125 pounds.

Regnault gives, for the weight of one litre of mercury, 13.5959 kilograms. The degree Fahrenheit is § of the length of the degree Centigrade.

Let
$$k = \frac{13.5050 \times 2.204621}{30.3702}$$
;

then the equations B and C have for the reduction to degrees Fahrenheit, and pounds on the square inch,

$$\log p = a_1 + \log k - b\alpha^{n} + c\beta^{n},$$

$$\log p = a_1 + \log k - b_1\alpha_1^{n} + c_1\beta_1^{n}.$$

The resulting equations, which were used in calculating Table I, are :-

B. For steam from 32° to 212° F., in pounds on the square inch, $\log p = a_2 - b\alpha_2^n + c\beta_2^n.$ $a_2 = 3.025908.$ $\log b = 0.6117400.$ $\log c = 8.13204 - 10.$ $\log \alpha_2 = 9.998181015 - 10.$ $\log \beta_2 = 0.0038134.$ n = l - 32.

C. For steam from 212° to 428° F., in pounds on the square inch,

$$\log p = a_2 - b_1 \alpha_2^n + c_1 \beta_2^n.$$

$$a_2 = 3.743976.$$

$$\log b_1 = 0.4120021.$$

$$\log c_1 = 7.74168 - 10.$$

$$\log \alpha_2 = 9.998561831 - 10.$$

$$\log \beta_2 = 0.0042454.$$

$$n = t - 212.$$

^{*} Proceedings of the Am. Acad. of Arts and Sciences, 1882-83, also Additional Observations, etc.

[†] Phil. Transactions, cxlvi., 1856.

All of the foregoing equations make the pressure a function of the temperature on the scale of the air-thermometer. It will be assumed that the difference between that scale and the absolute scale may be neglected.

Pressure of Other Vapors. — Regnault determined also the pressure of a large number of saturated vapors at various temperatures, and deduced equations for each. The equations and the constants as determined by him for the commoner vapors are given in the following table:

	log p	а	ь	c
Alcohol	$a - b\alpha^{n} + c\beta^{n}$ $a + b\alpha^{n} - c\beta^{n}$ $a - b\alpha^{n} - c\beta^{n}$ $a - b\alpha^{n} - c\beta^{n}$ $a - b\alpha^{n} - c\beta^{n}$	5.4562028 5.0286298 5.2253893 5.4011662 12.0962331	0 .0002284 2 .9531281	0 .0668673 0 .2857386

	log a	log β	n	Limits.
Alcohol	T.99708557 0.0145775 T.9974144 T.9977628 T.9997120	T.9409485 T.996877 T.9868176 T.9911997 T.9949780	$ \begin{array}{c} t + 20 \\ t + 20 \\ t - 20 \\ t + 20 \\ t + 20 \end{array} $	- 20°, + 150° C. - 20°, + 120° C. + 20°, + 164° C. - 20°, + 140° C. - 20°, + 188° C.

Zeuner * states that there is a slight error in Regnault's calculation of the constants for aceton, and gives instead

$$\begin{array}{ll} \log & p = a - b\alpha^n + c\beta^n; \\ & a = 5.3085419; \\ \log b\alpha^n = + 0.5312766 - 0.0026148 \, t; \\ \log c\beta^n = - 0.9645222 - 0.0215592 \, t. \end{array}$$

Differential Coefficient $\frac{dp}{dt}$.—As will be seen later, the differential coefficient $\frac{dp}{dt}$ is used in calculating the volume and density of saturated vapors.

From the general equation of the form,

$$\log p = a + b\alpha^n + c\beta^n,$$

differentiation gives

$$\frac{1}{p}\frac{dp}{dt} = \frac{1}{M^2}b\log\alpha \cdot \alpha^n + \frac{1}{M^2}c\log\beta \cdot \beta^n,$$

in which M is the modulus of the common system of logarithms.

^{*} Mechanische Warmetheoric.

PROPERTIES OF STEAM AND OTHER VAPORS.

The equation may be written,

$$\frac{\mathrm{I}}{p}\frac{dp}{dt}=A\alpha^n+B\beta^n.$$

The calculation of the values of the constants gives the following results latitude 45°:—

French units.

B. For o° to 100° C., mm. of mercury,

$$\log A = 8.8512729 - 10.$$

$$\log B = 6.69305 - 10.$$

$$\log \alpha_1 = 9.996725828 - 10.$$

$$\log \beta_1 = 0.0068641$$
.

C. For 100° to 220° C., mm. of mercury,

$$\log A = 8.5495158 - 10.$$

$$\log B = 6.34931 - 10.$$

$$\log \alpha_1 = 9.997411296 - 10.$$

$$\log \beta_1 = 0.0076418$$
.

English units.

B. For 32° to 212° F., pounds on the square inch,

$$\log A = 8.5960005 - 10.$$

$$\log B = 6.43778 - 10.$$

$$\log \alpha_2 = 9.998181015 - 10.$$

$$\log \beta_2 = 0.0038134.$$

C. For 212° to 428° F., pounds on the square inch,

$$\log A = 8.2942434 - 10.$$

$$\log B = 6.09403 - 10.$$

$$\log \alpha_2 = 9.998561831 - 10.$$

$$\log \beta_2 = 0.0042454.$$

The following table gives values for several other vapors:

	Sign.		Log (Aan)	Log (Bβn)			
	Aan	Вβп					
cohol	+++++	-++++	$\begin{array}{c} -1 \ .1720041 - 0 \ .0029143 \ t \\ -1 \ .3396624 - 0 \ .0031223 \ t \\ -1 \ .3410130 - 0 \ .0025856 \ t \\ -1 \ .4339778 - 0 \ .0022372 \ t \\ -1 \ .8611078 - 0 \ .0002880 \ t \\ -1 \ .3268535 - 0 \ .0026148 \ t \\ t, \ temperature \ C. \end{array}$	$\begin{array}{l} -2.9992701 - 0.0590515t\\ -4.4616396 + 0.0145775t\\ -2.0667124 - 0.0131824t\\ -2.0511078 - 0.0088003t\\ -1.3812195 - 0.0050220t\\ -1.9064582 - 0.0215592t \end{array}$			

Standard Temperature. — It is customary to refer all calculations for sees to the standard conditions of the pressure of the atmosphere (760 mm, mercury) and to the freezing-point of water. Formerly the freezing-point was taken as the standard temperature for water and steam as even by it is the initial point for tables of the properties of saturated vapors, at the investigation of the mechanical equivalent of heat by Rowland sulted in a determination of the specific heat of water with much greater elicacy than is possible by Regnault's method of mixtures, and showed at the freezing-point is not well adapted for the standard temperature r water. It has been the habit of many physicists for many years to ke 15° C. as the standard temperature, and this corresponds substantally with 62° F., at which the English units of measure are standard.

Mechanical Equivalent of Heat. — The most authoritative determination of the mechanical equivalent of heat appears to be that by Rowland,* om which the work required to raise the temperature of one pound of ater from 62° to 63° F. is

778 foot-pounds.

This is equivalent to

427 metre kilograms

the metric system. Since his experiments were made this important hysical constant has been investigated by several experimenters, and so a recomputation of his results has been made after a recomparison his thermometers. The conclusion appears to be that his results may a little small, but the differences are not important, and it is not certain at the conclusion is valid. There seems, therefore, no sufficient reason rechanging the accepted values given above.

Specific Heat of Water. — The most reliable determination of the ecific heat of water is that by Dr. Barnes,† who used an electrical ethod devised by Professor Callendar and himself, and who extended e method to and below freezing-point by carefully cooling water without e formation of ice to — 5° C. This method gives relative results with cat refinement, and gives also a good confirmation of Rowland's deterination of the mechanical equivalent of heat. Dr. Barnes reports lues of the specific heat of water up to 95° C. In the following tables results are quoted from 0° to 55° C.; from 55° to 95° his results have

^{*} Proc. Am. Acad., vol. xv. (N. S. vii), 1879.

[†] Physical Review, vol. xv, p. 71, 1902..

been slightly increased to join with results determined by recomputing Regnault's experiments on the heat of the liquid for water (which experiments range from 110° C. to 180° C.) by allowing for the true specific heat at low temperature from Dr. Barnes's experiments. The maximum effect of modifying Dr. Barnes's results is to increase the heat of the liquid at 95° by one-tenth of one per cent.

Temperature.		Specific	Temperature.		Temperature.		Specific	Temp	enture.	Buccifia
o.	F.	fleat.	C.	r.	float.	(* ,	г.	Ilmat.		
0 5 10 15 20 25 30 35 40	32 41 50 59 68 77 86 95 104	1 .0094 1 .00530 1 .00230 1 .00030 0 .99895 0 .99759 0 .99735 0 .99735	45 50 55 60 65 70 75 80 85	113 122 131 140 149 158 167 176 188	0.99760 0.99800 0.99860 0.99940 1.00040 1.00150 1.00275 1.00415	90 95 100 120 140 160 180 200 220	104 103 212 218 284 320 356 392 428	1 00705 1 00855 1 01010 1 01020 1 02230 1 02850 1 03475 1 04100 1 04760		

Heat of the Liquid. — The heat required to raise one unit of weight of any liquid from freezing-point to a given temperature is called the heat of the liquid at that temperature; and also at the corresponding pressure. Since the specific heat for water varies we may obtain the heat of the liquid by integration as indicated by the equation

$$q \approx \int c dt$$
.

In order to use this equation it would be necessary to obtain an empirical equation connecting the specific heat with the temperature; such an equation has not been proposed and would probably be complex. Another method is to draw a curve with temperatures as abscisse and specific heats as ordinates and integrate graphically. The fact that the specific heat is nearly equal to unity at all temperatures and that consequently the heat of the liquid for the Centigrade thermometer is not very different from the temperature suggests the following method:

Let
$$c = 1 + k$$

where k is the difference between the specific heat and unity at any temperature, k being positive or negative as the case may be.

$$q = t + \int kdt,$$

which may be obtained by plotting values of k as ordinates and integrating graphically, which will have the advantage that the required curve may be drawn to a large scale and give correspondingly accurate results. The values for the heat of the liquid for water in the tables were obtained in this way.

The following table gives equations for the heats of the liquid for various substances as determined by Regnault:

HEAT OF THE LIQUID.

Alcohol
$$q = 0.54754t + 0.0011218t^2 + 0.00002206t^3$$

Ether $q = 0.52901t + 0.0002959t^2$
Chloroform . . . $q = 0.23235t + 0.0000507t^2$
Carbon bisulphide . $q = 0.23523t + 0.0000815t^2$
Carbon tetrachloride $q = 0.19798t + 0.0000906t^2$
Aceton $q = 0.50643t + 0.0003965t^2$

Total Heat. — This term is defined as the heat required to raise a unit of weight of water from freezing-point to a given temperature, and to entirely evaporate it at that temperature. The experiments made by Regnault were in the reverse order; that is, steam was led from a boiler into the calorimeter and there condensed. Knowing the initial and final weights of the calorimeter, the temperature of the steam, and the initial and final temperatures of the water in the calorimeter, he was able, after applying the necessary corrections, to calculate the total heats for the several experiments.

As a conclusion of the work, he gives the following values for the total heats:—

IOO	б10	By equation, 609.6
63°	625	625.2
1000	637	
195°	666	

Assuming an equation of the form

$$H=A+Bt,$$

Regnault calculated the constants from the values given for 100° and 195°, and gives the equation

$$H = 606.5 + 0.305t$$
.

For the Fahrenheit scale the equation becomes

$$H = 1091.7 + 0.305 (t - 32).$$

An investigation of the original experimental results, allowing for the true specific heat of the water in the calorimeter, showed that the probable errors of the method of determining the total heat were larger than the deviations of the true specific heats from unity, the value assumed by Regnault; and, further, it appeared that his equation represents our best knowledge of the total heat of steam. There appears to be no reason for changing this equation till new experimental values shall be supplied. The deviation of individual experimental results from corresponding computations by the equation is likely to be one in five hundred. There is further some uncertainty whether the method of drawing steam from the boiler did not involve some error due to entrained moisture. The best check upon Regnault's results is a comparison with Knoblauch's work on superheated steam.

The total heats for various fluids are given by the following equations:

Ether	H = 94	$+ 0.45t - 0.00055556t^2$
Chloroform	H = 67	+ 0.1375t
Carbon bisulphide	H = 90	$+ 0.14601t - 0.0004123t^2$
Carbon tetrachloride .	H = 52	$+ 0.14625t - 0.000172t^2$
Aceton	H = 140.5	$t + 0.36644t - 0.000516t^2$

Specific Volume of Liquids. — The coefficient of expansion of most liquids is large as compared with that of solids, but it is small as compared with that of gases or vapors. Again, the specific volume of a vapor is large compared with that of the liquid from which it is formed. Consequently the error of neglecting the increase of volume of a liquid with the rise of temperature is small in equations relating to the thermodynamics of a saturated vapor, or of a mixture of a liquid and its vapor when a considerable part by weight of the mixture is vapor. It is, therefore, customary to consider the specific volume of a liquid to be constant.

Table XII, giving the specific volumes of various liquids, was taken from the *Phys.-Chem*. Tabellen of Landolt and Börnstein.

Volume of Water. — Table XIII gives the volumes of water compared with its volume at 4°. From 0° to 100° C., the values are those given by

INTRODUCTION.

Rossetti. Above 100°, the values are those calculated by the equation given by Hirn.*

Volumes of Liquids. — The volumes of liquids at high temperature compared with the volume at freezing-point, are represented by following equations given by Hirn: —

```
Water 100° C. to 200° C. (vol. at 4° C. =
                                                                          Logs.
  unity) . . . . . . . . . . . . v = 1 + 0.00010867875t
                                                                     6.0361445-
                                          +0.0000030073653t^2
                                                                     4.4781862-
                                          +0.0000000028730422t^3
                                                                      1.4583419-
                                          -0.00000000000066457031t^4 8.8225409
Alcohol 30° C. to 160° C. (vol. at 0° C. =
                                                                     6.8685991 -
  unity) . . . . . . . . . . . . . v = 1 + 0.00073892265t
                                                                     3.0233492-
                                          +0.00001055235t^2
                                          -0.000000092480842t^3
                                                                     2.9660517~
                                         +0.00000000040413507t^{4}
                                                                     0.6065278 -
Ether 30° C. to 130° C. (vol. at 0^{\circ} C. =
                                                                     7.1299817-
                   v = 1 + 0.0013489059t
                                          +0.0000065537t^2
                                                                     4.8164866 -
                                          -0.000000034490756t^3
                                                                     2.5377028-
                                         +0.00000000033772062t^{4}
                                                                     0.5285571 -
Carbon bisulphide 30° to 160° C. (vol. at
  0^{\circ} C. = unity) . . . . . . . . v = 1 + 0.0011680559t
                                                                     7.0674636-
                                                                     4.2172103 -
                                         +0.0000016489598t^2
                                         -0.00000000081119062t^{3}
                                                                     0.9091229 -
                                         \pm 0.000000000000046589t^4
                                                                     8.7849494 --
Carbon tetrachloride 30° to 160° C. (vol.
                      v = 1 + 0.0010671883t
    at 0^{\circ} C. = unity)
                                                                     7 .0282409 -
                                         +0.0000035651378t^2
                                                                     4 .5520763 -
                                          -0.00000014949281t^{8}
                                                                     2.1746202-
                                         +0.000000000085182318t^4 9.9303494-
```

Heat of Vaporization. — If the heat of the liquid be subtracted from the total heat, the remainder is called the heat of vaporization, and represented by r, so that

$$r = H - q$$
.

Internal and External Latent Heat. — The heat of vaporization ov comes external pressure, and changes the state from liquid to vapor constant temperature and pressure. Let the specific volume of a saturated vapor be s, and that of the liquid be σ , then the change volume is $s - \sigma = u$, on passing from the liquid to the vaporous sta The external work is

$$p(s-\sigma)=pu,$$

and the corresponding amount of heat, or the external latent heat, is

$$A p (s - \sigma) = A p u$$

A being the reciprocal of the mechanical equivalent of heat.

* Annales de Chimie et de Physique., 1867.

The heat required to do the disgregation work, or the internal latent heat, is

$$\rho = r - A \rho u$$
.

Specific Volume and Density of Steam. — On account of the great difficulty of direct determination of the weight of saturated steam, it is customary to calculate the specific volume of steam by aid of the following equation, derived by the application of the principles of thermodynamics to the general equation representing the properties of saturated vapor: —

$$s = \frac{r}{AT} \cdot \frac{1}{\frac{dp}{dt}} + \sigma,$$

in which A is the reciprocal of the mechanical equivalent of heat, T is the temperature from the absolute zero, and σ is the volume of one unit of weight of the liquid from which the vapor is formed. The differential coefficient $\frac{dp}{dt}$ can be calculated by aid of the equations on page 8.

The absolute temperature is obtained by adding 273 to the temperature in degrees Centigrade, or 459.5 to the temperature in degrees Fahrenheit.

The volumes and densities of saturated steam given in Tables I and III were calculated by this method.

It is of interest to consider the degree of accuracy that may be expected

from this method of calculating the density of saturated vapor. The value of r depends on H and q, the total heat and the heat of the liquid; the latter is now well known, but the total heat is probably in doubt to the extent of $\sigma_0^*\sigma_0^*$ and may be more. The absolute temperature T appears to be better known and may be subject to an error of no more than $\tau_0^*\sigma_0^*$ or $\tau_0^*\sigma_0^*$; and the mechanical equivalent $\frac{1}{A}$ of heat is perhaps as well determined as the absolute temperature. The least satisfactory factor in the expression is the differential coefficient $\frac{dp}{dt}$, which is derived by differentiating one of the empirical equations on pages 5 and 6. It is true that the resulting equations on page 8 afford a ready means of computing values of the coefficient with great apparent accuracy, but some idea of the essential vagueness of the method may be obtained by comparing computations of the specific volume of saturated steam at 212° C., a point for which

either equation B_1 or equation C_1 will give the pressure as 14.6967 pounds per square inch. The specific volume by aid of equation on page 14, using equation B_1 for determining the differential coefficient, is 26.62, while the differential coefficient from equation C_1 gives 26.71; the discrepancy is about $\frac{1}{300}$; or if the mean 26.66 be taken as the probable value, either computed value is subject to an error of $\frac{1}{600}$.

Quality or Dryness Factor. — All the properties of saturated steam, such as pressure, volume, and heat of vaporization, depend on the temperature only, and are determinable either by direct experiment or by computation, and are commonly taken from tables calculated for the purpose.

Many of the problems met in engineering deal with mixtures of liquid and vapor, such as water and steam. In such problems it is convenient to represent the proportions of water and steam by a variable known as the quality or the dryness factor; this factor, x, is defined as that portion of each pound of the mixture which is steam; the remnant, x - x, is consequently water.

Specific Volume of Wet Steam. — If a pound of a homogeneous mixture of water and steam is x part steam, then the specific volume may be represented by

$$v = xs + (1 - x) \sigma = xu + \sigma$$

where u is the increase of volume due to vaporization.

Intrinsic Energy. — It has been shown that the heat of vaporization can be broken into the two parts A pu and ρ , the first being required to do external work and the second internal work; the latter part together with the heat of the liquid form the heat equivalent of the intrinsic energy so that

$$E=\frac{\mathrm{I}}{A}(\rho+q),$$

or if only x part is vaporized

$$E=\frac{\mathrm{I}}{A}\left(x\rho+q\right).$$

Entropy. — In the discussion of steam-engines or other heat engines, it is convenient to begin by considering the way in which steam (or other working substance) would behave if the cylinder were made of non-conducting material. Afterwards the effect of the actual material can

be investigated. The expansion line which an indicator would draw under such conditions is called an adiabatic line. Calculations for adiabatic changes of steam can be made by aid of a special function devised for the purpose and called entropy. A discussion of adiabatic actions and of entropy can be found in any text-book on Thermodynamics; for example, on pages 17 and 31 of the Thermodynamics of the Steam Engine by the author. It is sufficient for our present purpose to consider that entropy can be expressed numerically and that the numerical values enter into the calculation of certain engineering problems.

It is customary to represent entropy in general by ϕ , but entropy may be represented by θ in dealing with a liquid like water.

The second law of thermodynamics enables us to deduce the equation

$$d\phi = \frac{dQ}{T},$$

in which dQ is an infinitesimal amount of heat added at the absolute temperature T. This equation is the basis of the calculation of entropy.

Entropy of Vaporization. — If a pound of steam at the temperature t (or absolute temperature T) is partially vaporized, the heat expended for that purpose is xr; the temperature being constant the above equation may be directly integrated giving

$$\phi - \phi_0 = \frac{xr}{T} = x \frac{r}{T}.$$

In Tables I, II, and III values of $\frac{r}{T}$ are given for each degree or each pound as the case may be.

Entropy of the Liquid. — The increase of entropy due to heating water from freezing-point to any temperature t may be represented by the equation

$$\theta = \int \frac{dq}{T} = \int \frac{cdt}{T}.$$

Inspection of the table on page 10 shows that the specific heat of water is but little larger than unity; it is convenient to represent it by the expression

$$c = 1 + k$$
;

this expression introduced in the preceding equation gives

$$\theta = \int \frac{dt}{T} + \int \frac{kdt}{T} = \log_e \frac{T}{T_0} + \int_{t_+}^t k \, \frac{dt}{T},$$

hich t_0 and T_0 are the temperature by the thermometer of freezing, the corresponding absolute temperature. The first part of the expression for the entropy of the liquid can be computed readily, the second part (which is small) can be determined graphically great precision. This method was used for the tables of the erties of saturated steam.

o obtain the entropy of any liquid named on page rr, we may first rentiate the proper equation to obtain dq and then integrate as eated by the equation

$$\theta = \int \frac{dq}{T}$$

he values given in Tables IV to IX were determined in this way, those for the two following tables were computed in the same ner.

ntropy of a Mixture of a Liquid and its Vapor. — The increase in opy due to heating a unit of weight of a liquid from freezing-point ne temperature t and then vaporizing v portion of it is

$$\theta + \frac{\alpha r}{T}$$
.

re θ is the entropy of the liquid, r is the heat of vaporization, and T is absolute temperature. For steam $\frac{r}{T}$ may be taken from the tables; other vapors it must usually be calculated.

or any other state determined by x_i and t_i we shall have, for the case of entropy above that of the liquid at freezing-point,

$$\frac{x_1r_1}{T_1} + \theta_1.$$

he change of entropy in passing from one state to another is

$$\phi - \phi_1 = \frac{xr}{T} + \theta - \frac{x_1r_1}{T_1} - \theta_1.$$

When the condition of the mixture of a liquid and its vapor is given by the pressure and value of x, then a table giving the properties at each pound may be conveniently used for this work.

Adiabatic Equation for a Liquid and its Vapor. — During an adiabatic change the entropy is constant, so that the preceding equation gives

$$\frac{x_1 r_1}{T_1} + \theta_1 = \frac{x_2 r_2}{T_2} + \theta_2 \cdot$$

When the initial state, determined by x_1 and t_1 or p_1 , is known and the final temperature t_2 , or the final pressure p_2 , the final value x_2 may be found by this equation. The initial and final volumes may be calculated by the equations

$$v_1 = x_1 u_1 + \sigma \text{ and } v_2 = x_2 u_2 + \sigma.$$

Tables of the properties of saturated vapor commonly give the specific volume s but

$$s = u + \sigma$$
.

The value of σ for water is 0.016, and for other liquids will be found in Table XII.

For example, one pound of dry steam at 100 pounds absolute has the following properties found in Table II:

$$t_1 = 327^{\circ}.6 \text{ F.}$$
 $\frac{r_1}{T_1} = 1.1228 \ \theta_1 = 0.4743 \ s_1 = 4.409 \ x_1 = 1.1228 \ \theta_2 = 0.4743 \ s_3 = 4.409 \ x_4 = 1.1228 \ \theta_3 = 0.4743 \ s_4 = 1.1228 \ \theta_4 = 0.4743 \ s_5 = 1.1228 \ \theta_5 = 1.1228 \ \theta_7 = 1.1228 \ \theta_7$

If the final pressure is 15 pounds absolute, we have

$$t_2 = 213^{\circ}$$
.0 F. $\frac{r_2}{T_2} = 1.4358$ $\theta_2 = 0.3141$ $s_2 = 26.21$

whence

$$1.5971 = 1.4358 x + 0.3141$$

 $\therefore x_2 = .8935$

The initial and final volumes are

$$v_1 = s_1 = 4.409$$

 $v_2 = x_2 u_2 + \sigma = 23.40$

Such a problem cannot be solved inversely, that is we cannot assume a final volume and determine directly the temperature and pressure corresponding. The Temperature-Entropy Table to be explained later however, give an approximate solution directly, and an exact solution aterpolation.

eternal Work during Adiabatic Expansion. — Since no heat is transed during an adiabatic expansion, all of the intrinsic energy lost is ged into external work, so that

$$W = E_1 - E_2 = \frac{1}{A} (q_1 - q_2 + x_1 \rho_1 - x_2 \rho_2)$$

or example, the external work of one pound of dry steam in expanding batically from 100 pounds to 15 pounds absolute is

$$W = 778 (208.1 - 181.3 + 1 \times 802.4 - 0.8035 \times 80.30)$$

 $W = 121.3 \times 778 = 94,370$ foot-pounds.

tention should be called to the unavoidable defect of this method of dation of external work during adiabatic expansion, in that it depends aking the difference of quantities which are of the same order of nitude. For example, the above calculation appears to give four as of significant figures, while, as a matter of fact, the total heat H which ρ is derived is affected by a probable error of $\frac{1}{500}$ or perhaps as Both the quantities

$$q_1 + x_1\rho_1$$
 and $q_2 + x_2\rho_2$

a numerical value somewhere near 1000, and an error of $\frac{1}{500}$ is ly equivalent to two thermal units, so that the probable error of the re-calculation is nearly two per cent. For a wider range of temperathe error is less, and for a narrower range it is of course larger. This ser should be borne in mind in considering the use of approximate ands of calculation, for example, by aid of a diagram like the temture-entropy diagram.

eat Contents. — The heat required to raise one pound of water from sing-point to a given temperature t corresponding to a pressure p, to vaporize a part x at that pressure is represented by

$$xr + q$$
;

quantity may be called the heat contents.

Rankine's Cycle. — An important investigation for the steam-engine may be made by aid of the accompanying figure which represents the

Fig. 1

quality x_1 is

indicator diagram from a steam-engine without clearance and with a nonconducting cylinder. admitted at an absolute pressure p_i from a to b; adiabatic expansion follows from b to c; finally the steam is exhausted from c to d at the pressure p_2 . The

external work during admission for one pound of steam having the

$$p_1 v_1 = p_1 (x_1 u_1 + \sigma);$$

the external work during expansion is

$$E_1 - E_2 = \frac{1}{A} (q_1 - q_2 + x_1 \rho_1 - x_2 \rho_2);$$

and the external work during exhaust is

$$p_2 v_2 = p_2 \left(x_2 u_2 + \sigma \right)$$

which must be subtracted since it is done by the piston on the steam. The effective work of the cycle is

$$p_{\scriptscriptstyle 1}v_{\scriptscriptstyle 1} + E_{\scriptscriptstyle 1} - E_{\scriptscriptstyle 2} - p_{\scriptscriptstyle 2}v_{\scriptscriptstyle 2}$$

or substituting the proper values

$$W = \frac{1}{A} (q_1 + x_1 \rho_1 + A \rho_1 x_1 u_1 - q_1 - x_2 \rho_2 - A \rho_2 x_2 u_2) + (p_1 + p_2) \sigma;$$

the last term is small and may be dropped.

Remembering that

$$r=\rho+Apu,$$

we have

$$W = \frac{1}{A} (q_1 + x_1 r_1 - q_2 - x_2 r_2) .$$

The values of r and q may be taken from Tables I, II, or III, and the value of x_2 can be determined by aid of the equation

$$\frac{x_{1}r_{1}}{T_{1}} + \theta_{1} = \frac{x_{2}r_{2}}{T_{2}} + \theta_{2}.$$

By the first law of thermodynamics the difference between the heat supplied to an engine and the heat rejected, is equivalent to the work done, provided there are no losses; therefore,

$$Q_1 - Q_2 = x_1 r_1 + q_1 - (x_2 r_2 + q_2).$$

This most important conclusion can be stated as follows: the heat anged into work by a steam-engine working on Rankine's cycle, is ual to the difference in the heat contents of the steam supplied to and hausted by the engine.

This same expression is found in the discussion of steam-turbines.

Problems of this nature can be solved immediately by aid of the emperature-Entropy Table.

Superheated Steam.—A dry and saturated vapor, not in contact with e liquid from which it is formed, may be heated to a temperature greater an that corresponding to the given pressure for the same vapor when turated; such a vapor is said to be superheated. When far removed om the temperature of saturation, such a vapor follows the laws of erfect gases very nearly, but near the temperature of saturation the eparture from those laws is too great to allow of calculations by them r engineering purposes.

All the characteristic equations that have been proposed have been erived from the equation

$$pv = RT$$
,

hich is very nearly true for the so-called perfect gases at moderate temeratures and pressures; it is, however, well known that the equation does of give satisfactory results at very high pressures or very low temperaires. To adapt this equation to represent superheated gas, a corrective rm is added to the right-hand side which may most conveniently be assumed to be a function of the temperature and pressure, so that calilations by it may be made to join on to those for saturated steam.

The most satisfactory characteristic equation of this sort is that given y Knoblauch,* Linde, and Klebe,

$$pv = BT - p (t + ap) \left[C \left(\frac{373}{T} \right)^8 - D \right]$$

the pressure is in kilograms per square metre, v is in cubic metres, and T is the absolute temperature by the Centigrade thermometer. The constants have the following values:

$$B = 47.10$$
, $a = 0.000002$, $C = 0.03T$, $D = 0.0052$.

In the English system of units, the pressures being in pounds per

^{*} Mitteilungen über Forschungsarbeiten, etc., Heft 21, S. 33, 1905.

square foot, the volumes in cubic feet per pound, and the temperatures in the Fahrenheit scale, we have

$$pv = 85.85 T - p (1 + 0.00000976 p) \left(\frac{150,300,000}{T^3} - 0.0833 \right)$$

The following equation may be used with the pressure in pounds per square inch:

$$pv = 0.5962 T - p (i + 0.0014 p) \left(\frac{150,300,000}{T^3} - 0.0833 \right)$$

The labor of calculation is principally in reducing the corrective term, and especially in the computation of the factor containing the temperature. Table XV gives values of this factor for each five degrees from 100° to 600° F.; the maximum error in the calculation of volume by aid of the table is about 0.4 of one per cent at 336 pounds pressure and 428° F.; that is at the upper limit of our table for saturated steam. At 150 pounds and 358° F., which is about the middle range of our table for saturated steam, the error is not more than 0.2 of one per cent, which is not greater than the probable error of the equation itself under those conditions. At lower pressures and at higher temperatures the error tends to diminish.

The following simple equation is proposed by Tumlirz* based on experiments by Battelli.

$$pv = BT - C_p,$$

where p is the pressure in kilograms per square metre, v the specific volume in cubic metres, and T the absolute temperature Centigrade. The constants to agree with Knoblauch's work should be

$$B = 47.10$$
, $C = 0.016$.

In the English system with the pressure in pounds per square foot and the volumes in cubic feet, for absolute temperatures Fahrenheit,

$$pv = 85.85 T - 0.256 p$$
.

This equation has a maximum error of 0.8 of one per cent as compared with Knoblauch's equation.

Specific Heat. — Two investigations have been made of the specific heat of superheated steam at constant pressure, one by Professor Knoblauch † and Dr. Jakob and the other by Professor Thomas

^{*} Math. Naturw. Kl. Wien, 1899, IIa S. 1058.

[†] Mitteilungen uber Forschungsarbeiten Heft 36, p. 109.

and Mr. Short; * the results of the latter's investigation have been communicated for use in this book in anticipation of the publication of the completed report.

Professor Knoblauch's report gives the results of the investigation made under his direction in the form of a table giving specific heats a various temperatures and pressures and in a diagram, which can be foun in the original memoir, and he also gives a table of mean specific heat from the temperature of saturation to various temperatures at severa pressures. This latter table is given here in both the metric system an in the English system of units.

SPECIFIC HEAT OF SUPERHEATED STEAM.

Kare	Man	cl.	and	Tab	٠,
$I \setminus \mathcal{H} U$	uuuu	ur	unu	Jako	าน

p Kg. per Sq. Cm. p Lbs. per Sq. In. ts Cent. ts Fahr.	1 14.2 99°	120°	143°	158°	169°	10 142.2 179°	187°	194°	200°	18 156.0 206°	2110
Fahr. Cent. 212° 100° 302° 150° 392° 200° 482° 250° 572° 300° 662° 350° 752° 400°	0 .462 0 .463 0 .464 0 .468	0 .478 0 .475 0 .474 0 .475 0 .477 0 .481	0 .502 0 .495 0 .492 0 .492	0 .530 0 .514 0 .505 0 .503	$\begin{array}{c} 0.532 \\ 0.517 \\ 0.512 \end{array}$	$\begin{array}{c} 0.552 \\ 0.530 \\ 0.522 \end{array}$	$\begin{array}{c} 0.570 \\ 0.541 \\ 0.529 \end{array}$	0 .588 0 .550 0 .536	0.609 0.561 0.543	0 .572 0 .550	0 .58 0 .55

The construction of this table is readily understood from the followin example: — Required the heat needed to superheat a kilogram of stear at 4 kilograms per square centimetre from saturation to 300° C. The saturation temperature (to the nearest degree) is 143° C.; so that the steam at 300° is superheated 157°, and for this is required the heat

$$157 \times 0.492 = 77.2$$
 calories.

The experiments of Professor Knoblauch were made at 2, 4, 6, and kilograms per square centimetre; the remainder of the table was obtained from the diagram which was extended by aid of cross-curves to the exteriodicated. Within the limits of the experimental work the table may have used with confidence, the greatest error being probably not more that

^{*} Thesis by Mr. Short, Cornell University.

one third of one per cent. Exterpolated results are probably less reliable than those obtained directly by Professor Thomas.

The following table gives the mean specific heat of superheated steam as measured on a facsimile of Professor Thomas's original diagram without exterpolation.

SPECIFIC HEAT OF SUPERHEATED STEAM.

Degrees of Superheat Fahr.	Pressure Lbs. per Sq. In. (Absolute.)						
	6	15	30	50	100	200	400
20° 50° 100° 150° 200° 250° 300°	0.536 0.522 0.503 0.486 0.471 0.456 0.442	0 .547 0 .532 0 .512 0 .496 0 .480 0 .466 0 .453	0 .558 0 .542 0 .524 0 .508 0 .424 0 .481 0 .468	0 .571 0 .555 0 .537 0 .522 0 .509 0 .496 0 .484	0 .593 0 .575 0 .557 0 .544 0 .533 0 .522 0 .511	0 .621 0 .600 0 .581 0 .567 0 .556 0 .546 0 .537	0.649 0.621 0.599 0.585 0.574 0.564 0.554

Here again the arrangement of the table can be made evident by an example: — Required the heat needed to superheat steam roo degrees at 200 pounds per square inch absolute. The mean specific heat from saturation is 0.557, so that the heat required is 55.7 thermal units.

Total Heat. — In the solution of problems that arise in engineering it is convenient to use the total amount of heat required to raise one pound of water from freezing-point to the temperature of saturated steam at the given pressure and to vaporize it and to superheat it at that pressure to the given temperature. This total heat may be represented by the expression

$$H = q + r + c_p (t - t_s)$$

where t is the temperature of the superheated steam, t_s is the temperature of saturated steam at the given pressure p, and q and r are the corresponding heat of the liquid and heat of vaporization. The mean specific heat c_p may usually be selected from one of the given tables without interpolation, as a small variation does not have a very large effect.

The total heats or heat contents of superheated steam in the temperature-entropy table were obtained by the following method. From Pro-

fessor Thomas's diagram giving mean specific heats, specific heats at various temperatures and at a given pressure were obtained, and the curves thus obtained were faired after a comparison with curves constructed with Professor Knoblauch's specific heats at those temperatures. These curves were then integrated graphically and the results checked by comparison with his mean specific heats.

Entropy. — By the entropy of superheated steam is meant the increase of entropy due to heating water from freezing-point to the temperature of saturated steam at the given pressure, to the vaporization and to the superheating at that pressure. This operation may be represented as follows:

$$\theta + \frac{r}{T_s} + \int_{T_s}^T \frac{c_n dt}{T}$$

in which T is the absolute temperature of the superheated steam, and T_s is the temperature of the saturated steam at the given pressure; θ and T can be taken from Table I. The last term was obtained for the temperature-entropy table by graphical integration of curves plotted with values of $\frac{c_p}{T}$ derived from the curves of specific heats at various temperatures just described under the previous section.

Properties of Sulphur Dioxide. — One of the most interesting and important applications of the theory of superheated vapors is found in the approximate calculation of properties of certain volatile liquids which are used in refrigerating-machines, and for which we have not sufficient experimental data to construct tables in the manner followed for the fluids already discussed.

All attempts in this line have followed the example of Ledoux, who made the first attempt and who naturally took for the basis of his investigations the form of equation proposed by Zeuner for superheated steam, namely,

$$pv = BT - Cp^a.$$

Investigations by Knoblauch already discussed show that this equation can be considered only a crude approximation for steam, and consequently less confidence can be placed on investigations by its aid than we formerly thought. Nevertheless, in our present condition and until more complete experimental data are available we are constrained to

use some such approximate method, and it does not appear profitable to recompute tables at this time.

Fortunately Regnault determined the relation of temperature and pressure, and gave the following equations for pressure in millimetres of mercury, the temperature being on the Centigrade thermometer.

SULPHUR DIOXIDE.	AMMONIA.
$\log p = a - b\alpha^n - c\beta^n$	$\log p = a - b\alpha^n - c\beta^n$
a = 5.6663790	a = 11.5043330
b = 3.0146890	b = 7.4503520
c = 0.1465400	c = 0.9499674
$\log \alpha = 9.9972989 - 10$	$\log \alpha = 9.9996014 - 10$
$\log \beta = 9.9872900 - 10$	$\log \beta = 9.9939729 - 10$
n = t + 28	n=t+22
Limits, $-28, +62$.	Limits, -22 , $+82$.

The corresponding equations for pressures in pounds per square inch for temperatures Fahrenheit are:

SULPHUR DIOXIDE.	AMMONIA.		
$\log p = a - b\alpha^n - c\beta^n$	$\log p = a - b\alpha^n - c\beta^n$		
a = 3.9527847	a = 9.7907380		
$\log b = 0.4792425$	$\log b = 0.8721769 - 10$		
$\log c = 9.1659562 - 10$	$\log c = 9.9777087 - 10$		
$\log \alpha = 9.9984994 - 10$	$\log \alpha = 9.9997786 - 10$		
$\log \beta = 9.99293890 - 10$	$\log \beta = 9.9966516 - 10$		
$n = t + 18^{\circ}.4 \text{ F.}$	$n = t + 7.6^{\circ} \text{ F.}$		

In the *Thermodynamics of the Steam-engine* by the author, pages 117 to 126, this calculation has been carried out with the best ascertained properties of the superheated vapors of sulphur dioxide and ammonia with the following results:

SULPHUR DIOXIDE.

AMMONIA.

French units,
$$pv = 14.5 T - 48 p^{0.22}$$
 $pv = 54.3 T - 142 p_{\frac{5}{4}}$
English units, $pv = 26.4 T - 184 p^{0.22}$ $pv = 99 T - 710 p_{\frac{1}{4}}$

The application of these equations to the vapors when saturated gives the following results:

HEAT OF VAPORIZATION.

SULPHUR DIOXIDE.

AMMONIA.

French units, r = 98 - 0.27t r = 300 - 0.8t

French units,
$$r = 98 - 0.27t$$
 $r = 300 - 0.8t$
English units, $r = 176 - 0.27(t - 32)$ $r = 540 - 0.8(t - 32)$

SPECIFIC HEAT OF THE LIQUID.

AMMONIA.

c = 0.4 c = 1.1Tables X and XI were calculated by aid of the equations written, a

SULPHUR DIOXIDE.

Tables X and XI were calculated by aid of the equations written, an may be of use for approximate calculations, in default of more reliable tables.

Other Data. — For convenience the following data are assembled:—

Weight of r litre (r cu. decimetre) of mercury . . . 13.5959 kilos. One horse power, in foot pounds per second . . . 550.

Normal pressure of the atmosphere {760 mm. of mercury. 10,333 kilos per sq. m 14.7 lbs. per sq. in.

One inch of mercury is equivalent to 0.4912 pound.

Explanation of Tables. — Table I, which in a sense is the fundamenta table for English units, has been computed by the proper equations and

methods as already explained, for each degree Fahrenheit; and may be relied upon to have no errors of calculation greater than half a unit in the last significant figure. The proper degree of accuracy to be attributed to any property may be judged from the preceding statements of data and transformations. In general, attention has been given to this matter each property being stated with the degree of accuracy considered proper avoiding superfluous figures; an exception will be found in the earlier

parts of Tables I and II where the heat of vaporization is stated to five significant figures, while the data may appear to warrant only four; but there are conveniences in keeping one decimal place throughout these tables for this property.

Table II is made by interpolation from Table I, but the work has been carried on in such a manner that it has practically the same degree of accuracy.

Table III was computed directly from the proper equation for each degree Centigrade. English equivalents are added so that ready conversions can be made from one system to the other or a combination of the two systems may be used.

Tables IV to IX were taken from "Zeuner's Mechanische Warmetheorie," making a correction for the true value of the mechanical equivalent of heat, instead of Joule's earlier value, and adding columns of entropy of the liquid.

Tables X and XI for sulphur dioxide and ammonia were calculated by the approximate method described earlier; though open to a considerable degree of error they may be used till better information can be obtained.

Tables XII and XIII do not appear to call for comment.

Table XIV has been computed to aid in reducing data from tests where pressures are recorded in inches of mercury. Pressures measured in inches of mercury are usually less than that of the atmosphere and the reading gives the vacuum, which is to be subtracted from the barometric reading to find the absolute pressure in inches of mercury. The table then gives the pressure in pounds per square inch which can be taken to Table II to find the properties of steam.

Table XV has been computed to reduce the labor of calculating the volume of superheated steam. It gives the value of the factor

$$\frac{150,300,000}{T^3} - 0.0833,$$

in Knoblauch's equation on page 21 for English units. By aid of this table the volume for a given temperature and pressure can be readily computed. The inverse calculation assuming the volume cannot be made directly, but such problems can be resolved by trial without much labor. If the pressure and volume are assumed the temperature can be found neglecting the correction term, and this will enable us to enter the table at nearly the right place.

TEMPERATURE-ENTROPY TABLE.

This table has been made to facilitate the solution of problems involving adiabatic action for steam and some other problems.

It gives for each degree Fahrenheit and for each hundredth of a unit of entropy, the quality, heat contents and specific volume, both for moist and for superheated steam. For convenience the pressures corresponding to the temperatures are also given.

The properties named may be more exactly stated as follows:—

Moist Steam

1

1

Quality, x; the portion of a pound which is steam. Heat contents, xr + q. Specific volume, $v = xu + \sigma$.

Superheated Steam

Quality, $t - t_{sat}$; the number of degrees of superheating. Heat contents, $r + q + c_p$ $(t - t_{sat})$. Specific volume, v.

The table is arranged in groups of eight triple columns, four on each of two pages, which face each other. Such a group is continued from the highest to the lowest temperature; then comes the next group of eight triple columns, etc. Commonly the solution of a given problem may be found in a single group or in two successive groups. It is important to note this feature of arrangement to avoid aimless search.

For engineering purposes it will be found sufficient to take the nearest temperature of saturated steam and the nearest column of entropy, and to take from the corresponding place in the table the required quantities. At the highest temperature (420° F.), the error of half a degree of temperature corresponds to an error of a pound and a half in pressure; the other properties have the following errors: heat contents 0.15 of a B.T.U., and specific volume 0.008 of a cubic foot, which latter amounts to half of one per cent. At lower temperature the variation of pressure is progressively less, but the other two properties named are affected to about the same degree. Such errors if they were carried into computations and united with other errors in such a way as to occasion greater uncertainties would be liable to be inconvenient; but when found in the

final results of computations and their limits known, are not likely to cause trouble.

On the other hand the error of half a hundredth of a unit of entropy will at 400° correspond to 0.51 of a per cent of priming or moisture in the steam, and will carry a like error into all of the work. This uncertainty of using the table without interpolation will be nearly the same throughout the table.

Should the errors named be considered to be too large in any case, greater accuracy can be had by interpolation. Direct interpolation for temperature or for entropy can be made with facility; cross-interpolation will be somewhat more troublesome.

The use of the tables can best be illustrated by a few examples.

Example 1.— Given the pressure by the gauge 150.3 pounds (165 absolute) and the priming 2.0 per cent (x = 0.980) to find the entropy, heat contents and specific volume. This condition is found most nearly on page 78 and gives

$$\phi = 1.54$$
 $xr + q = 1176.8$ $v = 2.699$

Example 2. — Given the pressure 150.3 pounds by the gauge and the temperature 508° F., to find the entropy, heat contents and specific volume. The superheating is 142° and the temperature of saturated steam corresponding to 165 pounds absolute is 366° F. These conditions are found on page 93 and give

$$\phi = 1.65$$
 $r + q + c_p (t - t_s) = 1274$ $v = 3.305$.

Example 3. — Required the amount of heat changed into work per pound of steam for Rankine's cycle, the initial pressure being 150.3 pounds by the gauge and the exhaust being under a vacuum of 26 inches of mercury. The steam initially has 1.0 per cent of priming, and the barometer stands at 30 inches of mercury.

The exhaust pressure is 4 inches of mercury which by Table XIV corresponds to r.96 pound. The initial absolute pressure is found by adding the equivalent of 30 inches of mercury or

The solution of this problem is found in the column for entropy 1.55.

	Þ	t	\boldsymbol{x}	xr + q	v
Initial	165	366	.990	1185.0	2.726
Final	2	126	.784	899.1	137.4
Heat cha	anged int	o work B.	r.U.	285.9	

Example 4. — Required the velocity of discharge from a nozzle which takes steam at 150.3 pounds by the gauge and expands down to 26 inches of vacuum; the initial priming being .or and the barometer being at 30 inches.

The available heat is the same as that for the previous problem, namely, 285.9 B.T.U. for an adiabatic expansion. The velocity without friction would be

$$V = \sqrt{2 \times 32.2 \times 778 \times 285.9} = 3786.$$

If an allowance of ten per cent be made for friction the velocity will be

$$V = \sqrt{2 \times 32.2 \times 778 \times 0.90 \times 285.9} = 3590.$$

The specific volume at exit can be found as follows: — The heat that would be changed into work with an allowance of ten per cent for friction will be

$$0.90 \times 285.9 = 257.2$$
 B.T.U.

Subtracting from the initial heat contents leaves

$$1185 - 257 = 928$$
 B.T.U.

for the heat contents at 126° F. at the discharge, and this property is found for the entropy 1.60; the corresponding specific volume is 142 cubic feet.

Example 5. — Suppose that the conditions of example 3 are applied to a steam-turbine which has four pressure stages. For adiabatic expansion the available heat per stage will be

$$285.9 \div 4 = 71.4 \text{ B.T.U.}$$

This quantity may be subtracted four times successively from the initial heat contents and the results will be the heat contents for the

PROPERTIES OF STEAM AND OTHER VAPORS.

termediate and final pressures. All the properties are to be located in e columns for entropy 1.55. The results are as follows:—

	INITIAL STAGE.	SECOND STAGE.	THIRD STAGE.	FOURTH STAGE.	DISCHARGE.
eat contents emperatures	1185.0 366	1113.5 299	1042.1 237	970.6 180	899.1 126
ressures	165	66.2	23.7	7.50	1.99

A full discussion of this method with allowance for friction and other sses together with its limitations will be found in the author's "Thermo-ynamics of the Steam Engine."

TABLE I.

SATURATED STEAM.

ENGLISH UNITS

Temperature, Degrees Fahr.	Pressure, Pounds per Square Inch.	Heat of the Liquid.	Heat of Vaporization.	Heat Equiva- lent of Inter- nal Work.	Heat Equiva- lent of Ex- ternal Work.	Entropy of the Liquid.	Entropy of Vaporiza- tion.	Specific Volume.	Weight, in Pounds, of One Ser Cubic Foot.	Temperature, Degrees Fahr.
t	p	q	r	ρ	Ари	0	$\frac{r}{T}$	8	γ	t
1 33	0.0890 ₃₆ 0.0926 ₃₇ 0.0963 ₃₉	0.0 1.0 2.0	1091 .7 1091 .0 1090 .3	1035 .8 1035 .0 1034 .2	56.0	0.0000 0.0021 0.0041	2 .2211 2 .2152 2 .2094	$3395_{127} \\ 3268_{123} \\ 3145_{116}$	$\begin{array}{c} 0.0002945_{115} \\ 0.0003060_{120} \\ 0.0003180_{121} \end{array}$	J 3#
35 36 37	$\begin{smallmatrix} 0.1002_{40} \\ 0.1042_{41} \\ 0.1083_{43} \\ \end{smallmatrix}$	3.0 4.0 5.0	1089 .6 1088 .9 1088 .2	1033 .5 1032 .7 1031 .9	56.2	0.0061 0.0082 0.0102	2 .2035 2 .1975 2 .1916	$\begin{array}{c} 3029\\2917\\107\\2810\\104 \end{array}$	$\begin{array}{c} 0.0003301_{127} \\ 0.0003428_{131} \\ 0.0003559_{136} \end{array}$	37
38 39 40	$\begin{smallmatrix} 0.1126_{44} \\ 0.1170_{46} \\ 0.1216_{48} \end{smallmatrix}$	6.1 7.1 8.1	1087 .4 1086 .7 1086 .0	1031 .1 1030 .3 1028 .5	56.4	0.0122 0.0142 0.0163	2.1858 2.1800 2.1741	$\begin{array}{c} 2706_{99} \\ 2607_{95} \\ 2512_{91} \end{array}$	$\begin{array}{c} 0.0003695_{141} \\ 0.0003836_{145} \\ 0.0003981_{150} \end{array}$	40
41 42 43	$\begin{smallmatrix} 0.1264_{49} \\ 0.1313_{51} \\ 0.1364_{53} \end{smallmatrix}$	9.1 10.1 11.1	1085.3 1084.7 1084.0	1028 .7 1028 .0 1027 .2	56.7	0.0183 0.0203 0.0223			$ \begin{array}{c} 0.0004131154 \\ 0.0004285161 \\ 0.0004446164 \end{array} $	
44 45 46		12.1 13.1 14.1	1083.3 1082.6 1081.9	1026 .4 1025 .7 1024 .9	56.9	0.0243 0.0262 0.0282	2.1459	209274	$ \begin{array}{c} 0.0004610170 \\ 0.0004780175 \\ 0.0004955181 \end{array} $	ו שבי ו
47 48 49	$\begin{smallmatrix} 0.1586 \\ 0.164662 \\ 0.170865 \end{smallmatrix}$	15.1 16.1 17.1	1080.5	1023 .3	57.2	0 .0302 0 .0322 0 .0342	2.1291	187866	0.0005136 0.0005324195 0.0005519195	
50 51 52	$\begin{smallmatrix} 0.1773 \\ 0.1839 \\ 0.1908 \\ 71 \end{smallmatrix}$	18.1 19.1 20.1	1078.4	1021.0	57.4	0 .0381	2.1124	168959	0.0005718 0.0005923213 0.0006135213	52
53 54 55	$\begin{smallmatrix} 0.1979 \\ 0.2052 \\ 76 \\ 0.2128 \\ 78 \end{smallmatrix}$	21 .1 22 .1 23 .1	1076.3	1018.	6 57.7	0 .0440	2.0960	1520_{52}^{4}	0.0006353 ₂₂₆ 0.0006579 ₂₃ 0.0006812 ₂₄	53 54 55 55
56 57 58	$\begin{smallmatrix} 0.2206 \\ 0.228781 \\ 0.237086 \end{smallmatrix}$	24 .1 25 .1 26 .1	1074.2	1016.	2 58.0	0 .0498	2.0797	7 137046	$ \begin{array}{c} 0.0007052 \\ 0.000729924 \\ 0.0007553 \\ 26 \end{array} $	
5Ω 60 61	$\begin{smallmatrix} 0.2456 \\ 0.2545 \\ 0.2637 \\ 94 \end{smallmatrix}$	27 .: 28 .: 29 .:	[1072.]	1013.	9 58.2	0 .0556	2.063	123744	$ \begin{array}{c} 0.0007816 \\ 0.0008084 \\ 0.0008362 \\ 28 \end{array} $	8 61
62 63	$\begin{array}{c} 0.2731_{98} \\ 0.2829_{10}^{10} \end{array}$	30.3							0.0008651 0.0008945 30	62 63

33

ē.	per	the	d .	Heat Equiva- lent of Inter- nal Work.	Ya-	id.	of 'a-	_	DENSITY.	Pemperature, Degrees Fahr.
Temperature, Degrees Fahr.	Pressure, Pounds I Square Inch.	of id.	Heat of Vap- orization.	f In	Heat Equiva- lent of Ex- ternal Work.	Entropy of the Liquid.	Entropy of Vaporiza- tion.	Specific Volume,	Teight, in Pounds, of One Cubic Foot.	rath rees r.
egre ahr	ssun oun qua	Feat of Liquid.	at ol riza	at E	nt E	trop ne L	Vap tion	ecifi Volu	ight Sour Tubi	npe Deg Pahi
EDE	H S H S H	He	Ö H	Heg	Hea Jen ten	E	편 _	Spe	We	Ter
t	p	q	r	Р	Apu	θ	$\frac{r}{T}$	8	γ	t
64	0.2929 ₁₀₄ 0.3033 ₁₀₇ 0.3140 ₁₁₀	32.1		1010.8	58.6	0.0633	2.0431	1081 ₃₇ 1044 ₃₃ 1011 ₃₃	0.0009249313	64
65	0.3033107	33 .1		1010.0		0.0652	2.0378	104433	$0.0009562_{326}^{313} \\ 0.0009888_{332}^{32}$	65 66
66	0.0220110		1068 .0	1009 .3	58.7	0.0671	2.0024	33		00
67	0.3250 ₁₁₄ 0.3364 ₁₁₇ 0.3481	35.1	1067.3	1008.5	58.8	0.0690	2.0272	978.5 ₃₁₆ 946.9 ₃₀₅ 916.4 ₂₉₄	$\begin{array}{c} 0.001022\\ 0.00105735\\ 0.00109235\\ 0.00109236 \end{array}$	67
68	$\begin{bmatrix} 0.3364_{117} \\ 0.3481_{121} \end{bmatrix}$	36 .1 37 .1	1066.6 1065.9	1007 .7 1006 .9	58.9 59.0	0.0709	2.0221 2.0169	946.9305	$0.001037_{35} \\ 0.00109235$	68 69
09	0.0201121	37 .1	1000.5	1000.0		0.0125	0200	294	36	
70	$\begin{smallmatrix} 0.3602_{124} \\ 0.3726_{128} \\ 0.3854_{132} \end{smallmatrix}$	38.1		1006.1	59.1	0.0747	2.0118	887.0 858.7283 831.4284	$\begin{smallmatrix} 0.001128 \\ 0.00116537 \\ 0.00120338 \\ 0.00120339 \end{smallmatrix}$	70 71
71 72	0.3726128	39 .1 40 .1	1064 .5 1063 .8	1005 .3 1004 .5		0.0766 0.0784	2.0066 2.0015	$\begin{array}{c} 838.7_{273} \\ 831.4_{264} \end{array}$	0.00120338	72
1 '					}			204	39	
73	$\begin{smallmatrix} 0.3986 \\ 0.4122 \\ 140 \\ 0.4262 \\ 144 \end{smallmatrix}$	41.1		1003.7		0.0803	1.9964 1.9914	805 .0 ₂₅₄ 779 .6 ₂₄₄ 755 .2 ₂₃₇	$ \begin{array}{c} 0.001242 \\ 0.00128341 \\ 0.00132542 \\ \end{array} $	73 74
74	0.4262140	42.1 43.1	1062.4 1061.7	$1002.9 \\ 1002.2$		0 0822 0 0841	1.9863	755.2244	0.00132542	75
1	144						1 0010			76
76 77	0.4406149	44 .1 45 .1	1061 .0 1060 .3	1001.4 1000.6		0.0859	1.9813 1.9763	708.7228	0.001367	76 77
78		46.1	1059.6	999.8		0.0896		$\begin{array}{c} 731.5_{228} \\ 708.7_{219} \\ 686.8_{212} \end{array}$	0.001456_{46}^{45}	78
1	197	,,,	1050 0	000 0	50.0	0.0015	1.9663			79
79 80	0.4805162	47.1 48.1	1058.9 1058.2	999.0		$0.0915 \\ 0.0934$	1.9614	645.2107	0.00155048	80
81	$\begin{smallmatrix} 0.4865_{162} \\ 0.5027_{167} \\ 0.5194_{171} \end{smallmatrix}$	49.1	1057.5	997.4		0.0952	1.9565	665.6 ₂₀₄ 645.2 ₁₉₇ 625.5 ₁₉₁	$ \begin{array}{c} 0.001502_{48} \\ 0.001550_{49} \\ 0.001599_{50} \end{array} $	81
	0 2062	FO 1	1056 0	996.7	60.2	0.0971	1.9516			82
82 83	1.5542	50 .1 51 .1	1056 .9 1056 .2	995.9		0.0989	1.9468	587.9185	0.00170152	83
84	$ \begin{array}{c} 0.5365_{177} \\ 1.5542181 \\ 0.5723_{187} \end{array} $	52.1	1055 .5	995 .1		0.1007	1.9420		$ \begin{array}{c} 0.001649\\ 0.00170152\\ 0.00175453\\ 0.00175454 \end{array} $	84
85	0.5010	53.1	1054.8	994.3	60.5	0.1026	1 .9372			85
86	0.6102192	54.1	1054.5	993.6	60.5	0.1044	1.9324	536.4160	0.001864_{58}^{55}	86
87	$ \begin{vmatrix} 0.5910 \\ 0.6102 \\ 197 \\ 0.6299 \\ 203 \end{vmatrix} $	55 .1	1053.4	992.8	60.6	0.1062	1.9276	520.4160	$ \begin{array}{c} 0.001808 \\ 0.001864 \\ 0.001922 \\ 59 \end{array} $	87
88			1052.7	992.0	60.7	0 .1081	1.9228	504.8,40	0.001981 0.00204160	88
89	0.6502 ₂₀₉ 0.6711 ₂₁₄	57.1	1052.0	991.2	60.8	0.1099	1.9180	490.0144	0.00204160	89
90	0.0020221	00.1	1051.3	990.4	60.9	0.1117	1.9132	4/5.0139	0.00210362	90
91	0.7146	59.1	1050.6	989.6	61.0	0.1135		461.7126	$\begin{array}{c} 0.002167 \\ 0.00223265 \\ \end{array}$	91
92	0.7372_{233}^{226}	60.1	1049.9	988.8	61.1	0.1153			$\begin{array}{c} 0.00223267 \\ 0.00229968 \end{array}$	92
93	$ \begin{array}{c} 0.7146 \\ 0.7372233 \\ 0.7605239 \end{array} $	61.1	1049.2	988.0	61.2	0.1171	1.8990			33
94	0.7844	62.1		987.2	61.3				$\begin{smallmatrix} 0.002367 \\ 0.00243871 \\ 0.00251173 \\ 0.00251174 \end{smallmatrix}$	94
95	$ \begin{array}{c} 0.7844 \\ 0.8090246 \\ 0.8342259 \end{array} $	63.1		986 .4 985 .0	61.4 61.5			398.4118	0.00251173	95 96
96	0 .0342259	64.1	1047.1	1. 000	01.0			1 118		
97	0.8601266	65.0		984.9				$\begin{bmatrix} 386.9 \\ 375.011 \end{bmatrix}$	0.002585	97
98	$ \begin{array}{c} 0.8601 \\ 0.8867 \\ 273 \\ 0.9140 \\ 281 \end{array} $	66.0 67.0		984.					0 .00266075 0 .00273878	99
	281		1010.1					100	0 000010	100
100	0.9421	68.0	1044.4	982.				1 344 B 8	0.00281882	100 101
101 102	$\begin{bmatrix} 0.9421_{288} \\ 0.9709_{291} \\ 1.000_{31} \end{bmatrix}$	69.0	1043.7	981 . 981 .				2 0 2 2 . 0	0 00298484	102
	1.000 31		1 .	1	1			0 225 0	0.003069	103
103	1.031 31	71.0		980. 979.				E 216 8 8		103
104	1.062 32	12.0	1041.1	919.	J 32 .2	*.100	10.20	310.5 8	8 90	1

Temperature, Degrees Fahr.	Pressure, Pounds per Square Inch.	Heat of the Liquid.	Heat of Vap- orization.	Heat Equiva- lent of Inter- nal Work.	Heat Equiva- lent of Ex- ternal Work.	Entropy of the Liquid	Entropy of Vaporiza- tion.	Specific Volume.	Weight, in Pounds, in Of One Cubic Foot.	Temperature, Degrees Fahr.
t	p .	q	r	ρ	Apu	θ	$\frac{r}{T}$	s	γ	t
105 106 107	$\begin{array}{c} 1.094_{33} \\ 1.127_{33} \\ 1.160_{35} \end{array}$	73.0 74.0 75.0	1041 .0 1040 .3 1039 .6	978 .7 977 .9 977 .1	62 .3 62 .4 62 .5	0 .1385 0 .1403 0 .1421	1 .8440 1 .8396 1 .8351	308.0 295.486 291.279	0.003247 ₉₃ 0.003340 ₉₄ 0.003434 ₉₆	105 106 107
108 109 110	1.195_{35} 1.230_{36} 1.266_{38}	76.0 77.0 78.0	1038 .9 1038 .2 1037 .5	976 .3 975 .5 974 .7	62.6 62.7 62.8	0 .1438 0 .1456 0 .1473	1 .8306 1 .8261 1 .8217	283 .3 ₇₇ 275 .6 ₇₅ 268 .1 ₇₂	$\begin{smallmatrix} 0.003530_{98} \\ 0.003628_{102} \\ 0.003730_{104}^{102} \end{smallmatrix}$	108 109 110
111 112 113	$egin{array}{c} 1.304_{38} \ 1.342_{39} \ 1.381_{40} \end{array}.$	79 .0 80 .0 81 .0	1036 .8 1036 .1 1035 .4	973 .9 973 .1 972 .3	62 .9 63 .0 63 .1	0 .1491 0 .1508 0 .1526	1.8173 1.8129 1.8085	$260.9_{71} \\ 253.8_{68} \\ 247.0_{66}$	$\begin{array}{c} 0.003834 \\ 0.003940 \\ 109 \\ 0.004049 \\ 111 \end{array}$	111 112 113
114 115 116	1.421 1.46241 1.50442	82 .0 83 .0 84 .0	1034 .7 1034 .0 1033 .3	971 .5 970 .7 969 .9	63 .2 63 .3 63 .4	0 .1543 0 .1560 0 .1578	1 .8042 1 .7998 1 .7955	240 .4 234 .064 227 .862	$\begin{smallmatrix} 0.004160 \\ 0.004274 \\ 116 \\ 0.004390 \\ 119 \end{smallmatrix}$	114 115 116
117 118 119	1 .547 1 .59144 1 .63645	85 .0 86 .0 87 .0	1032 6 1031 .9 1031 .2	969 .1 968 .3 967 .5	63 .5 63 .6 63 .7	0 .1595 0 .1612 0 .1630	1.7912 1.7868 1.7825	$\begin{array}{c} 221.8 \\ 216.058 \\ 210.357 \\ 210.355 \end{array}$	$\begin{array}{c} 0.004509 \\ 0.004630121 \\ 0.004755 \\ 128 \end{array}$	117 118 119
120 121 122	1 .683 1 .73047 1 .77949 50	88 .0 89 .0 90 .0	1030 .5 1029 .8 1029 .2	966 .7 966 .0 965 .3		0.1647 0.1664 0.1682	1.7782 1.7740 1.7699	$204.8_{199.553}_{194.352}$	$\begin{array}{c} 0.004883\\ 0.005013130\\ 0.005147134\\ 0.005147136 \end{array}$	120 121 122
123 124 125	$\begin{array}{c} 1.829 \\ 1.88051 \\ 1.93252 \\ 53 \end{array}$	91 .0 92 .0 93 .0	1028 .5 1027 .8 1027 .1	964 .5 963 .7 962 .9	64.1	0.1699 0.1716 0.1733	1.7657 1.7615 1.7573	189 .3 ₄₈ 184 .5 ₄₇ 179 .8 ₄₆	$\begin{smallmatrix} 0.005283\\ 0.005421138\\ 0.005562141\\ 0.005562146 \end{smallmatrix}$	123 124 125
126 127 128	1 .985 2 .04055 2 .09656 2 .09657	94 .0 95 .0 96 .0	1026 .4 1025 .7 1025 .0	962 .1 961 .3 960 .5	64.4	0.1750 0.1767 0.1784	1.7531 1.7489 1.7447	$175.2 \\ 170.745 \\ 166.443 $	$\begin{smallmatrix} 0.005708\\0.005857149\\0.006010\\155 \end{smallmatrix}$	126 127 128
129 130 131	2.153 2.21259 2.27260 2.27261	97 .0 98 .0 99 .0	1024 .3 1023 .6 1022 .9	959 .7 958 .9 958 .1	64.7	0.1801 0.1818 0.1835	1.7405 1.7364 1.7323	162.3 ₄₂ 158.1 ₃₉ 154.2 ₃₈	$ \begin{array}{c} 0.006165 \\ 0.006324159 \\ 0.006485161 \\ 164 \end{array} $	129 130 131
132 133 134	2.333 2.39663 2.46064	100 .0 101 .0 102 .0	1022 .2 1021 .5 1020 .8	957 .3 956 .5 955 .7	65.0	0.1852 0.1869 0.1886	1.7281 1.7240 1.7200	150 .4 ₃₇ 146 .7 ₃₆ 143 .1 ₃₆	$ \begin{array}{c} 0.006649 \\ 0.006817168 \\ 0.006990176 \end{array} $	132 133 134
135 136 137	2.526 2.59367 2.66269	103 .0 104 .0 105 .0	1020 .1 1019 .4 1018 .7	954.9 954.1 953.3	65.3	0.1902 0.1919 0.1936	1.7159 1.7118 1.7078	139 .5 ₃₄ 136 .1 ₃₃ 132 .8 ₃₂		135 136 137
138 139 140	2.732 2.80472 2.87773	106 .0 107 .0 108 .0	1018.0 1017.3 1016.6	952 .5 951 .7 950 .9	65.6	0.1952 0.1969 0.1986	1.7037 1.6997 1.6957	$\begin{array}{c} 129.6_{31} \\ 126.5_{31} \\ 123.4_{30} \end{array}$		138 139 140
141 142 143	2 .953 3 .02976 3 .10880	109 .0 110 .0 111 .0	1015.9 1015.3 1014.6	950 .1 949 .4 948 .6	65.9	0.2002 0.2019 0.2036	1.6879	$\begin{bmatrix} 120.4_{29} \\ 117.5_{28} \\ 114.7_{27} \end{bmatrix}$	$ \begin{array}{c} 0.008298 \\ 0.008502204 \\ 0.008710208 \\ \end{array} $	141 142 143
144 145	3 .188 3 .27083	112 .0 113 .0	· 1013 .9 1013 .2			0 .2052 0 .2069			$\begin{bmatrix} 0.008929 \\ 0.009143_{220}^{214} \end{bmatrix}$	144 145

36		•	SATU		D 0.	LEAM				
Temperature, Degrees Fahr.	Pressure, Pounds per Square Inch.	Heat of the Liquid.	Heat of Vap- orization.	Heat Equiva- lent of Inter- nal Work.	Heat Equiva- lent of Ex- ternal Work.	Entropy of the Liquid.	Entropy of Vaporiza- tion.	Specific Volume.	Weight, in Pounds, 3 of One Cubic Foot.	Temperature, Degrees Fahr.
	\overline{p}	q	r	ρ	Apu	θ	$\frac{r}{T}$	8	γ	t
146 147 148	3 .353 ₈₆ 3 .439 ₈₇ 3 .526 ₈₉	114.0 115.0 116.0	1012.5 1011.8 1011.1		66.4	0.2085 0.2102 0.2118	l 1.6683	106 .8 ₂₅ 104 .3 ₂₄ 101 .9 ₂₄	$ \begin{array}{c} 0.009363_{225} \\ 0.009588_{228} \\ 0.009816_{234} \end{array} $	146 147 148
149 150 151	$3.615_{91} \ 3.706_{93} \ 3.799_{95}$	117.0 118.0 119.0	1010 .4 1009 .7 1009 .0	943.0	66.7		1.6566	97 .24225	25	149 150 151
152 153 154	$3.894_{97} \ 3.991_{99} \ 4.090_{101}$	120.0 121.0 122.0	1008.3 1007.6 1006.9	940.7	66.9	0.2200	1.6450	90.68206	$ \begin{array}{c} 0.01077_{25} \\ 0.01102_{26} \\ 0.01128_{27} \end{array} $	152 153 154
155 156 157	4.191 4.295104 4.400105 4.400108	123 .0 124 .0 125 .0	1006 .2 1005 .5 1004 .8	938.3	67.2	0.2249	1.6336	84.66192	$ \begin{smallmatrix} 0.01155_{27} \\ 0.01182_{27} \\ 0.01209_{27} \end{smallmatrix} $	155 156 157
158 159 160	4.508 4.617109 4.729112	126 .0 127 .0 128 .0	1003 .4	935 .9	67.5	0.2298	3 1.622	79 .07176 77 .31 ₁₇	[] 3.32230	158 159 160
161 162 163	4.844 4.960116 5.079119	129 .0 130 .0 131 .0	1001 .4	933.0	67.8	0 .234	7 1.611	1 73 .93 16	$ \begin{smallmatrix} 0.01323 \\ 0.0135330 \\ 0.0138331 \\ 0.0138331 \end{smallmatrix} $	161 162 163
164, 165 166	5.200 5.324124 5.450126		999	3 931	2 68.1	0.239	5 1.600	2 69 .1715		164 165 166
167 168 169	5.579 5.710131 5.844134	135.0	997 .	2 928.	8 68 .4	0.244	3 1.589	$ \begin{array}{c cccc} 1 & 64.77_{14} \\ 5 & 63.37_{13} \end{array} $	1	167 168 169
170 171 172	5.981 6.120139 6.262142	138.0	995.	1 926.	4 68.7	0.249	1 1.578	$3 60.67_{12}^{13}$	0.0168436	170 171 172
173 174 175	6 .407 6 .554147 6 .704150	141.0	993.	0 924.	1 68 .9	9 0.253	8 1.567	$5 56.90_{12}$	0.01101ag	173 174 175
176 177 178	6 .858 7 .014156 7 .173159	144.0	990.	9 921	7 69 .	$2 \mid 0.258$	5 1.556	$59 53.39_{11}^{\circ}$	$\begin{bmatrix} 0.01834_{39} \\ 0.01873_{40} \\ 0.01913_{41} \end{bmatrix}$	176 177 178
179 180 181	7.335 7.500168 7.668168	147.	0 988.	8 919	3 69.	4 0.261 5 0.263 6 0.264	33 1.546	33 50 .141	01 0.0203143	179 180 181
182 183 184	7.840 8.014178 8.192188	150. 151. 152.	1 986	7 916	.9 69 .	8 0.268	30 1.53	58 47 .119	$\begin{bmatrix} 0.0212344 \\ 0.0216745 \end{bmatrix}$	182 183 184
185 186	8.373 8.558 ₁₈	153. 154.							$\begin{array}{c c} 2 & 0.02212 \\ 2 & 0.02258 \\ 47 \end{array}$	185 186

٩		per	the	ap-	Heat Equiva- lent of Inter- nal Work.	Heat Equiva- lent of Ex- ternal Work.	of uid.	Entropy of Vaporiza- tion.	j.	DENSITY.	Temperature, Degrees Fahr,
rati	Degrees Fahr.	Pressure, Pounds per Square Inch.	Heat of Liquid.	Heat of Vap- orization.	Equ of In	Equ of nal W	Entropy of the Liquid.	ropy apor	Specific Volume,	Weight, in Pounds, of One Cubic Foot.	pera egre ahr.
ume	Fab	Por Squ Inc	Heat	Heat oriz	Heat lent nal	Heat lent terr	Entr	Ent	Spe	Weg P.C. F.C.	Tem
٦	$\begin{bmatrix} t \\ t \end{bmatrix}$	r	q	r	ρ	Apu	в	$\frac{r}{T}$	8	γ	t
-	107	0 740	155 1	002 0	913.8	70.1	0 .2742	1.5219	43 .38	0.0230547	187
1:	187 188	$\substack{8.746\\8.937\\195\\9.132\\198}$	155 .1 156 .1	983.9 983.2	913.0	70.2	$0.2758 \\ 0.2773$	1.5185 1.5150	$\begin{array}{c} 43.38 \\ 42.5187 \\ 41.6683 \end{array}$	$\begin{smallmatrix} 0.02305_{47} \\ 0.02352_{48} \\ .0.02400_{49}^{48} \end{smallmatrix}$	188 189
1	189	9.132_{198}^{132}	157 .1	982.5	912.2				1	1	190
	190 191	9.330 ₂₀₂ 9.532	158 .1 159 .1	981.8 981.1	911.4	70.5	0 .2789 0 .2805	1.5116		$\begin{smallmatrix} 0.02449 & 50 \\ 0.0249951 \\ 0.02550 & 51 \end{smallmatrix}$	191
1	192	$\substack{\frac{9.330}{202}\\9.532}\\9.738\\209}$	160 .1	980.4	909.8	70.6	0.2820	Ì		0.0255051	192
	193 194	0 047	161 .1 162 .1	979.7 979.0	909.0		0.2835			$ \begin{array}{c} 0.02601 \\ 0.0265453 \\ 0.0270854 \end{array} $	193 194
	195	10.16_{22} 10.38_{22}	163.1	978.3			0.2866		36 .9473	0.0270854	195
	196	10 .60 ₂₂ 10 .82 ₂₃	164.1	977.6			0 .2882 0 .2897		$\begin{array}{c} 36.21_{71} \\ 35.50_{69} \\ 34.81_{67} \end{array}$	$ \begin{array}{c} 0.02762 \\ 0.0281755 \\ 0.0287356 \\ 0.0287356 \end{array} $	196 197
	197 198	$\begin{array}{c c} 10.82^{22} \\ 11.05^{23} \\ \end{array}$	165 .1 166 .2	976.9 976.1			0.2891		34 .8169	0.02873_{56}^{56}	198
1	199	ŀ	167.2	975.4	904.5	71.2		1.4813			199 200
	200 201	$\begin{array}{c} 11.28 \\ 11.5224 \\ 11.7624 \end{array}$	168 .2 169 .2	974.7	' 903 .·					$ \begin{smallmatrix} 0.0292958 \\ 0.0298759 \\ 0.0304660 \end{smallmatrix} $	201
1	202		-					1.471	1		202
1	203	12.00 ₂₅ 12.25 ₂₆	170 .2 171 .2	972.7	7 901.	2 71.5	0 .298	1.468	$2 \mid 31.59_{60}^{00}$	$ \begin{bmatrix} 0.0310660 \\ 0.0316661 \\ 0.0322762 \end{bmatrix} $	203 204
1	204	12.5126	172.2		. \			1	,	1	205
1	205 206	$\begin{bmatrix} 12.77_{26} \\ 13.03_{26} \\ 13.29_{27} \end{bmatrix}$	173.2			8 71.8	0 .303	4 1.458	5 29 .835	0.03289 0.0335266 0.0341866	206 207
	207	13.2927	175 .2	969.	9 898.	1				1	
1	208 209	13 .56 ₂₈ 13 .84 ₂₈	176 .2 177 .2				0 .306		$\begin{array}{c c} 0 & 28.70_{5} \\ 8 & 28.16_{5} \\ 5 & 27.63_{5} \end{array}$	$\begin{smallmatrix} 4 \\ 0.03484 \\ 0.03551 \\ 0.03619 \\ 70 \end{smallmatrix}$	209
1	210	14.1228	178 .3							1	
1	211	14 41	179 .3					0 1.442 5 1.439	A 26 667		211
١	$\frac{212}{213}$	14.70 ₂₉ 14.99 ₃₀	180 .3 181 .3						8 26.214		
1	214		182 .:	3 964.		.2 72.			25 .73	0.0388773	214 215
١	215 216	15.2930 15.5931 15.9031	183 184 .	3!964.	2 891 5 890					$\begin{array}{c c} 18 & 0.0396073 \\ 0.0396074 \\ 0.0403474 \end{array}$	216
1	217		185 .	1			9 0.320	00 1.42			917
	218	16.53_{22}^{32}	186.	3 962	.1 889	.1 73.	0 0 .32	15 1.420	32 24.34 00 23.90 38 23.46	$\begin{bmatrix} 0.0410876 \\ 0.0418476 \\ 0.0426376 \\ 0.$	218
	219	1	187.	1	1				27 23 03	0.04342	
	220 221		188 . 189 .	4 959	.9 886	.7 73	2 0.32	1.41	06 22.01	$\begin{array}{c c} 42 & 0.04342_{8} \\ 0.04423_{8} \\ 0.04505_{8} \end{array}$	$\begin{bmatrix} 1 & 221 \\ 2 & 222 \end{bmatrix}$
	222		190 .	4 959	.3 886	.0 73	1	-	1	1	
	223 224	18.2135	191 . 192 .					04 1.40	14 21 42	$\begin{array}{c c} 39 & 0.04587_8 \\ 0.04670_8 \\ 37 & 0.04754_8 \end{array}$	3 224 4 225
	225		193						l l	- 1	1
	226								54 20.67 23 20.29	$\begin{bmatrix} 38 & 0.04840 \\ 0.04929 \\ 36 \end{bmatrix}$	$\frac{9}{0}$ 226
	227	$\begin{bmatrix} 19.28_{37} \\ 19.65_{37} \end{bmatrix}$	195	.4 955	.8 882	2.1 73	.1 0.33	1.05	20.20	30 8	י ט

30										
Temperature, Degrees Fahr.	Pressure, Pounds per Square Inch.	Heat of the Liquid.	Heat of Vap- orization.	Heat Equiva- lent of Inter- nal Work.	Heat Equiva- lent of Ex- ternal Work.	Entropy of the Liquid.	Entropy of Vaporization.	Specific Volume.	Weight, in Pounds, of One Cubic Foot.	Temperature, Degrees Fahr.
t	p	q	~ ·	ρ	Apu	θ	$\frac{r}{T}$	3	у	t
228 229 230	20.02 ₃₈ 20.40 ₃₈ 20.78 ₃₉	196.5 197.5 198.5	955 .0 954 .3 953 .6	881 .2 880 .5 879 .7	73 .8 73 .8 73 .9	0.3363 0.3378 0.3392	1.3892 1.3861 1.3831	19 .93 ₃₅ 19 .58 ₃₄ 19 .24 ₃₃	$\begin{smallmatrix} 0.05018_{89} \\ 0.05107_{90} \\ 0.05197_{92} \end{smallmatrix}$	228 229 230
231 232 233	21.17 ₄₀ 21.57 ₄₁ 21.98 ₄₁	199.5 200.5 201.5	952 .9 952 .2 951 .5	878 .9 878 .2 877 .4	74.0	0.3407 0.3422 0.3436		02	$\substack{0.05289\\0.0538395\\0.0547897}$	231 232 233
234 235 236	$\begin{array}{ c c c c c }\hline 22.39_{41} \\ 22.80_{43}^{41} \\ 23.23_{43}^{43} \\ \hline \end{array}$	202.5 203.6 204.6	950 .8 950 .0 949 .3	875.7	74.3	0.3466	1.3679	17 .63 ₃₀ 17 .33 ₃₀	0.05575 ₉₉ 0.05674 ₉₉ 0.05773 ₁₀₁	234 235 236
237 238 239	23.66 24.0944 24.5345	205.6 206.6 207.6	948 .6 947 .9 947 .2	873 .4	74.5	0.3509	1.3590	$\begin{array}{c c} 16.74_{29}^{20} \\ 16.45_{28}^{20} \end{array}$	$\begin{array}{c} 0.05874_{102} \\ 0.05976_{103} \\ 0.06079_{105} \end{array}$	237 238 239
240 241 242	24.98 ₄₆ 25.44 ₄₆ 25.90 ₄₇		946 .5 945 .8 945 .1	871.	1 74.7	0.355	1 .3502	$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	0.06184 ₁₀₆ 0.06290 ₁₀₇ 0.06397 ₁₀₉	
243 244 245	26.37 ₄₈ 26.85 ₄₈ 27.33 ₄₉	1 1	944 .4 943 .7 943 .0	868.	75 .0	0.359	6 1.341	$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	0.00725114	
246 247 248	27 .82 ₅₀ .28 .32 ₅₀ 28 .82 ₅₂	214.7 215.7 216.7	942 .3 941 .6 940 .9	866.	4 75 .:	2 0.363	9 1.332	8 14.37 $\frac{1}{23}$	0.010.1118	
249 250 251	29 .34 ₅₂ 29 .86 ₅₂ 30 .38 ₅₄	217.7 218.8 219.8	939.	4 864.	0 75.	4 0.368	3 1.324	1 13.68 $^{20}_{22}$		
252 253 254	30 .92 31 .465		937.	3 861	.6 75 .	7 0.372	6 1.315	$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	0.0780812	3
255 256 257	32.57 33.145		935.	1 859	.2 75	.9 0 .376	38 1.307	$70 \mid 12.39_{20}$		2 257
258 259 260	34.29 34.886		933.	0 856	.9 76		11 1.298	36 11.81	$\begin{bmatrix} 0.08329_{13} \\ 0.08464_{13} \\ 0.08601_{13} \end{bmatrix}$	7 260
261 262 263	36.09 ₆ 36.71 ₆		930	.9 854	.5 76	.4 0.38	53 1.29	$\begin{array}{c ccccccccccccccccccccccccccccccccccc$)	3
264 265 266	37.96 ₆ 38.60 ₆		929 0 928	.8 852	.2 76	.6 0.38	95 1.28	$egin{array}{c c} 20 & 10.74 \\ 92 & 10.57 \\ 1 \end{array}$		60
267 268	39.91	7 236 8 237						64 10.41		31 267 268

				, ,	:0	1	44		DENSITY.	aī l
Temperature, Degrees	per	the	leat of Vap- orization.	Heat Equiva- lent of Inter- nal Work.	Heat Equiva- lent of Ex- ternal Work.	Entropy of the Liquid	Entropy of Vaporiza- tion.	ยู้	Weight, in Pounds, of One Cubic Foot.	Temperature, Degrees Fahr.
ratu	nds nds are	of uid	of A	Moi Par	Eqt of al W	Lig	opy tpor	ific	ut, ii Und On Oi; ot.	pers pre- pr.
Page 1	Pressure, Pounds I Square Inch.	Heat of Liquid.	Heat of orizati	eat. ent	Heat lent terns	ntrc the	Intr Va tio	Specific Volume,	For Por	E A A
Ter	Ta La	Ħ	Η̈́	Ħ	_				B	Ε .
t	p	q	r	ρ	Apu	θ	$\frac{r}{T}$	<u>s</u>	γ	
000	44 00	000 1	005.0	040 0	76.9	0.3951	1.2710	10 09	0.09907	269
269 270	41 .2669	238 .1 239 .1	925 .9 925 .2	849.0 848.2		0.3965	1.2683 1.2655	9.93715	0.100616	270
271		240.2	924.4	847 .4		0.3979	1.2655	$ \begin{vmatrix} 10.09 \\ 9.93715 \\ 9.785152 \\ 9.785149 \end{vmatrix} $	0.102216	271
272		241.2	923 .7	846.6	77 .1	0 .3993	1.2628	9.636	0.103816	272
273	44.0671	242.2	923.0	845.8	77.2	0.4007	1.2601	9.489144	$ \begin{array}{c} 0.1038_{16} \\ 0.1054_{16} \\ 0.1070_{16} \end{array} $	273 274
274	43 .35 ₇₁ 44 .06 ₇₂ 44 .78 ₇₄	243.2	922.3	845.0	77 .3	0.4021	1.2574			
275		244.2	921.6	844.2		0.4035	1.2547		0.1086 ₁₇ 0.1103 ₁₇ 0.1120-7	275 276
276 277		245.3 246.3	920.8 920.1	843 .4 842 .6		0 .4049 0 .4063	1.2520 1.2493	8.930136	0.1120_{17}^{17}	277
1		1		ļ	1			1		278
278		247.3	919.4 918.7			0.4077 0.4091	1.2466 1.2440	0 004104	0.1137 ₁₇ 0.1154 ₁₇	279
279	48 .5578	248.3 249.4				0.4104		8.536126	0.117117	280
1						0.4118	1.2387			281
281	50.12	250.4 251.4	917.2 916.6			0.4132	1.236	8.28512	$\begin{smallmatrix} 0.1189_{18} \\ 0.1207_{18} \\ 0.1225_{18} \end{smallmatrix}$	282
283		252.4	915.9			0.4146	1.233	8 .410 8 .285125 8 .16212	0.122518	283
284	I	253 .4	915.2	837.	78.1	0.4160	1.230	8.043	1 -	284
288	E 2 2083	254.5	914.4	836 .	78.1	0.4173	1.228	7.926^{11}	$ \begin{array}{c c} 0.126119 \\ 0.128019 \end{array} $	285 286
286	54 .2485	255.5	913.7	835 .	78.2	0.4187	1.225	11	3 0.120019	Į.
28		256.5	913.0				1.223	7.697 5.58611	$\begin{smallmatrix} 1 & 0.1299 & 19 \\ 0.1318 & 19 \\ 0.1337 & 20 \end{smallmatrix}$	287 288
288		257.5	912.3 911.5					7.586-19 7.475 ¹¹	0.133719	289
289		258 .6	1	1	1				-1	900
290	57.72	259 .6	910.8					უ ეცე ს	5 0.137720	290 291
29: 29:		260 .6 261 .6	910.3					7.15910	$\begin{bmatrix} 0.1357_{20} \\ 0.1377_{20} \\ 0.1397_{20} \end{bmatrix}$	292
1	I			1			1.207		-1	293
29	A 61 2093	262 .7 263 .7	908.0			0 .429	7 1.204	9 6.95610	$ \begin{array}{c c} 0 & .1417_{20} \\ 0 & .1437_{21} \\ 0 & .1458^{21} \end{array} $	294
29	62 .3395	264.7						5 7.056 9 6.956 3 6.857 97	21	295
29		265.7	7 906.	827.	5 79.0	0.432	1.199	8 6.760	0.1479	296
29	7 64 9597	266.7	905.	826.	7 79.1	0 .433	7] 1.197	2 6.665	0.1500^{21}_{21}	297 298
29	8 65.23 ₉₉	267 .8	905.	825.	9 79.1	0.435	1 1.194			}
29		268.8	904.		1 79.2		4 1.192	2 6.479	0.154322	299
30	o am ool()	0 269.8	903.					6 .479 6 .38891 6 .30088	$\begin{array}{c c} 0.1545_{22} \\ 0.1565_{22} \\ 0.1587_{22} \end{array}$	300
30	68.24 ¹⁰	$\begin{vmatrix} 2 \\ 3 \end{vmatrix} = 270.8$	902.	023.	i	1		1		
30	-	271.9	902.	2 822			5 1.184 8 1.182	00 6 1060	0.1609 ₂₃ 0.1632 ₂₃	302
30		3 272 .9 6 273 .9		5 822 8 821			2 1.179		$\begin{bmatrix} 0.1655_{23}^{23} \\ 0.1655_{23}^{23} \end{bmatrix}$	304
1										305
30	5 72.42 72.5010	8 274.9 276.	9 900. 0 899.				8 1.174	19 5.878	$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	306
30		9 277	0 898					74 5.959 19 5.8788 24 5.7988	$\begin{bmatrix} 0 & 1725_{24}^{24} \\ 0 & 1725_{24}^{24} \end{bmatrix}$	307
	75 60	278.	0 897	9 818	.0 79.	9 0.448	5 1.16			308
30		1 279	1 897						$\begin{bmatrix} 0.17324 \\ 0.177324 \end{bmatrix}$	309
1	11	3		1	I		1			

·	,					 ,			Designation	-5
Temperature, Degrees Fahr.	Pressure, Pounds per Square Inch.	Heat of the Liquid.	Heat of Vaporization.	Heat Equiva- lent of Inter- nal Work.	Heat Equiva- lent of Ex- ternal Work.	Entropy of the Liquid.	Entropy of Vaporiza- tion.	Specific Volume.	Weight, in Pounds, za of One Cubic Foot.	Temperature, Degrees Fahr.
t	p	q	r	ρ	Ари	θ	$\frac{r}{T}$	8	γ	t
310 311 312	77 .93 ₁₁₄ 79 .07 ₁₁₆ 80 .23 ₁₁₆	280 .1 281 .1 282 .1	896 .4 895 .7 895 .0	816 .4 815 .6 814 .8	80 .0 80 .1 80 .2	0 .4512 0 .4525 0 .4538	1.1649 1.1625 1.1600	5.564 ₇₄ 5.490 ₇₄ 5.416 ₇₃	$\substack{0.1797\\0.182124\\0.184625}$	310 311 312
313 314 315	$\substack{81.39\\82.57\\120\\83.77\\121}$	283 .2 284 .2 285 .2	894 .2 893 .5 892 .8	813 .9 813 .2 812 .4	80 .3 80 .3 80 .4	0 .4552 0 .4565 0 .4578	1.1576 1.1551 1.1527	$\substack{5.343\\5.272\\71\\5.201\\69}$	$\substack{0.1871 \\ 0.189726 \\ 0.192326}$	313 314 315
316 317 318	84 .98 ₁₂₂ 86 .20 ₁₂₃ 87 .43 ₁₂₅	286 .2 287 .3 288 .3	892 .1 891 .3 890 .6	811 .6 810 .8 810 .0	80 .5 80 .5 80 .6	0 .4592 0 .4605 0 .4618	1 .1503 1 .1479 1 .1455	5.132 ₆₈ 5.064 ₆₇ 4.997 ₆₆	$\substack{0.1949\\0.197526\\0.200127}$	316 317 318
319 320 321	$\begin{array}{c} 88.68_{127} \\ 89.95_{128} \\ 91.23_{129} \end{array}$	289 .3 290 .4 291 .4	889 .9 889 .1 888 .4	809 .2 808 .3 807 .6	80 .7 80 .8 80 .8	0 .4631 0 .4644 0 .4658	1.1431 1.1407 1.1383	$\begin{array}{c} 4.931 \\ 4.86764 \\ 4.80364 \\ \end{array}$	$\begin{array}{c} 0.2028 \\ 0.205527 \\ 0.208227 \\ \end{array}$	319 320 321
322 323 324	$\begin{array}{c} 92.52_{130} \\ 93.82_{132} \\ 95.14_{134} \end{array}$	292 .4 293 .4 294 .5	887 .8 887 .1 886 .3	806.1	80 .9 81 .0 81 .0	0.4671 0.4684 0.4697	1.1360 1.1336 1.1312	$\begin{array}{c} 4.741 \\ 4.67962 \\ 4.61861 \\ 60 \end{array}$	$\begin{array}{c} 0.2109 \\ 0.213728 \\ 0.216529 \end{array}$	322 323 324
325 326 327	$\begin{array}{c} 96.48_{135} \\ 97.83_{137} \\ 99.20_{14} \end{array}$	295 .5 296 .5 297 .5	885 .6 884 .9 884 .1	803 .7	81 .1 81 .2 81 .2	0.4710 0.4723 0.4736	1 .1289 1 .1265 1 .1241	4 .558 4 .49959 4 .44257	$\begin{array}{c} 0.2194_{29} \\ 0.2223_{29} \\ 0.2252_{29}^{29} \end{array}$	325 326 327
328 329 330	$^{100.6}_{102.014}_{103.4}_{14}$	298 .6 299 .6 300 .6	883 .4 882 .7 882 .0	801.3	81.4	0.4749 0.4762 0.4775	1.1218 1.1194 1.1171	4.32956 4.27356	$\begin{array}{c} 0.2281 \\ 0.231029 \\ 0.234030 \\ 0.234030 \end{array}$	328 329 330
331 332 333	$104.8_{14} \\ 106.2_{15} \\ 107.7_{15}$	301 .7 302 .7 303 .7	881 .2 880 .5 879 .8	798.9		0.4789 0.4802 0.4815	1.1147 1.1124 1.1101	4.113_{52}^{52}	$\begin{smallmatrix} 0.2370 \\ 0.240030 \\ 0.243131 \\ 31 \end{smallmatrix}$	331 332 333
334 335 336	$109.2_{15} \\ 110.7_{15} \\ 112.2_{15}$	304 .8 305 .8 306 .8	879 .0 878 .3 877 .6	796.5	81.8	0.4828 0.4841 0.4854	1.1078 1.1055 1.1032	$\begin{array}{c} 4.061 \\ 4.01051 \\ 3.96050 \\ \end{array}$	$\begin{smallmatrix} 0.2462\\ 0.249331\\ 0.252532\\ 0.252532\\ \end{smallmatrix}$	334 335 336
337 338 339	113.7 ₁₅ 115.2 ₁₆ 116.8 ₁₅	307 .9 308 .9 309 .9	876 .8 876 .1 875 .4	794.1	82.0	0 .4867 0 .4880 0 .4892	1.1009 1.0986 1.0963	$ \begin{array}{c} 3.910 \\ 3.86149 \\ 3.81348 \\ 47 \end{array} $	$ \begin{array}{c} 0.2557 \\ 0.259033 \\ 0.262333 \\ 0.262333 \end{array} $	337 338 339
340 341 342	$\begin{array}{c} 118.3\\ 119.916\\ 121.516 \end{array}$	310 .9 312 .0 313 .0	874 .7 873 .9 873 .3	791.7	82.2		1.0940 1.0918 1.0896	3.71947	$ \begin{array}{c} 0.2656\\ 0.268933\\ 0.272234\\ 0.272234 \end{array} $	340 341 342
343 344 345	123 .1 ₁₇ 124 .8 ₁₆ 126 .4 ₁₇	314 .0 315 .1 316 .1	872 .6 871 .8 871 .1	789 .4	82.4	0.4944 0.4957 0.4970	1.0850	$\begin{bmatrix} 3.584_{44}^{45} \\ 3.540_{43}^{44} \end{bmatrix}$	$\begin{smallmatrix} 0.2756\\ 0.2790\\ 34\\ 0.2825\\ 35 \end{smallmatrix}$	343 344 345
346 347 348	128 .1 ₁₇ 129 .8 ₁₇ 131 .5 ₁₇	317 .1 318 .2 319 .2	870 .4 869 .6 868 .9	787 .0	82.6		1.0783	$\begin{bmatrix} 3.455 & 42 \\ 3.413 & 42 \end{bmatrix}$	$\begin{array}{c} 0.2860 \\ 0.289535 \\ 0.293035 \\ 0.293036 \end{array}$	346 347 348
349 350	$^{133.2}_{134.9}{}^{17}_{18}$	320 .2 321 .3	868 .2 867 .4			0.5021 0.5034		$\begin{array}{c} 3.371 \\ 3.330 \\ 40 \end{array}$	$\begin{smallmatrix} 0.2966 \\ 0.3002 \\ 37 \end{smallmatrix}$	349 350

. 1	i I	o		44	اندیدا		س , ا	ī	DENSITY.	φ
Temperature, Degrees Fahr.	Pressure, Pounds per Square Inch.	Heat of the Liquid.	Heat of Vaporization.	Heat Equiva- lent of Inter- nal Work.	Heat Equiva- lent of Ex- ternal Work.	Entropy of the Liquid.	Entropy of Vaporization.	Specific Volume.	Weight, in Pounds, is of One Cubic Foot.	Temperature, Degrees Fahr.
lemi De Fa	Pres Po Sq. Inc.	Heal	Hear	Hear len nad	Heat len ter	Enti	Ent. Ct.	Spec	W FC & FG	Tem FD
t	p	q	r	ρ	Ари	θ	$\frac{r}{T}$	8	γ	t
351	136.7	322 .3	866 .7	783 .9	82.8	0.5047	1.0693	3.290	0.3039	351
352 353	$136.7_{18} \\ 138.5_{18} \\ 140.3_{18} $	323 .3 324 .4	866 .0 865 .2	783 .1 782 .3	82.9 82.9	0.5059 0.5072	1.0671 1.0649	$3.290_{39} \\ 3.251_{39} \\ 3.212_{38}$	$ \begin{array}{c} 0.3039\\0.307637\\0.311337\\ \end{array} $	352 353
354 355 356	$142.1\\143.918\\145.719$	325 .4 326 .4 327 .5	864 .5 863 .8 863 .0	781 .5 780 .8 779 .9	83.0	0 .5085 0 .5097 0 .5110	1 .0627 1 .0605 1 .0583	$3.174_{38} \\ 3.136_{38} \\ 3.098_{37}$	$\begin{array}{c} 0.3151 \\ 0.318938 \\ 0.322839 \end{array}$	354 355 356
357 358 359	$147.6_{19} \\ 149.5_{19} \\ 151.4_{19} \\$	328 .5 329 .5 330 .6	862 .3 861 .6 860 .8	779 .1 778 .4 777 .5	83.2	0 .5123 0 .5135 0 .5148	1 .0561 1 .0540 1 .0518	$\begin{array}{c} 3.061\\3.02536\\2.98935\end{array}$	$ \begin{array}{c} 0.3267 \\ 0.3306 \\ 39 \\ 0.3345 \\ 40 \end{array} $	357 358 359
360 361 362	153.3 ₂₀ 155.3 ₁₉ 157.2 ₂₀	331 .6 332 .6 333 .7	860 .1 859 .4 858 .7		83.4	0.5161 0.5173 0.5186	1.0496 1.0475 1.0453	$2.954 \\ 2.91935 \\ 2.88534$	$ \begin{array}{c} 0.3385 \\ 0.3426 \\ 41 \\ 0.3467 \\ 41 \end{array} $	360 361 362
363 364 365	$\begin{array}{c c} 159.2 \\ 161.220 \\ 163.220 \\ \end{array}$	334 .7 335 .7 336 .8	858 .0 857 .3 856 .5	773 .7	83.6	0.5199 0.5211 0.5224	1.0432 1.0410 1.0389	2.78533	$ \begin{array}{c} 0.3508 \\ 0.3549 \\ 0.3591 \\ 42 \end{array} $	363 364 365
366 367 368	$\begin{array}{c} 165.2 \\ 167.321 \\ 169.421 \\ \end{array}$	337 .8 338 .8 339 .9	855 .8 855 .1 854 .3	771 .4	4 83.7	0.5236 0.5249 0.5261	1 .0367 1 .0346 1 .0324	2.753_{32} 2.721_{21}^{32}	$ \begin{array}{c} 0.3633 \\ 0.367542 \\ 0.371843 \\ \end{array} $	366 367 368
369 370 371	$\begin{array}{ c c c }\hline 171.5\\ 173.621\\ 175.721\\ \hline 175.722\\ \hline \end{array}$	340 .0 341 .9 343 .0	853 .6 852 .9 852 .1	769 .	0 83 .9	0 .5274 0 .5286 0 .5299	1 .0281	2.628	$ \begin{array}{c} 0.3761 \\ 0.380544 \\ 0.384945 \end{array} $	369 370 371
372 373 374	177.9 180.122 182.322	344 .0 345 .0 346 .1		766.	7 84.0		1 .0217	$\begin{bmatrix} 2.539_{29}^{29} \\ 2.510_{29}^{29} \end{bmatrix}$	$\begin{array}{c} 0.3894 \\ 0.393945 \\ 0.398445 \\ 0.398446 \end{array}$	372 373 374
375 376 377	184.5 186.722	347 .1 348 .2 349 .2	848 .	4 764.	2 84.2	0 .5349 0 .5361 0 .5374	1 .0154	$\{2.453_{98}^{20}\}$	$\begin{smallmatrix} 0.4030 \\ 0.407747 \\ 0.412447 \\ 0.412447 \end{smallmatrix}$	375 376 377
378 379 380	191.3 193.623 195.923	350 .2 351 .3 352 .3	846.	2 761.	9 84.3	0.5398	1 .009	$\begin{bmatrix} 2 & .371_{27}^{27} \\ 2 & .344_{26}^{27} \end{bmatrix}$		378 379 380
381 382 383	198.2 200.624	353 .3 354 .4 355 .4	844.	1 759	.7 84.4	0.543	1.003	$0 2.292_{2}^{20}$	$\begin{bmatrix} 0.4314 \\ 0.436248 \\ 0.441149 \end{bmatrix}$	381 382 383
384 385 386	205 .4 207 .925		841.	9 757	.3 84 .6	0.547	3 0.996	$ \begin{array}{c cccc} 0 & 2.242 \\ 9 & 2.217 \\ \end{array} $		384 385 386
387 388 389	212.8 215.3 ₂₅		6 839	755	.0 84 .7	0.550	9 0.990	$\begin{array}{c c} 8 & 2.168 \\ 7 & 2.144 \\ 7 & 2.120 \\ 2 & 2.120 \\ \end{array}$	$\begin{array}{c c} 4 & 0.4614 \\ 0.466652 \\ 0.471852 \\ 3 & 0.471852 \end{array}$	387 388 389
390 391	220.4							2.097	$\begin{bmatrix} 0.4770 \\ 0.4823 \\ 54 \end{bmatrix}$	390 391

85.6

724.6

402.3 810.2

428

336.3

428 0.71881.392 0.59910.9129

TABLE II.

SATURATED STEAM.

ENGLISH UNITS.

Pressure, Pounds per Square Inch.	Temperature, Degrees Fahr.	Heat of the Liquid.	Heat of Vaporization.	Heat Equiva- lent of Inter- nal Work.	Heat Equiva- lent of Ex- ternal Work.	Entropy of the Liquid.	Entropy of Vaporization.	Specific Volume.	Weight, in G Pounds, as of One Scubic Foot.	Pressure, Pounds per Square Inch
p	t	q	r	ρ	Apu	θ	$\frac{r}{T}$	<i>s</i>	γ	p
1 2 3	$102.0_{243} \\ 126.3_{153} \\ 141.6_{115}$	94.3	1043 .1 1026 .2 1015 .5	981 .1 961 .9 949 .6	62 .0 64 .3 65 .9	0.1332 0.1756 0.2012	1 .8574 1 .7519 1 .6895	335 .3 _{161 .3} 174 .0 ₅₅ .4 118 .6 _{28 .0}	$\begin{array}{c} 0.00298_{277} \\ 0.00575_{268} \\ 0.00843_{261} \end{array}$	1 2 3
4 5 6	$^{153.1}_{162.378}_{170.168}$		1007 .5 1001 .2 995 .7	940 .6 933 .4 927 .1	66 .9 67 .8 68 .6	0.2201 0.2351 0.2478	1.6447 1.6100 1.5815	90.60 73.3811.56 61.828.32	$\begin{smallmatrix} 0.01104 \\ 0.01363259 \\ 0.01618251 \end{smallmatrix}$	4 5 6
7 8 9	176.960 182.954 188.349	144 .9 151 .0 156 .4		921 .8 916 .9 912 .8	69 .2 69 .8 70 .2	0.2584 0.2679 0.2763	1 .5571 1 .5359 1 .5174	47.194.06	$ \begin{smallmatrix} 0.01869 \\ 0.02119250 \\ 0.02368249 \\ 0.02368 \end{smallmatrix} $	7 8 9
10 11 12	$^{193.2}_{197.846}_{202.039}$	161 .4 166 .0 170 .2	976.3	908 .8 905 .2 901 .9	70.7 71.1 71.5		1.4853	$\begin{array}{c} 34.963.29 \\ 32.212.75 \\ 22.32 \end{array}$	$ \begin{array}{c} 0.02614 \\ 0.02860245 \\ 0.03105243 \end{array} $	10 11 12
13 14 15	$\begin{array}{c} 205.9 \\ 209.634 \\ 213.033 \end{array}$	174 .1 177 .8 181 .3	968.0	898 .8 895 .9 893 .0	72.1	0.3088	1.4467	27.862.03	$ \begin{array}{c} 0.03348 \\ 0.03590245 \\ 0.03817227 \\ 240 \end{array} $	13 14 15
16 17 18	$\begin{array}{c} 216.3_{31} \\ 219.4_{30} \\ 222.4_{28} \end{array}$	184 .6 187 .8 190 .8	961.1	888.0	73.1	0.3236	1.415	24 .65 23 .271 .38	0.04057 0.04297240 0.04535238	16 17 18
19 20 21	$\begin{bmatrix} 225.2 \\ 227.927 \\ 230.625 \end{bmatrix}$	193 .7 196 .5 199 .1	955.0	881.3	73.7	0.3362	1.389	2 19.95	0.04773 0.05011233 0.05248236	19 20 21
22 23 24	$\begin{bmatrix} 233.1_{24} \\ 235.5_{23} \\ 237.8_{22} \end{bmatrix}$	201 .6 204 .1 206 .4	949 .6	875.3	74.3	0.3472	1.366	18.24 ₇₅ 17.49 ₇₀ 16.79 ₆₃	$\begin{array}{c} 0.05484 \\ 0.0571923 \\ 0.0595423 \\ \end{array}$	
25 26 27	$\begin{bmatrix} 240.0 \\ 242.22 \\ 244.321 \\ 21 \end{bmatrix}$	208 .3 210 .9 213 .3	944.9	870.1	74.8	0 .357	1 .346	5 15.5855	0.06188 0.0642023 0.0665323	
28 29 30	246 .4 248 .319 250 .319	215 217 219	1 940.6	865 .3	75.3	0.3659	9 1.328	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	$ \begin{vmatrix} 0.06887 \\ 0.0711723 \\ 0.0734723 \\ 22 \end{vmatrix} $	28 29 30
31 32	252 .2 254 .0 ₁₈	221 .0 222 .		862.3 860 9	75.6 75.7	0.3714	1 .317 1 .312	$\begin{array}{c} 9 & 13.21 \\ 7 & 12.81 \\ 40 & 37 \end{array}$	$\begin{smallmatrix} 0.07576 \\ 0.07806 \\ 23 \end{smallmatrix}$	0 1 32

	1, 1									
	Pressure, Pounds per Square Inch.	Temperature, Degrees Fahr.	Heat of the Liquid.	Heat of Vap- orization.	Heat Equiva- lent of Inter- nal Work.	Heat Equiva- lent of Ex- ternal Work.	Entropy of the Liquid	Entropy of Vaporization.	Specific Volume,	Weight, in Founds, of One Cubic Foot.
1	p	t	q	r	ρ	Apu	θ	\overline{T}	s	γ
	33 34 35	255 .8 ₁₇ 257 .5 ₁₇ 259 .2 ₁₇	224 .6 226 .4 228 .1	935 .3 934 .0 932 .9	859 .4 858 .0 856 .7		0 .3764 0 .3790 0 .3814	1 .3075 1 .3026 1 .2979	12.44 ₃₄ 12.09 ₃₂ 11.77 ₃₀	$\begin{array}{c} 0.08037_{231} \\ 0.08268_{228} \\ 0.08496_{226} \end{array}$
	36 37 38	$\substack{ 260.9 \\ 262.516 \\ 264.115 }$	229 .8 231 .5 233 .1	931 .7 930 .5 929 .4	855 .4 854 .1 852 .9	76.4	0 .3837 0 .3859 0 .3881	1 .2932 1 .2887 1 .2844	$^{11.47}_{11.1829}_{10.9026}$	$\begin{array}{c} 0.08722 \\ 0.08948 \\ 226 \\ 0.09174 \\ 224 \end{array}$
	39 40 41	$\substack{265.6\\267.115\\268.615}$	234 .6 236 .2 237 .7	928 .3 927 .2 926 .2	851 .7 850 .5 849 .3		0 .3903 0 .3925 0 .3946	1 .2801 1 .2759 1 .2718	$10.64 \\ 10.3925 \\ 10.1524 \\ 10.1522$	$\begin{array}{c} 0.09398_{237} \\ 0.09625_{227} \\ 0.09852_{22} \end{array}$
	42 43 44	$\begin{array}{c} 270.1\\271.514\\272.914\\272.914\end{array}$	239 .2 240 .7 242 .1	925 .1 924 .1 923 . 1	848 - 1 847 . 0 845 . 9	77 .1	0.3967 0.3987 0.4006	1 .2679 1 .2641 1 .2604	$\begin{array}{c} 9.925 \\ 9.709216 \\ 9.502207 \\ 9.502198 \end{array}$	$\begin{smallmatrix} 0.1007_{23} \\ 0.1030_{22} \\ 0.1052_{23} \end{smallmatrix}$
	45 46 47	274 .3 275 .714 277 .013	243 .5 244 .9 246 .3	922 .1 921 .1 920 .1	844 .8 843 .7 842 .6	77.4	0.4025 0.4044 0.4062	1.2566 1.2529 1.2493	175	$\begin{smallmatrix} 0.1075 \\ 0.109722 \\ 0.112023 \\ 0.112022 \end{smallmatrix}$
1	48 49 50	$\begin{bmatrix} 278.3 \\ 279.613 \\ 280.812 \\ 13 \end{bmatrix}$	247 .6 248 .9 250 .2	919 .2 918 .3 917 .4	841 .6 840 .6 839 .6	77.7	0.4080 0.4098 0.4115	1 .2458 1 .2424 1 .2391	8.756 8.588168 8.429159 156	$\begin{smallmatrix} 0.1142 \\ 0.1164 \\ 22 \\ 0.1186 \\ 23 \end{smallmatrix}$
1	51 52 53	282 .1 283 .312 284 .512	251 .5 252 .7 253 .9	916.5 915.7 914.8	837.7	78.0	0 .4133 0 .4150 0 .4167		8.273 8.123150 7.981142 7.981139	$\begin{smallmatrix} 0.1209 \\ 0.123122 \\ 0.125322 \\ 0.125322 \end{smallmatrix}$
,	54 55 56	285 .7 286 .9 ¹² 288 .1 ¹¹	255 .2 256 .4 257 .6		834.7	78.3	0.4199	1.2232	7.580_{126}^{129}	0.131923
	57 58 59	$\begin{bmatrix} 289.2 \\ 290.3_{11} \\ 291.4_{11}^{11} \end{bmatrix}$	258 .8 259 .9 261 .0	910.6	832 .1	78.5	0.4246	1.2144	7.334_{115}^{120}	0.1385_{22}^{-1}
	60 61 62	292.5 293.611 294.711	262 .1 263 .2 264 .3		829 .4	i 78 .8		1.2060	$\begin{array}{c} 6.997110 \\ 6.892105 \\ 102 \end{array}$	0.1451_{22}^{22}
	63 64 65	$\begin{bmatrix} 295.7 \\ 296.710 \\ 297.811 \\ 297.810 \end{bmatrix}$	265 .4 266 .5 267 .5	905.9	827.0	79.0	0.4333	1.1980	$\begin{array}{c} 6.690^{100} \\ 6.592^{98} \\ \end{array}$	$ \begin{array}{c} 0.1473 \\ 0.149522 \\ 0.151722 \\ \end{array} $
	66 67 68	298.8 ₁₀ 299.8 ₁₀ 300.8 ₉	268 .6 269 .6 270 .6	903.7	824 .	5 79.3	0.4375	1.1902	$ \begin{smallmatrix} 6.499 \\ 6.40990 \\ 6.32287 \\ 6.32286 \end{smallmatrix} $	$ \begin{array}{c} 0.1539 \\ 0.156021 \\ 0.158222 \\ 0.158222 \end{array} $
	69 70 71	$\begin{bmatrix} 301.7 \\ 302.710 \\ 303.79 \end{bmatrix}$	271 .6 272 .6 273 .6	901.7	822 .	79.5	0.4414	1 .1829	$\begin{array}{c c} 6.15181 \\ 6.07079 \end{array}$	$ \begin{array}{c} 0.1604 \\ 0.162622 \\ 0.164721 \\ 0.164722 \end{array} $
	72 73	304.6 ₉ 305.5 ₁₀	274.5 275.5			0] 79.7			$\begin{array}{c} 5.991 \\ 5.915 \\ 74 \end{array}$	$\begin{smallmatrix} 0.1669 \\ 0.1691 \\ 21 \end{smallmatrix}$

SATURATED STEAM-TABLE II.

				RATE		TEAM-		GE II.	
Pressure, Pounds per Square Inch.	Temperature, Degrees Fahr.	Heat of the Liquid.	Heat of Vaporization.	Heat Equiva- lent of Inter- nal Work.	Heat Equiva- lent of Ex- ternal Work.	Entropy of the Liquid.	Entropy of Vaporiza- tion.	Specific Volume.	Weight, in Pounds, Front Of One
	t	q	r	ρ	Apu	θ	$\frac{r}{T}$	8	
74 75 76	306 .5 ₉ 307 .4 ₉ 308 .3 ₉	276 .5 277 .4 278 .3	898.9 898.3 897.7	819 .1 818 .6 817 .9	79.8	0.4477	1.1736 1.1714 1.1691	5.76972	0 .17: 0 .17: 0 .17:
77 78 79	$309.2_{9} \\ 310.1_{8} \\ 310.9_{9}$	279 .2 280 .1 281 .0	897 .0 896 .4 895 .8		0.08	0.4513		5.560 ₆₆ 5.494 ₆₃	0.17 0.17 0.18
80 81 82	$311.8_9 \ 312.7_8 \ 313.5_9$	281 .9 282 .8 283 .7	895.1 894.5 893.9	814.3	80.2	0.4548	1.1583	5.36861	0.18 0.18 0.18
83 84 85	314 .4 ₈ 315 .2 ₈ 316 .0 ₈	284.6 285.4 286.2	893.2 892.7 892.1	812.3	80.4	0.4581	1 .1522	5.246 ₅₈ 5.188 ₅₇	
86 87 88	316.8 ₈ 317.6 ₈ 318.4 ₈	287 .1 287 .9 288 .8	890.9	810.3	80.0	0.4614	1.146	5.020_{53}	0.19 0.19 0.20
89 90 91	319 .2 ₈ 320 .0 ₈ 320 .8 ₈	289 .5 290 .3 291 .1	889.3	3 808.	4 80.	8 0.464	1 .140	7 4.86450	0.20 0.20 0.20
92 93 94	321 .6 ₈ 322 .4 ₇ 323 .1 ₈	291 .9 292 .7 293 .5	887.	806.	6 80.	9 0.467	5 1.135	$ \begin{array}{c c} 0 & 4.718 \\ 4.671 \\ 4.671 \\ 4.671 \end{array} $	3 0.2.
95 96 97	323.9 324.6 325.4	294.3 295.3 295.9	1 885.	9 804.	8 81.	1 0.470	4 1.129	8 4.580	0.23 0.23 0.23
98 99 100	326 .1 326 .9 327 .6	296.6 297.3 298.	884.	3 803.	0 81.	2 0.473	3 1.126 3 1.124 3 1.122	$3 4.450_4^{11}$	$\begin{bmatrix} 0.22 \\ 0.2 \\ 0.2 \\ 0.2 \end{bmatrix}$
101 102 103	328 .37 329 .07 329 .77	7 298 .3 299 .0 7 300 .3	6 882.	7 801	3 81	.4 0.476	3 1.119	$4 \ 4.328_4$	$ \begin{array}{ccc} 0 & 0.2 \\ 0 & 0.2 \\ 0 & 0.2 \end{array} $
104 105 106	330 .4 331 .1 331 .8	301.	8 881	1 799	.6 81	.5 0.479	1 1.114	$ 5 4.212_3$	$\begin{array}{c c} 8 & 0.2 \\ 7 & 0.2 \\ 0.2 \end{array}$
107 108 109	332.5 333.2 333.9	7 303. 303. 304.	9 879	.7 798	.0 81	.7 0.48	1.109	$\begin{array}{c c} 12 & 4.138_3 \\ 66 & 4.102_3 \\ 4.067_3 \end{array}$	6 0.2 5 0.2 5 0.2
110 111 112	334.6 335.2 335.9	5110	0 878	.2 796	.4 81	.8 0.48	14 1.10	3.998_{3}^{3}	3 0.5 3 0.5
1	1	i i	- 1	1	1	- 1	1	1	1

877 .2 795 .3 81 .9 0 .4861 1 .1018 3 .932₃₂ 876 .7 794 .8 81 .9 0 .4869 1 .1004 3 .900₃₂

 $336.6_{6} \\ 337.2_{7}^{6}$

307 .4 308 .1

 $0.2 \\ 0.2$

	1									
Pressure, Pounds per Square Inch.	Temperature, Degrees Fahr.	the	Heat of Vaporization.	Heat Equiva- lent of Inter- nal Work.	Heat Equiva- lent of Ex- ternal Work.	Entropy of the Liquid.	Entropy of Vaporiza-	Je.	DENSITY.	Pressure, Pounds per Square Inch.
sure r Sq	pera	feat of Liquid.	of	Mor Edu	Eq.	ğ	opy pori	Specific Volume,	Veight, in Pounds, of One Cubic Foot.	ure, mds Squ h.
8 4 8 H	EQ.	Heat	Jeat	eat lent nal	feat lent tern	the	Intraction	peci V	Por Por	Por Per Inc
	l t	q	r	Pρ	Apu	θ	r	מס'	F	Δ.
		\ 	ļ				\overline{T}		γ	
115 116	337.9 ₆ 338.5 ₆	308.8	876.2	794.3	82.0		1.0988	3.86831	0.258521	115
117	339.17	309 .5 310 .1	875 .7 875 .3	793.8 793.3	82.0 82.0	0.4886 0.4894	1.0974	$3.868_{31} \\ 3.837_{30} \\ 3.807_{31}$	$ \begin{array}{c c} 0.2585 \\ 0.260621 \\ 0.262722 \end{array} $	116 117
118	330 8	310.8	874.8	792.8	82 .1	0.4902	1.0946		0.2640	118
119 120		311.4	874.4	792.3	82.1	0.4911	1.0931	$3.776_{30} \ 3.746_{29} \ 3.717_{28}$	$\begin{array}{c c} 0.2649 \\ 0.267021 \\ 0.269121 \\ \end{array}$	119
1	341.07	312.0	874.0	791 .8	82.2	0.4919	1.0918		20	120
121 122	341.7 ₆ 342.3 ₆	312.7 313.3	873 .5 873 .0	791.3 790.7	82.2 82.3	0 .4927 0 .4935	1.0903 1.0889	$3.689_{28} \ 3.661_{28} \ 3.633_{28}$	$ \begin{array}{c c} 0.2711 \\ 0.273221 \\ 0.275321 \\ 0.275321 \end{array} $	121 122
123	342.96	313.9	872.6	790.2	82.3	0.4943	1.0875	3.63328	0.275321	123
124	343.5	314.5	872.2	789 .8	82.3	0.4951	1.0861		0.2774	124
125 126	344.1 ₆ 344.7 ₆	315 .1 315 .8	871 .8 871 .3	789 .3 788 .8	$82.4 \\ 82.4$	0.4959	1.0848	$\begin{array}{c} 3.605_{27} \\ 3.57826 \\ 3.55226 \end{array}$	$ \begin{array}{c c} 0.2774 \\ 0.279521 \\ 0.281521 \end{array} $	125
l	1					0.4967	1.0835		0.281521	126
127 128	345.3 ₆ 345.9 ₆	316.4 317.0	870 .9 870 .4	788 .3 787 .9	82.5 82.5	$0.4975 \\ 0.4981$	1.0821 1.0808	$\frac{3.526}{50026}$	0.283621	127 128
129	345 .96 346 .56	317.6		787.5	82.5	0.4989	1.0794	$\begin{array}{c} 3.526_{26} \\ 3.500_{25} \\ 3.475_{25} \end{array}$	$ \begin{array}{c} 0.2836_{21} \\ 0.285721 \\ 0.2878_{21} \end{array} $	129
130	347.16	318.3	869.5	787.0	82.6	0.4997	1.0781	3.450		130
131 132	$347.1_{6} \\ 347.7_{6} \\ 348.3_{6}$	318 .9 319 .5	869 .1 868 .7	786.5 786.1	$82.6 \\ 82.6$	$0.5004 \\ 0.5012$	1.0768	$3.450_{25} \\ 3.425_{24} \\ 3.401_{24}$	$\begin{array}{c} 0.2899 \\ 0.292021 \\ 0.294121 \end{array}$	131
			1	i			1.0754	24	0.254121	132
133 134	$348.9_{6} \\ 349.5_{5} \\ 350.0_{6}$	320.1 320.7	868 .3 867 .8	785.6 785.1	$82.7 \\ 82.7$	0.5019 0.5027	$1.0740 \\ 1.0727$	3.377 ₂₄ 3.353°	0.2962_{20}	133 134
135	350.0_{6}^{3}	321 .3	867.4	784.7	82.7	0.5034	1.0715	$\begin{array}{c} 3.377 \\ 3.35324 \\ 3.32923 \end{array}$	$\begin{array}{c} 0.2962 \\ 0.298220 \\ 0.300321 \end{array}$	135
136	350.66	321.9	867.0	784.2	82.8	0.5042	1.0702	3.306_{23} 3.283_{22}^{23} 3.261_{22}^{23}		136
137 138	$\begin{array}{c} 350.6_{6} \\ 351.2_{5} \\ 351.7_{6} \end{array}$	322.4 323.0	866 .6 866 .2	783 .8 783 .4	82 .8 82 .8	0.5049	1.0689 1.0677	3.283_{22}^{23} 3.261_{21}^{22}	$\begin{array}{c} 0.3024 \\ 0.304521 \\ 0.306621 \\ 0.306620 \end{array}$	137 138
139	352.36	323 .6	865 .8	782.9		l	1	21		
140	352.9_{5}^{6} 353.4_{6}^{6}	324.2	865 .3	782.4	82.9 82.9	0.5062 0.5070	1.0664 1.0651	$egin{smallmatrix} 3 & .240 \\ 3 & .218 \\ 21 \\ 3 & .197 \\ 21 \end{bmatrix}$	0.308021	139 140
141	353 .46	324.8	864 .9	781.9	82.9	0.5077	1.0640	3.197_{21}^{21}	$\begin{array}{c} 0.3086 \\ 0.310721 \\ 0.312821 \\ \end{array}$	141
142 143	354 .0 ₅ 354 .5 ₆	325.4 326.0	864.5	781.5	83.0	0.5085	1.0627	3.17621	0.3149	142
144	355 .1 ₅	326.5	864 .1 863 .7	781 .1 780 .7	83 .0 83 .0	0.5092 0.5098	1.0616 1.0603	$3.176_{21} \\ 3.155_{21} \\ 3.134_{21}^{21}$	$\begin{array}{c} 0.3149 \\ 0.317021 \\ 0.319121 \\ 0.319121 \end{array}$	143 144
145		327.0	863.4	780 .3	83 .1	0.5105	1.0592			145
146 147	355 .6 ₅ 356 .1 ₆ 356 .7 ₅	327.6	863.0	779.9	83.1	0.5112	1.0581	$\begin{array}{c} 3.113\\ 3.09319\\ 3.07420 \end{array}$	$\begin{array}{c} 0.3212 \\ 0.323321 \\ 0.325320 \\ 0.325321 \end{array}$	146
	350.75	328 .1	862 .6	779 .5	83 .1	0.5119	1.0568			147
148 149	357 .2 ₅	328 .7 329 .2	862.2 861.8	779 .0 778 .6	83.2 83.2	0.5125 0.5131	1.0557 1.0546	3.054	0.3274	148 149
150	357 .2 ₅ 357 .7 ₆ 358 .3 ₅	329 .8	861.4	778.2	83.2	0.5138	1.0534	$\begin{array}{c} 3.054_{19} \\ 3.035_{19} \\ 3.016_{19} \end{array}$	$\begin{array}{c} 0.3274 \\ 0.329420 \\ 0.331521 \\ \end{array}$	150
151		330.4	861.0	777.8	83.3	0.5145	1 .0522	1		151
152 153	358 .8 ₅ 359 .3 ₅ 359 .8 ₅	330 .9 331 .4	860.6 860.3	777.4 777.0	83.3 83.3	0.5152	1.0511	$\begin{array}{c} 2.997 \\ 2.97819 \\ 2.96018 \end{array}$	$\begin{array}{c} 0.3336 \\ 0.335721 \\ 0.337821 \\ 0.337821 \end{array}$	152
j	505.05	1	1	-	1	0.5159	1.0500		0.337821	153
154 155	360.3 ₆ 360.9 ₅	331 .9 332 .4	859 .9 859 .6	776.6 776.2	83 .4 83 .4	0.5166 0.5172	1 .0489	$2.942_{18} \\ 2.924_{18}$	$\substack{0.3399\\0.3420}_{21}^{21}$	154 155
	- 5				·-		/	18	21	

	ire,	the	ų,	ra- ser-	Va-	jd.	g g		DENSITY.	re
Inch.	Temperature, Degrees Fahr.	Heat of t	Heat of Vaporization.	Heat Equiva- lent of Inter- nal Work.	Heat Equivalent of External Work.	Entropy of the Liquid.	Entropy of Vaporiza- tion,	Specific Volume.	Weight, in Pounds, of One Gubic Foot.	Pressure, Pounds per Square Inch.
	t	q	r	ρ	Apu	θ	$\frac{r}{T}$	s	γ	p
•	361 .4 ₅ 361 .9 ₅ 362 .4 ₅	333 .0 333 .5 334 .1	859 .2 858 .8 858 .4	775 .8 775 .3 774 .9	83 .4 83 .4 83 .5	0.5178 0.5184 0.5191		$\begin{smallmatrix} 2.906_{17} \\ 2.889_{17} \\ 2.872_{17} \end{smallmatrix}$	$\begin{array}{c} \textbf{0.3441}_{20} \\ \textbf{0.3461}_{21} \\ \textbf{0.3482}_{21} \end{array}$	156 157 158
	$ \begin{array}{r} 362.9 \\ 363.45 \\ 363.95 \\ \end{array} $	334 .6 335 .1 335 .6	858 .1 857 .7 857 .4	774.6 774.2 773.9	83.5 83.5 83.5	0.5198 0.5204 0.5210	1 .0434 1 .0423 1 .0412	$2.855 \atop 2.83817 \atop 2.821 \atop 17$	$\substack{0.3503 \\ 0.352421 \\ 0.354521}$	159 160 161
	364 .4 ₅ 364 .9 ₅ 365 .4 ₅	336 .1 336 .7 337 .2	857 .0 856 .6 856 .2	773.4 773.0 772.6	83.6 83.6 83.6	0.5216 0.5222 0.5229	1.0402 1.0391 1.0381	$^{2.804}_{2.78816}_{162.77216}$	$\begin{array}{c} \textbf{0.3566} \\ \textbf{0.358721} \\ \textbf{0.360821} \\ \textbf{0.360821} \end{array}$	162 163 164
	$ \begin{array}{r} 365.9 \\ 366.45 \\ 366.94 \\ \end{array} $	337 .7 338 .2 338 .7	855 .9 855 .5 855 .2	772.2 771.8 771.5	83 .7 83 .7 83 .7	0.5235 0.5241 0.5247	1.0370 1.0359 1.0348	$2.756_{15} \\ 2.741_{15} \\ 2.726_{15}$	$\substack{0.3629\\0.364920\\0.366920}$	165 166 167
	367.3 ₅ 367.8 ₅ 368.3 ₅	339 .2 339 .7 340 .2	854.8 854.5 854.1	771 .1 770 .7 770 .3	83.7 83.8 83.8	0.5253 0.5259 0.5265	1.0338 1.0328 1.0318	$\substack{\frac{2.711}{2.69615} \\ 2.68115}$	$\substack{\begin{array}{c} 0.3689 \\ 0.370921 \\ 0.373021 \\ 0.373021 \end{array}}$	168 169 170
	$\begin{array}{c} 368.8 \\ 369.2 \\ 369.7 \\ 5 \end{array}$	340 .7 341 .2 341 .6	853 .7 853 .4 853 .1	770.0 769.6 769.2	83 .8 83 .8 83 .9	0.5271 0.5277 0.5283	1.0308 1.0298 1.0288	$\substack{\frac{2.666}{2.65214}\\ 2.65215\\ 2.63714}$	$\substack{0.3751\\0.377120\\0.379221\\21}$	171 172 173
	$370.2_{570.75}$ $370.7_{4371.1_{5}}^{4}$	342 .1 342 .6 343 .1	852 .7 852 .4 852 .0	768.8 768.4 768.0	83.9 83.9 83.9	0.5289 0.5295 0.5301	1.0277 1.0266 1.0257	2.623 ₁₅ 2.608 ₁₄ 2.594 ₁₄	$\substack{0.3813\\0.383421\\0.385521\\0}$	174 175 176
	371.6 372.15 372.5 4 372.5 5	343 .6 344 .0 344 .5	851 .7 851 .4 851 .1	767.7 767.4 767.1	83 .9 84 .0 84 .0	0.5306 0.5312 0.5317	1.0247 1.0237 1.0227	2.580 ₁₄ 2.566 ₁₃ 2.553 ₁₃	$\substack{0.3876\\0.389721\\0.391820}$	177 178 179
	373.0_{4} 373.4_{5}^{4} 373.9_{4}^{5}	344 .9 345 .4 345 .9	850 .8 850 .5 850 .1	766.8 766.4 766.0	84.0 84.0 84.1	0.5323 0.5329 0.5335	1.0217 1.0207 1.0197	2.540 ₁₃ 2.527 ₁₄ 2.513 ₁₃	$\begin{array}{c} 0.3938 \\ 0.395820 \\ 0.397921 \end{array}$	180 181 182
	374.3 ₅ 374.8 ₄ 375.2 ₅	346 .4 346 .9 347 .4	849.7 849.3 849.0	765.6 765.2 764.9	84.1 84.1 84.1	0.5340 0.5346 0.5351	1.0188 1.0179 1.0170	$\begin{array}{c} 2.500 \\ 2.48712 \\ 2.47513 \end{array}$	$\begin{array}{c} 0.4000 \\ 0.402121 \\ 0.404120 \\ 0.404121 \end{array}$	183 184 185
	$375.7_4 \\ 376.1_5^4 \\ 376.6_4^5$	347 .8 348 .3 348 .8	848.7 848.3 848.0	764.6 764.2 763.8	84 .1 84 .2 84 .2	0.5357 0.5363 0.5368	1.0161 1.0152 1.0142	$2.462_{12} \\ 2.450_{13} \\ 2.437_{12}$	$\begin{smallmatrix} 0.4062\\ 0.408220\\ 0.410321\\ 0.410321\\ \end{smallmatrix}$	186 187 188
	377.0 ₄ 377.4 ⁴ 377.9 ⁵	349 .2 349 .7 350 .1	847 .7 847 .4 847 .1	763.5 763.2 762.8	84.2 84.2 84.3	0.5374 0.5379 0.5385	1.0133 1.0124 1.0115	$\begin{array}{c} 2.425 \\ 2.41312 \\ 2.40111 \\ \end{array}$	$\begin{array}{c} 0.4124 \\ 0.414521 \\ 0.416621 \\ \end{array}$	189 190 191
	378.3 ₅ 378.8 ₄ 379.2 ₄	350 .6 351 .0 351 .5	846.7 846.4 846.1	762 .4 762 .1 761 .8	84 .3 84 .3 84 .3	0.5390 0.5395 0.5400	1.0106 1.0097 1.0088	$2.390_{12} \\ 2.37812 \\ 2.36611$	$\begin{smallmatrix} 0.4186 \\ 0.420620 \\ 0.422721 \\ 0.422721 \end{smallmatrix}$	192 193 194
	379 .64 380 .05	351 .9 352 .3	845 .8 845 .5	761 .5 761 .2	84 .3 84 .3	0.5406 0.5412	1.0080 1.0071	$2.355_{12} \\ 2.343_{12}$	${0.4248\atop0.4269}_{20}^{21}$	195 196

per	ure,	the	ap-	Heat Equiva- lent of Inter- nal Work.	Heat Equiva- lent of Ex- ternal Work.	of uid	Entropy of Vaporiza-tion.	9.	DENSITY.	a ber
ure, inds are b.	erati grees grees	feat of Liquid.	of V zatio	Pa P	al of the	opy Liq	ropy apor	ific	Teight, in Pounds, of One Cubic Foot.	sure, unds uare ch.
Pressure, Pounds 1 Square Inch.	Temperature, Degrees Fahr.	Heat Lig	Heat of Vaporization.	Heat lent nal	leat lent tern	Entropy of the Liquid	Ent Çi	Specific Volume.	Wei Poof	Pressure, Pounds I Square Inch.
p	t t	q	r	ρ	Apu	θ	$\frac{r}{T}$	8	γ	<i>p</i>
107	200 5	250 0	845 .2	760*.8	84.4	0.5417	1.0062	2.331	0.4289	197
197 198	380 .5 380 .9	352 .8 353 .2	844.9	760.5	84.4	0.5422	1.0053	$\begin{bmatrix} 2.331 \\ 2.319 \\ 2.309 \\ 10 \end{bmatrix}$	$\begin{array}{c} 0.4289_{20} \\ 0.4309_{20} \\ 0.4329_{20} \end{array}$	198 199
199	381.3	353.6	844.6	760 .2	84.4	0.5427				
200 201	381 .7 382 .2	354.1 354.5	844.3 844.0	759 .9 759 .5	84.4	0.5432 0.5437	1.0035	0 06010	$\substack{0.4349\\0.436920\\0.438921}$	200 201
202	382.6	354.9		759 .2		0.5443	1.0018	1 17	0.4389_{21}^{20}	202
203	383.0	355.4		758.9		0.5448			$ \begin{array}{c} 0.4410 \\ 0.443121 \\ 0.445120 \\ 0.445121 \end{array} $	203 204
204 205	383 .4 383 .8	355.8 356.3		758.6 758.2		0.5453 0.5458		2.24611	$0.445120 \\ 0.445121$	205
206	384.2	356.8		757.8	84.6	0.5463	.9986			206
207	384.6	357.2	842.1	757.5	84.6	0.5469	.997	2.226	$ \begin{array}{c} 0.4472 \\ 0.449321 \\ 0.451421 \\ 0.451420 \end{array} $	207
208	385 .1	357.6		757 .2					0.4524	209
209 210	385 .5 385 .9	358.0 358.4		756 .9 756 .6		0.5484	.995	2.195_{10}^{10}	$ \begin{array}{c c} 0.4534 \\ 0.455521 \\ 0.457621 \\ 0.457621 \end{array} $	210
211	386.3	358.8		756.3	84.6	0.5489	.994	1	0.457621	211
212	386.7	359 .2		756.0		0.5493			$ \begin{array}{c c} 0.4597 \\ 0.461720 \\ 0.463821 \\ \end{array} $	212 213
213 214	387 .1 387 .5	359.6						$\begin{bmatrix} 2.157_{10}^{10} \\ 2.157_{10}^{10} \end{bmatrix}$	0.4638_{21}^{21}	214
215	387 .9	360.5	839 .7	755.0	84.7	0.550	.990	9 2.147	0.4659	215
216 217	388.3 388.7	360 .9 361 .3	839.5	754.8				$\begin{array}{c c} 9 & 2.147 \\ 1 & 2.137 \\ 3 & 2.128 \\ 9 \end{array}$	$ \begin{array}{c c} 0.4659 \\ 0.468021 \\ 0.470121 \\ \end{array} $	216 217
				1					0.4721	218
218 219	389 .1	361.	1 838 .6	753	84.8	0.552	8 .987	8 2.110	$ \begin{array}{c c} 0.4721 \\ 0.474120 \\ 0.476221 \\ 0.476220 \end{array} $	219 220
220	389 .8	362.	838 .3	753.	5 84.8	0.553				
221 222	390.2 390.6	362. 363.							$ \begin{array}{c} 0.4782 \\ 0.480321 \\ 0.482421 \\ 0.482421 \end{array} $	221 222
223	391.0		7 837					2.0749		223
224	391.4	364.		752.	4 84.8	0.555		2.065	$\begin{smallmatrix} 0.4845_{21} \\ 0.4866_{20} \\ 0.4886_{21} \\ \end{smallmatrix}$	224 225
225 226	391.8								0.488620	226
227	392.6	1		4 751.	5 84.	0.556	.98	l l		227
228	392.9	365.	7 836.	1 751	2 84.	9 0.557	.980	2.030°_{0}	$ \begin{array}{c} 0.4907 \\ 0.4928 \\ 0.4949 \\ 0.4949 \\ 20 \end{array} $	228 229
229	393 .3	1	j	1	}	1				
230 231							.97	$84 \mid 2.005^{\circ}_{0}$	0.4969_{21} 0.4990_{21}	231
232									0.001120	202
233								69 1.988	0.503120	233 234
234 235									$ \begin{array}{c} 0.5031 \\ 0.505120 \\ 0.507120 \\ 0.507121 \end{array} $	235
236		9 368	.8 833	.9 748	.9 85	.0 0.56	06 .97	48 1.964	$\begin{array}{c} 0.5092 \\ 0.5112 \\ 21 \end{array}$	236
237							.97	1.9568	0.511221	237

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Pressure, Pounds per Square Inch.	Temperature, Degrees Fahr.	Heat of the Liquid.	Heat of Vap- orization.	Heat Equiva- lent of Inter- nal Work.	Heat Equiva- lent of Ex- ternal Work.	Entropy of the Liquid.	Entropy of Vaporiza-tion.	Specific Volume.	Weight, in Pounds, of One Cubic Foot.	Pressure, Pounds per Square Inch.
p	t	q	r	ρ	Ари	θ	$\frac{r}{T}$	s	γ	p
238 239 240	396 .7 397 .0 397 .4	369 .7 370 .1 370 .4	833.3 833.0 832.7	748.3 748.0 747.7	85 .0 85 .0 85 .0	0.5620	.9732 .9725 .9718	1.948 ₈ 1.940 ₈ 1.932 ₇		238 239 240
241 242 243	397 .8 398 .1 398 .5	370 .7 371 .1 371 .5	832.6 831.3 832.0	747 .5 747 .2 746 .9	85 .1 85 .1 85 .1	0.5629 0.5633 0.5638	.9711 .9604 .9696	1.925 ₈ 1.917 ₇ 1.910 ₈	$ \begin{array}{c} 0.5195 \\ 0.521520 \\ 0.523621 \\ 0.523621 \end{array} $	241 242 243
244 245 246	398 .9 399 .2 399 .6	371 .9 372 .2 372 .6	831 .7 831 .5 831 .2	746 .6 746 .4 746 .1	85.1 85.1 85.1	0.5642 0.5646 0.5651	.9688 .9681 .9674	1.902 ₇ 1.895 ₈ 1.887 ₈	$ \begin{array}{c} 0.5257 \\ 0.527821 \\ 0.527821 \\ 0.529921 \end{array} $	244 245 246
247 248 249	399 .9 400 .3 400 .6	373 .0 373 .4 373 .7	830 .9 830 .6 830 .4	745 .8 745 .5 745 .3	85.1 85.1 85.1	0.5655 0.5659 0.5664	.9668 .9661 .9654	$1.879_{7} \\ 1.872_{7} \\ 1.865_{7}$	$ \begin{array}{c} 0.5320 \\ 0.534120 \\ 0.536120 \end{array} $	247 248 249
250 251 252	401.0 401.3 401.7	374.1 374.5 374.8	830 .1 829 .9 829 .7	745 .0 744 .7 744 .5	85 .1 85 .2 85 .2	0.5668 0.5672 0.5676	.9647 .9641 .9634	1.858_{7} 1.851_{7} 1.844_{7}	$\begin{array}{c} 0.5381 \\ 0.540120 \\ 0.542121 \end{array}$	250 251 252
253 254 255	402.0 402.4 402.7	375 .2 375 .6 375 .9	829 .4 829 .1 828 .9	744 .2 743 .9 743 .7	85.2 85.2 85.2	0.5681 0.5685 0.5689	.9627 .9620 .9613	$1.837_7 \\ 1.830_7 \\ 1.823_7$	$\begin{array}{c} 0.5442 \\ 0.546321 \\ 0.548421 \\ 0.548421 \end{array}$	253 254 255
256 257 258	403 .1 403 .4 403 .8	376 .3 376 .7 377 .0	828.6 828.3 828.1	743 .4 743 .1 742 .9	85.2 85.2 85.2	0.5693 0.5698 0.5702	.9606 .9599 .9592	$\substack{1.816 \\ 1.8097 \\ 1.8026}$	$\substack{0.5505\\0.552621\\0.554721\\21}$	256 257 258
259 260 261	404.1 404.5 404.8	377 .4 377 .8 378 .1	827 .8 827 .5 827 .3	742.6 742.3 742.0	85 .2 85 .2 85 .3	0.5706 0.5710 0.5714	.9585 .9578 .9572	$1.796_{7} \\ 1.789_{6} \\ 1.783_{7}$	$\begin{smallmatrix} 0.5568 \\ 0.5588 \\ 0.5609 \\ 21 \end{smallmatrix}$	259 260 261
262 263 264	405 .2 405 .5 405 .8	378 .5 378 .8 379 .2	827 .0 826 .8 826 .5	741 .7 741 .5 741 .2	85 .3 85 .3 85 .3	0.5718 0.5722 0.5726	.9565 .9559 .9552	$1.777_{7} \\ 1.770_{7} \\ 1.763_{6}$	$\begin{smallmatrix} 0.5630 \\ 0.565121 \\ 0.567221 \\ 0.567221 \end{smallmatrix}$	262 263 264
265 266 267	406 .2 406 .5 406 .8	379 .6 379 .9 380 .2	826 .2 826 .0 825 .8	740.9 740.7 740.5	85.3 85.3 85.3	0.5730 0.5734 0.5738	.9545 .9539 .9532	1.757_7 1.750_6 1.744_6	$\begin{array}{c} 0.5693 \\ 0.571420 \\ 0.573421 \\ \end{array}$	265 266 267
268 269 270	407 .2 407 .5 407 .9	380 .6 380 .9 381 .3	825 .5 825 .3 825 .0	740.2 740.0 739.7	85.3 85.3 85.3	0.5742 0.5746 0.5750	.9525 .9519 .9512	1.738_6 1.732_6 1.726_6	$\begin{smallmatrix} 0.5755 \\ 0.577621 \\ 0.579721 \\ 0.579720 \end{smallmatrix}$	268 269 270
271 272 273	408 .2 408 .5 408 .8	381 .6 382 .0 382 .3	824 .8 824 .5 824 .3	739 .5 739 .2 738 .9	85 .3 85 .3 85 .4	0.5754 0.5759 0.5763	.9505 .9499 .9493	1.720_7 1.713_6 1.707^6	$\begin{smallmatrix} 0.5817 \\ 0.583821 \\ 0.585921 \\ \end{smallmatrix}$	271 272 273
274 275 276	409 .2 409 .5 409 .8	382.7 383.0 383.4	824.0 823.8 823.5	738.6 738.4 738.1	85.4 85.4 85.4	0.5767 0.5771 0.5775	.9486 .9480 .9474	1.701 ₆ 1.695 ₆ 1.689 ₆	$\begin{array}{c} 0.5880 \\ 0.590121 \\ 0.592221 \\ \end{array}$	274 275 276
277 278	410.2 410.5	383.7 384.0	823 .3 823 .1	737 .9 737 .7	85 .4 85 .4	0.5779 0.5782	.9467 .9460	$\frac{1.683}{1.677}$	$0.5943_{21} \ 0.5964_{21}$	277 278

															4
303 304 305 306 307 308 309 310 311 312 313 314 315 316 317	304 305 306 307 308 309 310 311 312 313 314	304 305 306 307 308 309 310	304 305 306 307	304		300 301 302	297 298 299	294 295 296	291 292 293	288 289 290	285 286 287	282 283 284	279 280 281	<i>p</i>	Pressure, Pounds Square Inch.
418.3 418.6 418.9 419.2 419.5 419.8 420.1 420.4 420.7 421.0 421.3 421.6 421.9 422.2 422.5	418.6 418.9 419.2 419.5 419.8 420.1 420.4 420.7 421.0 421.3 421.6	418.6 418.9 419.2 419.5 419.8 420.1 420.4	418.6 418.9 419.2 419.5	418.6		417.4 417.7 418.0	416.5 416.8 417.1	415.6 415.9 416.2	414.6 414.9 415.3	413.7. 414.0 414.3	412.7 413.0 413.4	411.8 412.1 412.4	410 .8 411 .1 411 .4	t	Temperatur Degrees Fahr.
392 .2 392 .5 392 .8 393 .1 393 .5 393 .8 394 .4 394 .8 395 .1 395 .4 395 .7 396 .0 396 .3 396 .6	392.5 392.8 393.1 393.5 393.8 394.1 394.4 394.8 395.7	392.5 392.8 393.1 393.5 393.8 394.1 394.4	392.5 392.8 393.1 393.5	392.5		391.3 391.6 391.9	390.3 390.6 390.9	389 .3 389 .7 390 .0	388 .3 388 .6 388 .9	387 .4 387 .7 388 .0	386 .4 386 .7 387 .1	385 .4 385 .7 386 .0	384 .4 384 .7 385 .0	q	Heat of the Liquid.
817.3 817.1 816.9 816.7 816.4 816.2 816.0 815.8 815.5	817.3 817.1 816.9 816.7 816.4 816.2 816.0 815.8 815.5 815.3 815.0 814.8	817.3 817.1 816.9 816.7 816.4 816.2	817.3 817.1 816.9 816.7 816.4	817.3 817.1	011.0	818.0 817.7 817.5	818.7 818.5 818.3	819.4 819.1 318.9	820 .1 819 .9 819 .7	820.7 820.5 820.3	821 .4 821 .2 820 .9	822 .1 821 .9 821 .7	822.8 822.6 822.4	r	Heat of Va orization
731 .8 731 .6 731 .4 731 .2 730 .9 730 .7 730 .5 730 .3 730 .0 729 .8 729 .5 729 .2 729 .0 728 .8	731 .8 731 .6 731 .4 731 .2 730 .9 730 .7 730 .5 730 .3 730 .0 729 .8 729 .5 729 .2	731 .8 731 .6 731 .4 731 .2 730 .9 730 .7 730 .5 730 .3	731 .8 731 .6 731 .4 731 .2 730 .9	731 .8 731 .6	102.0	732.5 732.2 732.0	733 .2 733 .0 732 .8	733 .9 733 .6 733 .4	734.6 734.4 734.2	735 .2 735 .0 734 .8	776 .0 735 .8 735 .5	736 .7 736 .5 736 .3	737 .4 737 .2 737 .0	Ρ	Heat Equiv lent of Int nal Work.
85 .5 .5 .5 .5 .5 .5 .5 .5 .5 .5 .5 .5 .5	85.5.5 85.5.5 85.5.5.5 85.5.5 85.5.5 85.5.5 85.5.6 85.6	85.5 85.5 85.5 85.5 85.5 85.5 85.5	85.5 85.5 85.5 85.5	85 .5 85 .5	65.5	85 .5 85 .5 85 .5	85 .5 85 .5 85 .5	85.5 85.5 85.5	85 .5 85 .5 85 .5	85 .5 85 .5 85 .5	85 .4 85 .4 85 .4	85.4 85.4 85.4	85.4 85.4 85.4	Apu	Heat Equiv lent of E ternal Wo
0.5876 0.5880 0.5884 0.5891 0.5894 0.5901 0.5905 0.5908 0.5912	0.5876 0.5880 0.5884 0.5888 0.5891 0.5894 0.5901 0.5905 0.5908 0.5912 0.5916	0.5876 0.5880 0.5884 0.5888 0.5891 0.5894 0.5898 0.5901	0.5876 0.5880 0.5884 0.5888 0.5891	0 .5876 0 .5880	0.3873	0.5866 0.5869 0.5873	0.5854 0.5858 0.5862	0 .5843 0 .5847 0 .5851	0.5832 0.5836 0.5840	0 .5821 0 .5825 0 .5829	0.5809 0.5813 0.5817	0.5798 0.5802 0.5806	0.5786 0.5790 0.5794	θ	Entropy o the Liqui
.9311 .9306 .9300 .9294 .9288 .9282 .9277 .9271 .9255 .9260 .9254 .9249	.9311 .9306 .9300 .9294 .9288 .9282 .9277 .9271 .9255 .9260 .9254 .9249	.9311 .9306 .9300 .9294 .9288 .9282 .9277	.9311 .9306 .9300 .9294 .9288	.9311 .9306	.9311	.9328 .9322 .9317	.9345 .9340 .9334	.9363 .9357 .9351	.9382 .9377 .9370	.9399 .9393 .9387	.9416 .9410 .9404	.9435 .9429 .9423	.9454 .9448 .9442	$\frac{r}{T}$	Entropy (Vaporist
1.543 ₅ 1.538 ₅ 1.538 ₅ 1.538 ₅ 1.528 ₄ 1.519 ₅ 1.519 ₅ 1.509 ₄ 1.509 ₅ 1.495 ₅ 1.490 ₅ 1.485 ₅ 1.480 ₅ 1.485 ₅ 1.475 ₄	1.543 ₅ 1.538 ₅ 1.533 ₅ 1.524 ₄ 1.519 ₅ 1.519 ₅ 1.504 ₄ 1.500 ₅ 1.495 ₅ 1.490 ₅	1.543 ₅ 1.538 ₅ 1.533 ₅ 1.528 ₄ 1.524 ₄ 1.519 ₅	1.543 ₅ 1.538 ₅ 1.533 ₅		1.0105	$\begin{array}{c} 1.558\\1.5535\\1.5485\\1.5485\end{array}$	$\begin{array}{c} 1.574 \\ 1.5685 \\ 1.5635 \end{array}$	1 .589 1 .5845 1 .5795	1.605 $1.6005 $ 1.5956	1.621_{5} 1.616_{5} 1.611_{6}	$^{1.638}_{1.6325}$ $^{1.632}_{1.627}$	$1.654_{5} \\ 1.649_{6} \\ 1.643_{5}$	$1.672_{6} \\ 1.666_{6} \\ 1.660_{6}$	<i>s</i>	Specific Volume.
$\begin{array}{c} 0.648 \\ 0.6502 \\ 0.6522 \\ 0.6542 \\ 0.6562 \\ 0.6582 \end{array}$	$\begin{array}{c} 0.648_2 \\ 0.650_2 \\ 0.652_2 \\ \end{array}$ $\begin{array}{c} 0.654_2 \\ 0.656_2 \\ 0.658_2 \\ \end{array}$ $\begin{array}{c} 0.660_2 \\ 0.662_2 \\ 0.664_2 \\ \end{array}$ $\begin{array}{c} 0.666_3 \\ 0.669_2 \\ 0.671_2 \\ \end{array}$	$\begin{array}{c} 0.648 \\ 0.6502 \\ 0.6522 \\ 0.6542 \\ 0.6562 \\ 0.6582 \end{array}$	$\begin{array}{c} 0.648 \\ 0.650 \\ 0.652 \\ 2 \end{array}$	i	2	$\begin{array}{c} 0.642 \\ 0.644 \\ 0.646 \\ 2 \end{array}$	$\substack{0.635\\0.637^2\\0.639^2_3}$	$\begin{array}{c} 0.629 \\ 0.631 \\ 0.633 \\ 2 \end{array}$	$\substack{0.623\\0.625\\2\\0.627\\2}$	$\begin{array}{c} 0.616_{2} \\ 0.618_{2}^{2} \\ 0.620_{3}^{2} \end{array}$	$\begin{array}{c} 0.610 \\ 0.612 \\ 0.614 \\ 2 \end{array}$	$\substack{0.604\\0.6062\\0.6082}$	$\substack{0.5985_{2}\\0.600_{2}\\0.602_{2}^{2}}$	У	Weight, in Pounds, of One Cubic Foot.
303 304 505 306 307 308 309 310 311 312 313 314 315 316 317	303 304 505 306 307 308 310 311 312 313 314	303 304 505 306 307 308 309 310	303 304 505 306 307	303 304	002	300 301 302	297 298 299	294 295 296	291 292 293	288 289 290	285 286 287	282 283 284	279 280 281	<i>p</i>	Pressure, Pounds Square Inch.

SATURATED STEAM-TABLE II.

P.	je,	the	<u> 4</u> .	er-	F. 7. 7.	đ.	of L		DENSITY.
Pressure, Pounds per Square Inch.	Temperature, Degrees Fahr.	Heat of the Liquid.	Heat of Vaporization.	Heat Equiva- lent of Inter- nal Work.	Heat Equiva- lent of Ex- ternal Work.	Entropy of the Liquid.	Entropy of Vaporiza-tion.	Specific Volume.	Weight, in Pounds, of One Cubic Foot.
p	t	q	r	ρ	Apu	θ	$\frac{r}{T}$	5	γ
320 321 322	423 .4, 423 .7 424 .0	397 .5 397 .8 398 .1	813.6 813.4 813.1	728 .0 727 .8 727 .5		0.5936 0.5940 0.5943		$\substack{1.462\\1.457\\1.457\\4\\1.453\\5}$	$\begin{array}{c} 0.683_{3} \\ 0.686_{2} \\ 0.688_{3} \end{array}$
323 324 325	424 .2 424 .5 424 .8	398 .4 398 .7 399 .0	812.9 812.7 812.5	727 .3 727 .1 726 .9	85.6	0.5946 0.5949 0.5952	.9193	$\begin{array}{c} 1.448_{5} \\ 1.443_{4} \\ 1.439_{5} \end{array}$	$\begin{array}{c} 0.691 \\ 0.6932 \\ 0.6952 \end{array}$
326 327 328	425 .1 425 .4 425 .7	399 .3 399 .6 399 .9		726.5	85.6	0.5956 0.5959 0.5963	.9176	$\begin{array}{ c c c }\hline 1.434_4\\ 1.430_4\\ 1.426_4\\ \end{array}$	$ \begin{array}{c c} 0.697 \\ 0.6992 \\ 0.7012 \end{array} $
329 330 331	426.0 426.2 426.5	400 .2 400 .5 400 .8	811.4	725 .8	85.6	0.5970	.9161	$\begin{array}{ c c c c }\hline 1.422_5\\ 1.417_4\\ 1.413_4\\ \end{array}$	$ \begin{array}{c c} 0.703_{3} \\ 0.706_{2}^{3} \\ 0.708_{2}^{2} \end{array} $
332 333 334	426 .8 427 .1 427 .4	401 .1 401 .4 401 .7	810.8	725 .2	85.6	0.5980	.9145	$ \begin{array}{ c c c c c } \hline 1.409_4\\1.405_4\\1.401_4\\\hline \end{array} $	$ \begin{bmatrix} 0.710 \\ 0.712 \\ 0.714 \\ 2 \end{bmatrix} $
335 336	427 .6 427 .9	402.0 402.3						1.397 1.393 ⁴	$\begin{array}{c c} 0.716 \\ 0.718^2 \end{array}$

TABLE III.

SATURATED STEAM.

FRENCH AND ENGLISH CONVERSION TABLES.*

re, Jenti-		PRESSURE.		HEAT THE LI		HEA VAPORI	T OF ZATION.	LENT	Equiva- of In- Work.	e, Jahr.
Temperature, Degrees Centi- grade.	Milli- meters of Mer- cury.	Kilo- grams per Square Centi- meter.	Pounds per Square Inch.	Calories.	B.T.U.	Calories.	B.T.U.	Calories.	B.T.U.	Temperature, Degrees Fahr.
t	p	p	p	q	q	r	r	ρ	ρ	t
0 1 2	4.602 ₃₃₉ 4.941 ₃₆₂ 5.303 ₃₈₆	$\begin{array}{c} .006257_{461} \\ .006718_{492} \\ .007210_{525} \end{array}$	$\begin{smallmatrix} 0.0890_{65} \\ 0.0955_{71} \\ 0.1026_{74} \end{smallmatrix}$	0.00 1.01 2.02	0.0 1.8 3.6	606 .5 605 .8 605 .1	1091 .7 1090 .4 1089 .1	575.4 574.6 573.8	1035 .8 1034 .4 1033 .0	32 33 .8 35 .6
3 4 5	5.689 6.100436 6.536465	.007735 ₅₅₈ .008293 ₅₉₃ .008886 ₆₃₃	$\begin{smallmatrix} 0.1100_{79} \\ 0.1179_{85} \\ 0.1264_{90} \\ \end{smallmatrix}$	3 .03 4 .03 5 .04	5.5 7.3 9.1	604 .4 603 .7 603 .0	1087 .9 1086 .6 1085 .3	573.1 572.3 571.5	1031 .5 1030 .1 1028 .7	37.4 39.2 41.0
6 7 8	7.001 7.494493 8.019557	$\begin{array}{c} .009519 \\ .010198679 \\ .01090 \\ 76 \end{array}$	$\substack{0.1354_{95}\\0.1449_{102}\\0.1551_{107}}$	6 .04 7 .05 8 .05	10 .9 12 .7 14 .5	602 .3 601 .5 600 .8	1084 .1 1082 .8 1081 .6	570 .7 569 .9 569 .1	1027 .3 1025 .9 1024 .5	42.8 44.6 46.4
9 10 11	8.576 9.167591 9.795665	$\begin{array}{c} .01166_{80} \\ .01246_{86} \\ .01332_{90} \end{array}$	$\begin{array}{c} 0.1658\\ 0.1773115\\ 0.1894\\ 129 \end{array}$	9 .05 10 .06 11 .06	16.3 18.1 19.9	599.5	1080 .3 1079 .1 1077 .8	568.3 567.6 566.8	1023 .1 1021 .7 1020 .3	
12 13 14	$\begin{bmatrix} 10.46\\11.16\\75\\11.91\\79 \end{bmatrix}$	$ \begin{array}{c c} .01422_{95} \\ .01517_{102} \\ .01619_{108}^{108} \end{array} $	$\substack{0.2023\\0.2159136\\0.2303144\\0.2303}$	12.06 13.06 14.06		597.4	1076.6 1075.3 1074.1	566.0 565.2 564.4	1018.9 1017.5 1016.1	53.6 55.4 57.2
15 16 17	$\begin{bmatrix} 12.70 \\ 13.5484 \\ 14.4288 \\ 14.4294 \end{bmatrix}$.01727 .01841114 .01961 ₁₂₇	$ \begin{smallmatrix} 0.2456 \\ 0.2619163 \\ 0.2789170 \\ 181 \end{smallmatrix} $	15.06 16.06 17.06	28.9	595.3	1072.8 1071.6 1070.3	562.9	1014.7 1013.3 1011.9	
18 19 20	$\begin{bmatrix} 15.36\\16.3599\\17.40105\\17.40110 \end{bmatrix}$.02088 .02223135 .02366143 .02366149	$ \begin{bmatrix} 0.2970 \\ 0.3162_{192} \\ 0.3364_{214}^{202} \end{bmatrix} $	18.06 19.06 20.06	34.3	593.2	1069 .1 1067 .8 1066 .6			66.2
21 22 23	18.50 19.66116 20.89123 130	.02515 .02673158 .02840167	$ \begin{array}{c} 0.3578 \\ 0.3803225 \\ 0.4041250 \end{array} $		39.7	591.1	1064.1	558.1	1006.3 1004.9 1003.4	69.8 71.6 73.4
24 25 26	22.19 23.55136 24.99144 24.99152	.03017 .03202185 .03398196 .03398206	0.4291	24.06 25.05 26.05	45.1	589.0	1060.3	555.8		77.0
27	26.51,00	.03604			48.7	587.6	1057 .8	554.3	997.8	80.6

TABLE III.

SATURATED STEAM.

FRENCH AND ENGLISH CONVERSION TAB

enti-	HE Equiva OF Ex	LENT TER-	the	of tion.	Spec Volu		
Temperature, Degrees Centigrade.	Calories.	B.T.U.	Entropy of Liquid.	Entropy of Vaporization.	Cubic Meters per Kilo.	Cubic Feet per Pound.	Weight in Kilo- grams of One
t	A pu	Apu	0	$\frac{r}{T}$	8	8	γ
0 1 2	31.1 31.2 31.3	55.9 56.0 56.2	0 0.0037 0.0074	2.2211 2.2105 2.2000	$212.0_{138} \\ 198.2_{132} \\ 185.0_{122}$	$\substack{\frac{3395}{2120}\\3175\\212}\\2963\\195}$	0 .00471 0 .00504 0 .00540
3 4 5	31.3 31.4 31.5	56 .3 56 .5 56 .6	0.0110 0.0146 0.0183	2.1890 2.1789 2.1684	$^{172.8}_{161.6}_{104}_{151.2}_{96}$	$\begin{array}{c} 2768 \\ 2589 \\ 168 \\ 2421 \\ 153 \end{array}$	0.00578 0.00618 0.00661
6 7 8	31 .6 31 .7 31 .7	56.8 56.9 57.1	$\begin{array}{c} 0.0219 \\ 0.0256 \\ 0.0290 \end{array}$	2.1583 2.1482 2.1379	$\begin{bmatrix} 141.6_{91} \\ 132.5_{83} \\ 124.2_{78} \end{bmatrix}$	$\begin{array}{c} 2268146 \\ 2122133 \\ 1989124 \end{array}$	0 .00706 0 .00754 0 .00805
9 10 11	31 .8 31 .9 32 .0	57 .2 57 .4 57 .5	0.0326 0.0361 0.0397	2.1279 2.1180 2.1081	$116.4_{71} \\ 109.3_{68} \\ 102.5_{62}$	$\begin{array}{ c c c c }\hline 1865 & 116 \\ 1749 & 107 \\ 1642 & 99 \\ \hline \end{array}$	0 .00859 0 .00914 0 .00978
12 13 14	32 .1 32 .2 32 .3	57.7 57.8 58.0	0.0433 0.0467 0.0502	2.0983 2.0885 2.0786	90.4253		0 .01038 0 .01108 0 .0117
15 16 17	32 .3 32 .4 32 .5	58.1 58.3 58.4		2.0691 2.0595 2.0502	75.1644	$\begin{array}{c} 1279_{75} \\ 1204_{71} \\ 1133_{66} \end{array}$	0 .0125 0 .0133 0 .0141
18 19 20	32.6 32.7 32.8	58.6 58.7 58.9	0.0675		62.73_{36}^{36}	$\begin{array}{c} 1067_{62} \\ 1005_{558} \\ 946.9_{540} \end{array}$	0.0150 0.0159 0.0169

0.0743

0.0776

0.0811

0.0845

0.0878

0.0911

59.1

59.2

59.4

59.5

59.7

59.9

21

22

23

24

25

26

32.9

33.0

33.0

33.1

33.2

33.3

2.0129

2.0035

1.9945

1.9854

1.9763

1.9673

 $\begin{array}{c} 55.74_{316} \\ 52.58_{296} \\ 49.62_{278} \end{array}$

 $\substack{46.84 \\ 44.25259 \\ 41.8228}$

 $\substack{892.9 \\ 842.2}_{474}_{794.8}$

 $\begin{array}{c} 750.3_{416} \\ 708.7_{388} \\ 669.9_{365} \end{array}$

0.0179

0.0190

0.0201

0.0213

0.0226

0.0239

HEAT

	re, Cent		PRESSURE			LIQUID.	VAPOR	AT OF LIZATION.	LENT	of In- L Work.	e, ahr.
	Temperature, Degrees Cent	Milli- 'd meters of Mer- cury	Kilo- grams per Square Centi- meter.	Pounds per Square Inch.	ದಿ Calories.	b B.T.U.	ء Calories,	, B.T.U.	ъ Calories.	B.T.U.	Temperature, Degrees Fahr.
	. 31 32 33	33.41 ₁₉₅ 35.36 ₂₀₆ 37.42 ₂₁₅	$\begin{smallmatrix} 0.04543_{265} \\ 0.04808_{279} \\ 0.05087_{294} \end{smallmatrix}$	$\begin{array}{c} 0.6462_{377} \\ 0.6839_{397} \\ 0.7236_{417} \end{array}$	31 .04 32 .04 33 .04	55.9 57.7 59.5	585.0 584.3 583.6	1052.9 1051.6 1050.3	551.2 550.4 549.6	992.2 990.7 989.2	87.8 89.6 91.4
	34 35 36	39.57 ₂₂₆ 41.83 ₂₃₈ 44.21 ₂₄₉	$\begin{array}{c} 0.05381_{307} \\ 0.05688_{323} \\ 0.06011_{339} \end{array}$	$\begin{array}{c} 0.7653_{437} \\ 0.8090_{460} \\ 0.8550_{481} \end{array}$	34 .03 35 .03 36 .03	61.3 63.1 64.9	582.9 582.2 581.5	1049 .0 1047 .8 1046 .6	548.8 548.1 547.3	987.8 986.4 985.0	93.2 95.0 96.8
	37 38 39	46.70 ₂₆₁ 49.31 ₂₇₄ 52.05 ₂₈₆	0.06350 ₃₅₅ 0.06705372 0.07077 ₃₈₉	0.9031 ₅₀₅ 0.9536 ₅₃₀ 1.0066 ₅₅₃	37.02 38.02 39.02	66.6 68.4 70.2	580.8 580.1 579.4	1045.4 1044.2 1042.9	546.5 545.7 544.9	983.6 982.2 980.9	98.6 100.4 102.2
	40 41 42	54.91 ₃₀₁ 57.92 ₃₁₄ 61.06 ₃₂₉	$\begin{smallmatrix} 0.07466_{410} \\ 0.07876_{427} \\ 0.08303_{447} \\ \end{smallmatrix}$	1 .0619 ₅₈₃ 1 .1202 ₆₀₇ 1 .1809 ₆₃₆	40 .02 41 .01 42 .01	72.0 73.8 75.6	578.7 578.0 577.3	1041 .7 1040 .4 1039 .2	544.1 543.3 542.5	979.5 978.1 976.6	104.0 105.8 107.6
	43 44 45	64.35 ₃₄₅ 67.80 ₃₆₀ 71.40 ₃₇₆	513	1 .2445 1 .3113694 1 .3807729	43 .01 44 .01 45 .00	77.4 79.2 81.0	576.6 575.9 575.2	1037 .9 1036 .7 1035 .4	541.7 540.9 540.1	975.2 973.7 972.3	109 .4 111 .2 113 .0
	46 47 48	75.16 ₃₉₄ 79.10 ₄₁₁ 83.21 ₄₃₀	585	1.4536 ₇₆₂ 1.5298 ₇₉₅ 1.6093 ₈₃₁	46.00 47.00 48.00	82.8 84.6 86.4	574.5 573.8 573.1	1034.1 1032.9 1031.6	539 .3 538 .5 537 .7	970.9 969.5 968.0	114.8 116.6 118.4
	49 50 51	87.51 ₄₄₇ 91.98 ₄₆₇ 96.65 ₄₈₉	0.11899 ₆₀₈ 0.12507 ₆₃₄ 0.13141 ₆₆₃	$\substack{1.6924_{865}\\1.7789_{901}\\1.8690_{944}}$	48.99 49.99 50.99	88.2 90.0 91.8	572.4 571.8 571.1	1030 .5 1029 .2 1027 .9	537 .0 536 .3 535 .5	966.7 965.3 963.9	120 .2 122 .0 123 .8
		$101.54_{510} \\ 106.64_{531} \\ 111.95_{554}$	$\begin{smallmatrix} 0.13804_{693} \\ 0.14497_{723} \\ 0.15220_{754} \\ \end{smallmatrix}$	$\substack{1.9634_{986}\\2.0620_{1027}\\2.1647_{1072}}$	51.99 52.99 53.98	93.6 95.4 97.2	570 .4 569 .7 569 .0	1026 .7 1025 .4 1024 .2	534.6 533.8 533.0	962.4 961.0 959.5	125 .6 127 .4 129 .2
		$^{117.49}_{123.25}_{601}_{625}$	0.15974 ₇₈₃ 0.16757 ₈₁₇ 0.17574 ₈₅₀	$egin{array}{c} 2.2719 \\ 2.3833 \\ 1162 \\ 2.4995 \\ 1209 \end{array}$	54.98 55.98 56.98	99.0 100.8 102.6	568.3 567.6 566.9	1022 .9 1021 .7 1020 .4	532.2 531.5 530.8	958 .1 956 .7 955 .3	131 .0 132 .8 134 .6
		$^{135.51}_{142.02678}_{678}_{148.80705}$	$\begin{array}{c} 0.18424_{884} \\ 0.19308_{922} \\ 0.20230_{959} \end{array}$	$2.6204_{1259} \ 2.7463_{1311} \ 2.8774_{1363}$		104.4 106.2 108.0	566 .2 565 .5 564 .8	1019.2 1017.9 1016.6	530.0 529.2 528.4	953.8 952.4 950.9	136 .4 138 .2 140 .0
		155 .85 ₇₃₃ 163 .18 ₇₆₂ 170 .80 ₇₉₂	$\substack{0.21189\\0.22185996\\0.232221037\\0.232221075}$	$egin{array}{c} 3.0137_{1418} \ 3.1555_{1474} \ 3.3029_{1531} \end{array}$	62.97	109 .8 111 .6 113 .4	564.1 563.4 562.7	1015.3 1014.1 1012.9	527.6 526.8 526.0	949 .5 948 .0 946 .7	141 .8 143 .6 145 .4
		178.72 ₈₂₃ 186.95 ₈₅₅ 195.50 ₈₈₈	0.26580_{1207}^{1163}	$egin{array}{c} 3.4560_{1592} \ 3.6152_{1654} \ 3.7806_{1717} \end{array}$	65.98	115.2 117.0 118.8	562.0 561.3 560.6	1011.7 1010.4 1009.2	525.1 524.3 523.5	945.2 943.8 942.4	147 .2 149 .0 150 .8
	67 68 69	$204.38_{9}22$ $213.60_{9}57$ $223.17_{9}92$	$\substack{0.27787\\0.290411254\\0.30342\\1348}$	3.9523 ₁₇₈₃ 4.1306 ₁₈₅₁ 4.3157 ₁₉₁₈	66.98 67.98 68.98	120.6 122.4 124.2	559 .9 559 .2 558 .5	1007.8 1006.6 1005.3	522.7 521.9 521.1	940 .9 939 .5 938 .0	152.6 154.4 156.2
L		222 00	0.21600	4 5075	60 00	100 0	FFF 0	1004 1	F00 F		

Jre, Cen	OF EX	TER-	of ti	of ratio		UME.	ii s	- n s o	ure, s Fa
Temperature, Degrees Cen grade.	Calories.	B.T.U.	Entropy Liquid.	Entropy of Vaporizatio	Cubic Meters per Kilo.	Cubic Feet Per Pound.	Weight, ir Kilo- grams, of One Cubic Meter.	Weight, in Pounds, of One Cubic Foot.	Temperature, Degrees Fal
t	Apu	Apu	θ	$\frac{r}{T}$. s	<u> </u>	γ	γ	t
31 32 33	33.8 33.9 34.0	60.7 60.9 61.0	0.1077 0.1110 0.1142		31.72 ₁₆₇ 30.05 ₁₅₇ 28.48 ₁₄₈	$508.1_{267} \\ 481.4_{252} \\ 456.2_{237}$	0.03153 ₁₇₅ 0.03328 ₁₈₃ 0.03511 ₁₉₃	$\begin{array}{c} 0.001968\\ 0.002077115\\ 0.002192120 \end{array}$	87.8 89.6 91.4
34 35 36	34.1 34.1 34.2	61.2 61.4 61.6	0.1175 0.1207 0.1239	1.0011	$\begin{array}{c} 27.00_{138} \\ 25.62_{131} \\ 24.31_{124} \end{array}$	$\substack{432.5 \\ 410.223 \\ 389.4} \\ \substack{208 \\ 199}$	$ \begin{array}{c} 0.03704 \\ 0.03903 \\ 0.04114 \\ 221 \end{array} $	$\begin{smallmatrix} 0.002312\\ 0.002438130\\ 0.002568\\ 138 \end{smallmatrix}$	93.2 95.0 96.8
37 38 39	34.3 34.4 34.5	61.7 61.9 62.0	0.1272 0.1304 0.1336		$23.07_{116} \\ 21.91_{110} \\ 20.81_{103}$	$\begin{array}{c} 369.5 \\ 351.0 \\ 177 \\ 333.3 \\ 165 \end{array}$	$\begin{smallmatrix} 0.04335 \\ 0.04564229 \\ 0.04805251 \end{smallmatrix}$	$\begin{array}{c} 0.002706 \\ 0.002849143 \\ 0.003000157 \end{array}$	98.6 100.4 102.2
40 41 42	34.6 34.7 34.8	62.2 62.4 62.6	0.1368 0.1399 0.1431	1.8485 1.8405 1.8324	19.78 ₉₈ 18.80 ₉₂ 17.88 ₈₆	316.8 ₁₅₇ 301.1 ₁₄₇ 286.4 ₁₃₈	$ \begin{array}{c} 0.05056 \\ 0.05319 \\ 274 \\ 0.05593 \\ 282 \end{array} $	$\begin{array}{c} 0.003157\\ 0.003321164\\ 0.003492176 \end{array}$	104.0 105.8 107.6
43 44 45	34.9 35.0 35.1	62.7 62.9 63.1	0.1463 0.1494 0.1526	1.8243 1.8164 1.8085	$\begin{array}{c} 17.02_{82} \\ 16.2078 \\ 15.4273 \end{array}$	$\begin{smallmatrix} 272.6 \\ 259.5 \\ 125 \\ 247.0 \\ 117 \end{smallmatrix}$	$\begin{smallmatrix} 0.05875 \\ 0.06173298 \\ 0.06485312 \\ 0.06485322 \end{smallmatrix}$	$\begin{array}{c} 0.003668\\ 0.003854186\\ 0.004049\\ 201 \end{array}$	109.4 111.2 113.0
46 47 48	35 .2 35 .3 35 .4	63.3 63.4 63.6	0.1557 0.1588 0.1619	1.8007 1.7929 1.7851	14.69 ₆₉ 14.00 ₆₆ 13.34 ₆₃	235 .3 ₁₁₀ 224 .3 ₁₀₆ 213 .7 ₁₀₁	$\begin{smallmatrix} 0.06807\\ 0.0714336\\ 0.07496353\\ 0.07496372\end{smallmatrix}$	0.004250 0.00445822 0.00467923	114.8 116.6 118.4
. 49 50 51	35 .5 35 .6 35 .7	63 .7 63 .9 64 .1	0.1650 0.1682 0.1713	1.7774 1.7699 1.7623	12.71 ₅₈ 12.13 ₅₅ 11.58 ₅₃	203 .6 ₉₃ 194 .3 ₈₈ 185 .5 ₈₅	$ \begin{array}{c} 0.07868\\ 0.08244376\\ 0.08636392\\ 414 \end{array} $	0.004912 0.00514724 0.00539125	9
52 53 54	35 .8 35 .9 36 .0	64.3 64.4 64.6	0.1743 0.1774 0.1804	1.7548 1.7472 1.7397	$11.05_{50} \\ 10.55_{47} \\ 10.08_{45}$	177.0 ₈₀ 169.0 ₇₅ 161.5 ₇₃	$ \begin{array}{c} 0.09050 \\ 0.09479442 \\ 0.09921469 \end{array} $	$\begin{smallmatrix} 0.005650_{26} \\ 0.005917_{27} \\ 0.006192_{29} \end{smallmatrix}$	125.6 127.4 129.2
55 56 57	36 .1 36 .2 36 .2	65.0	0.1835 0.1865 0.1895	1.7323 1.7249 1.7175	9.628 9.203425 8.800 ₃₈₃	$\frac{141.062}{62}$	$ \begin{array}{c} 0.1039 \\ 0.1087 \\ 49 \\ 0.1136 \\ 52 \end{array} $	$ \begin{array}{c c} 0.006485_{29} \\ 0.006784_{30} \\ 0.007092_{32} \end{array} $	9 131.0 132.8 134.6
58 59 60	36 .3 36 .4 36 .5	65.5	0.1925 0.1955 0.1986	1.7102 1.7029 1.6957	8.417 8.054363 7.703326	$\begin{array}{c} 134.8 \\ 129.058 \\ 123.452 \end{array}$		$ \begin{array}{c} 0.007418_{33} \\ 0.007752_{34} \\ 0.008100_{36} \end{array} $	136.4 138.2 140.0
61 62 63	36.6 36.7 36.8	66.1	0.2016 0.2046 0.2075	1.6815	7.377 7.065 6.768	$\begin{array}{c} 118.2 \\ 113.2 \\ 48 \\ 108.4 \\ 46 \end{array}$	0.1356 ₅₉ 0.1415 ₆₃ 0.1478 ₆₅	0.008460 ₃₇ 0.008834 ₃₈ 0.009225 ₃₉	141.8 143.6 145.4
64 65 66	36 .9 37 .0 37 .1	66.6	0.2135	1.6605	6.483 6.213 5.959 242	$\begin{array}{c} 103.8 \\ 99.5440 \\ 95.4538 \end{array}$	$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	$ \begin{bmatrix} 0.009634_{41} \\ 0.01005_{43} \\ 0.01048_{44} \end{bmatrix} $	150.8
67 68 69	37 .2 37 .3 37 .4	67.1		1.6398	5.717 5.484	91.58 ₃₇ 87.84 ₃₅ 84.29 ₃₅	74 0 .1823 ⁷⁴ 0 .1900 ⁸⁰		152.6 154.4 156.2
1	05.5	07 4	0.000	1 6261	1	80.88	0 1980	0.01236	158.0

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313.59 326.801321 340.48 1415

354.63 369.27 1514 384.41 1567

400 .08₁₆₁₉ 416 .27₁₆₇₄

433 .01 1730

450 .31 468 .181846 486 .64 1907

505.71₁₉₆₉ 525.40₂₀₃₂ 545.72₂₀₉₈

566 .70 588 .342233 610 .672303

 $\begin{array}{c} 633.70 \\ 657.45 \\ 2448 \\ 681.93 \\ 2524 \end{array}$

 $\begin{array}{c} 707.17 \\ 733.192602 \\ 760.00275 \end{array}$

 $\begin{array}{c} 787.5 \\ 815.8292 \\ 845.0301 \end{array}$

104 875.1

72.99

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81.02

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84.03

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95.11

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103.2

104.2

131.4

133.2

135.0

136.8

138.6

140.4

142.2

144.0

145.8

147.6

149.4

151.2

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162.1

163.9

165.7

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171.2

173.0

174.8

176.6

178.5

180.3

182.1

183.9

185.7

HEAT OF

re, Cent		PRESSURE.		THE I	JIQUID.	VAPOR	IZATION.
Temperatur Degrees (grade.	Milli- meters of Mer- cury.	Kilo- grams per Square Centi- meter.	Pounds per Square Inch.	Calories.	B.T.U.	Calories.	B.T.U.
t	p	<i>p</i>	p	q	\boldsymbol{q}	r	r
71 72	243 .39 254 .07 1107	0.33091 0.34544 ₁₅₀₆	4.7067 4.9132 ₂₁₄₁	70.98 71.99			1002.9 1001.6

5.3493₂₂₉₉ 5.5792₂₃₈₃ 5.8175₂₄₆₇

 $\begin{array}{c} 6.0642 \\ 6.31972555 \\ 6.5842 \\ 2736 \end{array}$

 $\begin{array}{c} 6.8578 \\ 7.14092831 \\ 7.43373030 \end{array}$

7.7367 8.04993231 8.37303351

8.7081₃₄₅₆ 9.0537₃₅₆₉ 9.4106₃₆₈₄

 $\begin{smallmatrix} 0.42636_{1797} \\ 0.44433_{1860} \\ 0.46293_{1924} \\ \end{smallmatrix}$

0.54395 0.565982272

0.588702368

0.61238 0.636562506

 0.66162_{2593}^{2500}

 $\begin{array}{c} 0.68755_{2680} \\ 0.71435_{2760} \\ 0.74195_{2855} \\ \end{array} \begin{array}{c} 9.779_{381} \\ 10.160_{393} \\ 10.553_{406} \end{array}$

 $\begin{vmatrix} 0.77050 \\ 0.799883037 \\ 0.830253130 \end{vmatrix} 10.959 \\ 11.377432 \\ 11.809445$

 $\begin{smallmatrix} 0.86155_{3233} & 12.254_{460} \\ 0.893883327 & 12.714_{473} \\ 0.92715_{3430} & 13.187_{488}^{488} \\ \end{smallmatrix}$

 $\begin{vmatrix} 0.96145_{3535} \\ 0.99680_{3650} \\ 1.0333_{374} \end{vmatrix} \begin{vmatrix} 13.675_{503} \\ 14.178519 \\ 14.697_{532} \end{vmatrix}$

 $\substack{15.229\\15.776\\565\\16.341\\582}$

16.923

 $1.0707_{386} \\ 1.1093_{397} \\ 1.1490_{408}$

1.1898

PRESSURE.

 $\frac{4.9132}{5.1273}$ 265 .14¹¹⁰⁷ 1148 0.36050_{1559}^{1506} 276.62 288.51 300.83 1276 $\begin{bmatrix} 0.37609 \\ 0.392261617 \\ 0.40900 \\ 1736 \end{bmatrix}$

555.1

554.4

553.7

553.0

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539.0

538.3

537.6

536.8

536.1

535.4

534.7

187.6 534.0 961.1

HEAT OF

555.8 1000.4

999.1

997.9

996.6

995.4

994.2

992.9

991.6

990.3

989.1

987.8

986.6

985.3

984.0

982.8

981.5

980.3

979.0

977.8

976.6

975.2

974.0

972.7

971.4

970.1

969.0

967.6

966.3

965.0

963.7

962.5

Calories ρ 519.7 518.9 518.1 517.3 516.5

515.7

514.8

514.0

513.2

512.5

511.7

510.9

510.1

509.3

508.5

507.7

506.9

506.1

505.2

504.5

503.9

503.1

502.2

501.4

500.6

499.8

499.0

498.4

497.5

496.6

495.8

494.9

494.1

493.4 888.0

T.U. фi ρ 935.3 933.9 932.4 931.0 929.6

928.2

926.8

925.4

923.9

922.5

921.1

919.6

918.2

916.7

915.3

913.9

912.5

911.0

909.6

908.2

906.9

905.5

904.0

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899.7

898.3

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895.4

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892.5

891.0

889.6

HEAT EQUIVA-

LENT OF IN-TERNAL WORK.

Temperature, Degrees Fahr. t 159.8 161.6 163.4 165.2 167.0 168.8 170.6

172.4 174.2

176.0 177.8

179.6

181.4

183.2

185.0

186.8

188.6

190.4

192.2

194.0

195.8

197.6

199.4

201.2

203.0

204.8

206.6

208.4

210.2

212.0

213.8

215.6

217.4

219.2

١,	e, en	OF E	XTER-	+3	ioi	VOLU	JME.		
E	Temperature, Degrees Cen grade.	Calories.	D.T.G	Entropy of Liquid.	Entropy of Vaporization	Cubic Meters per Kilo.	Cubic Feet per Pound.	Weight, in Kilo- grams, of One Cubic Meter.	Weight, in Pounds, of One Cubic Foot,
	t	Apu	Apu	θ	$\frac{r}{T}$	s	<i>s</i>	Υ .	γ
	71 72 73	37.6 37.7 37.8	67.6 67.8 67.9	0.2311 0.2340 0.2369	1.6194 1.6126 1.6060	4.850 4.659191 4.475184	77.69 ₃₀₆ 74.63 ₂₉₅ 71.68 ₂₈₁	$\begin{array}{c} 0.2062_{84} \\ 0.2146_{89} \\ 0.2235_{91} \end{array}$	0.01287 ₅₃ 0.01340 ₅₅ 0.01395 ₅₇
	74 75 76	37 .9 38 .0 38 .1	68.1 68.3 68.5	0.2398 0.2427 0.2456	1.5994 1.5928 1.5862	$\begin{smallmatrix} 4.300 \\ 4.134166 \\ 3.974160 \\ 152 \end{smallmatrix}$	$\begin{array}{c} 68.87_{266} \\ 66.21_{255} \\ 63.66_{244} \end{array}$	$\begin{smallmatrix} 0.2326_{93} \\ 0.2419_{97} \\ 0.2516_{100} \end{smallmatrix}$	$\begin{smallmatrix} 0.01452_{58} \\ 0.01510_{61} \\ 0.01571_{62} \end{smallmatrix}$
	77 78 79	38.2 38.3 38.4	68.6 68.8 68.9	0.2484 0.2513 0.2541	1.5797 1.5733 1.5668	3.822 3.677145 3.538139 132		$ \begin{array}{c} 0.2616_{104} \\ 0.2720_{106} \\ 0.2826_{110} \end{array} $	0.01633 ₆₅ 0.01698 ₆₇ 0.01765 ₆₉
	80 81 82	38.4 38.5 38.6	69.3	0.2570 0.2598 0.2626	1.5540	$\begin{bmatrix} 3.406 \\ 3.278128 \\ 3.157121 \\ 117 \end{bmatrix}$	50.57187		0.01834 ₇₀ 0.01904 ₇₃ 0.01977 ₇₆
	83 84 85	38.7 38.8 38.9	69.8		1.5351	$\begin{bmatrix} 3.040 \\ 2.929111 \\ 2.822107 \\ 2.822102 \end{bmatrix}$	48 .70 ₁₇₈ 46 .92 ₁₇₂ 45 .20 ₁₆₄		0.02053 ₇₈ 0.02131 ₈₁ 0.02212 ₈₄
	86 87 88	39 .0 39 .1 39 .2	70.3	0.2767	1.5164	$\begin{bmatrix} 2.720 \\ 2.62298 \\ 2.52993 \\ 2.52990 \end{bmatrix}$	43 .56 42 .00 149 40 .51 144	$ \begin{bmatrix} 0.3676_{138} \\ 0.3814_{140} \\ 0.3954_{146} \end{bmatrix} $	$ \begin{array}{c} 0.02296 \\ 0.0238188 \\ 0.02469 \\ 91 \end{array} $
	89 90 91	39 .3 39 .4 39 .4	70.8	0.2851	1.4981	$ \begin{array}{c} 2.439 \\ 2.35386 \\ 2.27182 \\ 80 \end{array} $	39 .07 37 .68 36 .38 128		$ \begin{array}{c} 0.02560_{94} \\ 0.02654_{95} \\ 0.02749_{100} \end{array} $
	92 93 94	39 .6 39 .6 39 .7	71.5	0.2934	1.4801	$\begin{bmatrix} 2.191\\ 2.11576\\ 2.04372\\ 2.04371 \end{bmatrix}$	35 .10 33 .88 117 32 .71	$\begin{smallmatrix} 0.4564_{164} \\ 0.4728_{167} \\ 0.4895_{176} \end{smallmatrix}$	
	95 96 97	39 .8 39 .9 40 .0	71.7	7 0.3010	1.4623	$\begin{bmatrix} 1.972 \\ 1.90567 \\ 1.84065 \\ 2 \end{bmatrix}$	31.59 30.51 29.47	0.5071 0.5249186 0.5435189	$ \begin{array}{c} 0.03166_{112} \\ 0.03278_{115} \\ 0.03393_{118} \end{array} $
	98 99 100	40 . 40 . 40 .	1 72.	2 0 .309	7 1 .4448		28 .48 ₉₄ 27 .54 ₈₈ 26 .66 ₈₂	$ \begin{array}{c} 0.5624 \\ 0.5817193 \\ 0.6006194 \end{array} $	$ \begin{array}{c} 0.03511\\ 0.03631120\\ 0.0375119\\ \end{array} $
	101 102 103		5 72.	8 0.317	9 1.4276	1.560_{51}^{33}		$ \begin{array}{c} 0.6200 \\ 0.6410210 \\ 0.6627 \\ 227 \end{array} $	$ \begin{bmatrix} 0.03870 \\ 0.04002132 \\ 0.04137142 \end{bmatrix} $
	104 105 106	40.	7 73.	$2 \mid 0.325$	9 1 .4106	1.412_{45}^{47}	23 .37 ₇₆ 22 .61 ₇₂ 21 .89 ₇₀	$ \begin{array}{c} 0.6854 \\ 0.7082228 \\ 0.7315233 \\ \end{array} $	0.04279 0.04423145 0.04568151
	107 108 109	40.	9 73.	$6 \mid 0.333$	9 1.3941	1.281_{41}^{42}	21 .19 20 .52 19 .86 62	$ \begin{array}{c} 0.7559 \\ 0.7806 247 \\ 0.8065 259 \\ 0.8065 261 \end{array} $	102
	<u> </u>			مممما	1 0001	1 001	10.04	0 6358	0.05197

ent		PRESSURE	•	THE I	LIQUID.	VAPOR	IZATION.	LENT	of In- L Work.	ahr.	
P. Degrees Cent grade.	Milli- content of Mercury.	Kilo- grams d per Square Centi- meter.	Pounds Pounds Square Inch.	A Calories.	a B.T.U.	→ Calories.	* B.T.U.	ъ Calories.	B.T.U.	* Temperature, Degrees Fahr.	
11 12 13	1111.4 ₃₇₇ 1149.1 ₃₈₈ 1187.9 ₃₉₈	1.5110 1.5623513 1.6151541	$\begin{array}{c} 21.492_{729} \\ 22.221_{751} \\ 22.972_{769} \end{array}$	111.3 112.3 113.3	200.3 202.1 203.9	529.1 528.4 527.7	952.3 951.1 949.8	488.0 487.2 486.5	878.3 877.0 875.4	231.8 233.6 235.4	l
14 15 16	$\substack{1227.7\\1268.7\\410\\1310.7\\432}$	1.6692 1.7248572 1.7820588	23.741 ₇₉₂ 24.533 ₈₁₃ 25.346 ₈₃₆	114.3 115.3 116.4	205.8 207.6 209.4	527.0 526.3 525.5	948.5 947.2 945.9	485.6 484.8 484.0	874. 0 872. 6 871. 2	237.2 239.0 240.8	
17 18 19		1.8408 ₆₀₃ 1.9011 ₆₁₉ 1.9630 ₆₃₅	26. 182 27. 040858 27. 920904	117.4 118.4 119.4	211.2 213.0 214.9	524.8 524.1 523.4	944.5 943.3 942.2	483.2 482.4 481.7	869.7 868.3 867.0	242.6 244.4 246.2	
20 21 22	1587.7_{506}^{492}	2.0265 2.0918668 2.1586688	28.824 ₉₂₈ 29.752 ₉₅₁ 30.703 ₉₇₈	120.4 121.4 122.5	216.7 218.5 220.4	522.7 522.0 521.2	940.9 939.6 938.2	480.9 480.2 479.3	865. 6 864. 2 862. 7	248.0 249.8 251.6	
23 24 25	$\substack{1638.3 \\ 1690.1532 \\ 1743.3545}$	$\substack{2.2274\\2.2978704\\2.3701742}$	31.681 32.6831.002 33.7111.055	123.5 124.5 125.5	222. 2 224. 1 225. 9	520.5 519.8 519.1	937.0 935.7 934.4	478.5 477.7 476.9	861. 2 859. 8 858. 4	253.4 255.2 257.0	
26 27 28		$2.4443760 \ 2.5203779 \ 2.5982798$	34.766 35.8471.081 36.9551.135	126.5	227.7 229.5 231.4	518. 4 517. 6 516. 9	933. 2 931. 8 930. 6	476.2 475.3 474.5	857. 0 855. 5 854. 2	258.8 260.6 262.4	
29 30 31	$\begin{array}{c} 1969.7 \\ 2029.8 \\ 617 \\ 2091.5 \\ 633 \end{array}$	2. 6780 2. 7599837 2. 8436861	$38.090 \atop 39.2551.165 \atop 40.4451.225$	129.6 130.6 131.6	233.3 235.1 236.9	516. 2 515. 6 514. 9	929.3 928.1 926.8	473.7 473.0 472.3	852.8 851.4 850.0	264.2 266.0 267.8	
	2154. 8 2219. 5663 2285. 8679	2.9297 3.0176902 3.1078922	$^{41.670}_{42.9211.251}_{231.282}_{44.203}$	134.7	238.7 240.6 242.4	514. 2 513. 5 512. 8	925.5 924.2 922.9	471.5 470.6 469.8	848.6 847.0 845.6	269.6 271.4 273.2	
5 6 7	2353. 7 ₆₉₅ 2423. 2 ₇₁₂ 2494. 4 ₇₂₈	3.2000 ₉₄₆ , 3.2946 ₉₆₈ 3.3914 ₉₉₀	45.515 46.8601.345 48.2371.408	135.7 136.7 137.7	244. 2 246. 0 247. 9	512.1 511.4 510.7	921.6 920.2 919.0	469.1 468.2 467.4	844. 2 842. 7 841. 3	275.0 276.8 278.6	
8 9 0	2567. 2 ₇₄₅ 2641. 7 ₇₆₂ 2717. 9 ₇₈₀	$3.4904_{1012} \\ 3.5916_{1037} \\ 3.6953_{1062}$	$\begin{array}{c} 49.645 \\ 51.085 \\ 1.475 \\ 52.56 \\ 1.51 \end{array}$	138.8 139.8 140.8	249.7 251.6 253.4	510.0 509.2 508.6	917.6 916.5 915.2	466.6 465.8 465.0	839.8 838.5 837.1	280.4 282.2 284.0	
1 2 3	2795. 9 ₇₉₈ 2875. 7 ₈₁₆ 2957. 3 ₈₃₅	$\begin{array}{c} 3.8015 \\ 3.909811083 \\ 4.02081132 \end{array}$		141.8 142.8 143.9	255.3 257.1 259.0	507.9 507.0 506.2	913.8 912.6 911.2	464. 2 463. 4 462. 6	835. 6 834. 2 832. 8	285.8 287.6 289.4	
4 5 6		4. 1340 4. 25001160 4. 36891189 4. 36891209	58.80 60.45 1.65 62.14 1.69 1.72	144.9 145.9 146.9	260.8 262.7 264.5	505.5 504.8 504.1	908.6	461.8 461.0 460.2	831. 4 829. 9 828. 5	291.2 293.0 294.8	
7 3 3 3 3 3 3 3 3	$\begin{bmatrix} 3302.5_{911} \\ 3393.6_{931} \\ 3486.7_{952} \end{bmatrix}^{4}$	4. 4898 4. 61421244 4. 7408 1293	63.86 65.63 1.77 67.43 1.80 1.84	148.0 149.0 150.0	266. 4 268. 2 270. 1	503.3 502.6 501.9	904.8	459.4 458.7 457.9	827. 2 825. 7 824. 3	296.6 298.4 300.2	
115	2501 0 4	0701	20 07	777 0	074 0	***					

Ţ.		_	2 2 2	2 2	2 2 2	2 2 2	2 2	2 2	2 2 2	2 2	2 2	22	20	29	2:3
ISITY.	Weight, in Pounds, of One Cubic Foot.	γ	$ \begin{bmatrix} 0.05362_{172} \\ 0.05534_{177} \\ 0.05711_{185} \end{bmatrix} $	$ \begin{array}{c} 0.05896_{183} \\ 0.06079_{187} \\ 0.06266_{194} \end{array} $	$ \begin{array}{c} 0.06460 \\ 0.06662202 \\ 0.06863211 \end{array} $	$ \begin{array}{c} 0.07074 \\ 0.07289215 \\ 0.07508219 \\ \end{array} $	$ \begin{array}{c} 0.07734 \\ 0.07962228 \\ 0.08196234 \\ 0.08196243 \end{array} $	$\begin{array}{c} 0.08439\\ 0.08688249\\ 0.08937254 \end{array}$	$ \begin{array}{c} 0.09191 \\ 0.09461270 \\ 0.09718282 \end{array} $	$\substack{0.1000\\0.1028\\29\\0.1057\\29}$	$\begin{smallmatrix} 0.1086 \\ 0.1116 \\ 0.1147 \\ 0.1147 \\ 31 \end{smallmatrix}$	$\substack{0.1178\\0.1210\\33\\0.1243\\33}$	$\substack{0.1276\\0.1310\\35\\0.1345\\36}$	$\substack{0.1381\\0.141736\\0.145437\\0.145438}$	$\substack{0.1492\\0.153038\\0.156940}$
DEN	Weight, in Kilo- grams, of One Cubic Meter.	Υ	$\begin{array}{c} 0.8591_{274} \\ 0.8865_{284} \\ 0.9149_{294} \end{array}$	$\substack{0.9443_{294}\\0.9737_{303}\\1.004_{31}}$	$^{1.035}_{3.06733}_{3.1.10034}$	$\substack{1.134_{33}\\1.167_{36}\\1.203_{36}}$	$^{1.239}_{1.27637}$ $^{1.313}_{38}$	$egin{array}{c} 1.351_{f 40} \ 1.391_{f 40} \ 1.431_{f 42} \end{array}$	$\substack{\frac{1.473}{1.514}}_{1.514}$ $\substack{\frac{43}{43}}$ 1.557	$\begin{array}{c} 1.602_{45} \\ 1.647_{46} \\ 1.693_{47} \end{array}$	1.740 ₄₈ 1.788 ₅₀ 1.838 ₅₀	1.888 ₅₁ 1.939 ₅₃ 1.992 ₅₃	2.045 ₅₄ 2.099 ₅₆ 2.155 ₅₇	$\begin{smallmatrix} 2.212\\ 2.27058\\ 2.32960 \end{smallmatrix}$	2.389 2.45163 2.51463
JME.	Cubic Feet per Pound.	<i>s</i>	18.65 ₅₈ 18.07 ₅₆ 17.51 ₅₅	16.96 ₅₁ 16.45 ₄₉ 15.96 ₄₈	43	$14.14_{13.72}_{13.72}_{40}_{40}_{13.32}_{39}$	12.93 ₃₇ 12.56 ₃₇ 12.19 ₃₄		$10.88_{10.57_{28}} \\ 10.29_{29}$	$^{10.00}_{\substack{9.728266\\9.462258}}$	$\begin{array}{c} 9.204 \\ 8.957 \\ 240 \\ 8.717 \\ 230 \end{array}$	8 .487 8 .262225 8 .043209	$\substack{7.834\\7.631203\\7.433198\\7.433191}$	$\begin{array}{c} 7.242 \\ 7.056186 \\ 6.877179 \end{array}$	$\substack{6.704\\6.536168\\6.372\\159}$
Volu	Cubic Meters per Kilo.	s	1.164 1.128 35 1.093 34	$\begin{smallmatrix} 1.059 & 32 \\ 1.027 & 31 \\ 0.9961 & 300 \end{smallmatrix}$		$\substack{0.8822\\0.8566256\\0.8315242}$	216	$\substack{0.7399\\0.7188211\\0.6986202\\195}$	$\begin{smallmatrix} 0.6791\\ 0.6604187\\ 0.6421177 \end{smallmatrix}$	$\begin{smallmatrix} 0.6244 \\ 0.6073171 \\ 0.5907166 \\ 0.5907160 \end{smallmatrix}$	$\begin{array}{c} 0.5747 \\ 0.5592150 \\ 0.5442144 \end{array}$	$\begin{array}{c} 0.5298 \\ 0.5158 \\ 137 \\ 0.5021 \\ 130 \end{array}$	$\begin{bmatrix} 0.4891 \\ 0.4764 \\ 124 \\ 0.4640 \\ 119 \end{bmatrix}$	$\begin{bmatrix} 0.4521 \\ 0.4405 \\ 112 \\ 0.4293 \\ 108 \end{bmatrix}$	$\begin{bmatrix} 0.4185 \\ 0.4080 \\ 102 \\ 0.3978 \\ 98 \end{bmatrix}$
f	Entropy of Vaporization	$\frac{r}{T}$	1.3776 1.3722 1.3668	1.3614 1.3560 1.3507	1 .3455 1 .3403 1 .3351	1 .3299 1 .3247 1 .3195	1.3144 1.3093 1.3042	1 .2992 1 .2942 1 .2892	1 .2842 1 .2792 1 .2743	1 .2694 1 .2645 1 .2596	1 .2547 1 .2499 1 .2451	1 .2403 1 .2356 1 .2309	1 .2262 1 .2215 1 .2168	1 .2121 1 .2075 1 .2029	1 .1983 1 .1937 1 .1892
of t	Entropy of Liquid.	θ	0.3418 0.3445 0.3471	0.3498 0.3524 0.3550	0.3576 0.3602 0.3628	0.3654 0.3680 0.3705	0.3731 0.3756 0.3782	0.3807 0.3833 0.3858	0 .3884 0 .3909 0 .3934	0.3959 0.3985 0.4010	0 .4035 0 .4060 0 .4085	0.4110 0.4135 0.4160	0 .4185 0 .4209 0 .4234	0 .4259 0 .4283 0 .4307	0 .4332 0 .4356 0 .4380
XTER-	B.T.U.	Apu ——	74.0 74.2 74.3	74.5 74.6 74.7	74.9 75.0 75.2	75.3 75.4 75.6	75 .7 75 .9 76 .0	76.1 76.3 76.4	76 .6 76 .7 76 .8	77 .0 77 .1 77 .3	77 .4 77 .5 77 .7	77 .8 78 .0 78 .1	78.2 78.3 78.5	78.6 78.7 78.8	79.0 79.1 79.3
OF E	Calories.	Apu ——	41 .2 41 .3 41 .3	41 .4 41 .5 41 .6	41 .6 41 .7 41 .8	41 .9 41 .9 42 .0	42.1 42.2 42.3	42.3 42.4 42.5	42.6 42.6 42.7	42.8 42.9 43.0	43.0 43.1 43.2	43 .3 43 .3 43 .4	43.5 43.6 43.6	43.7 43.8 43.9	44.0 44.0 44.1
ure, Cen	Temperature, Degrees Cen grade.		111 112 113	114 115 116	117 118 119	120 121 122	123 124 125	126 127 128	129 130 131	132 133 134	135 136 137	138 139 140	141 142 143	144 145 146	147 148 149

190	187 188 189	184 185 186	181 182 183	178 179 180	175 176 177	172 173 174	169 170 171	166 167 168	163 164 165	160 161 162	157 158 159	154 155 156	151 152 153	t	Temperatur Degrees (grade.
9426207	$\begin{array}{c} 8824 \\ 9021 \\ 9021 \\ 201 \\ 9222 \\ 204 \end{array}$	8253 8440 191 8631 193	7712 7889181 8070183	7198 7366 171 7537 175	6712 ₁₅₉ 6871 ₁₆₂ 7033 ₁₆₅	6251 6402151 6555 ₁₅₇	5816 5959145 6104 ₁₄₇	5405 ₁₃₄ 5539 ₁₃₇ 5676 ₁₄₀	$\begin{array}{c} 5017 \\ 5144127 \\ 5273 \\ 132 \end{array}$	$\substack{4651.4\\4770.91218\\4892.7\\1243}$	4307 .1 4419 .5 1148 4534 .3 1171	$\begin{array}{c} 3983.3 \\ 4089.0 \\ 1079 \\ 4196.9 \\ 1102 \end{array}$	3679.1 ₉₉₃ 3778.4 ₁₀₁₄ 3879.8 ₁₀₃₅	<i>p</i>	Milli- meters of Mer- cury.
12.815 ₂₈₂	11.997 12.265 12.538 277	11 .221 11 .476255 11 .735259 11 .735262	$ \begin{array}{c} 10.485 \\ 10.726241 \\ 10.972249 \end{array} $	$\begin{smallmatrix} 9.7860 \\ 10.014 \\ 233 \\ 10.247 \\ 238 \end{smallmatrix}$	$ \begin{array}{c} 9.1251 \\ 9.34172166 \\ 9.56172200 \\ 9.56172243 \end{array} $	$\substack{8.4987\\8.70402053\\8.91212081\\2130}$	7.9074 ₁₉₃₃ 8.1007 ₁₉₈₃ 8.2990 ₁₉₉₇	$\begin{array}{c} 7.3485\\ 7.53061821\\ 7.7169\\ 1905 \end{array}$	$\substack{6.8212\\6.99341722\\7.16921793}$	$\substack{6.3241\\6.48651624\\6.65241659}$	$\begin{array}{c} 5.8558 \\ 6.0084 \\ 1561 \\ 6.1645 \\ 1596 \end{array}$	$\begin{array}{c} 5.4157_{1435} \\ 5.5592_{1469} \\ 5.7061_{1497} \end{array}$	5.0023 ₁₃₅₀ 5.1373 ₁₃₇₈ 5.2751 ₁₄₀₆	p	Kilo- grams per Square Centi- meter.
182 .274 .01	170 .64 ₃ .81 174 .45 ₃ .89 178 .34 ₃ .93	159.60 163.223.62 166.913.73	$\begin{bmatrix} 149.13 \\ 152.563.43 \\ 156.063.50 \\ 3.54 \end{bmatrix}$	$\begin{bmatrix} 139.19 \\ 142.443.25 \\ 145.753.31 \\ 3.38 \end{bmatrix}$	$\begin{bmatrix} 129.79 \\ 132.873.08 \\ 136.003.13 \\ 3.19 \end{bmatrix}$	$\begin{smallmatrix} 120.88 \\ 123.802.92 \\ 126.76 \\ 3.03 \end{smallmatrix}$	$^{112.47}_{115.222.75}_{22.82}_{118.042.84}$	$104.52 \atop 107.112.59 \atop 109.762.65 \atop 2.71$	$\begin{array}{c} 97.02 \\ 99.472.45 \\ 101.972.50 \end{array}$	$89.95_{2.31}$ $92.262.36$ $94.622.40$	$\begin{array}{c} 83.29 \\ 85.462.17 \\ 87.682.22 \\ 27.682.27 \end{array}$	$\begin{array}{c} 77.03 \\ 79.072.04 \\ 81.162.13 \end{array}$	$\begin{array}{c} 71.15\\73.071.92\\73.031.96\\75.032.00 \end{array}$	<i>p</i>	Pounds per Square Inch.
192.3			183 .0 184 .0 185 .0	179 .9 180 .9 181 .9	176 .8 177 .8 178 .8	173 .7 174 .7 175 .7	170 .6 171 .6 172 .6	167.5 168.5 169.5	164 .4 165 .4 166 .5	161 .3 162 .3 163 .4	158.2 159.3 160.3	155.1 156.2 157.2	152.1 153.1 154.1	<u>q</u>	Calories.
346.	342 344	334 .9 336 .8 338 .0	329 .3 331 .2 333 .0	323 .7 325 .6 327 .8	318 .2 320 .0 321 .8	312.6 314.5 316.3	307.0 308.9 310.7	301 .5 303 .3 305 .1	295 .9 297 .7 299 .6	290 .4 292 .2 294 .1	284 .8 286 .7 288 .5	279 .2 281 .1 283 .0	273 .8 275 .6 277 .4	<i>q</i>	B.T.U.
1 472 .	4 473 .6 2 492 .9	8 475 .8	2 478.0	3 480 .2	482.4	484.6	486.8	488.9	491.0	494.0 493.2 492.5	496 .1 495 .4 494 .7	498.2 497.6 496.9	500 .6 499 .8 499 .1		Calories.
2 849 .	852.0 851.5	8 856 .	860.4	864.4	868.3	872.3	876.1	881 .4 880 .1 878 .8	885 .2 883 .9 882 .7	889 .1 887 .8 886 .6	893.0 891.8 890.4	897.0 895.7 894.4	900 .9 899 .6 898 .4		B.T.U.
9 425 .	$\begin{vmatrix} 427.426.426. \end{vmatrix}$	5 429 .	431 .8	434.1	436.5	438.9	441.2	444 .3 443 .6 442 .8	446 .8 445 .9 445 .1	449 .1 448 .2 447 .5	451 .5 450 .7 449 .9	453 .9 453 .1 452 .4	456 .3 455 .5 454 .7	ρ	Calories.
5 765 .	0 768. 3 767.	3 772 .	3 777 .	781 .4	785 .6 784 .2	790.0	794.1	799 .8 798 .5 797 .0	804.1 802.6 801.3	808 .3 806 .9 805 .5	812.7 811.3 809.8	817.0 815.6 814.1	821 .4 820 .0 818 .5	ρ	B.T.U.
8 374.0	7 370 .4 2 372 .2	9 365 .6 5 366 .8	359 .67 361 .4	354 .2 356 .0	348 .8 2 350 .6	343.4	338.0	332.6	327.2	320.0 321.8 323.6	314.6 316.4 318.2	309 .2 311 .0 312 .8	303.8 305.6 307.4	t	Temperatu Degrees I

			വധാ	999	60 60 60	6.9 6.9 6.9	63 63 63									
in Is,	Weight, in Pounds, of One Cubic Foot.	γ	$\begin{smallmatrix} 0.1650_{42} \\ 0.1692_{42} \\ 0.1734_{43}^{43} \end{smallmatrix}$	$\substack{0.1777\\0.182144\\0.186646}$		$ \begin{array}{c} 0.2055 \\ 0.210449 \\ 0.215450 \\ 0.215451 \end{array} $	$ \begin{array}{c} 0.2205 \\ 0.225853 \\ 0.2310 \\ 55 \end{array} $	$ \begin{array}{c} 0.2365 \\ 0.242055 \\ 0.247555 \\ 0.247557 \end{array} $	$\begin{smallmatrix} 0.2532\\ 0.259058\\ 0.264861 \end{smallmatrix}$	$\begin{smallmatrix} 0.2709 \\ 0.2769 \\ 0.2833 \\ 62 \end{smallmatrix}$	$\begin{smallmatrix} 0.2895 \\ 0.296065 \\ 0.302565 \\ 0.67 \end{smallmatrix}$	$ \begin{array}{c} 0.3092 \\ 0.316068 \\ 0.322868 \\ 0.322870 \end{array} $	$ \begin{array}{c c} 0.3298 \\ 0.336971 \\ 0.344172 \\ 0.344174 \end{array} $	$ \begin{array}{c} 0.3515 \\ 0.359176 \\ 0.366679 \end{array} $	$ \begin{array}{c c} 0.3745 \\ 0.382378 \\ 0.390279 \\ 0.390282 \end{array} $	0.398483
in	Weight, in Kilo-grams, of One Cubic Meter.	γ	$2.643 \atop 2.71068 \atop 2.77869$	$2.847_{71} \\ 2.918_{72} \\ 2.990_{73}$	$\begin{array}{c} 3.063_{75} \\ 3.138_{76} \\ 3.214_{78} \end{array}$	3 .292 ₇₈ 3 .370 ₈₁ 3 .451 ₈₁	3 .532 ₈₅ 3 .617 ₈₄ 3 .701 ₈₇	3 .788 3 .87689 3 .965 ₉₂	4 .057 ₉₂ 4 .149 ₉₄ 4 .243 ₉₅	4.338 4.437100 4.537101	4.638 ₁₀₄ 4.742 ₁₀₃ 4.845 ₁₀₅	4.950 5.061111 5.171110	5.283 5.397114 5.513116	5.631 ₁₁₉ 5.750 ₁₂₂ 5.872 ₁₂₇		5 .382
	Cubic Feet per Pound.	<i>s</i>	6 .060 ₁₄₉ 5 .911 ₁₄₄ 5 .767 ₁₄₁	5 .626 ₁₃₆ 5 .490 ₁₃₂ 5 .358 ₁₂₈	5 .230 ₁₂₅ 5 .105 ₁₂₂ 4 .983 ₁₁₆	4 .867 4 .753 ₁₁₁ 4 .642 ₁₀₇	$\substack{\frac{4.535}{4.429100}\\4.329100\\4.329100}$	$\begin{array}{c} 4.229\\ 4.13396\\ 4.04091 \end{array}$	$\begin{array}{c} 3.949\\ 3.86188\\ 3.77685\\ \end{array}$	3.692 ₈₁ 3.611 ₈₀ 3.531 ₇₆	3 .455 ₇₆ 3 .379 ₇₃ 3 .306 ₇₀	3.236 ₇₁ 3.165 ₆₇ 3.098 ₆₆	$ \begin{array}{c} 3.032\\2.96862\\2.90661 \end{array} $	2 .845 2 .785 2 .728 58	2.670 2.61654 2.56353	
lo.	Cubic Meters per Kilo.	s	88		$ \begin{smallmatrix} 0.3265_{78} \\ 0.3187_{76} \\ 0.3111_{73} \end{smallmatrix} $	$\begin{smallmatrix} 0.3038_{71} \\ 0.2967_{69} \\ 0.2898_{67} \end{smallmatrix}$	$\begin{smallmatrix} 0.2831_{66} \\ 0.2765_{63} \\ 0.2702_{62} \end{smallmatrix}$	$\begin{array}{c} 0.2640 \\ 0.2580 \\ 58 \end{array}$	$ \begin{smallmatrix} 0.2465 \\ 0.241055 \\ 0.235753 \\ 0.235752 \end{smallmatrix} $	$\begin{array}{c} 0.2305 \\ 0.2254 \\ 50 \end{array}$	0.2109_{45}^{47}	$\begin{bmatrix} 0.1976_{42}^{41} \\ 0.1934_{41}^{41} \end{bmatrix}$	$ 0.1853_{30}^{40}$	$\begin{array}{c c} 0.173936 \\ 0.170336 \\ 0.366 \end{array}$	$\begin{bmatrix} 0.1667_{34} \\ 0.1633_{33} \end{bmatrix}$	6 0.1567
o iza	Entropy o Vaporiza	$\frac{r}{T}$	1 .1802 1 .1757 1 .1713	1 .1769 1 .1625 1 .1681	1.1637 1.1593 1.1560	1 .1407 1 .1364 1 .1321	1 .1278 1 .1236 1 .1194	1 .1152 1 .1110 1 .1068	1 .1027 1 .0986 1 .0945	1.0904 1.0863 1.0823	1.0743	1 .0623	1 .0505	1 .0389	1 .027	3 1 .019
Jo.	Entropy Liquid.	θ	0 .4429 0 .4453 0 .4477	0 .4501 0 .4525 0 .4549	0 .4573 0 .4596 0 .4620	0 .4644 0 .4668 0 .4692	0.4715 0.4739 0.4763	0.4786 0.4810 0.4833	0 .4857 0 .4880 0 .4903	0.4926 0.4949 0.4972	0 .4995 0 .5018 0 .5041	0.5064 0.5087 0.5110	0.5146	0.5224	0.5293	0.533
ork.	B.T.U.	Apu	79.5 79.7 79.8	80 .0 80 .1 80 .2	80 .4 80 .5 80 .7	80 .8 80 .9 81 .0	81 .2 81 .3 81 .4	81 .5 81 .6 81 .8	81 .9 82 .0 82 .1	82 .2 82 .4 82 .5	82.6 82.7 82.8	82.9 83.0 83.1	83 .2 83 .3 83 .4	83 .5 83 .6 83 .7	83 .8 83 .9 84 .0	84.1
nal W	Calories.	Apu	44.3 44.3 44.4	44 .5 44 .6 44 .6	44.7 44.8 44.8	44.9 45.0 45.1	45.1 45.2 45.3	45 .3 45 .4 45 .4	45.5 45.6 45.7	45.8	46.0	46.2	46.3	46.5	3 46.6	46.8
s J	Femperatur Degrees C grade.	t	151 152 153	154 155 156	157 158 159	160 161 162	163 164 165	166 167 168	169 170 171	172 173 174	175 176 177	178 179 180	181 182 183	184 185 186	187 188 189	190

02		OAI			****					
re, Jenti-		Pressure		HEATHE I	T OF JIQUID		T OF	LENT	Equiva- of In- Work.	re, Fahr.
Temperature, Degrees Centi- grade.	Milli- meters of Mer- cury.	Kilo- grams per Square Centi- meter.	Pounds per Square Inch.	Calories.	B.T.U.	Calories.	B.T.U.	Calories.	B.T.U.	Temperature, Degrees Fahr.
t	p	<i>p</i>	<i>p</i>	q	q	$oxed{r}$	<i>r</i>	ρ	ρ	
191 192 193	$\substack{ 9633 \\ 9844211 \\ 10058_{218} }$	13.097 ₂₈₇ 13.384 ₂₉₁ 13.675 ₂₉₇	$186.28_{4.08}$ $190.36_{4.14}$ $194.50_{4.22}$	193.3 194.4 195.4	349.8	471.5 470.7 470.0	848.6 847.1 845.9	424 .8 423 .9 423 .2	764.4 763.0 761.6	375 .8 377 .6 379 .4
194 195 196	$\substack{10276\\10498\\226\\10724\\229}$	13 .972 ₃₀₁ 14 .273 ₃₀₈ 14 .581 ₃₁₁	$\substack{198.72\\203.014.29\\207.384.37\\207.384.43}$	196 .4 197 .5 198 .5	355.4	469 .2 468 .5 467 .8	844.7 843.4 842.0	422 .4 421 .6 420 .8	760 .3 758 .9 757 .4	381 .2 383 .0 384 .8
197 198 199	$\begin{array}{c} 10953 \\ 11186 \\ 238 \\ 11424 \\ 240 \end{array}$	14 .892 ₃₁₇ 15 .209 ₃₂₄ 15 .533 ₃₂₆		199 .5 200 .6 201 .6	361.1	467 .1 466 .3 465 .6	840.7 839.4 838.0	420.0 419.2 418.4	756 .1 754 .6 753 .2	386.6 388.4 390.2
200 201 202	$11664 \\ 11909 \\ 249 \\ 12158 \\ 253$	15 .859 ₃₃₄ 16 .193 ₃₃₇ 16 .530 ₃₄₅	255.56 _{4.74} 230.30 _{4.81} 235.11 _{4.89}	202 .7 203 .7 204 .7	364 .8 366 .7 368 .5	464 .8 464 .1 463 .4	836.7 835.5 834.1	417.6 417.0 416.3	751 .8 750 .5 749 .1	392.0 393.8 395.6
203 204 205	$\begin{array}{c} 12411 \\ 12668257 \\ 12930262 \\ 265 \end{array}$	16 .875 ₃₄₈ 17 .223 ₃₅₇ 17 .580 ₃₅₉	$\substack{240.00\\244.974.97\\250.03}_{5.12}$	205 .8 206 .8 207 .9		462.6 461.9 461.1	832 .7 831 .4 830 .1	415.4 414.7 413.8	747 .7 746 .4 745 .0	397.4 399.2 401.0
206 207 208	$13195_{270}\\13465_{274}\\13739_{279}$	$\begin{array}{c} 17.939_{368} \\ 18.307_{372} \\ 18.679_{379} \end{array}$	$\substack{255.15 \\ 260.375.22 \\ 265.675.30 \\ 265.40}$	208 .9 210 .0 211 .0		4604 4596 4589	828.8 827.5 826.1	413.1 412.3 411.6	743 .6 742 .2 740 .9	402 .8 404 .6 406 .4
209 210 211	14018 ₂₈₃ 14301 ₂₈₇ 14588 ₂₉₂	19 .058 ₃₈₄ 19 .442 ₃₉₀ 19 .832 ₃₉₈	$\begin{array}{c} 271.07 \\ 276.545.41 \\ 282.095.55 \\ 5.64 \end{array}$	212.0 213.1 214.1	383.5	458 .1 457 .5 456 .7	824.8 823.5 822.1	410.7 410.1 409.3	739 .5 738 .1 736 .7	408.2 410.0 411.8
212 213 214	14880 ₂₉₇ 15177 ₃₀₁ 15478 ₃₀₇	$\begin{array}{c} 20.230_{404} \\ 20.634_{409} \\ 21.043_{418}^{418} \end{array}$	287 .73 293 .485 .75 299 .305 .82 5 .94	215.2 216.2 217.3	389.2	456 .0 455 .3 454 .5		408 .6 407 .9 407 .0	735.3 734.1 732.7	413.6 415.4 417.2
215 216 217	15785 16096311 16411315	21 .461 21 .884 22 .312 436	$305.24_{6.01} \\ 311.25_{6.09} \\ 317.34_{6.21} $	218.3 219.3 220.4	394.8	453.8 453.1 452.3	816.8 815.4 814.1	406 .3 405 .5 404 .8	729.9	419.0 420.8 422.6
218 219 220	$16732_{326} \\ 17058_{331} \\ 17389$	22 .748 23 .191 23 .642		221 .4 222 .5 223 .5		450.8	811.4	404.0 403.3 402.5	725.8	424 .4 426 .2 428 .0

SATURATED STEAM-TABLE III.

			~					
e, enti-	HE Equiv	AT ALENT XTER-	the	ion.	Spec Volu		Dens	SITY.
Temperature, Degrees Centi-	Calories.		Entropy of Liquid.	Entropy of Vaporization.	Cubic Meters per Kilo.	Cubic Feet per Pound.	Weight, in Kilo-grams, of One Cubic	Weight, in Pounds, of One
t	Apu	Apu	θ	$\frac{r}{T}$	s	8	γ	γ
191 192 193	46.9	84.2 84.3 84.3		1 .0158 1 .0121 1 .0084	$egin{array}{c} 0.1535_{31} \ 0.1504_{30} \ 0.1474_{30} \end{array}$	$2.459_{50} \\ 2.409_{48} \\ 2.361_{48}$	6.515 ₁₃₄ 6.649 ₁₃₅ 6.784 ₁₄₁	0.406 0.415 0.423
194 195 196	47.0	84 .4 84 .5 84 .6		1 .0047 1 .0010 0 .9973	$\substack{0.1444\\0.1415}_{28}$ $\substack{0.1415\\28}$ 0.1387	$\begin{smallmatrix} 2.313 \\ 2.26745 \\ 2.22243 \end{smallmatrix}$	$\begin{array}{c} 6.925_{142} \\ 7.067_{143} \\ 7.210_{143} \end{array}$	0 .432 0 .441 0 .450
197 198 199	47.1	84.7 84.7 84.8		0 .9936 0 .9899 0 .9862	$\substack{0.1360\\0.133327\\0.130626}$		7.353 ₁₄₉ 7.502 ₁₅₅ 7.657 ₁₅₆	0.458 0.468 0.478
200 201 202	. 47.2	84.9		0.9826 0.9790 0.9754	$\begin{smallmatrix} 0.1280_{26} \\ 0.1254_{24} \\ 0.1230_{24} \end{smallmatrix}$	$\begin{smallmatrix} 2.051 \\ 2.009 \\ 1.970 \\ 38 \end{smallmatrix}$	$\begin{array}{c} 7.813\\ 7.974\\ 156\\ 8.130\\ 162 \end{array}$	0.487 0.497 0.507
203 204 205	47.3	85.1		0.9718 0.9682 0.9646		$\begin{bmatrix} 1.932_{37} \\ 1.895_{37} \\ 1.858_{37} \end{bmatrix}$	8.292 ₁₆₁ 8.453 ₁₆₈ 8.621 ₁₇₄	0.517 0.527 0.538
206 207 208	47.4	85.2	0.5690 0.5712 0.5733	0 .9610 0 .9575 0 .9540	0.1115_{21}^{22}	1.821 ₃₅ 1.786 ₃₄ 1.752 ₃₃	8.795 ₁₇₄ 8.969 ₁₇₂ 9.141 ₁₇₉	0.549 0.559 0.570
209 210 211	47.5	85 .4	0.5777	0.9505 0.9470 0.9435	0.1052_{20}^{21}	1.719 1.68633 1.65330	9.320 9.506186 9.690184	0.581 0.593 0.605
213 213 214	3 47.5	85.5			0.099419	$\begin{smallmatrix} 1.622\\ 1.59230\\ 1.56230\\ 1.56230\\ \end{smallmatrix}$	$\begin{smallmatrix} 9.872_{188} \\ 10.06_{20} \\ 10.26_{20} \end{smallmatrix}$	0.616 0.628 0.640
211 210 21	3 47.6	85.5		0.9298 0.9264 0.9230	0.0938_{18}^{18}	$\begin{smallmatrix} 1.532_{29} \\ 1.503_{29} \\ 1.474_{28} \end{smallmatrix}$	${ 10.46 \atop 10.6620 \atop 10.8720 \atop 20 }$	0.652 0.668 0.678
218 219 220	3 47.6	85.6	0 .5948 0 .5969 0 .5991	0.9162	0.0886_{17}^{17}	$\begin{array}{c} 1.446_{27} \\ 1.419_{27} \\ 1.392^{27} \end{array}$	$\begin{array}{c} 11.07 \\ 11.2922 \\ 11.5123 \end{array}$	0.693 0.704 0.718

TABLE IV.

SATURATED VAPOR OF ETHER.

FRENCH UNITS.

Temperature, Degrees Centi- grade.	Pressure, Millimeters of Mercury.	Heat of the Liquid.	Total Heat,	Heat of Vaporization,	Heat equivalent of Internal Work.	Heat equivalent of External Work.	Entropy of the Liquid.	Specific Volume.	Weight, in Kilos, of One Cubic Meter.	Temperature, Degrees Centigerade,
t	р	q	H	r	ρ	Apu	θ	s	γ	t
0	184.39	0.00	94.00	94.00	86 .45	7.55	0.0000	1.278	0.728	0
10 20 30	286 .83 432 .78 634 .80	5.32 10.70 16.14	98 .44 102 .78 107 .00	93.12 92.08 90.86	85 .37 84 .13 82 .72	7.75 7.95 8.14	0.01909 0.03772 0.05593	0.5741 0.4013	1.742 2.492	10 20 30
40 50	907.04 1264.8	21.63 27.19	111 .11 115 .11	89 .48 87 .92	81.15 79.41	8.33	$0.07374 \\ 0.09117$		3.746 4.744	40 50
60	1725.0	32.80	119.00	86.20	77.53	8.67	0.1083	0.1580	6.329	60
70 80 90 100 110 120	2304.9 3022.8 3898.3 4953.3 6214.6 7719.2	38 .48 44 .21 50 .00 55 .86 61 .77 67 .74	122.78 126.44 130.00 133.44 136.78 140.00	84.30 82.23 80.00 77.58 75.01 72.26	75 .49 73 .32 71 .03 68 .62 66 .13 63 .57	8.81 8.91 8.97 8.96 8.88 8.69	0.1250 0.1415 0.1576 0.1735 0.1891 0.2045	0.1203 0.0932 0.0731 0.0577 0.0459 0.0364	8.313 10.73 13.68 17.33 21.79 27.47	70 80 90 100 110 120

TABLE V.

SATURATED VAPOR OF ALCOHOL.

FRENCH UNITS.

Temperature, Degrees Centigrade,	Pressure, Sillimeters Of Mercury.	Heat of the Liquid.	н Total Heat.	Heat of Vaporization.	Heat equivalent of Internal Work.	Heat equivalent of External Work.	Entropy of the Liquid.	 Specific Volume. 	Weight, in Kilos, of One Cubic Acter.	Temperature, Degrees Centigrade.
0	12.70	0.00	236 .5	236 .50	223 .38	13 .12	0.0000	32 .21	0.03105	0
10 20 30	24 .23 44 .46 78 .52	5.59 11.42 17.49	$244.4 \\ 252.0 \\ 258.0$	238 .81 240 .58 240 .51	225 .29 226 .56 226 .03	14.02	0.01996 0.04003 0.06029	9.847	0.05750 0.1016 0.1738	10 20 30
40 50 60	133 .69 219 .90 350 .21	23 .71 30 .21 37 .37	262.0 264.0 265.0	238 .29 233 .79 227 .63	223 .44 218 .59 212 .38	15.10	0.08073 0.1014 0.1223	3.465 2.143 1.359	0.2886 0.4666 0.7358	40 50 60
70 80 90	541 .15 812 .91 1189 .3	44 .58 52 .11 59 .97	265 .2 265 .2 266 .0	220 .62 213 .09 206 .03	205 .28 197 .69 190 .54	15.40	0.1435 0.1650 0.1868	0 .8855 0 .5921 0 .4073	1.129 1.689 2.455	70 80 90
100 110 120	1697.6 2367.6 3231.7	68 .18 76 .74 85 .67	267 .3 269 .6 272 .5	199 .12 192 .86 186 .83	183 .54 177 .15 170 .97	15.71	0.2090 0.2315 0.2544	0.2874 0.2083 0.1544	4.801	100 110 120
130 140 150	4323.0 5674.6 7318.4	94.98 104.70 114.82	276 .0 280 .5 285 .3	181 .02 175 .80 170 .48	164.99 159.55 154.03	16.25	0.2776 0.3013 0.3254	0.1170 0.0905 0.0714	11.05	130 140 150

TABLE VI. SATURATED VAPOR OF CHLOROFORM.

FRENCH UNITS.

Temperature, Degrees Centi- grade.	Pressure, Millimeters of Mercury.	Heat of the Liquid,	Total Heat.	Heat of Vaporization.	Heat equivalent of Internal Work.	Heat equivalent of External Work.	Entropy of the Liquid.	Specific Volume.	Weight, in Kilos, of One Cubic A	Temperature, Degrees Centi-
t	<i>p</i>	q 	<i>H</i>	r	ρ	A pu	θ	8	γ	t
0	59 .72	0.00	67.00	67.00	62.45	4.55	0.00000	2 .377	0.4207	0
10 20 30	100 .47 160 .47 247 .51		69.75	65.08	61 .29 60 .14 59 .00	4.75 4.94 5.10	0.00836 0.01646 0.02432	1.475 0.9601 0.6437	0.6780 1.042 1.554	10 20 30
40 50 60	369 .26 535 .05 755 .44	11.74	73 .87	63.13 62.13 61.13	57 .87 56 .73 55 .60	5.26 5.40 5.53	0.03196 0.03940 0.04664	0.4449 0.3155 0.2291	2.248 3.170 4.356	40 50 60
70 80 90	1042.1 1407.6 1865.2	16 .51 18 .91 21 .32	76 .62 78 .00 79 .37		54 .45 53 .31 52 .16	5.66 5.78 5.89	0.05369 0.06057 0.06729	0.1700 0.1286 0.0991	5.88 7.78 10.09	70 80 90
100 110 120	2428.5 3111.0 3925.7	23 .74 26 .17 28 .61	82.12	55.95	51 .01 49 .84 48 .67	6.00 6.11 6.22	0.07386 0.08027 0.08655	0.0777 0.0618 0.0500	16.18	100 110 120
130 140 150	4885.1 6000.2 7280.6	31 .06 33 .52 35 .99		53.81 52.73 51.63	47 .48 46 .30 45 .10	6.33 6.43 6.53	0.09270 0.09872 0.10462	0.0410 0.0340 0.0286	29.4	130 140 150
160	8734.2	38 .47	89.00	50.53	43.90	6.63	0.11041	0.0243	41.2	160

TABLE VII.

SATURATED VAPOR OF CARBON BISULPHIDE.

FRENCH UNITS.

me.

Dens

Temperature, Degrees Cer grade.	Pressure, Millimeters of Mercury.	Heat of the Liquid.	Total Heat.	Heat of Vaporizatic	Heat equivale of Internal Work,	Heat equivale of External Work.	Entropy of the Liquid.	Specific Volun	Weight, in Kilos, of
t	<i>p</i>	<i>q</i>	H	r	ρ	A pu	θ	8	γ
0	127 .91	0.00	90.00	90.00	82.76	7.24	0.00000	1.766	0.
10 20 30	198 .46 298 .03 434 .62		91.42 92.76 94.01	89 .06 88 .02 86 .88	81 .58 80 .31 78 .97	7.48 7.71 7.91	0.00847 0.01670 0.02472	1.177 0.8071 0.5684	0. 1. 1.
40 50 60	617.53 857.07 1164.5		95 .18 96 .27 97 .28	85 .64 84 .31 82 .87	77.54 76.04 74.45	8.10 8.27 8.42	0.03252 0.04013 0.04756	0.4098 0.3017 0.2264	3.3
70 80 90	1552.1 2032.5 2619.1	16 .86 19 .34 21 .83	99.04	79.70		8.56 8.67 8.77	0.05482 0.06192 0.06886	0.1338	7.
100 110 120	3325.2 4164.1 5148.8	24 .34 26 .86 29 .40	101.07		67.29 65.31 63.24	8.85 8.90 8.94	0.07566 0.08233 0.08886	0.0837 0.0674 0.0549	
130 140 150	6291.6 7604.0 9095.9	31.96 34.53 37.12	102.36		58.88	8.96 8.95 8.92	0.09527 0.10157 0.10775	0.0375	26.

TABLE VIII.

SATURATED VAPOR OF CARBON TETRACHLORIDE.

FRENCH UNITS.

Temperature, Degrees Centi- grade.	Pressure, Millimeters of Mercury.	Heat of the Liquid.	Total Heat.	Heat of Vaporization.	Heat equivalent of Internal Work.	Heat equivalent of External Work.	Entropy of the Liquid.	Specific Volume,	Weight, in Kilos, of One Cubic Meter.	Temperature, Degrees Centi- grade.
t	р	q	H	r	ρ	Apu	θ	8	γ	t
0	32 .95	0.00	52.00	52.00	48.54	3 .46	0.00000	3 .272	0.3056	0
10	55 .97	1.99	53 .44	51 .45	47 .85	3.60	0.00714	2.005	0 .4987	10
20	90 .99	3.99	54 .86	50 .87	47 .13	3.74	0.01409	1.283	0 .7794	20
30	142 .27	6.02	56 .23	50 .21	46 .33	3.88	0.02087	0.8510	1 .175	30
40	214 .81	8 .06	57.58	49 .52	45 .51	4.01	0.02749	0.5831	1.715	40
50	314 .38	10 .12	58.88	48 .76	44 .62	4.14	0.03396	0.4109	2.434	50
60	447 .43	12 .20	60.16	47 .96	43 .69	4.25	0.04028	0.2969	3.368	60
70	621 .15	14 .30	61 .40	47.10	42 .75	4.35	0.04648	0.2192	4.562	70
80	843 .29	16 .42	62 .60	46.18	41 .74	4.44	0.04255	0.1650	6.061	80
90	1122 .3	18 .55	63 .77	45.22	40 .50	4.72	0.05849	0.1263	7.92	90
100	1467.1	20 .70	64 .90	44 .20	39 .62	4.58	0.06433	0.0980	10.20	100
110	1887.4	22 .87	66 .01	43 .14	38 .52	4.62	0.07006	0.0770	12.99	110
120	2393.7	25 .06	67 .07	42 .01	37 .36	4.65	0.07569	0.0611	16.37	120
130	2996 .9	27 .27	68 .10	40 .83	36 .18	4.65	0.08122	0.0490	20 .41	130
140	3709 .0	29 .49	69 .10	39 .61	34 .95	4.63	0.08666	0.0395	25 .3	140
150	4543 .1	31 .73	70 .07	38 .34	33 .75	4.59	0.09201	0.0321	31 .2	150
160	5513.1	34.00	71.00	37.00	32.47	4.53	0.09729	0.0262	38.2	160

TABLE IX.

SATURATED VAPOR OF ACETON.

FRENCH UNITS.

										_
Temperature, Degrees Centi- grade.	Pressure, Millimeters of Mercury.	Heat of the Liquid.	Total Heat.	Heat of Vaporization.	Heat equivalent of Internal Work.	Heat equivalent of External Work,	Entropy of the Liquid.	Specific Volume.	Weight, in Kilos, of Cone Cubic Articles.	m-management.
t	p	q	H	r	ρ	Apu	θ	8	γ	
ļ		***************************************								-
0	63.33	0.00	140.50	140.50	131 .82	8.68	0.00000	4.275	0.2339	
10 20 30	110.32 180.08 280.05	5.10 10.29 15.55	144.11 147.62 151.03	139 .01 137 .33 135 .48	129 .51 127 .16 124 .83	9.50 10.17 10.65	0.01832 0.03627 0.05389		0.3723 0.5688 0.8425	
40 50 60	419.35 608.81 860.96	20 .89 26 .31 31 .81	154.33 157.53 160.63	133 .44 131 .22 128 .82	121 .39 119 .86 117 .22	11.05 11.36 11.60	0.07119 0.08820 0.1049	0.8227 0.5830 0.4215	1.215 1.715 2.372	
70 80 90	1189 .9 1611 .1 2140 .8	37.39 43.05 48.79	163.62 166.51 169.30	126 .23 123 .46 120 .51	114.43 111.49 108.41	11 .80 11 .97 12 .10	0.1214 0.1376 0.1536	0.3106 0.2328 0.1773	3.220 4.296 5.640	
100 110 120	2796 .2 3594 .3 4552 .0	54.61 60.50 66.48	171.98 174.56 177.04	117.37 114.06 110.56	105 .17 101 .78 98 .23	12.20 12.28 12.33	0.1694 0.1850 0.2004	0.1372 0.1076 0.0856	7.289 9.294 11.68	
130 140	5684 .9 7007 .6	72.54 78.67	179 .42 181 .69	106 .88 103 .02	94.53 90.67	12.35 12.35	0.2156 0.2306	0.0689 0.0561	14.51 17.83	

TABLE X.

SATURATED VAPOR OF AMMONIA.

ENGLISH UNITS.

Degrees Fah- renheit.	Pressure, Pounds per Square Inch.	Heat of the Liquid.	Total Heat.	Heat of Vaporization.	Heat equivalent of Internal Work,	Heat equivalent of External Work.	Entropy of the Liquid.	Specific Volume.	Weight, in pounds, of One Cubic Foot.	Temperature, Degrees Fah- renheit,
t	p	Q	H	<i>r</i>	ρ	Apu	θ	8	γ	t
-40	9.93	-79	519	598	550	48	$ \begin{array}{r} -0.1737 \\ -0.1607 \\ -0.1482 \end{array} $	26.1	0.0383	-40
-35	11.53	-74	520	594	546	48		22.6	0.0442	-35
-30	13.36	-68	522	590	541	49		19.7	0.0507	-30
-25 -20 -15	15 .40 17 .70 20 .25	$-63 \\ -57 \\ -52$	523 525 526	586 582 578	537 532 528	49 50 50	$ \begin{array}{r} -0.1354 \\ -0.1229 \\ -0.1102 \end{array} $	17.3 15.2 13.3	0.0580 0.0660 0.0750	-25 -20 -15
-10 -5 0	23 .10 26 .25 29 .74	$-46 \\ -41 \\ -35$	528 529 531	574 570 566	524 519 515	50 51 51	$ \begin{array}{r} -0.0982 \\ -0.0859 \\ -0.0738 \end{array} $	11 .8 10 .5 9 .32	0.0848 0.0956 0.108	-10 -5 0
5 10 15	33 .58 37 .80 42 .43	$-30 \\ -24 \\ -19$	532 534 535	562 558 554	511 506 502	51 52 52	$ \begin{array}{r} -0.0619 \\ -0.0501 \\ -0.0386 \end{array} $	8.31 7.44 6.68	0.120 0.134 0.150	5 10 15
20	47 .49	-13	537	550	497	53	$ \begin{array}{r} -0.0271 \\ -0.0157 \\ -0.0044 \end{array} $	6.02	0.166	20
25	53 .01	-8	538	546	493	53		5.43	0.184	25
30	59 .01	-2	540	542	489	53		4.92	0.203	30
35	65 .53	3	541	538	484	54	0.0067	4.46	0.225	35
40	72 .59	9	543	534	480	54	0.0177	4.06	0.247	40
45	80 .21	14	544	530	475	55	0.0287	3.70	0.270	45
50	88 .44	20	546	526	471	55	0.0395	3.38	0.296	50
55	97 .30	25	547	522	467	55	0.0502	3.09	0.323	55
60	106 .82	31	549	518	462	56	0.0608	2.84	0.352	60
65	117.04	· 36	550	514	458	56	0.0713	2.61	0.383	65
70	127.98	42	552	510	454	56	0.0817	2.40	0.416	70
75	139.67	47	553	506	449	57	0.0921	2.22	0.451	75
80	152 .15	53	555	502	445	57	0.1023	2.05	0.488	80
85	165 .47	58	556	498	441	57	0.1124	1.90	0.527	85
90	179 .64	64	558	494	436	58	0.1224	1.76	0.568	90
95	194.70	69	559	490	432	58	0.1324	1.63	0.612	95
100	210.70	75	561	486	428	58	0.1423	1.52	0.657	100

TABLE XI.

SATURATED VAPOR OF SULPHUR DIOXIDE.

ENGLISH UNITS.

	7								1	T
re, Fah-	per Inch.	φ.	ئد	at of Vaporization.	Heat equivalent of Internal Work.	Heat equivalent of External Work.	f the	Specific Volume.	Density.	
Temperature, Degrees Fah- renheit,	essure, Pounds per Square Inch,	Heat of the Liquid.	Total Heat.	of aporiz	eat equival of Internal Work,	at equivale of External Work,	Entropy of the Liquid.	fic Ve	eight, in pounds, of One Cubic Foot.	-
Tem! De rer	Pressure, Pound Square	Heat	Tota	Heat of Vapo	Heat of W	Heat of W	Entr	Speci	Weight, pound One C	8
t	р	q	H	r	ρ	Apu	θ	8	γ	
-40	3.14	-29	166	195	182 180	13	-0.0632	23.0	0.0434	
-35 -30	3.70 4.34	$ \begin{array}{r} -27 \\ -25 \end{array} $	167 168	194 193	179	14 14	-0.0584 -0.0539	19.7 17.0	0.0507 0.0590	
-25 -20	5.07 5.90	$-23 \\ -21$	168 169	191 190	177 176	14 14	$ \begin{array}{r} -0.0492 \\ -0.0447 \end{array} $	14.7 12.7	0.0682 0.0785	
-15	6.83	19	170	189	175	14	-0.0401	11.1	0.0901	
-10 -5	7.88	$-17 \\ -15$	170 171	187 186	173 172	14 14	-0.0357 -0.0312	9 .73 8 .56	0.103 0.117	
0	10 .35	-13	172	185	170	15	-0.0268	7.54	0.133	
5 10	11 .81 13 .41	-11 -9 -7	172 173 174	183 182 181	168 167 166	15 15 15	-0.0225 -0.0182	6.67 5.93 5.29	0.450 0.169 0.189	
15	15 .19			179	164	15	-0.0140	4.72	0.189	
20 25 30	17.15 19.30 21.66	$ \begin{array}{r} -5 \\ -3 \\ -1 \end{array} $	174 175 176	179 178 177	163 162	15 15 15	-0.0098 -0.0057 -0.0016	4.23	0.212	
35	24.24	1	176	175	160	15	0.0024	3.43	0.291	
40 45	27.06 30.12	3 5	177 177	174 172	158 156	16 16	0.0064 0.0104	3.10 2.81	0.322 0.356	
50,	33 .45	7	178	171	155	16	0.0144	2.58	0.390	
55 60	37 .07 40 .98	9 11	179 179	170 168	154 152	16 16	0.0182 0.0221	2.32 2.11	0.430 0.473	
65 70	45 .20	13 15	180 181	167 166	151 150	16 16	0.0259 0.0297	1.94 1.78	0.516 0.563	
75	49 .75 54 .64	17	181	164	148	16	0.0297	1.63	0.614	
80 85	59 .90 65 .54	19 21	182 183	163 162	146 145	17 17	0.0372 0.0409	1.50 1.38	0.668 0.725	
90	71.57	23	183	160	143	17	0.0445	1 .27	0.786	
95 100	78 .02 84 .90	25 27	184 185	159 158	142 141	17 17	0.0482 0.0518	1.18 1.09	0.849 0.917	

PROPERTIES OF STEAM AND OTHER VAPORS.

TABLE XII.

SPECIFIC GRAVITY AND SPECIFIC VOLUME OF LIQUIDS.

Name of Liquid.	Specific Gravity, compared with Water at 4° C.	Specific Volume. Cubic Meters per Kilo.
Alcohol, C_2H_6O	0.736 [Kopp, 1860] 1.527 [Thorpe, 1880] 1.2922 [Thorpe, 1880] 1.6320 [Thorpe, 1880] 0.81 [Zander, 1882] 1.4336 [Andréeff, 1859]	0.001240 0.001358 0.000655 0.000774 0.000613 0.00123 0.0006981 0.001571

TABLE XIII.

VOLUME OF WATER.

Vol. at 4° C. = 1.

[Rossetti, 1871] and [Hirn, 1867].

Cemper- ature.	Volume.	Temper- ature.	Volume.	Temper- ature.	Volume.	Temper- ature.	Volume.
10	1.000253	60	1.01691	110	1.0512	160	1 .1018
20	1.001744	70	1.02256	120	1.0599	170	1 .1139
30	1.00425	80	1.02887	130	1.0694	180	1 .1268
40	1.00770	90	1.03567	140	1.0795	190	1 .1403
50	1.01195	100	1.04312	150	1.0903	200	1 .1544

TABLE XIV.

CONVERSION TABLE.

INCHES OF MERCURY AND POUNDS PER SQUARE INCH.

		1	2	3	4	5	6	7	8	9
0	0.00	0.05	0.10	0.15	0.20	0.25	0.29	0.34	0.39	0.44
1	0.49	0.54	0.59	0.64	0.69	0.74	0.79	0.84	0.88	0.93
2	0.98	1.03	1.08	1.13	1.18	1.23	1.28	1.33	1.38	1.42
3	1.47	1.52	1.57	1.62	1.67	1.72	1.77	1.82	1.87	1.91
4	1.96	2.01	2.06	2.11	2.16	2.21	2.26	2.31	2.36	2.41
5	2.46	2.51	2.55	2.60	2.65	2.70	2.75	2.80	2.85	2.90
6	2.95	3.00	3.05	3.09	3.14	3.19	3.24	3.29	3.34	3.39
7	3.44	3.49	3.54	3.59	3.63	3.68	3.73	3.78	3.83	3.88
8	3.93	3.98	4.03	4.08	4.13	4.18	4.22	4.27	4.32	4.37
9	4.42	4.47	4.52	4.57	4.62	4.67	4.72	4.76	4.81	4.86
10	4.91	4.96	5.01	5.06	5.11	5.16	5.21	5.26	5.30	5.35
11	5.40	5.45	5.50	5.55	5.60	5.65	5.70	5.75	5.80	5.85
12	5.89	5.94	5.99	6.04	6.09	6.14	6.19	6.24	6.29	6.34
13	6.39	6.43	6.48	6.53	6.58	6.63	6.68	6.73	6.78	6.83
14	6.88	6.93	6.97	7.02	7.07	7.12	7.17	7.22	7.27	7.32
15	7.37	7.42	7.47	7.52	7.56	7.61	7.66	7.71	7.76	7.81
16	7.86	7.91	7.96	8.01	8.06	8.10	8.15	8.20	8.25	8.30
17	8.35	8.40	8.45	8.50	8.55	8.60	8.64	8.69	8.74	8.79
18	8.84	8.89	8.94	8.99	9.04	9.09	9.14	9.19	9. 23	9.28
19	9.33	9.38	9.43	9.48	9.53	9.58	9.63	9.68	9. 73	9.77
20	9.82	9.87	9.92	9.97	10.02	10.07	10.12	10.17	10. 22	10.27
21	10.32	10.37	10.41	10.46	10.51	10.56	10.61	10.66	10.71	10.76
22	10.81	10.86	10.90	10.95	11.00	11.05	11.10	11.15	11.20	11.25
23	11.30	11.35	11.40	11.44	11.49	11.54	11.59	11.64	11.69	11.74
24	11.79	11.84	11.89	11.94	11.99	12.03	12.08	12.13	12.18	12.23
25	12.28	12.33	12.38	12.43	12.48	12.53	12.57	12.62	12.67	12.72
26	12.77	12.82	12.87	12.92	12.97	13.02	13.07	13.11	13.16	13.21
27	13.26	13.31	13.36	13.41	13.46	13.51	13.56	13.61	13.66	13.70
28	13.75	13.80	13.85	13.90	13.95	14.00	14.05	14.10	14.15	14.20
29	14.24	14.29	14.34	14.39	14.44	14.49	14.54	14.59	14.64	14.69
30	14.74	14.78	14.83	14.88	14.93	14.98	15.03	15.08	15.13	15.18

Table XV.

Values of the factor $\frac{150,300,000}{T^3}$ — 0.0833.

		,						
Tem	perature.	Value.	Ten	nperature.	Value.	Ten	perature.	Value of
Fahr.	Abs.	Factor.	Fahr.	Abs.	Factor.	Fahr.	Abs.	Factor.
200	659.5	0.441	335	794 .5	0.216	470	929 .5	0.104
205	664.5	0.429	340	799 .5	0.211	475	934 .5	0.101
210	669.5	0.417	345	804 .5	0.205	480	939 .5	0.098
215	674.5	0.405	350	809 .5	0.200	485	944 .5	0.095
220	679.5	0.395	355	814 .5	0.195	490	949 .5	0.092
225	684.5	0.385	360	819 .5	0.190	495	954 .5	0.090
230	689.5	0.375	365	824 .5	0.185	500	959.5	0.087
235	694.5	0.365	370	829 .5	0.180	505	964.5	0.084
240	699.5	0.356	375	834 .5	0.175	510	969.5	0.082
245	704.5	0.347	380	839 .5	0.171	515	974.5	0.079
250	709.5	0.338	385	844 .5	0.166	520	979.5	0.077
255	714.5	0.329	390	849 .5	0.162	525	984.5	0.074
260	719 .5	0.320	395	854 .5 ·	0.158	530	989.5	0.072
265	724 .5	0.312	400	859 .5	0.153	535	994.5	0.070
270	729 .5	0.304	405	864 .5	0.149	540	999.5	0.067
275	734.5	0.296	410	869 .5	0.145	545	1004.5	0.065
280	739.5	0.288	415	874 .5	0.141	550	1009.5	0.063
285	744.5	0.281	420	879 .5	0.138	555	1014.5	0.061
290	749 .5	0.274	425	884 .5	0.134	560	1019.5	0.059
295	754 .5	0.267	430	889 .5	0.131	565	1024.5	0.057
300	759 .5	0.260	435	894 .5	0.127	570	1029.5	0.055
305	764.5	0 .253	440	899 .5	0.123	575	1034.5	0.053
310	769.5	0 .247	445	904 .5	0.120	580	1039.5	0.051
315	774.5	0 .240	450	909 .5	0.117	585	1044.5	0.049
320 325 330	779 .5 784 .5 789 .5	0.234 0.228 0.222	455 460 465	914.5 919.5 924.5	0.113 0.110 0.107	590 595	1049 .5 1054 .5	0.047 0.045

TEMPERATURE-ENTROPY TABLE.

This table gives the properties of moist and of superheated steam at each degree of temperature Fahrenheit, and for each hundredth of a unit

of entropy.

At the left hand of each page are given the temperatures and the corresponding pressures of saturated steam; the lines across the tables are, therefore, constant pressure lines, and for moist steam are also constant temperature lines.

The table is divided by a broken line which corresponds roughly to the saturation line; properties to the left of that line are for moist steam and to the right are for superheated steam.

The triple-columns are headed with the entropy, and are constant entropy lines; they can be used for solving problems concerning adiabatic operations in a closed cylinder, and similar problems.

At any point in the table, determined by the entropy and the pressure (or the corresponding temperature of saturated steam), there are given three properties:—

- (1) The quality, which for moist steam is the proportion of a pound that is steam, and for superheated steam is the number of degrees of superheating.
- (2) The heat contents, or the number of thermal units required to change a pound of water at freezing into steam at the given pressure and with the given quality.
 - (3) The specific volume in cubic feet per pound.

For examples, solved by aid of the table, see page 30.

TEMPERATURE-ENTROPY TABLE.

	7	,			1			,			,		
re, Fabr.	e.		1.52			1.53			1.54			1.55	
Temperature, Degrees Fahr.	Pressure, Pounds per Square Inch.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.
420 419 418	308.6 305.2 301.9	2	1212 1211 1210	1.515 1.526 1.540	17 16 15	1221 1220 1219	1 .555 1 .572 1 .580	32 31 30	1230 1229 1228	1 .596 1 .610 1 .625	47 46 44	1239 1238 1237	1.645 1.659 1.672
417 416 415	298.7 295.4 292.2		1209 1208.5 1207.5	1.555 1.581 1.597	14 13 12	1218 1217 1216	1.595 1.610 1.623	29 28 27	$\begin{array}{c c} 1227 \\ 1227 \\ 1226 \end{array}$	1 .640 1 .654 1 .669	43 42 41	1236 1235 1234	1.686 1.701 1.715
414 413 412	289 .0 285 .9 282 .7	9981 9974 9965	1206 .6 1205 .7 1204 .7	1.629	11 10 9	1215 1214 1213	1 638 1.650 1.663	$\frac{26}{25}$	1225 1224 1223	1 .682 1 .697 1 .711	40 39 38	1233 1232 1231	1 .730 1 .744 1 .759
411 410 409	279 .6 276 .5 273 .5	9958 9949 9942	1203 .8 1202 .8 1201 .9	1.677	8 7 6	1212 1212 1211	1 .678 1 .695 1 .710	$\frac{23}{21} \\ 20$		1 .726 1 .740 1 .758	37 36 35	1230 1229 1228	1 .774 1 .790 1 .805
408 407 406	270 .5 267 .5 264 .5	9934 9926 9920	1201 .0 1200 .0 1199 .2	1 .728 1 .746	5 4 3	1210 1209 1208	1 .725 1 .740 1 .755	19 18 17	1217	1 .772 1 .788 1 .803	34 32 31	1227 1226 1225	1 .820 1 .837 1 .853
405 404 403	261 .6 258 .6 255 .7	9912 9904 9896	1198 .2 1197 .3 1196 .3	1.763 1.781 1.799	$\begin{smallmatrix}2\\1\\0\end{smallmatrix}$	1206	1 .771 1 .787 1 .805	16 15 14	1215	1 .820 1 .836 1 .853	30 29 28	1224 1223 1222	1 .869 1 .886 1 .902
102 101 100	252 .9 250 .0 247 .2	9888 9881 987 4	1195.3 1194.3 1193.4	1.818 1.836 1.854	9992 9985 9977	$\begin{array}{c} 1204.0 \\ 1202.9 \\ 1202.0 \end{array}$	1.856	13 12 11	1212	1 .869 1 .885 1 .902	27 26 25	$\begin{array}{c} 1221 \\ 1220 \\ 1219 \end{array}$	1.920 1.936 1.953
399 398 397	244 .4 241 .7 238 .9	9865 9858 9851	1192 .4 1191 .5 1190 .6	1.892	9968 9961 9954	1201 .0 1200 .0 1199 .1	1.913	9 8 7	1208	1 .920 1 .938 1 .946	24 22 21	$\begin{array}{c} 1218 \\ 1217 \\ 1216 \end{array}$	1 .971 1 .990 2 .007
96 95 94	236 .2 233 .5 230 .8	9843 9835 9828	1189.6 1188.6 1187.7	1.931 1.951 1.971		1198.1 1197.2 1196.3		$\begin{matrix} 6 \\ 5 \\ 4 \end{matrix}$	1206	1 .964 1 .992 2 .010	20 19 18	$\begin{array}{c} 1215 \\ 1214 \\ 1213 \end{array}$	2 .025 2 .044 2 .063
93 92 91	228 .2 225 .6 223 .0	9819 9813 9804	1186 .7 1185 .8 1184 .8	2.012	9921 9914 9905	1195.3 1194.3 1193.3	2.012 2.033 2.054	$\begin{smallmatrix} 3\\2\\1\end{smallmatrix}$	1203	2.030 2.048 2.067	17 16 15	$\begin{array}{c} 1212 \\ 1211 \\ 1210 \end{array}$	2.082 2.100 2.120
90 89 88	220 .4 217 .8 215 .3	9796 9789 9781	1183 .9 1182 .9 1181 .9	2 .054 2 .075 2 .097	9898 9890 9881	1192 .3 1191 .4 1190 .4	2.075 2.097 2.119	9999 9991 9983	1200 .9 2 1199 .9 1198 .9	2.096 2.118 2.141	$\begin{array}{c c} 14 \\ 12 \\ 11 \end{array}$	1209 1208 1207	2.140 2.160 2.180
87 86 85	212.8 210.3 207.9	9773 9765 9757	1180 .9 1179 .9 1179 .0	2.119 2.141 2.163	9874 9865 9857	1189 .4 1188 .4 1187 .4	2.141 2.163 2.185		1197 .8 1196 .8 1195 .8		10 9 8	1206 1205 1204	2 .200 2 .220 2 .241
84 83 82	205 .4 203 .0 200 .6	9750 9744 9735	1178.0 1177.1 1176.1	2.209	9851 9843 9835	1186 .5 2 1185 .5 2 1184 .5 2	2.208 2.232 2.254	9951 9943 9934	1194.8 1193.9 1192.9	2 .231 2 .254 2 .277	7 6 5	1203 1202 1201	2.262 2.284 2.306
81	198.3	9727	1175.12	2.255	9827	1183.52	2.278	9926	1191.9	3.301	4	1200	2 328

Heat Con- tents.	1278 1277 1276	1275 1274 1273	1272 1271 1270	1268 1267 1266	1265 1264 1263	1262 1261 1260	$\begin{array}{c c} 1258 \\ 1257 \\ 1256 \end{array}$	1255 1254 1253	1252 1251 1250	1248 1247 1246	1245 1244 1243	1242 1241 1240	1239 1238 1237	1235 1254 1233	1232 1231 1229	1228 1227 1226
Quality.	114 113 112	110 109 108	106 105 104	102 101 100	98 97 96	94 93 92		86 85 84	82 81 80	78 77 76	ı	1	i e	62 61 60	58 57 55	54 52 51
Specific Volume.	1.778 1.792 1.808	1 .822 1 .838 1 .854	1 .870 1 .886 1 .902	1 .919 1 .934 1 .950	1 .967 1 .984 2 .002	2 .020 2 .037 2 .055	$\begin{bmatrix} 2.073 \\ 2.091 \\ 2.110 \end{bmatrix}$	$\begin{bmatrix} 2.129 \\ 2.147 \\ 2.165 \end{bmatrix}$	2 .184 2 .204 2 .224	$2.244 \\ 2.265 \\ 2.286$	$2.306 \\ 2.327 \\ 2.349$	$2.370 \\ 2.391 \\ 2.413$	$2.434 \\ 2.458 \\ 2.480$	$\begin{array}{c} 2.502 \\ 2.526 \\ 2.550 \end{array}$	2.575 2.599 2.624	2.648 2.672 2.699
Heat Con- tents.	1268 1267 1266	$^{1265}_{1264}_{1263}$	1262 1260 1259	1258 1257 1256	1255 1254 1253	1252 1251 1250	1249 1248 1247	1246 1245 1244	1242 1241 1240	1239 1238 1237	1236 1235 1234	1233 1232 1231	1230 1229 1228	1227 1226 1224	1223 1222 1221	1220 1219 1218
Quality.	97 96 95	94 92 91	90 88 87	86 85 83	82 81 79	78 77 75	74 73 72	70 69 68	66 65 64	63 61 60	59 57 56	55 54 52	51 50 48	47 46 44	43 42 41	39 38 37
Specific Volume.	1 .728 1 .743 1 .758	1 .773 1 .788 1 .803	1 .819 1 .834 1 .851	1 .867 1 .883 1 .900	1 .916 1 .933 1 .950	1.967 1.984 2.002	2.019 2.037 2.054	$\begin{bmatrix} 2.073 \\ 2.092 \\ 2.110 \end{bmatrix}$	$2.139 \\ 2.148 \\ 2.167$	2 .186 2 .205 2 .225	2.245 2.266 2.287	$\begin{bmatrix} 2.308 \\ 2.330 \\ 2.351 \end{bmatrix}$	$\begin{bmatrix} 2.372 \\ 2.394 \\ 2.418 \end{bmatrix}$	2.440 2.463 2.486	2.509 2.533 2.556	$2.580 \\ 2.605 \\ 2.630$
Heat Con- tents.	$\begin{array}{c} 1258 \\ 1257 \\ 1256 \end{array}$	$\begin{array}{c} 1255 \\ 1254 \\ 1253 \end{array}$	$\begin{array}{c} 1252 \\ 1251 \\ 1250 \end{array}$	1249 1248 1247	1246 1245 1244	1243 1242 1241	1240 1239 1238	1237 1236 1234	1233 1232 1231	1230 1229 1228	$\begin{array}{c} 1227 \\ 1226 \\ 1225 \end{array}$	1224 1223 1222	1221 1220 1219	1218 1217 1216	1215 1214 1213	1211 1210 1209
Quality.	79 78 77	76 75 73	72 71 70	68 67 66	65 63 62	61 60 59	57 56 55	54 53 51	50 49 48	46 45 44	43 42 40	39 38 37	35 34 33	32 30 29	28 27 26	24 23 22
Specific Volume.	1.686 1.701 1.716	1.731 1.745 1.760	1.776 1.791 1.806	1 .821 1 .837 1 .853	1 .869 1 .885 1 .902	1 .918 1 .934 1 .950	1.967 1.984 2.002	$\begin{array}{c} 2.020 \\ 2.038 \\ 2.057 \end{array}$	$2.075 \\ 2.094 \\ 2.113$	$\begin{bmatrix} 2.131 \\ 2.150 \\ 2.170 \end{bmatrix}$	$\begin{bmatrix} 2.190 \\ 2.210 \\ 2.230 \end{bmatrix}$	$\begin{bmatrix} 2.250 \\ 2.271 \\ 2.293 \end{bmatrix}$	$2.315 \\ 2.338 \\ 2.360$	2.383 2.405 2.429	$2.452 \\ 2.476 \\ 2.500$	2.524 2.548 2.572
Heat Con- tents.	1249 1247 1246	1245 1245 1244	1243 1242 1241	1240 1239 1238	1237 1236 1235	1234 1233 1232	1231 1230 1229	1228 1227 1225	1224 1223 1222	1221 1220 1219	1218 1217 1216	1215 1214 1213	1212 1211 1210	1209 1208 1207	1206 1205 1204	1203 1202 1201
Quality.	64 62 61	60 59 58	57 55 54	53 52 51	49 48 47	46 45 43	42 41 40	39 38 36	35 34 33	32 30 29	28 27 26	24 23 22	21 20 18	17 16 15	14 12 11	10 9 8
Pressure, Poper Squar	308.6 305.2 301.9	298.7 295.4 292.2	289 .0 285 .9 282 .7	279.6 276.5 273.5	270.5 267.5 264.5	261.6 258.6 255.7	252.9 250.0 247.2	244 .4 241 .7 238 .9	236 .2 233 .5 230 .8	228 .2 225 .6 223 .0	220.4 217.8 215.3	212.8 210.3 207.9	205 .4 203 .0 200 .6	198.3 195.9 193.6	191.3 189.0 186.7	184.5 182.3 180 1
Temperatur Degrees F	420 4 19 4 1 8	417 416 415	414 413 412	411 410 409	408 407 406	405 404 403	402 401 400	399 398 397	396 395 394	393 392 391	390 389 388	387 386 385	384 383 382	381 350 379	378 377 376	375 374 373
ı							l						İ			

			1111	11111	1 1 1	1111	1 1 1	1 1 1	1 1	1 1 1	111	111	111	1	1 1	1 I 1 I
	Quality.	9951 9943 9934	9925 9917 9908	9901 9892 9883	9875 9867 9860	$9852 \\ 9843 \\ 9834$	9826 9818 9809	9801 9793 9784	9775 9767 9758	9750 9742 9733	9725 9717 9708	9700 9692 9684)676)667)659)650)642)634	1617	1
	Specific Volume.	2.531 2.558 2.585	2.613 2.642 2.670	$\begin{array}{c} 2.699 \\ 2.728 \\ 2.758 \end{array}$	2.788 2.819 2.850	$2.882 \\ 2.914 \\ 2.946$	$2.979 \\ 3.012 \\ 3.047$	3 .081 3 .115 3 .150	3 .186 3 .222 3 .259	3 .335	3,451	3.572	3 .698 🗄	3 .787 3 .831 3 .877	,969	.065
1.54	Heat Con- tents.	1182 .9 1181 .9 1180 .9	1179 .9 1178 .9 1177 .8	1176 .8 1175 .8 1174 .8	1173.7 1172.7 1171.7	1170 .7 1169 .7 1168 .6	1167.6 1166.6 1165.6	1164 .6 1163 .5 1162 .5	1161 .4 1160 4 1159 .3	157.3	154.2		148 .9 147 .9 146 .8	145.7 144.7 143.7	142.6 141.5 140.5	139.4
	Quality.	9853 9845 9836		9796	9779 9772 9764	9748	9724	9699 1	9674 1	9659 1	$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	1601 1	1576 1)559 1)552 1)544 1	1527 [1]	511 1
3	Specific Volume.	.6 2.532	6 2.616	6 2.701	5 2.762 5 2.792 5 2.822	5 2.886	4 2 .984 1	4 3.086	3 3 .191 9	3 .303 9	3.417	3.538 9	3.663 9	3.795 9	3.931 9	4.027 9
1.53	Quality. Heat Contents.	9756 1174 .6 9748 1173 .6 9739 1172 .6	9731 1171 .6 9723 1170 .6 9715 1169 .5	9708 1168 .6 9700 1167 .6 9691 1166 .5	$egin{array}{c c} 9683 & 1165 .5 \\ 9676 & 1164 .5 \\ 9669 & 1163 .5 \\ \hline \end{array}$	$egin{array}{c c} 9661 & 1162.5 \\ 9653 & 1161.5 \\ 9645 & 1160.5 \\ \hline \end{array}$	$ \begin{array}{c c} 9637 & 1159.5 \\ 9629 & 1158.4 \\ 9621 & 1157.4 \end{array} $	$\begin{array}{c c} 0612 & 1156.4 \\ 0605 & 1155.4 \\ 0597 & 1154.3 \end{array}$	0588 1153 .3 0581 1152 .3 0572 1151 .3	0564 1150 .3 0556 1149 .3 0548 1148 .2	0540 1147 .2 0533 1146 .2 0524 1145 .1		494 1140 .9 485 1139 .9 477 1138 .8	461 1136.8	437 1133 .6	421 1131 .5
	Specific Volume.	3 2.481 3 2.508 3 2.535	3 2.563 3 2.591 3 2.618	3 2.676	2 .734 2 .765 2 .795	2 .827 2 .858 2 .890	2 .921 2 .955 2 .988	[3.055]	3.125 3.160 3.195	3 .233 3 .271 3 .308	3 .384 9	3.504 9	$3.628 \mid 9$	3.759 9	3.894 9	3.988 9 4.037 9
1.52	Heat Contents.	1165.3	1162.3	1159.3	1157.3 1156.3 1155.3	[1153.3]	1151.3 1150.3 1149.3	1147.3	1144.2	1142.2 1141.2 1140.2	1138.1	1136.1 1135.0 1134.0	1131.9	1129 .8 1128 .8 1127 .8	1126.7 1125.7 1124.7	1123.7 1122.6 4
	Quality.	9650	9626	9611 9603 9595	9587 9580 9573	9565 9558 9550	9542 9535 9526	9518 9511 9503	9495 9487 9479	9471 9465 9456	9448 9441 9432	$\begin{array}{c} 9425 \\ 9418 \\ 9410 \end{array}$	9403 9394 9387	9378 9371 9363	9347	32
Pound	Pressure, Poper Squar	2 177 .9 1 175 .7 0 173 .6	171 .5 169 .4 167 .3	165 .3 163 .2 161 .2	159 .2 157 .2 155 .3	153 .3 151 .4 149 .5	147 .6 145 .8 143 .9	142 .1 140 .3 138 .5	136 .7 135 .0 133 .2	131 .5 129 .8 128 .1	126.4 124.8 123.2	121 .5 119 .9 118 .4	116.8 115.2 113.7	112.2 110.7 109.2	107.7 106.3 104.8	93 93
e, ahr	Temperature, Degrees Fahr	1	68	38	63 62 61	359	56	53		7	14	1	39 38 37	35		103.4 93 102.0 93

	222	222	223	ကကက	വാധാ	നാനാ	cococo	Colesto	6.56.56.5	4	3	60000	40000	4	Н	0 1	9 8 7	
Heat Con- tents.	1225 1224 1223	$\begin{array}{c} 1222 \\ 1221 \\ 1219 \end{array}$	1218 1217 1216	$\begin{array}{c} 1215 \\ 1214 \\ 1213 \end{array}$	$\begin{array}{c} 1212 \\ 1211 \\ 1209 \end{array}$	1208 1207 1206	1205 1204 1203	1202 1201 1199	1198 1197 1196	1195 1194	1193	1192 1191 1189	1188 1187 1186	1185 1184	1183.	1182 . 1181 . 1180 .	1178. 1177. 1176.	1175 . 1174 .
Quality.	50 49 47	46 . 45 43	42 41 39	38 37 35	34 33 31	30 29 27	26 25 23	22 21 19	18 17 15	14 13	ii	10 9 7	6 5 3	2	9995	9985 9976 9967	9958 9949 9940	9932 9921
Specific Volume.	$egin{array}{c} 2.724 \ 2.751 \ 2.778 \ \end{array}$	2 .802 2 .831 2 .859	2.886 2.913 2.941	$\begin{array}{c} 2.970 \\ 2.999 \\ 3.027 \end{array}$	3 .055 3 .086 3 .118	3 .149 3 .181 3 .211	3 .243 3 .275 3 .308	3 .342 3 .377 3 .411	3 .447 3 .481 3 .518	3.552		3 .665 3 .707 3 .750	3 .794 3 .838 3 .883	3.975	1	1	4 .217 4 .268 4 .320	4.372 4.424
Heat Con- tents.	1217 1216 1215	1214 1213 1212	1211 1209 1208	$^{1207}_{1206}_{1205}$	1204 1203 1202	1201 1200 1198	1197 1196 1195	1194 1193 1192	1190 1189 1188	1187	1186 .3 1185 .2	1184 .1 1183 .0 1182 .0	1180 .9 1179 .8 1178 .7	1177 .6 1176 .5	1175 .4	1174 .3 1173 .2 1172 .1	1171 .0 1170 .0 1168 .9	1167 .8 1166 .6
Quality.	35 34 33	32 30 29	28 26 25	24 23 21	20 19 17	16 15 13	$^{12}_{11}_{10}$	8 7 6	4 3 2	0 9994	9984	9975 9968 9958	9950 9940 9932	9922 9913	9904	9895 9886 9878	9869 9859 9851	9843 9833
Specific Volume.	2 .654 2 .680 2 .706	2 .732 2 .760 2 .786	2 .814 2 .842 2 .870	2 .899 2 .928 2 .957	2 .986 3 .017 3 .047	3 .079 3 .108 3 .135	3.170 3.206 3.242	3 .278 3 .315 3 .352	3.430		3.590	3.631 3.673 3.716	3.759 3.803 3.848	3 .939		4.033 4.080 4.130	4.229	4.333 4.384
Heat Con- tents.	1208 1207 1206	1205 1204 1203	1202 1201 1200	1199 1198 1197	1196 1195 1193	1192 1191 1190.0	1189 .0 1187 .9 1186 .8	1185 .7 1184 .7 1183 .6	1182 .6 1181 .6 1180 .5	1179.4	1178 .3 1177 .2	1176 .1 1175 .1 1174 .0	1172 .9 1171 .8 1170 .7	1169 .6 1168 .5	1167.5	1166 .4 1165 .3 1164 .2	1163 .1 1162 .1 1161 .0	1159 .9 1158 .8
Quality.	21 19 18	17 16 14	13 12 11	10 8 7	6 5 3	$\begin{array}{r} 2\\1\\\hline 9998\end{array}$	9989 9980 9971	9962 9954 9945	9936 9928 9919	9910 9901	9892	9884 9876 9867	9859 9849 9841	9831 9823	9814	9805 9796 9788	9779 9770 9762	9754 9744
Specific Volume.	2.596 2.620 2.646	2.672 2.700 2.725	2 .752 2 .782 2 .812	2 .843 2 .874 2 .906	2 .938 2 .971 3 .004	3 .070	3 .141 3 .176 3 .211	3 .247 3 .284 3 .321	3 .359 3 .398 3 .436	3 .475	3 .516 3 .556	3 .597 3 .639 3 .681	3 .724 3 .768 3 .812	3 .857 3 .903	3 .949	3 .996 4 .043 4 .092	4 .140 4 .192 4 .243	4 .294 4 .346
Heat Con- tents.	1200 1198 1197	1196 1195 1194	1193 .3 1192 .3 1191 .2	1190 .2 1189 .2 1188 .1	1187 .1 1186 .1 1185 .0	1183 .9 1182 .9 1181 .9	1180 .8 1179 .8 1178 .7	1177 .6 1176 .6 1175 .5	1174 .5 1173 .5 1172 .4	1171.3	1169 .2	1168 .1 1167 .1 1166 .0	1164 .9 1163 .8 1162 .7		1	1158 .5 1157 .4 1156 .3	11154	1152 .0 1150 .9
Quality.	7 5 4	$\begin{array}{c} 3 \\ 2 \\ 1 \end{array}$	9997 9988 9979	9971 9963 9955	9946 9938 9929	9921 9913 9904	9895 9887 9878	9869 9861 9851	9843 9835 9826	9817 9809	9800	9792 9785 9776	9767 9758 9750	9741 9732	9724	9707	9690 9680 9673	9665 9655
Pressure, Poper Squa	177 .9 175 .7 173 .6	171 .5 169 .4 167 .3	165.3 163.2 161.2	159 .2 157 .2 155 .3	153 .3 151 .4 149 .5	147 .6 145 .8 143 .9	142 .1 140 .3 138 .5	136 .7 135 .0 133 .2	131 .5 129 .8 128 .1	126 .4 124 .8	123 .2	121 .5 119 .9 118 .4	116 .8 115 .2 113 .7	$\frac{112.2}{110.7}$	109.2	107 .7 106 .3 104 .8	103 .4 102 .0 100 .6	99.2 97.8
Temperatu Degrees l	372 371 370	368	366 365 364	363 362 361	359	356	354 353 352	351 350 349	347		343	341	339 338 337	335	1	332	329	327 326

	Specific Volume.	4.464	4.633	4.808	1. 929 1. 992 5. 054	5. 184	. 385	. 596	. 819	. 053	. 297	.556	826	112	311 411 514	729	947
1.00	Heat Con- tents.	140.8 139.8 138.7	137. 6 136. 6 135. 5	134. 4 133. 3 132. 1	131.1 130.0 128.9	127.8 126.7 125.6	$\begin{bmatrix} 24.5 \\ 23.4 \\ 22.3 \end{bmatrix}$	21.3 20.1 18.9	17.9 16.8 15.6	14. 5 6 13. 5 5 12. 3 6	11.2 10.0 08.9	$07.86 \\ 06.76 \\ 05.66$	$ \begin{array}{c} 04.56 \\ 03.46 \\ 02.26 \end{array} $	$ \begin{array}{c c} 01.17 \\ 00.07 \\ \hline 98.97 \\ \end{array} $	$\begin{array}{c} 97.77 \\ 96.57 \\ 95.47 \end{array}$	$egin{array}{c} 94.37 \ 93.27 \ 92.17 \end{array}$	90.97
	Quality.	9541	9518	9492	9475 9466 9458	9441 [1	9415 1	9390 1	9365 1	9341 1	9314 1	9290 1	264 1	9238 [1]	9222 9213 9204	1189 10	171 10
	Specific Volume.	4.423	4. 534 4. 591 4. 646	4.763	1.946	6.137	. 336	. 476 . 546 . 618	. 767	. 998	. 159 . 241 . 325	. 498	. 675 . 765 . 859	049 9	345 9	661 9	877
1.04	Heat Con- tents.	1133.0 1131.9 1130.9	1129.8 1128.8 1127.7	1126.6 1125.5 1124.4	1123.44 1122.34 1121.2	1120.15 1119.05 1117.95	116.8 115.7 114.6	113.6 112.4 5 111.3	110.3 5 109.2 5 108.0 5	106.95 105.95 104.86	103.76 102.56 101.46	$ \begin{array}{c} 100.3 \\ 099.2 \\ 098.1 \\ \end{array} $	$ \begin{array}{c c} 097.06, \\ 095.96, \\ 094.86. \end{array} $	$ \begin{array}{c} 093.66. \\ 092.57. \\ 091.47. \end{array} $	090.3 089.1 088.0 7.	086.9 7. 085.8 7. 084.7 7.	083.67.
	Quality.	9461 9452 9444	9437 9430 9421	9405	9380	9355	9330 1	9314 9305 9296	9280 1	9257 1	9240 9231 9223 1	207	0191 1 0182 1 0174 1	157	131 10	109 10	0091 10
	Specific Volume.	4.382	4.548	1.719	. 900	. 025 . 090 . 154	. 287	. 495	. 714	. 865 . 944 . 023	185	439 9	705 9	986 9	281 9	594 9	809 9
1.00	Heat Con- tents.	1125. 2 1124. 1 1123. 1	1122. 0 1121. 0 1119. 9	1118.84 1117.84 1116.64	$\begin{array}{c} 1115.6 \\ 4\\ 1114.6 \\ 4\\ 1113.5 \\ 4 \end{array}$	$\begin{array}{c} 1112.45 \\ 1111.35 \\ 1110.25 \end{array}$	1109.25 1108.15 1107.05	106. 0 5 104. 8 5 103. 7 5	$\begin{array}{c} 102.7 \\ 101.6 \\ 5.100.4 \\ 5.100.4 \end{array}$	099.3 098.3 097.2 6.	096. 1 6. 095. 0 6. 093. 9 6.	$ \begin{array}{c cccc} 092.8 & 6. \\ 091.7 & 6. \\ 090.6 & 6. \end{array} $	089. 5 6. 088. 4 6. 087. 3 6.	$ \begin{array}{c cccc} 086.2 & 6. \\ 085.1 & 6. \\ 084.0 & 7. \end{array} $	082.9 7. 081.7 7. 080.6 7.	079.5 7. 078.4 7. 077.3 7.	076.27.
	Quality.	9372 9364 9356		9317	9293	9277 9269 9261	9244	9220 1	9196 1	9180 1 9173 1 9164 1	9148 1	124	100 1	075 1	050 1	1028 10	010 1
	Specific Volume.	4.340	4.595	1.675	1.855	. 979 . 042 . 106	238	. 376 . 444 . 515	. 662	. 890 9	. 128 9	382 9	645 9	924 9	216 9	420 9 526 9 633 9	739 9
1.02	Heat Contents.	1117.3 1116.3 1115.2	1114.2 1113.2 1112.1	1111.1 1110.0 1108.9	1107.9 1106.8 1105.8	1104.74 1103.65 1102.55	101.5 100.4 099.3	098.35 097.15 096.05	095.05 093.95 092.85	091.75 090.75 089.65	088. 5 6. 087. 4 6. 086. 3 6.	085. 2 6. 084. 1 6. 083. 1 6.	082. 0 6. 080. 9 6. 079. 8 6.	078.7 6. 077.6 6. 076.5 7.	075. 4 7. 074. 3 7. 073. 2 7.	$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	068.8 7.
	Quality.	9284 9276 9268	9262 9255 9246	9230	9207	9191 9183 9175	9159	9144 9135 9127	9111 1	9089 1	9064 1	9041 1	9017 1	3993 1	3969 [10	3954 3947 3939	3930 1
oun re	Pressure, Poun per Square Inch.	95. 1 93. 8 92. 5	91. 2 90. 0 33. 7	87.4 86.2 85.0	83.8 82.6 81.4	80.2 79.1 77.9	76.8 75.7 74.6	73.5 72.4 71.4	0.3 9.3 8.2	7. 2 6. 2 5. 2	3.3	0.5	7.7	5.1	2.6	0.1	8.55
e, Jahn	Temperature, Degrees Fah	324 323 322	321 320 319	317 316	314	311	308	305	02 (99 6	97 96 95	93 6	90 5	87 5	84 5	31 5	79 4

re, Fahr	Pound		1.00			1.01							
Temperature, Degrees Fahl	Pressure, Pour per Square Inch.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con-	Specific Volume.	Quality.	Heat Contents.	Specific Volume.
323	95. 1 93. 8 92. 5	9637 9629 9620	1148.7 1147.6 1146.5	4. 452 4. 505 4. 562	9726 9717 9708	1156.5 1155.4 1154.3	4.491 4.546 4.603	9814 9805 9796	1164.3 1163.2 1162.1	4.532 4.587 4.645	9903 9893 9885	1172.2 1171.1 1169.9	4.628 4.686
320	91. 2 90. 0 88. 0	9613 9605 9596	1145.4 1144.4 1143.2	4.618 4.676 4.733	9701 9693 9683	1153.2 1152.2 1151.0	4.659 4.718 4.776	9889 9781 9770	1161.0 1160.0 1158.8	[4.760]	987 7 9868 9858	1168.8 1167.8 1166.6	4.744 4.803 4.861
317	87.4 86.2 85.0	9587 9579 9569	1142.2 1141.0 1139.9	4.792 4.852 4.912	9675 9666 9656	1149.9 1148.8 1147.6	4.896	9762 9753 9743	1157.7 1156.6 1155.4	[4.939]	9849 9840 9830	1165.5 1164.4 1163.1	4.922 4.983 5.045
315 314 313	83.8 82.6 81.4	9562 9553 9544	1138.9 1137.8 1136.7	4.974 5.037 5.101	9648 9640 9631	1146.6 1145.5 1144.4	0.083	9735 9726 9717	1154.3 1153.2 1152.1	5.063 5.128 5.192	9822 9813 9804	1162.1 1161.0 1159.8	5.108 5.173 5.238
312 311 310	80.2 79.1 77.9	9536 9527 9518	1135.5 1134.4 1133.3	5.165 5.231 5.297	9622 9613 9604	1143.2 1142.1 1141.0	5. 212 5. 279 5. 345	9708 9699 9690	1151.0 1149.8 1148.7	5. 258 5. 325 5. 391	9794 9785 9776		5.372 5.439
308	76.8 75.7 74.6	9510 9501 9492	1132. 2 1131. 1 1130. 0	5.434	9595 9586 9577	1139.9 1138.8 1137.6	5.482	9681 9672 9663	1147.6 1146.4 1145.3	5.461 5.531 5.603	9767 9757 9748	1155.3 1154.1 1153.0	5.508 5.579 5.652
306 305 304	73.5 72.4 71.4	9484 9474 9466	1128. 9 1127. 7 1126. 6	5.647	9569 9559 9551	1136. 6 1135. 3 1134. 2	5.626 5.697 5.771	9655 9644 9635	1144.2 1143.0 1141.8	5.823	9720	1151.9 1150.6 1149.5	$\begin{bmatrix} 5.798 \\ 5.873 \end{bmatrix}$
302	70.3 69.3 68.2	9458 9449 9441	1125.5 1124.4 1123.2	5.872		1133. 2 1132. 0 1130. 8	5.847 5.924 6.002	9618	1140.8 1139.6 1138.5	5.899 5.977 6.055	9712 9702 9694	1148.4 1147.2 1146.3	5.949 6.028 6.107
299	67.2 66.2 65.2	9432 9424 9416	1122. 1 1121. 1 1119. 9	$\lfloor 6.107 \rfloor$	9508	11128.6	6. 080 6. 161 6. 243	9592	1136.2	6. 134 6. 216 6. 298	9676	1144.9 1143.8 1142.	8 6.270
297 296 298	64.3 63.3 62.3	9407 9398 9390	1118.8 1117.6 1116.5	6. 270 6. 353 6. 439	9490 9481 9473	1126.4 1125.2 1124.1	6. 326 6. 410 6. 497	9574 9564 9556	1132.7	6. 382 6. 466 6. 554	9648		$\begin{bmatrix} 6.523 \\ 6.611 \end{bmatrix}$
29:	61.4 60.5 259.5	9381 9373 9364	1115. 4 1114. 3 1113.	6.526 6.614 6.704	9456	1122.9 1121.8 1120.6	3 6.673	9538	11129.4	$\begin{bmatrix} 6.642 \\ 6.731 \\ 6.823 \end{bmatrix}$	9621	1138. 1136. 1135.	6.699 6.790 6.880
29: 29: 28:	58.6 57.7 9 56.8	9355 9347 9338	1112.0 1110.9 1109.	6.795 6.887 6.981	9438 9429 9421	1119.8 1118.4 1117.	6.855 6.947 7.043	9511	1125.9	6. 915 7. 008 7. 104	9593	1134. 1133. 1132.	6 6.975 4 7.068 2 7.166
28	8 56.0 7 55.1 6 54.2	9328 9320 9312	1108. 1107. 1106.		9402	1116. 1114. 1113.	7. 140 7. 238 7. 337	9492 9484 9475	1123.4 1122.4 1121.	7. 202 4 7. 301 2 7. 401	9574 9566 9557	1131. 1129. 1128.	9 7.364
28	5 53.4 4 52.6 3 51.7	9304 9294 9286	1104.	0 7.470	9375	1112. 1111. 1110.	7.440 4 7.54 3 7.646	9467 9456 9448	1120. 1118. 1117.	7. 504 9 7. 607 7 7. 715	9548 9537 9529	1127. 1126. 1125.	3 7.672
28	2 50.9 1 50.1 0 49.3	9277 9270 9262	1101. 1100. 1099.	8 7. 68' 7 7. 79' 5 7. 90'	9358 9351 9342	1109. 1108. 1106.	7.754 1 7.865 9 7.97	9431	1116. 1115. 1114.	7.82 7.93 8.04	9520 9512 9503	1124. 1122. 1121.	9 8.001
27	9 48.5	9252	1098.	$\frac{1}{2}$ 8.01	9332	1105. 1104	7 8.08 5 8 21	9412	1113.	$ \begin{array}{c c} & 18.15 \\ & 8.27 \\ \end{array} $	6 9493 2 9484	1120 . 1119.	5 8. 225 2 8. 343

ture,	Poun		4	Je.		i i	ne.		1.01	je.		1.5.	
Temperature, Degrees Figh	Pressure, Poun per Square Inch,	Quality.	Heat Con-	Specific Volume.	Quality.	Heat Con-	Specific Volume	Quality.	Heat Con-	Specific Volume.	Quality.	Heat Contents.	Specific Volume.
276 275 274	45.52	8907 8898 8891	1065. 4 1064. 3 1063. 2	8.077 8.192 8.310	8987 8978 8970	1072. 8 1071. 7 1070. 5	8.385	9067 9058 9050	1080. 2 1079. 0 1077. 8	8. 221 8. 339 8. 459	9147 9137 9129	1087. 1086. 1085.	41841
273 272 271	43.35	8883 8875 8867	1062. 1 1061. 0 1059. 9	8. 431 8. 555 8. 679	8962 8954 8946	1069. 4 1068. 3 1067. 2	8.631	9042 9033 9025	1076.7 1075.6 1074.5	8. 582 8. 708 8. 833	9121 9113 9104	1084. 1082. 1081.	1 0 72
270 269 268	41.95 41.26 40.58	8859 8851 8843	1058.7 1057.6 1056.5	8.805 8.932 9.066	8937 8929 8921	1066. 0 1064. 9 1063. 8	9.012	9016 9008 9000	1073.3 1072.2 1071.0	9.091	9095 9087 9078	1080. 6 1079. 5 1078. 3	0 176
267 266 265	39.91 39.26 38.60	8835 8826 8818	1055. 4 1054. 2 1053. 1	9. 199 9. 331 9. 473	8904	1062. 6 1061. 4 1060. 3	9.414	8992 8983 8974	1069.9 1068.7 1067.6	9.497	900T [1077. 1 1075. 9 1074. 8	II Q 570
264 263 262	37.96 37.33 36.71	8803	1051.9 1050.8 1049.7	9.755	8880	1059. 2 1058. 1 1056. 9	0.841	8966 8958 8950	1066. 4 1065. 3 1064. 1	9.927 9	9030	1073.6 1072.5 1071.3	110.01
261 260 259	36. 09 35. 48 34. 88	8788 8780 8771	1048. 6 1047. 4 1046. 3	0. 05 0. 20 0. 36	8865 8857 8848	1055. 8 1 1054. 6 1 1053. 4 1	0.14 0.29 0.45	8934	1063.0 1061.8 1060.6	0.38 9	9020 9011 9002	1070. 2 1069. 0 1067. 8	10.32 10.47 10.63
258 257 256	34. 29 33. 71 33. 14	8755	$ \begin{array}{c cccc} 1045.1 & 1\\ 1044.0 & 1\\ 1042.9 & 1 \end{array} $	0.67	8839 8832 8823	1052.21 1051.11 1050.01	0.61 0.77 0.93	8909	1059.4 1058.3 1057.2	0.86 8	3993 3985	1066.6 1065.5 1064.3	10.79 10.95
255 254 253	32.01	8730 []	$ \begin{array}{c cccc} 1041.7 & 1 \\ 1040.5 & 1 \\ 1039.4 & 1 \end{array} $	1.18 3	8815 8806 8798	1048.8 1047.6 1046.5	1.11 1.28 1.46	8883	1056.0 1054.7 1053.6	1.38 8	8959 H	1063. 1 1061. 9 1060. 8	11.30 11.48 11.65
252 251 250	30.38	8714 8707 8698	1038.2 1037.1 1035.9	1.54 1.72 1.90	3782 1	$\begin{bmatrix} 045.4 \\ 044.2 \\ 043.0 \end{bmatrix}$	1.82	8858	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	1.92 8	3942 1 3934 1 3925 1	059.6 058.4 057.2	11.84 12.02 12.21
249 248 247	28.82	8682 1	1034.8 11 1033.6 11 1032.5 11	2. 09 2. 27 2. 47	3757 1	041.9 040.7 039.6	2.38	8832 [1	1048.9 13 1047.7 13 1046.6 13	$2.49 \mid 8$	916 907 1 900	056. 0 054. 8 053. 7	12.40 12.59 12.79
246 245 244	27.33	8666 1 8658 1 8650 1	031.3 13 030.2 13 029.0 13	2. 66 2. 85 3. 07	3733 1	038. 4 1: 037. 3 1: 036. 1 1:	2.96	8807 1	1045. 4 1044. 3 1043. 1	3.09 8	891 1 882 1 874 1	052.5 051.3 050.1	12.99 13.18 13.41
41	25.90	8635 1	$\begin{bmatrix} 027.9 & 13 \\ 026.8 & 13 \\ 025.6 & 13 \end{bmatrix}$	3.50 8	3709 II	035. 0 1: 033. 8 1: 032. 6 1:	3.61	8783 [1	$\begin{bmatrix} 042.0 & 13 \\ 1040.8 & 13 \\ 1039.6 & 13 \end{bmatrix}$	3.73 8	857 [1	049.0 047.8 046.6	13.63 13.84 14.07
38	24.53	8619 8610 8603	024. 4 13 023. 2 14 022. 0 14	3.94 4.16 4.40 8	684 1	$031.414 \\ 030.214 \\ 029.014$	1.29 8	8758 1	038.3 14 037.2 14 036.0 14	. 41 8	840 832 1 823	$045.3 \\ 044.2 \\ 043.0$	14. 29 14. 53 14. 77
36	23. 23 8	8587 1	020. 9 14 019. 7 14 018. 5 15	1.88 8	660 1	$egin{pmatrix} 027. & 9 & 14 \ 026. & 7 & 15 \ 025. & 5 & 15 \ \end{bmatrix}$	5.01 8	8733 1	034. 8 14 033. 6 15 032. 4 15	13 86	815 1 806 1 797 1	041.8 040.6 039.4	15.01 15.26 15.51
33	21.98 8	3562 [1]	017.3 15 016.1 15 014.9 15	6.63 8	635 1	$024.2 15 \\ 023.1 15 \\ 021.9 16$. 77 8	3707 1	031.2 15 030.0 15 028.8 16	.90 8	788 1	038.1 036.9	15.77 16.03 16.30
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		11111111	1 1 1	1	1	1	111	1111	1 1 1	1	1	1	1	1	1	1	1
	Quality.	9466 9456 9447	9429	9401	9373	9355 9346 9337	9329 9320 9310	9301 9292 9283	9273 9263 9254	9246 9236 9227	9218 9208 9200	9190 9181 9172	9163 9154 9145	9136 9127 9118	9108 9099 9090	9080 9071 9062	9053
	Volume.	516 631 755	$882 \\ 012 \\ 142$	274 408 548	688 826 975	27	74	23	59 77 95	33	91	52	19	89	64	43	98
	Specific	8	9.	9.	9.	10	10	11.	11 11 11	12	12	13	14	14	15	16	16
	Heat Con- tents.	1109 .6 1108 .4 1107 .2	1106.1 1104.9 1103.7	1102.5 1101.3 1100.1	1098.9 1097.7 1096.5	1095.3 1094.2 1093.0	1091.8 1090.6 1089.4	1088.1 1087.0 1085.8	1084. 6 1083. 3 1082. 1	1080.9 1079.7 1078.5	1077.3 1076.0 1074.8	1073.6 1072.5 1071.3	1070.1 1068.8 1067.6	1066.3 1065.1 1063.9	1062.7 1061.5 1060.2	1058.9 1057.7 1056.4	1055.2
	Quality.	9377	9359 9350 9341	9332 9323 9314	9305 9295 9286	9277 9269 9260	9252 9243 9233	9224 9215 9206	9196 9187 9178	9170 9161 9152	9142 9133 9125	9115 9106 9098	9080	9062 9053 9044	9035 9026 9017	9007 8998 8989	8980
	Specific Volume.	8.438 8.558 8.681	8.806 8.935 9.064	9.196 9.328 9.467	9.606 9.743 9.891	10.04 10.18 10.34	10.65	11.14	11.67	12.23	12.81	13.41	14.08	14.77	15.52	16.30	16.84
	Heat Con- tents.	1102.2 1101.1 1099.9	1098.8 1097.6 1096.4	$\begin{array}{c} 1095.2 \\ 1094.1 \\ 1092.9 \end{array}$	1091.7 1090.4 1089.3	1088.1 1087.0 1085.8	1084.6 1083.4 1082.2	1080.9 1079.8 1078.6	1077. 4 1076. 1 1075. 0	1073.8 1072.6 1071.4	1070. 2 1069. 0 1067. 8	1066. 6 1065. 4 1064. 2	1063. 0 1061. 8 1060. 6	1059.3 1058.1 1056.9	1055.7 1054.5 1053.3	1052.0 1050.8 1049.5	1048.3
	Quality.	9306 9297 9288	$\begin{array}{c} 9280 \\ 9271 \\ 9262 \end{array}$	9253 9244 9235	9227 9217 9208	9200 9191 9182	9174 9165 9156	9147 9139 9130	9120 9111 9102	9094 9085 9076	9067 9058 9050	9041 9031 9023	9014 9006 8997	8988 8979 8971	8961 8953 8944	8934 8926 8916	8908
	Specific Volume,	8.366 8.484 8.607	8.731 8.859 8.987	9.117 9.249 9.387	9.525 9.661 9.807		10.56	10.88 11.05 11.22	11.57	11.94 12.13 12.31	12.51 12.70 12.90	13 20	13.96	14.65	15.39	16.17	16.71
	Heat Con- tents.	1094.9 1093.7 1092.5	1091. 4 1090. 3 1089. 1	1087.9 1086.8 1085.6	1084. 4 1083. 2 1082. 1	1080.9 1079.7 1078.5	1077.4 1076.2 1075.0	1073.8 1072.7 1071.5	1070.3 1069.0 1067.9	1066.7 1065.5 1064.3	1063.1 1061.9 1060.7	1059.5 1058.4 1057.2	1056. 0 1054. 8 1052. 6	1052.3 1051.1 1049.9	1048.7 1047.5 1046.3	1045.0 1043.8 1042.6	1041.4
	Quality.	9217	9192	9174 9165 9157	9139	9122 9113 9105	9097 9088 9079	9070 9062 9053	9035	9018 9009 9001	8983			8914 8905 8897	8880	8861 8853 8844	8835
oun re	Pressure, Poun per Square Inch.	46. 26 45. 52 44. 78	44.06 43.35 42.64	41.95 41.26 40.58	39.91 39.26 38.60	37.96 37.33 36.71	36.09 35.48 34.88	34. 29 33. 71 33. 14	32.57 32.01 31.46	30.92 30.38 29.86	29.34 28.82 28.32	27.82 27.33 26.85	26.37 25.90 25.44	24. 98 24. 53 24. 09	23. 66 23. 23 22. 80	22.39 21.98 21.57	21.18
re, Fab	Temperature, Degrees Fab	275	272	270 269 268	266	264 263 262	260	257	254	251	248		242	239	236	233	231
		deposition of the control of the con												*			

9	re, Fahr.	ound				1.5		_				1.	53	3	_				1	. 54	4					1.	55		
Tomporotin	Degrees Fahr.	Pressure, Pounds	Inch.	Quality.	_	Heat Con-	tents.		Specific Volume.	Quality.		Heat Con	tents.		Specific	Volume.	Onality	. Camp	,	Heat Con-	concs.	Specific	Volume.	Quality.		Heat Con-	tents.		Specific
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-la	Heat Col	1043.4	1039.7	1036.0	1032.2	1028.51	1024.7	1020.9	1017.1	1014.6 1013.3 1012.1	1009.5	1007.0 1005.6 1004.3	1001.8	997.9	330.1	995.4 994.1
	Quality.	8872	8845	8820	8802 8792 8783	8765	8739	8712	8685	8657	8632	8604	8577	8550		8523
je	Specific	17.86	118.79	19.44 19.78 20.13	20.48 20.84 21.21	21.96	$\begin{array}{c} 22.74 \\ 23.11 \\ 23.48 \end{array}$	24.34	[25.70]	26.65 27.13 27.63	9 28.67	29.75 30.31 30.88	2 32.07	133.94	i	335.95
1.56	Heat Contents.	1036.5	1032.8	1030.4 1029.2 1028.0	1026.7 1025.4 1024.2	1021.7	1019.3 1018.0 1016.8	1014.2	1010.5	1007.9 1006.7 1005.5	1002.9	1000.4 999.1 997.8	995.2	991.4	I .	987.6
	Quality.	8809 8800 8791	8782 8774 8765	8757 8749 8740	8731 8721 8713	8704 8695 8687	8678 8669 8660	8652 8643 8634	8625 8616 8607	8598 8589 8581	8573 8564 8555	8547 8537 8528	8519 8510 8502	8493 8483 8475		8466 8457 8449
, Poun Juare	Pressure, Pound per Square Inch.	20.02 19.64 19.28	18.91 18.56 18.21	17.86 17.52 17.19	16.86 16.53 16.21	15.90 15.59 15.29	14.99 14.70 14.41	14.12 13.84 13.57	13.29 13.03 12.77	12.51 12.25 12.01	11.76 11.52 11.28	11.05 10.82 10.60	10.38 10.16 9.95	9.74 9.53 9.33	1	9.13 8.94 8.75
es Fah	Temperature, Degrees Fahr	227	224	221	218	215	213 212 211	209	206	204 203 202	200	197	195 194 193	192 191 190	,	189 188 187

6	ahr.	onno e.	-		1.5)2			_	1	. 0.	3					1.	54				1	. 55	5		
Temperatur	Degrees Fahr.	Pressure, Pound per Square	Quality.		Heat Con-	tents.		Specific Volume.	Quality.		Heat Con-	-	Specific	volume.	Quality.	_ -	Heat Con-	tents.		Volume.	Quality.		Heat Con- tents.	:	Specific	volume.
18 17 17	30 79 78	7.50 7.34 7.17	812 811 811	9 0)51)50)49	. 4	40 41 42	0.75 1.56 2.40	8192 8184 8176	95	8. 6. 8 5. 6	3 4	1.0 1.8 2.7	39	8257 8249 8240		964 963 961	. 5 . 2 . 9	41 42 43	1.40 2.22 3.07	8322 8313 8304	2 97 3 96 4 96	0.8 9.6 8.3	444	1. 2. 3.	72 55 41
17 17 17	77 76 75	7.01 6.86 6.70	810 809 808	4 9	47. 46. 45.	. 6	45	3. 26 4. 15 5. 04	8158 8150	95 95	3. (1. 7	4.	3.6 4.5 5.4	0 10	8232 8223 8214	99	60 59 58.	. 7 . 3 . 1	44	. 95 . 85 . 75	8287	96	7.0 5.7 4.4	4 4 4	4. 5. 6.	29 20 11
17	73	6.55 6.41 6.26	8078 8078 806	0 9	44. 42. 41.	9	45 46 47	. 96 . 91 . 88	8142 8133 8125	950 949 947	0. 5 9. 2 7. 9	4:	6.3 7.2 3.2	385	8206 8197 8188	9	56. 55. 54.	5	47	. 69 . 65 . 63	1 2261	961	3.1 (.9).6	4 4 4	7. 8. 9.	05 02 01
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140 139	2	. 953 . 877 . 804	7801 7792 7784	900	1.5 0.2 8.9	2 9	93. 96. 98.	16	7860 7851 7843	907. 906. 904.	2	94. 96. 99.	89	7	7920 7910 7902	91	3.5 2.2 0.8		95. 97. 99.	35 61 96	7979 7969 7961	919. 918. 916.	2	96 98 100	. 0 . 3 . 7	6
138 137 136	2 2	. 732 . 662 . 593	7776 7767 7758	89° 89°	7.6 6.2 4.9	10	00. 03. 05.	8 6	7834 7825 7817	903. 902. 900.	5 2 2 8 2	101. 103. 106.	5 9 4	7	7893 788 4 7875	90	8. 1	. 1	02. 04. 07.	7	7952 7942 7934	915. 914. 912.	1	103 105 108	. 1 . 5 . 0	
135	2	. 526	7750	893	3.6	10	08.	1	7808	899.	5	108.	9	2	7866	90.	5.5	1	09.	7	7925	911.	4	110	. 5	

1.09	Quality. Heat Contents. Specific Volume.	$3.55 \mid 8571 \mid 995.1 \mid 43.89$	5.32 8553 992.5 45.6 6.24 8543 991.1 46.5 7.18 8534 989.8 47.5	$9.13 \mid 8515 \mid 987.2 \mid 49.5$	2. 23 8487 983. 1 52. 6	4. 44 8468 980. 4 54. 8 5. 59 8459 979. 1 56. 0 6. 75 8449 977. 7 57. 1	9.18 8430 975.0 59.6	3.06 8403 971.0 63.5	5.81 8384 968.3 66.2 7.24 8375 966.9 67.7 8.71 8366 965.6 69.2	0.23 8356 964.2 70.7 1.76 8347 962.8 72.2 3.34 8337 961.5 73.8	6.64 8318 958.7 77.2	0. 12 8300 956. 0 80. 7 11. 92 8290 954. 6 82. 5 3. 77 8281 953. 3 84. 3	$egin{array}{c cccc} 5.64 & 8271 & 951.8 & 86.2 \ 7.60 & 8262 & 950.5 & 88.2 \ 9.63 & 8252 & 949.1 & 90.2 \ \hline \end{array}$	3.75 8233 946.3 94.4	$0.5 \mid 8205 \mid 942.1 \mid 101.3$	07.8 8177 938.0 108.0	3.0 8158 935.2 113.
	Specific Volume.	42.70 43.55 44.42	45.32 46.24 47.18	48.14 49.13 50.14	51.16 52.23 53.32	54.44 55.59 56.75	57.95 59.18 60.43	61.73 63.06 64.42	65.81 67.24 68.71	70.23 71.76 73.34	74.97 76.64 78.35	80.12 81.92 83.77	85.64 87.60 89.63	91.65 93.75 95.93	98.20 100.5 102.9	105.3 107.8 110.4	113.0
1 .50	Heat Con- tents.	990.3 988.7 987.4	986.1 984.8 983.5	982.1 980.8 979.5	978.1 976.8 975.5	974.2 972.8 971.5	970.1 968.8 967.5	966.1 964.8 963.5	962.1 960.7 959.4	958.1 956.7 955.3	954. 0 952. 6 951. 2	949. 9 948. 5 947. 2	945. 8 944. 4 943 0	941.7 940.3 938.9	937. 6 936. 1 934. 8	932.0	929.2
	Quality.	8516 8507 8498	8489 8479 8470	8461 8452 8442	8433 8423 8414	8405 8396 8387	8377 8368 8359	8349 8341 8332	8323 8313 8304	8295 8286 8276	8267 8258 8248	8239 8230 8221	8211 8202 8192	8183 8173 8164	8156 8146 8137	8128 8118 8109	8100
	Specific Volume.	42.37 43.22 44.08	44. 98 45. 89 46. 82	47.78 48.76 49.76	50.78 51.83 52.92	54.03 55.17 56.33	57.51 58.74 59.98	61.27 62.59 63.94	65.32 66.74 68.20	69.71 71.23 72.80	74.42 76.08 77.77	79.53 81.32 83.16	85.01 86.96 88.97	90.99 93.07 95.23	97.49 99.80 102.2	104.6 107.0 109.6	112.2
1 .51	Heat Con- tents.	983.6 982.3 981.1	979.8 978.4 977.1	975 ·8 974.5 973.2	971.8 970.5 969.2	967.9 966.6 965.2	$963.9 \\ 962.6 \\ 961.2$	959.9 958.6 957.3	955.9 954.6 953.3	951.9 950.5 949.2	947.9 946.5 945.1	943.8 942.4 941.1	939.7 938.4 937.0	935.7 934.3 932.9	931.6 930.2 928.8	926.0	923.3
	Quality.	8451 8442 8433	8424 8415 8406	8397 8388 8379	8369 8360 8351	8342 8333 8324	8315 8306 8296	8287 8280 8270	8261 8252 8243	8234 8224 8215	8206 8197 8188	8179 8169 8160	8151 8142 8133	8124 8114 8105	8097 8087 8078	8069 8060 8050	8041
	Specific Volume.	42.05 42.88 43.74	44.63 45.54 46.46	47.42 48.39 49.39	50.39 51.44 52.52	53.62 54.76 55.90	57.08 58.30 59.53	60.81 62.13 63.46	64.83 66.24 67.70	69.19 70.70 72.26	73.86 75.51 77.20	78 .94 80 .72 82 .54	84.39 86.32 88.32	90.32 92.39 94.54	96.77 99.07 101.4	103.8 106.3 108.8	111.4
OG. 1	Heat Con- tents.	977.2 976.0 974.7	973.4 972.1 970.8	969.5 968.2 966.9	965.5 964.2 962.9	961.6 960.3 959.0	957.7 956.3 955.0	953.7 952.4 951.1	949.7 948.4 947.1	945.8 944.4 943.0	941.7 940.4 939.0	937.7 936.3 935.0	933.7 932.3 930.9	929.6 928.2 926.9	925.6 924.2 922.8	921.5 920.1 918.7	917.3
	Quality.	8386 8378 8369	8360 8351 8342	8333 8324 8315	8306 8297 8288	8279 8270 8261	8252 8243 8234	8225 8218 8209	8199 8190 8182	8173 8163 8154	8146 8136 8127	8118 8109 8100	8091 8082 8073	8964 8055 8046	8038 8028 8019	8010 8001 7992	7983
un e	Pressure, Pound per Square Inch.	7.50 7.34 7.17	7. 01 6. 86 6. 70	6.55 6.41 6.26	6.12 5.98 5.84	5.71 5.58 5.45	5.32 5.20 5.08	4.960 4.844 4.729	4.617 4.508 4.400	4. 295 4. 191 4. 090	3.991 3.894 3.799	3.615	3. 439 3. 353 3. 270	3.108	2.953 2.877 2.804	2.732 2.662 2.593	2.526
ahı	Temperature, Degrees Fah	180 179 178	177 176 175	173	171 170 169	168 167 166	165 164 163	161	159 158 157	156 155 154	153 152 151	150 149 148	147 146 145	144 143 142	141 140 139	138 137 136	135

	Temperature,	ressure, Poun	per Square Inch.	Quality.	Heat Con-	و ا	Quality,	Heat Con-		Specific Volume.	Quality.	Heat Con-		Specific Volume.	Quality.	Heat Con.	tents.	Specific	oimie.
		1			-	_		-	-1	-Sr	<u>~</u>	He	- -	S	-\	- -H	<u>.</u>	Spe	
	132 131 130	$\frac{2}{2}$.	$\begin{array}{c} 272 \\ 212 \end{array}$	7724 7715 7707	888.	5 116. 2 119. 9 121.	0 7773	894.	. 1	117.0 119.9 122.8	7831	901. 900. 898.	0 1	17.9 20.8 23.9	3 7889	9 1905	. 9	118. 121. 124.	6
	129 128 127	$\frac{2}{2}$.	096 040	7698 7690 7681	884.	2 128.	0 7747	890.	1	125. 9 128. 9 132. 1	7813 7804 7795	897. 895. 894.	9 1	26.8 29.9 33.1	7862	901	.8	127. 130. 134.	8
	126 125 124	1.9	932	7672 7664 7655	880.	2 137.	8 7721	887. 886. 884.	4 1 6	135.4 138.8 142.3	7778	893. 891. 890.	9 ī	36. 4 39. 8 43. 3	7834	897	. 8	137. 140. 144.	4 9
	123 122 121	1.8 1.7 1.7	329 779 730	7646 7638 7630	877. 876. 874.	1 148.	7 7703 7694 7687	883. 881. 880.	9	145.8 149.5 153.3	7760 7751 7743	889. 887. 886.	7 î.	46.9 50.6 54.5	7807	895 893	0 5	148. 151. 155.	0 7
	120 119 118	1.6	336	7622 7613 7604	873. 872. 870.	1 160.	7678 7669 7660	879. 877. 876.	9	157.2 161.3 165.5	7734 7725 7716	885. 883. 882.	- 1	58. 4 62. 5 66. 7		1002	8	159.4 163.6 167.9	5 6
	117 116 115	1.5 1.5 1.4	647 604 62	7596 7587 7579	869. 867. 866.	9 172.8	7651 7642 7634	875. 873. 872.	7	169.7 174.1 178.6	7707 7698 7690	880. 9 879. 4 878. 3	1;	70.9 75.4 79.9	7763 7754 7745	886. 885. 883.	6	172.2 176.6 181.2	2
- 1	114 113 112	1.3	81	7 570 7561 7552	865. 863. 862.	186.7	7625 7616 7608	871.0 869.6 868.2	31	183.3 188.1 193.1	7680 7671 7663	876.7 875.3 873.9	18	34.6 39.5 34.5	7736 7727 7718	882. 881. 879.	4	186. 0 190. 8 195. 9	
-13	111 110 109	1.2	66	7543 7535 7526	861.2 859.8 858.4	202.0	7598 7590 7581	866. 8 865. 4 864. 1	1 :	198. 2 203. 5 208. 9	7653 7645 7635	872.5 871.1 869.7	19	9.7 5.0 0.4	7708 7700 7690	878. 876. 875.	2	193. 9 201. 1 206. 4 211. 9	
- 1 :	108 107 106	1.1	60	7518 7508 7500	857. 6 855. 6 854. 2	218.6	7572 7563 7554	862.7 861.3 859.9	1 2	214.5 220.2 226.2	7627 7617 7609	868.3 866.9 865.5	21 22	6.1 1.8 7.8	7681 7672 7663	874. 872. 871.	0 9	211. 9 217. 6 223. 4 229. 4	
12	105 104 103	1.0	62	7491 7482 7474	852.8 851.4 850.1	237.0	7546 7536 7528	858.5 857.1 855.7	1 2	232. 4 238. 8 245. 3	7591	864. 1 862. 7 861. 3	23 24	4.1 0.5 7.1	7654 7645 7636	869.8 868.3 866.9	8 2	235.7 242.2 248.8	
1	02 1 01 0 00 0). 9'.	711	7465 7457 7448	848.7 847.3 845.9	250.2 257.1 264.2	7519 7511 7502	854.3 852.9 851.5	222	252.0 259.0 266.1	7565	859. 9 858. 5 857. 1	25 26	3.8 0.8 8.0	7627 7618 7609	865. 8 864. 1 862. 7	2	255.6 262.7 269.9	
	99 0 98 0 97 0). 88	371 '	7439 7431 7422	844.5 843.1 841.8	271.7 279.3 287.2	7493 7484 7475	850.1 848.7 847.4	2	73.6 81.3 89.2	7546 7537	856. 7 854. 2 852. 9	27	5.6 3.3 1.3	7600 7591 7581	861.3 859.8 858.5	2 2	77. 5 85. 3 93. 3	
	96 0 95 0 94 0	1.80	9 7	7414 7405 7396	840.4 839.0 837.6	295.4 303.8 312.4	7458	846.0 844.6 843.1	3	97.5 05.9 14.7	7511 8	351.5 350.1 348.7	1	9 6	7573 7564	857. 1 855. 7 854. 2	3 3	01.7 10.3 19.1	
1	93 0 92 0 91 0	.73	1 7 7 7 5 7	379	836. 2 834. 8 833. 4	321.4 330.6 340.3	7431	841.7 840.3 838.9	3.	$23.6 \\ 33.0 \\ 42.7$	7493 7484 7475	347. 3 345. 8 344. 4	325 335 345	5.9	7546 7536	852.8 851.3 849.9	3.	28. 2 37. 7 47. 5	
1	90 0 89 0 88 0	. 67	1 7	352	832.0 830.6 829.1	350.1 360.3 370.7	7413 7404 7395	837.5 836.1 834.6	3; 3; 3;	62.8	7456 8	343.0 341.6 340.1	355 365 375	5.1	7518	848.4 847.0 845.5	3.	57.5 67.9 78.6	
L	87 0.	. 63	0 7	335	827.7	381.7	7387	333.2	35	84.4	7/20 0	20 7	200			- 10. U	٥	10.0	

Fahr	Pound tare		1.56			1.57			1.00			1.00	
Temperature, Degrees Fahr	Pressure, Pour per Square Inch.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con-	Specific Volume	Quality.	Heat Con- tents.	Specific Volume.
132 131 130	2.332 2.272 2.212	7955 7946 7937	913.2 911.8 910.4	119.6 122.5 125.5	8004	919. 1 917. 7 916. 3	120.5 123.4 126.4	$8071 \\ 8062 \\ 8052$	$925.0 \\ 923.6 \\ 922.2$	121.4 124.3 127.3	8129 8119 8110	930.9 929.5 928.1	122.3 125.2 128.2
128	2.153 2.096 2.040	7928 7919 7910	909.1 907.7 906.3	128.7 131.8 135.0	7986 7976 7967	915.0 913.6 912.2	129. 6 132. 7 136. 0	8043 8033 8024	920.8 919.4 918.0	130.5 133.7 137.0	8100 8091 8081	926.7 925.3 923.9	131.5 134.6 137.9
125	1.985 1.932 1.880	7901 7891 7882	904.9 903.6 902.1	138.4 141.9 145.4	7958 7948 7939	910.8 909.4 908.0	139.4 142.9 146.5	8015 8005 7996	916.6 915.3 913.8	140.4 143.9 147.5	8072 8062 8052	922.5 921.1 919.6	141.4 145.0 148.6
123 122 121	1.829 1.779 1.730	7873 7864 7856	900.8 899.3 898.0	149.0 152.8 156.7	7930 7920 7912	906.6 905.1 903.8	150.1 153.9 157.8	7986 7977 7968	912.5 911.0 909.6	151.2 155.0 159.0	8043 8033 8025	918.3 916.8 915.4	152.3 156.1 160.1
119	1.683 1.636 1.591	7846 7837 7828	896.6 895.2 893.8	160.7 164.8 169.1	7903 7893 7884	902.4 901.0 899.6	161.8 166.0 170.3	7959 7949 7940	908.2 906.8 905.4	163.0 167.2 171.5	8015 8005 7996	914.0 912.6 911.1	164.2 168.4 172.7
117 116 115	1.547 1.504 1.462	7819 7809 7801	892.4 890.9 889.6	173.4 177.9 182.5	7875 7865 7856	898. 2 896. 7 895. 3	174.7 179.2 183.8	7931 7921 7912	903.9 902.4 901.0	175.9 180.4 185.1	7986 7976 7967	909.7 908.2 906.8	177.1 181.7 186.4
113	1.421 1.381 1.342	7782	888. 2 886. 8 885. 4	187.3 192.2 197.3	7847 7837 7828	893.9 892.5 891.1	193.6	7902 7892 7883	899.6 898.2 896.8	194.9 200.1	7958 7948 7938	905.4 904.0 902.5	196.3 201.5
1110	1.304 01.266 1.230	7755	884.0 882.5 881.1	202.5 207.9 213.5	7819 7809 7800	889.7 888.2 886.8	204.0 209.4 215.0	7874 7864 7855	895.4 893.9 892.5	1	7929 7919 7909	901.1 899.6 898.2	$\begin{array}{c c} 212.3 \\ 218.0 \end{array}$
100 100 100	1. 19 7 1. 16 6 1. 12	7736 7726 7717	879.7 878.3 876.8	$\begin{bmatrix} 219.2 \\ 225.0 \\ 231.1 \end{bmatrix}$	7790 7781 7772	885.4 884.0 882.8	220.7 226.6 232.7	7845 7835 7826	891.0 889.6 888.1	228.2 1 234.3	7900 7890 7880	896.7 895.3 893.8	229.8 235.9
10	1.09 1.06 1.03	2 7699	874.	0 243.9	7763 7753 7744	881. 879. 878.	$\begin{bmatrix} 239.1 \\ 245.6 \\ 252.4 \end{bmatrix}$	7807	886. 885. 883.	240.8 247.3 8 254.1	7871 7861 7851	892.4 890.9 889.8	249.0 5 255.9
1 10	$ \begin{bmatrix} 1.00 \\ 1.97 \\ 0.94 \\ \hline $	1 7672	869.	257.4 7 264.5 3 271.8	7726	876. 875. 873.	259.3 266.4 273.7	7779	879.	4 275.6	7833 7823	888.0 886.4 885.0	0 277.5
9	9 0.91 8 0.88 7 0.86	7 7644	₹ \865 <i>.</i>	4 287.3	7707 7697 7688	872. 871. 869.	0 289.3	7760 7751 7741	876.	0 283.4 5 291.3 1 299.4	7804 7794	880.	1
9	6 0.83 5 0.80 4 0.78	9 7617	7 861.	2 312.4	Ll 7670	868. 866. 865.	8 314. (3 7723	8 1872.	7 308. 3 316. 8 325.	7776 7766	876.	4 328.0
9	0.76 02 0.73 01 0.71	7598 7 7589 5 7579	858. 9 856. 9 855.	9 340.	7641	863. 862. 860.	9 332.3 4 342.4 9 352.4	1 7694	₹ \867.	9 344.	3 7746	874. 873. 871.	4 347.1 9 357.2
8	0.69 0.67 0.65	756	0 853. 1 852. 1 851.	5 370.	5 7613	859. 858. 856.	4 362. 0 373. 5 383.	7678 7668 7658	5 863.	5 375.	6 7717	868.	9 378.1
	0.63	754	2 849.	5 392.	7594	855.	1 395. 6 406	2 7649 8 763	860. 7 859	5 397. 0 409.	9 7698 6 7688	866. 864.	0 400.6 5 412.4

	Specific	2.0 2.0 2.0	2.08 2.09 2.09	2.11 2.13 2.15	2.16 2.18 2.20	2 .225 2 .241 2 .261	2 .281 2 .300 2 .319	239 339 32 339 339 339 339	2 .400 2 .420 2 .441	2 .463 2 .486 2 .508	2 .530 2 .552 2 .574	2 .596 2 .620 2 .645	: .669 : 692 : .718	.742 .768 .792	.819 .844 .870	.897 .923 .952	020
63	1	937	3			AND THE PERSON NAMED IN COLUMN	reside and constitutions	Man of the same and	opening the state of the state	***************************************	11111	******	**************************************	\$2.8.8.2	2222	£	5
1.	Heat Con- tents.	1319 1318 1317	1316 1314 1313	$1312 \\ 1310 \\ 1309$	1308 1307 1306	1304 1303 1302	1301 1300 1299	1297 1296 1295	1294 1293 1291	290 289 288	287 285 284	283 282 281	280 278 277	276 275 274	272 271 270	269 268 266	265
	Quality.	191 190 188	187 185 183	182 180 179	177 175 174	172 171 169	66	63 61 60	57	52	19 1 17 1 16 1	13 1	8 1	$3 \mid 1$	0 1 9 1 7 1	6 1	1 1
	Volume.	85	35	35	0 8 6	5 4 1	0 1	9 1	1 1 1 1		14 14 14	14 14 14	14 13 13	13 13 13	13 12 12	12 12 12	12
62	Specific	1.97 1.98 2.00	$\begin{bmatrix} 2.01 \\ 2.03 \\ 2.05 \end{bmatrix}$	2.06 2.08 2.10	2.120 2.138 2.156	2.175 2.194 2.211	$\begin{array}{c} 2.230 \\ 2.250 \\ 2.270 \end{array}$	2.290 2.309 2.329	$\begin{array}{c} 2.350 \\ 2.370 \\ 2.390 \end{array}$	$\begin{array}{c} 2.411 \\ 2.432 \\ 2.454 \end{array}$	2 .476 2 .499 2 .520	2 .542 2 .564 2 .587	2.610 2.634 2.658	2.680 2.705 2.730	2.755 2.782 2.808	.833 .860 .887	.914
1.	Heat Con- tents.	1309 1307 1306	1305 1304 1303	1302 1300 1299	$\begin{array}{c} 1298 \\ 1297 \\ 1296 \end{array}$	$\begin{array}{c} 1295 \\ 1294 \\ 1293 \end{array}$	1291 1290 1289	1288 1287 1286	1284 1283 1282	1281 1280 1279	1277 1276 1275	1274 1273 1271	1269 3	266 2	$262 \mid 2$	258 2	256 2
	Quality.	172 170 169	167 166 164	163 161 160	158 157 155	154 152 151	149 148 146	145 143 142	140 139 137	136 134 133	131 130 128	127 125 123	120	116 .	11 1	08 1 07 1 05 1	04 1
	Specific Volume.	1 .920 1 .935 1 .952	1 .969 1 .984 2 .002	2 .019 2 .036 2 .053	$egin{array}{c} 2.071 \ 2.089 \ 2.106 \end{array}$	$egin{array}{c} 2.124 \ 2.141 \ 2.160 \end{array}$	2 .178 2 .197 2 .216	2 .235 2 .254 2 .273	.292 .312 .332	.352 .374 .395	.416 .437 .459	.482 .504 .526	.550 .572 .595	.620 .643 .669	717	794	849
1.01	tents.	298 297 296	294 293 292	90	87	84 83 82	81 80 79	78 2 76 2 75 2	3 2	$\begin{bmatrix} 1 & 2 \\ 9 & 2 \\ 8 & 2 \end{bmatrix}$	$6 \mid 2$	$\begin{bmatrix} 4 & 2 \\ 3 & 2 \\ 1 & 2 \end{bmatrix}$	$\begin{bmatrix} 2 \\ 2 \\ 3 \end{bmatrix}$	$\begin{bmatrix} 2 \\ 2 \end{bmatrix}$	12.	12.	2.
1	Heat Con-	0 12	$egin{array}{c c} 7 & 129 \\ 6 & 129 \\ 4 & 129 \\ \hline \end{array}$	129	128	128 128 128	128 128 1279	1278 1276 1275	1274 1273 1272	1271 1269 1268	1267 1266 1265	1264 1263 1261	1260 1259 1258	$\begin{array}{c} 1257 \\ 1256 \\ 1255 \end{array}$	$\begin{array}{c} 1254 \\ 1253 \\ 1251 \end{array}$	$\begin{array}{c} 1250 \\ 1249 \\ 1248 \end{array}$	1247
	Quality.	2 155 3 156 3 149	147 5 146 144	142	139 137 136	134 133 131	130 129 127	126 124 123	121 120 118	117 115 114	113 111 110	108 107 105	104 102 101	99 98 97	95 94 92	91 89 88	86
	Specific Volume.	1.872 1.888 1.903	1 .920 1 .935 1 .951	1.969 1.986 2.003	$\begin{array}{c} 2.020 \\ 2.036 \\ 2.054 \end{array}$	2.072 2.090 2.109	2.127 2.145 2.164	2 .183 2 .202 2 .220	2 .240 2 .260 2 .280	2.301 2.322 2.343	2.365 2.387 2.409	2.430 2.450 2.472	.494 .518 .540	.563 .586 .610	.623 .656 .680	.706 .730 .757	781
2.00	Heat Con- tents.	1289 1287 1286	1285 1284 1283	1281 1280 1279	1278 1277 1276	1275 1273 1272	1271 1270 1269	1268 1267 1266	1264	1259	1258 1257 1256	1253 1252	250 249	$\begin{bmatrix} 247 \\ 246 \end{bmatrix} \begin{bmatrix} 2 \\ 2 \end{bmatrix}$	$\begin{bmatrix} 243 & 2\\ 242 & 2 \end{bmatrix}$	$\begin{vmatrix} 240 & 2 \\ 239 & 2 \end{vmatrix}$	238 2
	Quality.	134 132 131	$\frac{129}{128}$ $\frac{127}{127}$	125 124 122	121 119 118	117 115 114	112 111 110	108 107 105	104 103 101	100 98 97	96 94 93	92 90 89	86 84	82	77 76	$\begin{array}{c c} 73 & 1 \\ 2 & 1 \end{array}$	0 1
Poun uare	Pressure, Poun per Square Inch.	308 .6 305 .2 301 .9	298 .7 295 .4 292 .2	289 .0 285 .9 282 .7	279 .6 276 .5 273 .5	270 .5 267 .5 264 .5	261 .6 258 .6 255 .7	50 .0 47 .2	41 .7 38 .9	33 .5 30 .8	28 .2 25 .6 23 .0	20 .4 17 .8 15 .3	7.9	0.6	5.9 3.6		5 7
ıre, Fah	Temperature, Degrees Fah	420 419 418	417 416 415		409	407 406	404 403	401 400	398 2 397 2	394 2	92 2 91 2	89 2 88 2	86 2 85 2	83 20 82 20	30 19 79 19	7 18 6 18	5 18 4 18

TEMPERATURE-ENTROPY TABLE.

e, ahr.	e.		1.64			1.65			1.66		
Temperature, Degrees Fahr.	Pressure, Pounds per Square Inch.	Quality	Heat Con- tents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.	Quality.
420	308 .6	212	1330	2.065	233	1341	2.117	255	1352	2.166	277
419	305 .2	210	1328	2.082	231	1339	2.133	254	1351	2.184	275
418	301 .9	209	1327	2.099	230	1338	2.151	252	1349	2.202	273
417	298 .7	$207 \\ 206 \\ 204$	1326	2.116	228	1337	2.170	250	1348	2 .220	272
416	295 .4		1325	2.133	226	1335	2.186	248	1347	2 .238	270
415	292 .2		1324	2.150	224	• 1334	2.204	247	1346	2 .256	268
414 413 412	289 .0 285 .9 282 .7	202 201 199	1322 1321 1320	2.169 2.186 2.204	$\begin{array}{c} 223 \\ 221 \\ 219 \end{array}$	1333 1332 1330	2.222 2.240 2.260	$245 \\ 243 \\ 241$	1345 1343 1342	2.274 2.293 2.311	266 264 263
411	279 .6	198	1319	2.222	$218 \\ 216 \\ 214$	1329	2.278	240	1341	2.330	261
410	276 .5	196	1318	2.240		1328	2.296	238	1339	2.349	259
409	273 .5	194	1316	2.260		1326	2.314	236	1338	2.369	257
408	270.5	193	1315	2.279	213	1325	2.333	234	1336	2.389	256
407	267.5	191	1314	2.297	211	1324	2.352	233	1335	2.408	254
406	264.5	189	1313	2.316	209	1323	2.372	231	1334	2.428	252
405 404 403		188 186 185	1312 1310 1309	2.335 2.354 2.374	$\frac{208}{206}$ $\frac{204}{204}$	1322 1320 1319	2.392 2.412 2.433	229 227 226	1333 1331 1330	2.449 2.469 2.490	250 248 246
402 401 400	250.0	183 181 180	1308 1307 1306	2.394 2.415 2.437	203 201 199	1318 1317 1315	2.454 2.475 2.496	$224 \\ 222 \\ 221$	1329 1328 1327	2.511 2.533 2.554	245 243 241
399	241.7	178	1304	2 .459	198	1314	2.518	219	1326	2.577	239
398		176	1303	2 .480	196	1313	2.539	217	1324	2.600	237
397		175	1302	2 .502	194	1312	2.560	215	1323	2.620	236
396	233.5	173	1301	2.523	193	1311	2.582	213	1321	2.644	234
395		172	1300	2.546	191	1309	2.605	212	1320	2.668	232
394		170	1298	2.569	189	1308	2.629	210	1319	2.690	230
393	225.6	168	1297	2.591	188	1307	2.650	208	1318	2.715	228
392		167	1296	2.614	186	1306	2.675	207	1317	2.740	227
391		165	1295	2.638	184	1304	2.700	205	1315	2.764	225
390	217.8	163	1293	2.660	183	1303	2.724	203	1314	2.788	223
389		162	1292	2.685	181	1302	2.748	201	1312	2.815	221
388		160	1291	2.710	179	1300	2.772	200	1311	2.840	220
387	210.3	159	1290	2.734	177	1299	2.798	198	1310	2.866	218
386		157	1289	2.759	176	1298	2.822	196	1309	2.892	216
385		155	1287	2.784	174	1297	2.850	194	1307	2.919	214
384	203.0	154	1286	2.809	173	1296	2.876	193	1306	2.945	212
383		152	1285	2.835	171	1295	2.902	191	1305	2.973	210
382		150	1283	2.861	169	1293	2.930	189	1304	3.000	209
381		149	1282	2.889	167	1292	2.958	187	1302	3.029	207
380		147	1281	2.914	166	1291	2.984	186	1301	3.056	205

ture, es Fahr	, Pound Juare		1.60	- 1		1.61	l di		1.62			1.63	
Temperature, Degrees Fahr	Pressure, Pour per Square Inch.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con-	Specific Volume.	Quality.	Heat Con-	Specific Volume.
372 371 1 370	77.9 75.7 73.6	66 65 63	1235 1234 1232	2.860 2.888 2.914	82 81 79	1243 1242 1241	2.927 2.954 2.980	99 98 96	1253 1252 1250	2.996 3.024 3.052	116 115 113	1262 1261 1259	3.060 3.087 3.017
369 1 368 1 367 1	71 .5 69 .4 67 .3	62 61 59	1231 1230 1229	2.941 2.970 2.998	78 76 75	1240 1239 1238	3 .010 3 .039 3 .069	94 93 91	1249 1248 1246	3.080 3.110 3.140	111 100 108	1258 1257 1256	3.147 3.177 3.206
366 1 365 1 364 1	$\begin{array}{c} 65.3 \\ 63.2 \\ 61.2 \end{array}$	58 56 55	1228 1226 1226	3 .027 3 .055 3 .084	$73 \\ 72 \\ 70$	1236 1235 1234	3.098 3.127 3.155	90 88 87	1245 1244 1243	3 .170 3 .200 3 .229	107 105 104	1255 1253 1252	3.237 3.267 3.300
363 362 361 1	.59 .2 .57 .2 .55 .3	54 52 51	1225 1223 1222	3.114 3.142 3.175	69 67 66	1233 1232 1231	3 .185 3 .215 3 .246	85 84 82	1242 1241 1239	3 .260 3 .291 3 .322	102 100 99	1251 1250 1249	3.332 3.364 3.397
360 1 359 1 358 1	51.4	49 48 46	1221 1220 1218	3 .206 3 .238 3 .269	65 63 62	1230 1228 1227	3 .277 3 .310 3 .340	81 79 78	1238 1237 1236	3 .354 3 .388 3 .422	97 96 94	1247 1246 1245	3.430 3.463 3.498
357 1 356 1 355 1	47.6 45.8 43.9	45 44 42	1217 1216 1215	3 .300 3 .333 3 .366	60 59 57	1226 1225 1224	3 .374 3 .406 3 .440	76 75 73	1235 1234 1233	3 .457 3 .490 3 .525	93 91 89	1244 1243 1241	3.532 3.569 3.605
354 14 353 14 352 13	42 .1 40 .3 38 .5	41 39 38	1214 1213 1212	3 .399 3 .433 3 .467	56 54 53	$\begin{array}{c} 1223 \\ 1221 \\ 1220 \end{array}$	3 .473 3 .509 3 .543	72 70 69	1232 1230 1229	3.561 3.597 3.633	88 86 85	1240 1239 1238	3.641 3.680 3.716
351 1: 350 1: 349 1:	36 .7 35 .0 33 .2	37 35 34	1211 1209 1208	3 .500 3 .536 3 .571	51 50 49	1219 1218 1217	3 .579 3 .615 3 .651	$\frac{67}{66}$	1228 1227 1226	3 .670 3 .707 3 .745	83 82 80	1237 1236 1234	3.754 3.790 3.829
348 13 347 13 346 13	29 .8	32 31 30	1207 1206 1205	3.608 3.644 3.680	47 46 44	1216 1215 1213	3 .690 3 .727 3 .761	63 61 59	1225 1223 1222	3 .782 3 .820 3 .860	78 77 75	1233 1232 1231	3.867 3.906 3.945
345 13 344 13 343 13	24.8	28 27 25	1204 1203 1201	3 .719 3 .758 3 .795	43 41 40	$1212 \\ 1211 \\ 1210$	3 .800 3 .840 3 .880	58 56 55	1221 1219 1218	3 .898 3 .939 3 .979	74 72 71	1230 1229 1228	3.985 4.024 4.063
342 12 341 1 340 1	21 .5 19 .9 18 .4	24 23 21	1200 1199 1198	3 .833 3 .873 3 .913	38 37 36	1209 1208 1207	3 .920 3 .960 4 .000	53 52 50	1217 1216 1215	4 .019 4 .059 4 .099	69 67 66	1226 1225 1224	4.105 4.145 4.188
339 11 338 11 337 11	16 .8 15 .2 13 .7	20 18 17	1197 1196 1195	3 .951 3 .996 4 .040	34 33 31	1205	4 .040 4 .080 4 .120	49 47 46	1213	4 .140 4 .181 4 .223	64 63 61	1222 1221 1220	4.230 4.275 4.320
336 11 335 11 334 10	12 .2 10 .7 09 .2	16 14 13	1194 1192 1191	4.080 4.122 4.168	30 28 27	1201	4 .165 4 .209 4 .250	44 43 41	1209	4. 269 4.310 4.355	60 58 56	1219 1218 1216	4.365 4.410 4.458
333 10 332 10 331 10	06.3	11 10 9	1190 1189 1188	4 .210 4 .255 4 .300	25 24 22	1198 1197 1196	4 .295 4 .343 4 .390	40 38 37	1206	4 .400 4 .447 4 .495	55 53 52	1215 1214 1213	4.503 4.551 4.600
330 10 329 10 328 10	02.0	7 6 4	1186	4.345 4.390 4.440	21 20 18	1195 1194 1193	4 .435 4 .485 4 .533	35 34 32	1202	4 .542 4 .590 4 .635	50 49 47	1212 1211 1209	4.646 4.695 4.747
207 (00 0	2	1100	4 400	177	1100	1 500	21	1000	4 600	-10	1000	4 700

			7	!)	; }	<u>;</u>)	7	3	;) [) [3	5	
c ime.	Specific Volume.	3.360 3.390 3.421	3. 453 1. 487 3. 519	3.550 3.584 3.618	3.650 3.685 3.720	3. 755 3. 790 3. 828	3.865 3.903 3.939	3.978 4.019 4.058	4. 097 4. 137 4. 179	4. 222 4. 266 4. 309	4.351 4.397 4.440	4. 488 4. 531 4. 580	4. 629 4. 680 4. 729	4. 780 4. 830 4. 880	4 000	4.930 4.983 5.035	4.983
1.67	Heat Con- tents.	1301 1300 1298	1297 1295 1294	$\begin{array}{c} 1293 \\ 1292 \\ 1290 \end{array}$	$\begin{array}{c} 1289 \\ 1288 \\ 1287 \end{array}$	1285 1284 1283	$\begin{array}{c} 1281 \\ 1280 \\ 1279 \end{array}$	$\begin{array}{c} 1277 \\ 1276 \\ 1275 \end{array}$	1274 1272 1271	1270 1268 1267	1266 1265 1263	1262 1261 1260	1258 1257 1255	1254 1253 1252	1250	1249	1249
y.	Quality.	191 189 187	185 183 181	180 178 176	174 172 171	169 167 165	163 162 160	158 156 15 4	153 151 149	147 145 144	142 140 138	136 135 133	131 129 127	126 124 122	100	120 118 116	118
e ıme.	Specific	3. 287 3. 315 3. 345	3.377 3.409 3.440	3.470 3.503 3.538	3.570 3.604 3.638	3.673 3.707 3.740	3.779 3.813 3.850	3.886 3.931 3.970	4.010 4.050 4.090	4. 130 4. 172 4. 215	4. 258 4. 300 4. 345	4.392 4.440 4.486	4.533 4.580 4.630	4.677 4.725 4.773	4 000	4.820 4.870 4.920	4.870
r. 66	Heat Con-	1291 1290 1288	$\begin{array}{c} 1287 \\ 1286 \\ 1285 \end{array}$	1283 1282 1281	$\begin{array}{c} 1280 \\ 1278 \\ 1277 \end{array}$	$\begin{array}{c} 1276 \\ 1275 \\ 1273 \end{array}$	1272 1271 1269	1268 1267 1266	1263	1259	1257 1256 1254	1252	1248	1245 1244 1243	1241	1240	1240 1239 1237 1236
у.	Quality	172 170 168	166 165 163	161 159 158	156 154 152	151 149 147	145 144 142	140 138 137	135 133 131	130 128 126	124 123 121	119 117 116	114 112 110	109 107 105	103	102 100	102
ine.	Specific Volume.	3. 215 3. 243 3. 272	3. 303 3. 334 3. 365	3. 395 3. 429 3. 461	3. 495 3. 527 3. 560	3.594 3.628 3.662	3. 699 3. 735 3. 771	3.806 3.843 3.882	3.920 3.960 3.999	4. 038 4. 079 4. 120	4. 161 4. 204 4. 248	4. 292 4. 337 4. 382	4. 429 4. 475 4. 520	4. 568 4. 618 4. 668	4.717	4.765 4.815	4. 765 4. 815 4. 865 4. 917 4. 969
s	Heat Con- tents.	1281 1280 1279	1277 1276 1275	1274 1273 1271	1270 1269 1268	$\begin{array}{c} 1266 \\ 1265 \\ 1264 \end{array}$	$\begin{array}{c} 1263 \\ 1261 \\ 1260 \end{array}$	$\begin{array}{c} 1259 \\ 1258 \\ 1257 \end{array}$	$\begin{array}{c} 1255 \\ 1254 \\ 1253 \end{array}$	$\begin{array}{c} 1252 \\ 1250 \\ 1249 \end{array}$	$\begin{array}{c} 1248 \\ 1246 \\ 1245 \end{array}$	1244 1243 1242	1240 1239 1238	$\begin{array}{c} 1237 \\ 1235 \\ 1234 \end{array}$	1233	1231 1230	1231 1230 1229 1228 1226
y.	Quality	152 151 149	147 146 144	142 141 139	137 135 134	132 130 129	$127 \\ 125 \\ 124$	122 120 119	117 115 114	112 100 109	107 105 104	102 100 99	97 95 93	92 90 88	87	85 83	85 83 82 80 78
ic ume.	Specific Volume.	3.142 3.171 3.200	3. 230 3. 260 3. 290	3. 320 3. 350 3. 383	3. 414 3. 447 3. 480	3.512 3.545 3.580	3.615 3.650 3.685	3.720 3.757 3.795	3.832 3.870 3.910	3.949 3.990 4.030	4.070 4.110 4.152	4. 198 4. 240 4. 284	4. 330 4. 375 4. 420	4.465 4.510 4.560	4.607	4.655 4.705	4. 755 4. 755 4. 805 4. 855
leat Con-	Heat (1271 1270 1269	1267 1266 1265	1264 1263 1261	1260 1259 1258	1257 1255 1254	1253 1252 1251	1249 1248 1247	1246 1244 1243	$1242 \\ 1241 \\ 1240$	1238 1237 1236	$\begin{array}{c} 1235 \\ 1234 \\ 1232 \end{array}$	1231 1230 1229	$\begin{array}{c} 1228 \\ 1226 \\ 1225 \end{array}$	1224	$\frac{1223}{1221}$	1223 1221 1220 1219 1218
y.	Quality	134 133 131	129 128 126	124 123 121	120 118 116	115 113 111	110 108 107	105 103 102	100 98 97	95 93 92	90 89 87	85 84 82	80 79 77	76 74 72	71	69 67	
Pressure, Poun per Square Inch.	Pressu per Incl	177.9 175.7 173.6	171.5 169.4 167.3	165.3 163.2 161.2	159. 2 157. 2 155. 3	153.3 151.4 149.5	147.6 145.8 143.9	142. 1 140. 3 138. 5	136. 7 135. 0 133. 2	131.5 129.8 128.1	126. 4 124. 8 123. 2	121.5 119.9 118.4	116.8 115.2 113.7	112. 2 110. 7 109. 2	107.7	106.3 104.8	106.3

ture, ss Fahr Pound uare		1.60		1.61			1.62			1.63	
Temperature, Degrees Fah Pressure, Poun per Square Inch.	Quality.	Heat Contents. Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.
324 95.1 323 93.8 322 92.5	9991 9982 9973	1180. 0 4. 61 1178. 9 4. 67 1177. 8 4. 72	0 11	1188 1187 1186	4.737 4.790 4.845	26 25 23	1196 1195 1194	4.845 4.900 4.955	41 29 38	1205 1203 1202	4.955 5.010 5.066
321 91.2 320 90.0 319 88.7	9964 9956 9946	1176.6 4.78 1175.6 4.84 1174.4 4.90	6 7	1185 1184 1182	4.900 4.957 5.012	22 20 19	1193 1192 1191	5.010 5.064 5.122	36 35 33	1201 1200 1199	5. 123 5. 179 5. 236
318 87.4 317 86.2 316 85.0	9937 9927 9917	$ \begin{vmatrix} 1173.3 & 4.96 \\ 1172.1 & 5.02 \\ 1170.9 & 5.08 \end{vmatrix} $	$\begin{bmatrix} 4\\2\\1\\1 \end{bmatrix}$	1181 1180 1179	5.068 5.125 5.182	17 16 14	1189 1188 1187	5.178 5.237 5.295	31 30 28	1197 1196 1195	5. 294 5. 351 5. 410
315 83.8 314 82.6 313 81.4	9909 9899 9890	1169. 8 5. 15 1168. 7 5. 21 1167. 6 5. 28	9 9986	1177.5 1176.4 1175.3	5. 199 5. 265 5. 330	13 11 10	1186 1184 1183	5.353 5.412 5.473	27 25 24	1194 1193 1192	5.470 5.530 5.590
312 80.2 311 79.1 310 77.9	9880 9871 9862	1166. 4 5. 35 1165. 3 5. 41 1164. 1 5. 48	9 9957	1174.1 1173.0 1171.8	5.466	8 7 5	1182 1181 1180	5.537 5.599 5.663	22 20 19	1190 1189 1188	5.655 5.718 5.780
309 76.8 308 75.7 307 74.6	9852 9843 9833	1163.0 5.55 1161.8 5.62 1160.6 5.70	8 9928	1170.6 1169.5 1168.3	5.605 5.677 5.751	4 2 1	1179 1177 1176	5.729 5.793 5.860	17 16 14	1186 1185 1184	5.850 5.910 5.980
306 73.5 305 72.4 304 71.4	9825 9814 9805	1159.5 5.77 1158.3 5.84 1157.1 5.92	5 9910 8 9899 4 9890	1167. 2 1165. 9 1164. 8	5.825 5.899 5.975	9995 9984 9974	1174.8 1173.6 1172.4	[5.950]	13 11 10	1183 1182 1181	6.04 6.11 6.18
303 70.3 302 69.3 301 68.2	9796 9787 9778	1156.0 6.00 1154.9 6.08 1153.7 6.16	0 9871	1163.7 1162.5 1161.3	6.053 6.133 6.213	9965 9956 9947	1171.3 1170.1 1168.9	[6.185]	8 6 5	1179 1178 1177	6. 25 6. 33 6. 40
300 67.2 299 66.2 298 65.2	9769 9760 9750	1152.5 6.24 1151.4 6.32 1150.2 6.40	3 9844	1160.1 1159.0 1157.8	6.294 6.378 6.462	9937 9928 9918	1167.7 1166.6 1165.4	6.432	3 2 0	1175 1174 1173	6. 48 6. 57 6. 65
297 64.3 296 63.3 295 62.3	9741 9731 9722	1149.0 6.49 1147.8 6.57 1146.7 6.66	2 9824 8 9814 7 9805	1156. 6 1155. 4 1154. 3	6.634	9908 9898 9889	1164. 2 1162. 9 1161. 8	6 691	$\begin{array}{c} 9991 \\ 9981 \\ 9972 \end{array}$	1171.7 1170.5 1169.3	6.747
294 61.4 293 60.5 292 59.5	9713 9704 9694	1145.5 6.75 1144.4 6.84 1143.2 6.94	6 9796 7 9787 9777	1153. 1 1151. 9 1150. 7	6.814 6.906 6.999	9879 9870 9859	1160. 6 1159. 4 1158. 2	6.872 6.964 7.058	$\begin{array}{c} 9962 \\ 9952 \\ 9942 \end{array}$	1168. 1 1166. 9 1165. 7	6.929 7.022 7.118
291 58.6 290 57.7 289 56.8	9685 9676 9667	$ \begin{vmatrix} 1142.0 & 7.03 \\ 1140.9 & 7.12 \\ 1139.7 & 7.22 \end{vmatrix} $	9 9758	1149.6 1148.4 1147.2	7.189	9850 9840 9831	1157. 1 1155. 9 1154. 7	7.249	$9933 \\ 9923 \\ 9913$	1164.5 1163.3 1162.1	7.310
288 56.0 287 55.1 286 54.2	9656 9647 9638	1138.5 7.32 1137.3 7.42 1136.2 7.52	6 9738 6 9729 9 9720	1146.0 1144.8 1143.6	7.488	9820 9811 9802	1153.5 1152.3 1151.1	7.449 7.551 7.655	9902 9893 9883	1160.9 1159.7 1158.5	7.512 7.614 7.719
285 53.4 284 52.6 283 51.7	9629 9619 9610	1135.0 7.63 1133.8 7.73 1132.6 7.84	7 9700 4 9691	1142.4 1141.2 1140.0	7.697 7.802 7.910	9792 9781 9772	1159.9 1148.6 1147.4	7.867	9874 9863 9853	1157.3 1156.1 115 4 .9	7.932
282 50.9 281 50.1 280 49.33	9601 9593 9584	1131. 4 7. 95 1130. 3 8. 06 1129. 1 8. 18	9682 9674 9664	1138.8 1137.6 1136.5	8. 022 8. 137 8. 251	9763 9754 9745	1146. 2 1145. 1 1143. 9	8.088 8.203 8.318	9844 9835 9826	1153.7 1152.5 1151.3	8.155 8.271 8.387

															5	7
Yolume.	420 478 533	590 650 710	770 835 900	965 03 10	. 17 . 24 . 31	. 39 . 46 . 53	. 60 . 67 . 75	5.84 5.92 5.99	7.07 7.15 7.24	7 .33 7 . 40 7 . 49	7.58 7.67 7.76	7.85 7.95 8.04	8.14 8.24 8.33	8.43 8.54 8.64	8.74 8.84 8.95	9.0 9.1 9.2
Specific	39 5. 37 5. 36 5.	34 5. 33 5. 32 5.	31 5. 29 5. 28 5.	25 6 24 6	223 6 221 6 220 6	218 6 216 6	214 213	210	206 205	202 201	198 197	1195 1193		1188 1187 1185	1184 1183 1182	1180 1179 1178
Heat Con-	12	1:	1 1	1	1	1	1	:		L	3	3	6	0	9 7 5	1
Quality.	104 102 100	98 97 95	93 91 89	· 88 86 84	82 80 79	77 75 73	71 70 68	66 64 62	61 59 57	55 54 52	50 48 46	44 43 41	37	$\begin{vmatrix} 32\\ 30 \end{vmatrix}$	3 29 3 27 7 25	3 23 9 21 0 20
Specific Volume.	5. 295 5. 350 5. 405	5. 465 5. 530 5. 590	5. 650 5. 715 5. 780	5.840 5.900 5.965	6.035 6.10 6.18	6. 25 6. 31 6. 39	6.46 6.54 6.61	6.69 6.76 6.84	6.92 7.00 7.08	7.16 7.24 7.33	7.41 7.50 7.59	7. 68 7. 77 7. 86	1	8.4	8.50 8.60 8.7	8.9
tents.	1230 1229 1227 5	1225 5	1221	1218 1217 1216	1213	1210 1209 1208		$\begin{array}{c} 1203 \\ 1202 \\ 1201 \end{array}$	1199 1198 1197	1196 1194 1193	1192 1191 1189	1188 1187 1185	1184 1183 1182	1180 1179 1178	1177 1175 1174	1172 1171 1170
Quality.	88 86 84	83 81 79	77 76 74	72 70 68	67 65 63	61 60 58	57 55 53	51 50 48	46 44 43	41 39 37	36 34 32	30 29 27	25 23 22	20 18 16	15 13 11	9 8 6
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0 21. 85 9214 217 16. 21 8994 1051. 3 21. 89 9064 1058. 0 22. 06 9144 1066. 0 21. 85 9214 217 16. 21 8994 1051. 3 21. 89 9064 1058. 0 22. 06 9144 1066. 0 21. 85 9214 216 15. 59 8975 1048. 7 22. 26 9045 1055. 4 22. 84 9115 1063. 5 22. 26 29195 215 15. 59 8976 1047. 4 23. 07 9036 1054. 1 23. 25 9105 1060. 9 23. 43 9175 213 14. 99 8956 1046. 2 23. 47 9026 1052. 9 23. 66 9096 1059. 6 23. 84 9165 212 14. 70 8947 1044. 9 23. 85 9017 1051. 6 24. 04 9086 1058. 3 24. 22 9156 211 14. 41 8938 1043. 6 24. 23 9007 1050. 3 24. 42 9076 1057. 0 24. 61 9146 210 14. 12 8928 1042. 3 24. 67 8997 1049. 0 24. 86 9067 1057. 0 24. 61 9146 206 13. 63 8890 1039. 7 25. 57 8978 1046. 4 25. 77 9047 1053. 0 25. 56 9126 206 13. 63 8890 1037. 1 26. 52 8059 1046. 4 25. 77 9047 1053. 0 25. 96 9116 207 13. 29 8900 1038. 4 26. 04 8068 1045. 0 26. 24 9037 1054. 3 25. 56 9126 206 13. 63 8890 1037. 1 26. 52 8059 1044. 7 26. 72 9027 1050. 4 26. 93 9096 205 12. 77 8881 1035. 8 27. 00 8949 1042. 4 27. 21 9018 1049. 1 27. 41 9086 205 12. 77 8881 1035. 8 27. 90 8930 1039. 8 28. 21 8998 1045. 2 28. 94 9057 27. 94 9058 27. 9	220 17. 19 9023 1055. 2 20. 78 9094 1062. 0 20. 94 9165 1068 8 21. 11 9235 219 16. 86 9013 1053. 9 21. 15 9084 1060. 7 21. 31 9154 1067 4 21. 48 9225 218 16. 53 9003 1052. 6 21. 52 9073 1059. 3 21. 69 9144 1066 0 21. 85 9214 217 16. 21 8994 1051. 3 21. 89 9064 1058 0 22. 06 9134 1064. 8 22. 23 9205 216 15. 59 8984 1050. 0 22. 27 9055 1056. 7 22. 45 9125 1063. 5 22. 62 9195 216 15. 59 8975 1048. 7 22. 66 9045 1055. 4 22. 84 9115 1062 23. 02 9185 214 15. 29 8966 1047. 4 23. 07 9036 1054. 1 23. 25 9105 1060. 9 23. 43 9175 213 14. 99 8956 1046. 2 23. 47 9026 1052. 9 23. 66 9096 1059. 6 23. 84 9165 212 14. 70 8947 1044. 9 23. 85 9017 1051. 6 24. 04 9086 1058. 3 24. 22 9156 211 14. 41 8938 1043. 6 24. 23 9007 1050. 3 24. 42 9076 1057. 0 24. 61 9146 210 14. 12 8928 1042. 3 24. 67 8997 1049. 0 24. 65 9067 1057. 0 24. 61 9146 220 13. 84 8919 1041. 0 25. 11 898. 1047. 7 25. 31 9057 1054. 3 25. 50 9126 208 13. 57 8909 1039. 7 25. 57 8978 1046. 4 25. 77 9047 1053. 0 25. 96 9116 207 13. 29 8900 1038. 4 26. 04 8968 1045. 0 26. 24 9037 1051. 7 26. 44 9106 206 13. 03 8890 1037. 1 26. 52. 8959 1043. 7 26. 72 9027 1050. 4 26. 93 9066 205 12. 77 8881 1035. 8 27. 90 8930 1041. 1 27. 70 9008 1047. 8 27. 99 9058 204 12. 51 8871 1034. 5 27. 49 8939 1041. 1 27. 70 9008 1047. 8 27. 99 9058 205 12. 25 8862 1033. 2 27. 99 8930 1041. 1 27. 70 9008 1044. 5 28. 94 9048 200 11. 52 8835 1029. 3 29. 58 8902 1035. 9 29. 80. 8970 1042. 5 30. 03. 9038 199 11. 28 8825 1028. 0 30. 13. 8893 1034. 6 30. 36. 8900 1041. 2 30. 59 9028 198 1. 05 88	220 17. 19 9023 1055. 2 20. 78 9094 1062. 0 20. 94 9165 1068 8 21. 11 9235 219 16. 86 9013 1053. 9 21. 15 9084 1060. 7 21. 31 9154 1067 4 21. 48 9225 216 15. 90 8984 1050. 0 22. 27 9055 1056. 7 22. 45 9125 1063. 5 22. 62 9195 216 15. 90 8984 1050. 0 22. 27 9055 1056. 7 22. 45 9125 1063. 5 22. 62 9195 215 15. 59 8975 1048. 7 22. 66 9045 1055. 4 22. 84 9115 1062. 2 23. 02 9185 214 15. 29 8966 1047. 4 23. 07 9036 1054. 1 23. 25 9105 1060. 9 23. 43 9175 213 14. 99 8956 1046. 2 23. 47 9026 1052. 9 23. 66 9096 1059. 9 23. 43 9175 212 14. 70 8947 1044. 9 23. 85 9017 1051. 6 24. 04 9086 1058. 8 24. 22 9156 211 14. 41 8938 1043. 6 24. 23 9007 1050. 3 24. 42 9076 1057. 0 24. 61 9146 210 14. 12 8928 1042. 3 24. 67 8997 1049. 0 24. 86 9067 1057. 0 24. 61 9146 210 14. 12 8928 1042. 3 24. 67 8997 1049. 0 24. 86 9067 1057. 0 24. 61 9146 210 14. 12 8928 1042. 3 24. 67 8997 1046. 4 25. 77 9047 1053. 0 25. 96 9116 200 13. 84 8919 1041. 0 25. 11 8988 1047. 7 25. 31 9057 1054. 3 25. 50 9126 206 13. 57 8900 1038. 4 26. 04. 8968 1045. 7 26. 79 9027 1050. 4 26. 93 9096 206 12. 77 8881 1035. 8 27. 00 8949 1042. 4 27. 21 9018 1049 1 27. 41 9086 204 12. 51 8871 1034. 5 27. 49 8939 1041. 1 27. 70 9008 1047. 8 27. 92 9076 203 12. 25 8862 1033. 2 27. 99. 8930 1038. 6 28. 72. 8989 1044. 2 28. 94. 9057 201 11. 76 8844 1030. 6 29. 04. 8912 1035. 9 29. 80. 8970 1043. 8 29. 8949 9057 201 11. 76 8844 1030. 6 29. 04. 8912 1035. 9 29. 80. 8970 1043. 8 29. 94. 9067 195 10. 88 8877 1028. 0. 30. 13. 8893 1041. 1 27. 70 9008 1047. 8 29. 94. 9057 196 10. 60.

		1.0∓					1.00					2.00				1.01	
	Quality.	Heat Con- tents.		Specific	volume.	Quality.	Heat Con-		Specific	voimie.	Quality.	Heat Contents.		Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.
	9385 9375 9365	1092.7 1091.4 1090.1	- 1	19.0	02	9457 9446 9436	1099 1098 1097	. 3	19.	17	9529 9518 9508	1106.5 1105.2 1103.9	1 1 1	8.99 9.31 9.65	9590	1113.3 1112.0 1110.7	19.46
	935 4 9345 9335	1088.8 1087.5 1086.2	3 2 2 2	19. 20. 20.	68 02 36	$\begin{array}{c} 9426 \\ 9416 \\ 9406 \end{array}$	1095 1094 1093	.7 .3 .1	19. 20. 20.	83 17 51	9497 9487 9477	1102.6 1101.2 1099.9	2	0.26	9559	1109.4 1108.0 1106.7	20.47
	9325 9316 9306	1084.9 1083.6 1082.3	3	20. 21. 21.	70 06 4 3	9396 9387 9377	1091 1090 1089	. 8 . 5 . 1	20. 21. 21.	86 22 60	9467 9458 9448	1098.6 1097.3 1095.9	222	1.02 1.38 1.76	9538 9529 9518	1105.4 1104.1 1102.7	21.17 21.54 21.92
	9296 9285 9275	1081.0 1079.6 1078.3	5 5	22.	19	9366 9355 9345	1087 1086 1085	. 4	22.	36	9437 9426 9415	1094.5 1093.1 1091.8	2	$2.53 \\ 2.92$	9507 9496 9486	1101.3 1099.9 1098.6	22.30 22.70 23.09
	9265 9255 9245	1077.0 1075.7 1074.4	7	22. 23. 23.	97 37 79	9335 9325 9315	1083 1082 1081	. 4	23.	55	9405 9395 9385	1090.5 1089.2 1087.8	2	4. 15	9475 9465 9454	1097.2 1095.9 1094.6	23.90
	$\begin{array}{c} 9235 \\ 9225 \\ 9215 \end{array}$	1073. 1 1071. 2 1070. 4	1 .	24. 24. 24.	20 59 98	9305 9295 9284	1079 1078 1077	.8 .4 .1	24. 24. 25.	39 78 17	9374 9364 9354	1086.5 1085.1 1083.8	222	4.57 4.96 5.36	9444 9434 9423	1093.3 1091.9 1090.6	24.75 25.15 25.55
	9205 9195 9185	1069. 1067. 1066.	174	25. 25. 26.	43 89 36	9274 9264 9254	1075 1074 1073	. 4	26.	09	9343 9333 9322	1082.5 1081.1 1079.7	2 2 2 2 2 2	5.82 6.28 6.76	9413 9402 9391	1089.2 1087.8 1086.4	26.48
	9175 9165 9154	1065. 1063. 1062.	71	27.	34	9243 9233 9223	1071 1070 1069	. 7). 4). 0	27. 27. 28.	05 54 04	9312 9302 9291	1078.4 1077.0 1075.7) 2	27.75	9381 9370 9360	1085.0 1083.7 1082.3	27. 45 27. 95 28. 45
	9144 9134 9125	1061. 1059. 1058.	7	28.	85	9213 9202 9193	1067 1066 1065	7.7 3.3 5.0	28. 29. 29.	55 07 60	9281 9270 9261	1074.3 1072.9 1071.6	3 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	28.76 29.29 29.82	9349 9338 9329	1079.6	28.97 29.50 30.04
	9115 9105 9095	1057. 1055. 1054.	0 7 3	29. 30. 31.	94 48 05	9183 9173 9163	1063 1062 1060	2.3	30.	.71	9251 9241 9230	1070.3 1068.9 1067.	9 3	30.94 31.51	9298	1075.	30.60 31.16 31.74
	9086 9074 9064	1053. 1051. 1050.	6	32.	. 21	9142	1059 1058 105	9.6 3.1 6.8	31 32 33	. 86 . 45 . 06	9220 9209 9198	1066. 1064. 1063.	2 7 3	$ \begin{array}{r} 32.10 \\ 32.69 \\ 33.31 \end{array} $	9288 9276 9265	1071. 1069.	32.33 32.93 33.55
3	9054 9044 9035	1047.	9 5 2	33 34 34	. 45 . 08 . 73	9121 9111 9101	105 105 105	4.1	134	. 33	9178	1062. 1060. 1059.	0 6 3	33.94 34.58 35.24	9255 9244 9234	1068. 1067. 1065.	34.19 134.83 835.50
3	9024 9014 9004	1043.	5	36	.06	9080		1.4 0.0 8.6	35 36 37	. 65 . 33 . 03	9157 9147 9137	1057. 1056. 1055.	5 1	36.60 37.30	9213 9203	1063.	4 36.18 0 36.86 6 37.57
3	8995 8984 8974	1039.	4	38	. 19	9050		5.9	9 38	. 47	9116	1053. 1052. 1051.	8 4 0	38. 02 38. 75 39. 50	9193 9182 9172	1058. 1057.	3 38.30 8 39.03 5 39.79
67	8964 8954 8944	1035.	7 4 0	39 40 41	. 69	9030 9020 9009	104	1.8	1 39 8 40 4 41). 77	7 9085	1049. 1048. 1046.	2	41.0	9150	1056. 1054. 1053.	$\begin{array}{c} 1 & 40.56 \\ 7 & 41.36 \\ 2 & 42.18 \end{array}$
1	8934	1032.	6	42	09	8999	103 103	9. (7.	$0 42 \\ 7 43$	$\frac{2.39}{3.23}$	9064 9054						$9 43.01 \\ 5 43.85$

137	1	141 140 139	143	147 146 145	149	153 152 151	155	158	162 161 160	165 164 163	167	170	173	177 176 175	180 179 178	Temperature, Degrees Fahi	re, Fahr
2.804 2.732 2.662	2.804	2.953 2.877 2.804	3.188 3.108 3.029	3.439 3.353 3.270	3.706 3.615 3.526	3.991 3.894 3.799	4. 295 4. 191 4. 090	4.617 4.508 4.400	4.960 4.844 4.729	5.32 5.20 5.08	5.71 5.58 5.45	6.12 5.98 5.84	6.55 6.41 6.26	7.01 6.86 6.70	7.34 \	Pressure, Poun per Square Inch.	oun
1	0400	8274 8264 8255	8302 8292 8283	8331 8322 8312	8360 8350 8341	8389 8379 8369	8417 8408 8398	8446 8436 8427	8473 8465 8456	8502 8493 8483	8531 8521 8512	8559 8550 8540	8588 8579 8569	8617 8607 8598	8636	Quality.	
945.4	1010.0	949.6 948.1 946.8	953.8 952.3 951.0	957.9 956.6 955.1	962.1 960.7 959.3	966.2 964.8 963.4	970.4 969.0 967.6	974.5 973.1 971.8	978.5 977.2 975.8	982.6 981.3 979.9	986.7 985.3 984.0	990.7 989.4 988.1	994. 8 993. 5 992. 1	998.9 997.5 996.1	1002.8 1001.5 1000.2	Heat Con- tents.	1.00
106.9 109.4	1	99.62 102.0 104.4	92.99 95.11 97.32	86.89 88.87 90.93	81.29 83.12 84.99	76.07 77.76 79.50	71.26 72.82 74.42	66.78 68.23 69.73	62.64 64.00 65.37	58.81 60.06 61.33	55.25 56.42 57.60	51.93 53.01 54.12	48.87 49.87 50.89	46.01 46.94 47.89	43.35 44.21 45.09	Specific Volume.	
8304 8294 8284	l	8333 8323 8314	8362 8352 8342	8391 8381 8371	8420 8410 8401	8450 8440 8430	8479 8469 8459	8508 8498 8489	8536 8527 8517	8565 8555 8545	8594 8584 8574	8623 8613 8603	8652 8643 8633	8681 8671 8662	8710 8700 8691	Quality.	
949.9	1	955.6 954.1 952.7	959.8 958.4 957.0	964.0 962.6 961.2	968.2 966.8 965.4	$972.4 \\ 971.0 \\ 969.5$	976.5 975.1 973.7	980.7 979.3 977.9	984.7 983.4 982.0	988.9 987.5 986.1	993.0 991.6 990.2	997.0 995.7 994.3	1001.2 999.8 998.5	1005.2 1003.8 1002.5	1009. 2 1007. 9 1006. 6	Heat Con- tents.	
107.6 110.1 112.7	I .	100.3 102.7 105.2	93.65 95.79 98.02	87.52 89.51 91.59	81.88 83.72 85.60	76.62 78.33 80.07	71.78 73.35 74.96	67. 27 68. 73 70. 23	63.10 64.47 65.85	59.24 60.50 61.78	55. 66 56. 84 58. 02	52.31 53.40 54.52	49.23 50.24 51.27	46.35 47.29 48.25	43.67 44.54 45.43	Specific Volume,	
8363 8352 8342	1	8392 8382 8372	8421 8411 8401	8451 8441 8431	8480 8470 8461	8510 8500 8490	8540 8530 8520	8569 8559 8550	8598 8589 8579	8627 8617 8607	8657 8647 8637	8676	8706	8735	8774 8765 8755	Quality.	
957.3 955.8	1	961.6 960.1 958.7	965.8 964.4 963.0	970.0 968.7 967.2	974.3 972.9 971.5	978.5 977.1 975.7	982.7 981.3 979.9	986.8 985.4 984.1	991.0 989.6 988.2	995. 1 993. 7 992. 4	999.3 997.9 996.5	1003.4 1002.0 1000.6	1007.5 1006.1 1004.8	1011.6 1010.2 1008.8	1015.6 1014.3 1012.9	Heat Con- tents.	1 . 1
108.4 110.9 113.5	1	101.0 103.4 105.9	94.32 96.47 98.72	88.14 90.15 92.24	82.47 84.31 86.22	77.17 78.89 80.65	72.30 73.88 75.50	67.76 69.23 70.74	63.56 64.93 66.33	59.67 60.94 62.23	56.07 57.25 58.45	52.70 53.79 54.92	49.59 50.61 51.65	46.69 47.64 48.60	43.99 44.87 45.76	Specific Volume.	
8421 8411 8401	1	8452 8441 8431	8481 8470 8461	8511 8501 8491	8541 8531 8521	8571 8561 8551	8601 8591 8581	8631 8621 8611	8660 8651 8641	8690 8680 8670	8720 8710 8700	8749 8740 8730	8780 8770 8760	8810 8799 8790	8839 8829 8820	Quality.	
963.3 961.8	1	967.6 966.1 964.7	971.9 970.4 969.0	976.1 974.7 973.3	980.4 978.9 977.6	984.6 983.2 981.8	988.8 987.4 986.0	993.0 991.6 990.3	997.2 995.8 994.4	1001.4 1000.0 998.6	1005.5 1004.1 1002.8	1009.7 1008.3 1006.9	1013.8 1012.5 1011.1	1018. 0 1016. 5 1015. 2	1022.0 1020.7 1019.3	Heat Con-	1 .
109.1 111.7 114.3	1	101.8 104.2 106.7	94.99 97.16 99.41	88.77 90.79 92.89	83.05 84.91 86.83	77.72 79.45 81.22	72.82 74.41 76.04	68.24 69.72 71.25	64.02 65.40 66.80	60.11 61.38 62.68	56.48 57.67 58.87	53.08 54.19 55.32	49.96 50.98 52.03	47.04 47.99 48.96	44.32 45.20 46.10	Specific Volume.	

	Specific	15. 16. 17.	18. 19. 50.	51 52 53	54 55 56	58 59 60	61 63 64	65 67 68	70 71 73	74 76 78	79 8 8	88	999		1	1	1
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	Heat Con-)47. 6)46. 2)44. 8	043.4 042.0 040.	039. 037. 036.	034. 033. 032.	030. 029. 027.	.026. .024. .023.	1022. 1020. 1019.	1017. 1016. 1014.	1013. 1012. 1010.	1009 1007 1006	1004 1003 1001	1000 998 997	996 994 993	991 990 988	l	1
	Quality.	087 1	056 1	$\begin{vmatrix} 0.024 & 1 \\ 0.014 & 1 \end{vmatrix}$	3992 1 3982 1	3961 1	3929 1 3919 1	8899 8888	8867 8857	8835 8824	8803 8793	8772 8761	8750 8740 8729	8719 8708 8698	8688 8677 8667	8656 8645 8635	8624
·	Volume	3.19	3.06 9.04 0.03	1.05 2.09 3.16	4. 24 5. 36 6. 52	7.70 8.91 0.14	1.40 2.71 4.03	5.40 6.81 8.24	39.71 71.22 72.77	74.37 75.99 77.66	79.38 81.14 82.98	84.81 86.7 88.6	90.6 92.7 94.8	96.9 99.2 01.5	.03.9 .06.3 .08.9	111.4 114.0 116.7	119.5 122.4
	Specific	4: 4: 4'	4 5	5	1	5	8 6	1	1 7	9 '	1	8	4	5 0 1	7	. 3	-1
	Heat Contents.	041.2 039.8 038.4	037.1 035.6 034.2	032.8 031.4 030.0	.028.6 .027.2 .025.8	1024.4 1022.9 1021.5	1020.1 1018.7 1017.3	1015.8 1014.5 1013.0	1011.6 1010.1 1008.8	1007.3 1005.9 1004.4	1003.0 1001. 1000.	998. 997. 995.	994. 992. 991.	1	984. 982.	978.	1
	Quality.	023 1	002 1992 1981 1	961 1 950 1	3940 1 3929 1 3919 1	898	3867 3856	8837	8805 8795	8774	8743	8722 8711 8701	8690 8680 8670	8638	8629 8618 8608	8597 8587 8576	8566
-	Volume.	5.86	8.69	51.72 52.78	53.85 54.97 56.12	57. 29 58. 50 59. 72	60. 97 62. 22 63. 58	64.94 66.34 67.76	69. 22 70. 72 72. 26	73.85 75.46 77.12	78. 83 80. 58 82. 37	84. 23 86. 11 88. 05	90.02 92.07 94.20	96.33 98.53 100.8	103.2 105.6 108.1	110.7 113.3 115.9	
	tents.	34.8 33.4 32.1	30.7 29.3 27.9	26.5 25.1 23.7)22.3)20.9)19.5	018.1 016.7 015.3	$013.9 \\ 012.4 \\ 011.0$	009.6 008.2 006.8	$005.4\\004.0\\002.6$	001.1 999.7 998.3	996.9 995.4 994.0	992. 6 991. 1 989. 7	988. 2 986. 8 985. 4				970. 9 969. 3
	Cuanty.	68 58 10 48	28 1	907 1 397 1 38 7 1	366 1	$egin{array}{c c} 846 & 1 \ 836 & 1 \ 825 & 1 \ \end{array}$	794	775	744 734	3724 3713 3703	3693 8682 8672	8662 8651 8641	8531 8621 8610	8600 8589 8579	8570 8559 8549	8539 8528 8518	8508
_		89	89	8 8	3 8	8 8 8	3 8	- 1	3 8 2 8 6 8	3 3)2	51	39 43 54	65 84 1	94	9 5 1	۱ ۵
	Specific Volume.	14.64 15.53 16.44	47, 38 48, 34 49, 31	50.32 51.35 52.40	53.47 54.58 55.72	56.88 58.08 59.30	60.54 61.85 63.13	64.46 65.8 67.2	68.7 70.2 71.7	73.3 74.9 76.5	78. 2 80. 0 81. 8	83. 6 85. 5 87. 4	89.3 91.4 93.8	95.0 97.8 100.	104. 107.	109. 112. 115.	
	tents.	28.4 27.0 25.7	24. 3 22. 9 21. 5	20. 2 18. 8 17. 4	16.0 14.6 13.2	11.8 10.4 09.0	$07.6 \\ 06.2 \\ 04.8$	03.4 02.0 00.6	999.2 997.8 996.4	995.0 993.6 992.1	990. 7 989. 3 987. 9	986. 5 985. 0 983. 6	982. 2 989. 8 979. 3	977.9 976.4 975.0	973.6 972.1 970.7	969.3 967.8 966.3	964.9
1.	Quality.	904 10 894 10 884 10	863 10	3833 10	2803 16	8773 10	8742 1	8713 1	8693 8682 8673	8662 8652 8642	8632 8622 8611	8601 8591 8581	8571 8561 8550	8540 8530 8520	8511 8500 8490	8480 8469 8459	1
re	per Square Inch.	34 8	. 01 . 86 . 70	. 41	.98	. 58	32 3.20 5.08	1.960 1.844 1.729	4.617 4.508 4.400	4. 295 4. 191 4. 090	3.991 3.894 3.799	3.706 3.615 3.526	3.439 3.353 3.270	3.188 3.108 3.029	2.953 2.877 2.804	2.732 2.662 2.593	1
Fahr	Degrees Fah	80 7 79 7 78 7	.77 7 .76 6 .75 6	74 6 73 6 172 6	171 6 170 5 169 5	168 5 167 5 166 5	165 164 163	162 161 160	158	155	153 152 151	149	146	143	141 140 139	137	l

ture,	es Fahr	Poun		£ .	ne.		1	e.	.,		<u>e</u>	
Tempera	Degrees Fal	Pressure Poun persquare Inch.	Quality.	Heat Con- tents.	Specific Volume	Quality	Mear Cap-			Mar C.		. Quality.
11	31	2.333 2.272 2.212	8187 8177 8168	936.9 935.4 934.0	126.1	8235	$942.8 \\ 941.3 \\ 939.9$		8303 8293 8283	948.7 947.3 945.8	$^{124.9}_{127.9}_{130.9}$	836 834
1	28	$egin{smallmatrix} 2.153 \ 2.096 \ 2.040 \end{smallmatrix}$	8158 8148 8139	931.2	132.4 135.6 138.9	8206	938, 5 937, 1 935, 7	133.3 136.5 139.9	1 1 44 1 1 1 1	942.9	$134.3 \\ 137.5 \\ 140.9$	833 831 831
1	.25	1,985 1,932 1,880	8129 8119 8109	926.9	142.4 146.0 149.6	8176	934 2 932 8 931 3	147 0 :	8243 8233 8223	-938.6	144.4 148.0 151.7	22.25
	23 122 121	1.829 1.779 1.730	8100 8090 8081	924. 1 922. 6 921. 2	153.3 157.2 161.2	8146 8138	929 9 928 4 927 0	158 3 162 3	8213 8203 8194		155.5 159.4 163.5	828 828 828
1 1	119	1.683 1.636 1.591	8071 8062 8052	918.4	165.3 169.5 173.9	8128 8118 8108	925 6 924 2 922 7	166.5 170.7 175.1	8184 8174 8164	929 9	167.6 171.9 176.3	828
	116	1.547 1.504 1.462	8042 8032 8023	914.0	178. 4 183. 0 187. 7	8098 8088 8079	921 2 919 7 918 3	179 6 184 2 189 0	8154 8144 8134		180.9 -185.5 -190.3	82.83
1:	113	1.421 1.381 1.342	8013 8003 7994	909.7	192 6 197 7 202 9	8068 8058 8049	915.4	194 0 199 0 204 3	\$124 \$114 \$104	922.6 921.1 919.6	195 3 200 4 205 7	813
	110	1.304 1.266 1.230	7984 7974 7964	906.8 905.3 903.9	208 3 213 8 219 5	8039 8029 8019	911 0	209 7 215 3 221 0	8094 8084 8074	918 2 916 7 915 2		81.81
	107	1. 195 1. 160 1. 127		901.0	$\begin{array}{c} 225.4 \\ 231.3 \\ 237.6 \end{array}$	8009 7999 7989	min 6	226 9 232 9 239 2	8064 8053 8044	913 7 912 3 910 8		81 80 80
	104	1.094 1.062 1.031	7915	896.5	$\begin{array}{c} 244 & 1 \\ 250 & 7 \\ 257 & 6 \end{array}$	7979 7969 7969	903 6 902 1 900 7		8034 8023 8013	907 N	247 4 254 2 261 1	80 80 80
	101	1.000 0.971 0.942	7887	892.	264 7 271 9 279 4	7950 7941 7930	899 2 897 7 896 2		8003 7994 7984	3464 3	268 3 275 6 283 2	80 80 80
	98	0.914 3 0.887 7 0.860	7857	887.7	2 287 3 7 295 3 3 303 6	7920 7910 7901	893.3	289 3 297 4 305 7	7974 7964 7954	SUN 5	291 2 299 4 307 7	80 80 80
	98	5 0, 834 5 0, 809 4 0, 784	7829	883.4	312 3 321 1 330 3	7891 7881 7871	HSH H	314 4 323 3 332 5	7944 7934 7924	896 (894 / 893 (
	92	0.761 20.737 10.71	7799	878.9	339 7 349 5 359 6		NN4 4	342 0 351 8 362 0	7914 7904 7894	HM9 1	344 3 354 2 364 5	79
	89	0, 693 0, 67 3 0, 650	7769	874.	370 0 4 380 7 391 7	7831 7821 7811	3879 5	372 5 383 2 394 3	7844 7873 7863	885.4	374 9 385 8 396 9	79

17770	e e		1.64			1.65			1.66			1.67	
T POSTONE	Pressure, Pounds per Square Inch.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.
1	2.333	8418	960.5	126.6	8476	966.4	127.5	8534	972.3	128.4	8592	978.3	129. 2
	2.272	8408	959.1	129.7	8466	965.0	130.5	8524	970.9	131.4	8581	976.8	132. 3
	2.212	8398	957.6	132.8	8455	963.5	133.7	8513	969.4	134.6	8571	975.3	135. 5
987	$egin{array}{c} 2.153 \ 2.096 \ 2.040 \end{array}$	8388 8377 8367	956.2 954.7 953.3	136.1 139.4 142.8	8445 8435 8424	962.0 960.6 959.1	$137.0 \\ 140.4 \\ 143.8$	$8503 \\ 8492 \\ 8482$	967.9 966.4 965.0	138.0 141.3 144.8	8560 8549 8539	972.3	138.9 142.3 145.8
6	1. 985	8357	951.8	146. 4	8414	957.6	147.4	8471	963.5	148.4	8528	969.3	149.4
5	1. 932	8347	950.4	150. 1	8404	956.2	151.1	8460	962.1	152.1	8517	967.7	153.1
4	1. 880	8336	948.8	153. 8	8393	954.6	154.9	8450	960.5	155.9	8507	966.3	156.9
3	1.829	8326	947.4	157.6	8388	953.2	158.7	8439	959.1	159.8	8496	964.9	160.8
2	1.779	8316	945.9	161.6	8372	951.7	162.7	8429	957.5	163.8	8485	963.3	164.9
1	1.730	8307	944.4	165.7	8363	950.2	166.8	8419	956.0	168.0	8476	961.8	169.1
9	1.683	8296	942.9	169.9	8353	948.7	171.1	8409	954.5	172.2	8465	960.3	173.4
	1.636	8286	941.5	174.3	8342	947.3	175.4	8398	953.0	176.6	8454	958.8	177.8
	1.591	8276	940.0	178.8	8332	945.8	180.0	8388	951.5	181.2	8444	957.3	182.4
6	1.547	8266	938.5	183.3	8321	944.3	184.6	8377	950.0	185.8	8433	955.8	187.0
	1.504	8255	937.0	188.0	8311	942.8	189.3	8366	948.5	190.6	8422	954.2	191.9
	1.462	8245	935.5	192.9	8301	941.3	194.2	8356	947.0	195.5	8412	952.8	196.8
4	1.421	8235	934.0	198. 0	8290	939.8	199.3	8346	945.5	200.6 205.9 211.3	8401	951.3	202.0
3	1.381	8224	932.6	203. 1	8280	938.3	204.5	8335	944.0		8390	949.8	207.2
2	1.342	8214	931.1	208. 5	8269	936.8	209.9	8325	942.5		8380	948.2	212.7
0	1.304 1.266 1.230	8194	929.6 928.1 926.6	214. 0 219. 7 225. 5	8259 8249 8238	935.3 933.8 932.3	215.5 221.1 227.0	8314 8303 8293	941.0 939.5 938.0	216.9 222.6 228.5	8369 8358 8347	946.7 945.2 943.7	$218.3 \\ 224.1 \\ 230.1$
8	1. 195	8173	925.1	231.5	8228	930.8	233.1	8282	936. 4	234. 6	8337	942.1	236.2
7	1. 160	8162	923.6	237.7	8217	929.3	239.3	8271	934. 9	240. 9	8326	940.6	242.4
6	1. 127	8152	922.1	244.1	8207	927.7	245.7	8261	933. 4	247. 3	8315	939.0	249.0
5	1.094	8142	920.6	250.8	8196	926. 2	252.4	8251	931.9	254. 1	8304	937.5	255.8
14	1.062	8131	919.1	257.6	8186	924. 7	259.3	8240	930.3	261. 0	8294	936.0	262.7
13	1.031	8121	917.6	264.7	8175	923. 2	266.4	8229	928.8	268. 2	8283	934.5	269.9
1	1.000 0.971 0.942	8102	916.1 914.5 913.0	$271.9 \\ 279.3 \\ 287.0$	8165 8155 8144	921.7 920.2 918.6	273.7 281.2 288.9		927.3 925.8 924.2	275. 5 283. 0 290. 8	8273 8263 8252	932.9 931.4 929.8	277.3 284.9 292.7
9	0.914	8081	911.5	295.1	8124	917.1	297.1	8188	922.7	299. 0	8241	928.3	301.0
98	0.887	8070	910.0	303.4		915.6	305.4	8177	921.2	307. 4	8230	926.7	309.4
97	0.860	8060	908.5	311.8		914.1	313.9	8166	919.7	316. 0	8220	925.2	318.0
)6	0.834	8051	907.1	320.7	8104	912.6	$322.8 \\ 332.0 \\ 341.4$	8157	918. 2	325. 0	8210	923.7	327.1
)5	0.809	8040	905.5	329.8	8093	911.1		8146	916. 7	334. 2	8199	922.2	336.3
)4	0.784	8030	904.0	339.2	8083	909.6		8135	915. 1	343. 6	8188	920.6	345.9
93	0.761	8019	902.5	348.8	8072	908.1	351.1	8125	913.6	353.4	8177	919.1	355.7
	0.737	8009	901.0	358.9	8062	906.5	361.2	8114	912.0	363.6	8167	917.5	365.9

Т																	
	Specific Volume.				•••	•••	•••		•••		•••			3.330 3.360	3.390 3.420 3.450	3.481 3.514 3.544	3 577
1.7	Heat Con- tents.								•••		•••			1360 1358	1357 1355 1354	1353 1351 1349	1348
	Quality.									 				300 298	296 294 292	290 287 285	283
U	Specific Volume.									 2.960	2.985 3.010 3.035	3.060 3.186 3.112	3 .140 3 .167 3 .296	3.223 3.251 3.280	3 .310 3 .340 3 .370	3 .400 3 .431 3 .464	3.497
1.7	Heat Con- tents.									 1364	1363 1361 1360	1358 1357 1355	1353 1352 1351	1349 1348 1347	1345 1344 1342	1341 1339	1337
	Quality.							•••		 299	297 295 293	291 289 286	284 282 280	278 276 274	272 270 268	266 264 262	260
	Specific Volume.					2.586 2.608	2.629 2.650 2.672	2.696 2.719 2.740	2.764 2.788 2.810	2.835 2.860 2.885	$2.910 \\ 2.936 \\ 2.961$	2.988 3.015 3.041	3.069 3.096 3.125	3 .152 3 .180 3 .209	3 .239 3 .266 3 .296	3 .325 3 .355 3 .385	3.418
1.0	Heat Con- tents.					1369 1368	1367 1365 1364	1362 1361 1360	1358 1357 1355	1354 1353 1351	1350 1349 1348	1346 1345 1344	1342 1341 1339	1338 1336 1335	1333 1332 1331	1329 1328 1327	1326
	Quality.					300 298	296 294 292	290 288 286	284 282 280	278 276 274	272 270 269	267 265 263	261 259 257	255 253 251	249 247 245	243 241 239	238
,	Specific Volume.	2.290 2.310	2.330 2.349 2.368	2.387 2.406 2.425	2.445 2.464 2.484	2.505 2.526 2.547	2.568 2.589 2.610	2.631 2.653 2.676	2.698 2.723 2.746	2.770 2.793 2.818	2.843 2.869 2.894	2.920 2.946 2.972	3 .000 3 .027 3 .054	3.082 3.110 3.139	3 .170 3 .198 3 .227	3 .257 3 .287 3 .317	3.346
1.00	Heat Con- tents.	1375 1373	1371 1370 1369	1368 1367 1365	1364 1362 1361	1359 1358 1357	1356 1354 1353	1351 1350 1349	1348 1347 1345	1344 1342 1341	1339 1338 1337	1336 1335 1333	1332 1330 1329	1327 1326 1325	1324 1322 1321	1319 1318 1317	1315
	Quality.	300 298	296 294 292	291 289 287	285 283 281	279 278 276	274 272 270	268 266 264	263 261 259	257 255 253	251 249 247	246 244 242	240 238 236	234 232 230	229 227 225	223 221 219	217
Pound uare	Pressure, Poun per Square Inch.	308 .6 305 .2 301 .9	298 .7 295 .4 292 .2	289 .0 285 .9 282 .7	279 .6 276 .5 273 .5	270.5 267.5 264.5	261 .6 258 .6 255 .7	$\begin{array}{c} 252.9 \\ 250.0 \\ 247.2 \end{array}$	244 .4 241 .7 238 .9	236 .2 233 .5 230.8	228 .2 225 .6 223 .0	220 .4 217 .8 215 .3	212 .8 210 .3 207 .9	205 .4 203 .0 200 .6	198 .3 195 .9 193 .6	191 .3 189 .0 186 .7	184.5
e,	Temperature, Degrees Fah	420 419 418	417 416 415	414 413 412	411 410 409	408 407 406	405 404 403	402 401 400	399 398 397	896 895 894	393 392 391	890 889 888	387 386 385	84 83 82	80	77	75

TEMPERATURE-ENTROPY TABLE.

П																	
	Specific Volume.	3. 673 3. 708 3. 740	3.775 3.810 3.845	3.882 3.918 3.955	3.990 4.028 4.065	4. 104 4. 141 4. 182	4. 221 4. 263 4. 305	4. 347 4. 390 4. 433	. 477 . 520 . 568	. 615 . 662 . 709	. 760 . 809 . 859	909 960 010	061 115 170	224 279 334	389 444 500	555 612 670	730
1.71	Heat Con- tents.	1343 1342 1340	1339 1338 1336	1334 1333 1332	330 329 328	324	320 -	315 4	11 4	07 4	03 4	99 4	4 5.	0 5.	6 5.	1 5.	8 5
	Quality.	276 274 272	270 268 266	261	255	248 1	242 1	35 1	31 1 29 1 27 1	22 13		12 10 12 12 12	3 12	7 12	1 128	4 128	127
	Volume.	328	94 28 63	31	40	54	1	3 2	0 2	0 2	1 2	2	20	19 19 19	19 19 18	18 18 18	18
	Specific	3.5 3.6 3.6	3. 69 3. 79 3. 76	3.79 3.83 3.86	3.90 3.94 3.97	4. 01 4. 05 4. 09	4.13 4.17 4.21	4. 251 4. 293 4. 337	4. 379 4. 420 4. 466	4. 512 4. 560 4. 608	4. 655 4. 704 4. 752	4. 800 4. 850 4. 900	1. 950 5. 000 5. 055	. 105 . 160 . 212	. 272 . 322 . 380	. 435 . 493 . 550	610
1.70	Heat Con- tents.	1333 1331 1330	1328 1327 1326	1324 1323 1321	1320 1319 1317	1316 1314 1312	1311 1310 1308	1307 1306 1304	1302	$1297 \mid \cdot$	1293 4	1289 4	285 5	281 5	276 5	272 5	269 5.
	Quality.	254 252 250	248 246 244	242 240 238	236 234 232	230 227 225	223 221 219	217 215 213	211 209 207	205 203 201	199 197 195	[91]	85 1	79 1	72 1	68 1 66 1 64 1	52 1
	Specific Volume.	3. 510 3. 541 3. 578	3. 610 3. 643 3. 679	3.711 3.748 3.781	3. 818 3. 853 3. 890	3.928 3.961 4.000	4. 040 4. 079 4. 119	4. 159 4. 199 4. 240	1. 282 1. 325 1. 370		. 597	. 740	887	990 040 092	200 1	370 1	487 1
. 69	tents.	20	16	12	8	3	0 .	3 4	1 4	444	4	4	4. 4. 4.	5.	5.	5. 5. 5.	5.
1.	Heat Con-	135 135 131	131	131 131 131	130 130 130	130 130 130	1300 1300 1299	1297 1296 1294	1293 1292 1290	1289 1287 1286	1285 1283 1282	$\begin{array}{c} 1280 \\ 1279 \\ 1278 \end{array}$	$\begin{array}{c} 1277 \\ 1275 \\ 1274 \end{array}$	1273 1271 1270	1268 1267 1266	1264 1263 1261	1260
	Quality.	230	224	218	214 212 210	208 206 204	203 201 199	197 195 193	191 189 187	185 183 181	179 177 175	·173 171 170	168 166 164	162 160 158	154	148	44
	Specific Volume.	3. 438 3. 469 3. 500	3.534 3.567 3.600	3. 634 3. 669 3. 702	3.738 3.773 3.809	3.845 3.880 3.918	3.954 3.991 4.029	4.069 4.109 4.149	1. 189 1. 230 1. 272	315 360 405	. 451 . 495 . 542	. 638 . 685	783	930	086	250 1	365 1
00	Heat Con- tents	311 310 309	307 306 305	303 302 301	300 298 297	95 94 92	91 90 89	86	32 30	8 4	4 4	$ \begin{vmatrix} 0 & 4 \\ 9 & 4 \end{vmatrix} $	8 4 4 5 4	3 4	5.	5.	5.
	Quality.	08	04 1	8 1	3 1	5 1:	2 12	12	$\begin{vmatrix} 12\\12 \end{vmatrix}$	112	12' 12' 12'	127 127 126	126 126 126	126 126 126	125 125 125	125 125 125	1252
_	Inch.	7 21 6 20	4 20 3 20	2 19	2 19: 3 19:	185	182 180	176 174	172 170 168	166 165 163	161 159 157	155 153 152	150 148 146	144 142 140	138 137 135	133 131 129	127 125
Poun	Pressure, Poun	177. 175. 173.	171. 169. 167.	165. 163. 161.	159. 2 157. 2 155. 3	153.3 151.4 149.5	43.9	40.3 38.5		- (4.8 3.2	9.9 8.4	5. 2 3. 7	9.2	3. 3 1. 8	- 1	. 2
ıre, Fab	Temperature, Degrees Fab	371 370	368	364	362 361	359] 358]	356 1 355 1	354 1 353 1 352 1	50 1: 49 1:	48 13 47 12 46 12	45 12 44 12 43 12			5 110 4 109	3 107 2 106 1 104	0 103 9 102 8 100	7 99 6 97
T				١	33	3	3	31	3£ 34		84 84	84: 84:	37	36 36 34	32 31		27 26

Specific Volume.	 					:::		 		 	5. 433 5. 488	5.545 5.600 5.660	5.717 5.775 5.836	5.898 5.960 6.023	6. 088 6. 154 6. 220	6. 285 6. 355 6. 435
Heat Con- tents.											1339 1338	1337 1335 1334	1333 1332 1330	1328 1327 1326	1324 1323 1321	1320 1318 1316
Quality.										•••	300 298	296 293 291	289 286 284	$281 \\ 279 \\ 277$	$274 \\ 272 \\ 269$	$267 \\ 264 \\ 262$
Specific Volume.								4.850 4.900	4.950 5.000 5.050	5.105 5.155 5.208	5.260 5.315 5.367	5.420 5.475 5.530	5.585 5.640 5.700	5.760 5.820 5.882	5.940 6.007 6.070	6.130 6.195 6.260
Heat Con- tents.								1344 1342	1341 1339 1338	1336 1335 1334	1332 1330 1329	1327 1326 1325	1323 1321 1320	1318 1317 1316	1314 1313 1311	1309 1308 1306
Quality.							• • •	299 296	294 292 290	287 285 283	280 278 276	$273 \\ 271 \\ 269$	$266 \\ 264 \\ 262$	259 257 255	252 250 247	245 243 240
Specific Volume.			• • • •	4. 260	4.302 4.343 4.385	4.428 4.470 4.513	4.557 4.602 4.647	4.695 4.743 4.790	4.839 4.889 4.935	4.985 5.037 5.090	5. 140 5. 193 5. 247	5.300 5.355 5.410	5. 463 5. 520 5. 580	5.638 5.695 5.750	5.810 5.868 5.928	5.990 6.052 6.115
Heat Con- tents.				 1349	1348 1346 1345	$1343 \\ 1342 \\ 1340$	1338 1337 1336	1335 1333 1331	1330 1328 1327	1325 1324 1322	1321 1319 1318	1316 1315 1314	1312 1310 1309	1308 1306 1305	1303 1301 1300	1299 1297 1295
Quality.				299	297 295 293	290 288 286	283 281 279	277 274 272	270 267 265	263 261 258	256 254 252	249 247 245	242 240 238	236 233 231	229 226 224	222 220 217
Specific Volume.	3.765 3.798 3.833	3.869 3.904 3.940	3.976 4.011 4.049	4.086 4.123 4.160	4. 200 4. 239 4. 279	4.319 4.360 4.400	4. 444 4. 488 4. 532	4.577 4.622 4.669	4.717 4.766 4.815	4.868 4.919 4.970	5.020 5.075 5.124	5. 179 5. 230 5. 286	5.340 5.395 5.450	5.502 5.560 5.620	5.675 5.735 5.795	5.850 5.910 5.970
Heat Con- tents.	1354 1353 1351	1349 1348 1347	$1345 \\ 1344 \\ 1343$	1341 1339 1338	1337 1335 1334	1333 1331 1329	1328 1327 1326	1324 1323 1321	1319 1318 1317	1315 1314 1312	1311 1309 1308	1307 1305 1304	1302 1300 1299	1298 1297 1295	1293 1292 1290	1289 1288 1286
Quality.	299 297 295	292 290 288	286 284 282	280 277 275	$273 \\ 271 \\ 269$	$267 \\ 264 \\ 262$	$\begin{array}{c} 260 \\ 258 \\ 256 \end{array}$	$254 \\ 252 \\ 249$	$247 \\ 245 \\ 243$	241 239 236	234 232 230	228 226 224	221 219 217	215 213 211	208 206 204	202 200 198
per Squa Inch.	77.9 75.7 73.6	71.5 69.4 67.3	65.3 63.2 61.2	.59. 2 .57. 2 .55. 3	53.3 51.4 49.5	147.6 145.8 143.9	142.1 140.3 138.5	136.7 135.0 133.2	131.5 129.8 128.1	126. 4 124. 8 123. 2	121.5 119.9 118.4	116.8 115.2 113.7	$112.2 \\ 110.7 \\ 109.2$	107.7 106.3 104.8	103.4 102.0 100.6	99.2 97.8 96.5
	2	9 8 7	6 5 4	3 2 1	9	6	4 3 2	0	8 7 6	.5 .4 .3	2 1 0	9 18 17	6 5 4	3 2 1	98	7 6 5

222	2	2	1		ı	l			-			-				
279 278 277	282 281 280	285 284 283	288 287 286	291 290 289	294 293 292	297 296 295	300 299 298	303 302 301	306 308 304	308 308 307	31: 31: 31:	31 31 31	21	32 32 31	32 32 32	Temperatur
48. 47. 47.	50.	52.	55.	58 57 56	60	163	66	69	72 72 1 71	3 7 5	L 79	5 8 4 8 3 8	7 8	0 9	4 9 3 9 2 9	Degrees 1
55 77 01	1	6	. 1	. 6 . 7 . 8	. 5	.3	. 2	0.3	3.5 2.4 1.4	5.7		$\begin{bmatrix} 3.8 \\ 2.6 \\ 1.4 \end{bmatrix}$	7.4 6.2 5.0	1. 2 0. 0 8. 7	5. 1 3. 8 2. 5	Fressure, Fressu
37 35 33	43 41 39	48 46 45	54 52 50	59 58 56	65 63 61	71 69 67	$76 \\ 74 \\ 72$	82 80 78	88 86 84	93 91 89	99 97 95	105 103 101	110 108 106	116 114 112	121 120 118	Quality.
1188 1186 1185	1192 1191 1189	1196 1194 1193	1200 1198 1197	1204 1203 1201	1208 1206 1205	1212 1210 1209	1215 1214 1213	1220 1218 1217	1224 1222 1221	1227 1226 1225	1232 1230 1229	1236 1234 1233	1239 1238 1237	1242	1246	Heat Con- tents.
9.27 9.38 9.50	8.94 9.05 9.16	8. 61 8. 72 8. 83	8. 32 8. 42 8. 51	8. 03 8. 13 8. 22	7.75 7.84 7.93	7.48 7.57 7.66	7.23 7.31 7.39	6.98 7.06 7.14	6.74 6.82 6.90	6.51 6.59 6.67	6.30 6.37 6.44	6.09 6.16 6.23	5.900 5.965 6.030	5.715 5.775 5.835	5.595	Specific Volume.
52 50 48	58 56 54	63 61 60	69 67 65	75 73 71	81 79 77	86 85 83	92 90 88	98 96 94	104 102 100	110 108 106	116 114 112	121 119 117	125	133 131 129	139 137 135	Quality.
1194	1200 1199 1197	1202	1208 1206 1205	1212 1210 1209	1216 1215 1213	1220 1219 1218	1224 1222 1221	1228 1227 1225	1232 1231 1229	1236 1235 1234	1240 1239 1238	1244 1243 1241	1248 1247 1245	1252 1251 1250	1257 1255 1254	Heat Con-
9.47 9.59 9.70	9. 14 9. 25 9. 36	8.81 8.91 9.02	8.50 8.60 8.70	8.20 8.30 8.40	7.92 8.01 8.10	7.65 7.74 7.83	7.39 7.48 7.57	7.14 7.22 7.30	6.89 6.97 7.05	6.66 6.74 6.81	6.44 6.51 6.59	6. 23 6. 30 6. 37	6.030 6.09 6.16	5.850 5.910 5.970	5.670 5.730 5.790	Specific Volume.
66 64 62	72 70 68	78 76 74	84 82 80	90 88 86	96 94 92	102 100 98	108 106 104	114 112 110	120 118 116	$126 \\ 124 \\ 122$	132 130 128	138 136 134	144 142 140	150 148 146	156 154 152	Quality.
1203 1202 1200	1207 1206 1205	1212 1210 1209	$1216 \mid 1214 \mid 1213 \mid$	1220 1218 1217	1224 1223 1221	1228 1227 1225	1232 1231 1229	1236 1235 1233	1240 1239 1238	1244 1243 1242	1249 1247 1246	1253 1251 1250	1257 1256 1254	1261 1260 1258	1265 1264 1262	Heat Con- tents.
9.67 9.78 9.90	9.33 9.44 9.55	9.00 9.10 9.22	8. 68 8. 79 8. 89	8.38 8.48 8.58	8. 09 8. 18 8. 28	7.82 7.91 8.00	7.55 7.64 7.73	7.30 7.38 7.47	7.05 7.14 7.22	6.82 6.89 6.97	6.60 6.67 6.74	6.380 6.450 6.525	6.175 6.240 6.310	5. 975 6. 040 6. 105	5.790 5.850 5.910	Specific Volume,
81 79 76	87 85 83	93 91 89	99 97 95	105 103 101	111 109 107	117 115 113	124 122 119	130 128 126	136 134 132	142 140 138	149 147 144	155 153 151	161 159 157	168 165 163	174 172 170	Quality.
1210 1	1215 1214 1212	1219 1218 1216	1223 1222 1221	1228 1226 1225	1232 1230 1229	1236 1235 1233	1240 1239 1237	1245 1243 1242	1249 1247 1246	1253 1251 1250	1257 1256 1254	1261 1260 1259	1266 1264 1263	1270 1268 1267	1274 1273 1272	Heat Con- tents.
9. 89 0. 02 0. 14	9. 54 9. 65 9. 77	9. 21 9. 32 9. 43	8.87 8.98 9.10	8.57 8.67 8.77	8.28 8.38 8.47	7.99 8.09 8.19	7.73 7.82 7.90	7. 46 7. 54 7. 63	7. 21 7. 29 7. 38	6.97 7.05 7.13	6.74 6.82 6.89	6.52 6.59 6.66	6.310 6.375 6.45	6. 105 6. 170 6. 240	5.910 5.975 6.040	Specific Volume,

	ıre, Fal	our										
	Temperature, Degrees Fa	Pressure, Pour per Square Inch.	Quality.	Heat Contents.	Specific Volume.	Quality.	Heat Contents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.	Quality.
	323	95.1 93.8 92.5	195 193 191	1284 1283 1282	6.05 6.11 6.18	215 213 210	1294 1293 1291	6. 19 6. 26 6. 33	238 236 233	1305 1304 1302	6.33 6.40 6.46	260 257 255
	320	91. 2 90. 0 88 7	189 187 185	1280 1279 1278	6.25 6.32 6.39	208 206 204	1290 1288 1287	6. 40 6. 46 6. 53	231 229 226	1300 1299 1297	6.53 6.60 6.67	252 250 248
	318 317 316	87.4 86.2 85.0	182 180 178	1276 1274 1273	6.45 6.53 6.60	201 199 197	1285 1284 1283	6.60 6.67 6.75	224 222 219	$\begin{array}{c} 1296 \\ 1295 \\ 1293 \end{array}$	6.75 6.83 6.90	245 243 240
	314	83.8 82.6 81.4	176 174 172	$\begin{array}{c} 1272 \\ 1270 \\ 1269 \end{array}$	6.67 6.75 6.82	194 192 190	1281 1279 1278	6.82 6.90 6.97	217 215 212	1291 1290 1288	6.98 7.06 7.14	238 235 233
Model Cooper - tax :	312 311 310	80.2 79.1 77.9	170 168 166	1268 1267 1265	6.90 6.97 7.05	185 183	1277 1275 1274	7.05 7.13 7.20	210 208 205	1287 1286 1284	7.22 7.30 7.38	$231 \\ 228 \\ 226$
	308	76.8 75.7 74.6	163 161 159	1263 1262 1261	7. 13 7. 20 7. 29	181 179 176	1272 1271 1269	7. 29 7. 37 7. 45	203 201 198	1283 1281 1279	7.46 7.54 7.63	224 221 219
- All Property of Communications of the Communication of the Communicati	305	73.5 72.4 71.4	157 154 152	1259 1257 1256	7.37 7.46 7.54	174 172 170	1267 1266 1265	7.53 7.62 7.70	196 194 191	1278 1277 1275	7.72 7.80 7.89	216 214 211
graph and and control	302	70.3 69.3 68.2	150 148 146	1255 1253 1252	7.63 7.71 7.80	167 165 163	1263 1262 1260	7.79 7.88 7.97	186	1273 1271 1270	7.98 8.07 8.16	209 207 204
	1 299	67.2 66.2 65.2	144 141 139	1250 1248 1247	7.89 7.99 8.08	158	1259 1257 1255	8.06 8.16 8.25	180 177	1269 1268 1266	8.25 8.35 8.44	202 199 197
	297 296 295	64.3 63.3 62.3	137 135 133	1246 1244 1243	8.17 8.26 8.36	154 151 149	1254 1252 1251	8.34 8.43 8.53	1	1264 1263 1261	8.54 8.64 8.74	1
	293	61.4 60.5 59.5	131 128 126	1242 1240 1238	8.40 8.50 8.60	147 145 143	1249 1248 1247	8. 63 8. 74 8. 84	168 165 163	1260 1258 1257	8.85 8.95 9.05	l
	291 290 289	58.6 57.7 56.8	124 122 120	1237 1236 1234	8.70 8.80 8.90	3 140 5 138 6 136	1245 1244 1242	8.98 9.08 9.10	5 158 156	1255 1253 1252	9.16 9.27 9.38	180 178 175
	287	56.0 55.1 54.2	118 116 113	1233 1232 1230	9.0 9.1 9.2	8 132	1241 1240 1238	9.27 9.38 9.50		1251 1249 1247	9.50 9.61 9.72	170
	284 284 283	53.4 52.6 51.7	111 109 107	1228 1227 1226	9.4 9.5 9.6	1 125	1236 1235 1234	9.6 9.7 9.8	1 147 2 144 4 142	1246 1244 1243	9.84 9.95 10.07	166 163 161
	28:	50.9 50.1 49.33	105 103 101	1224 1223 1222	9.7 9.8 9.9	4 120 6 118 8 116	1232 1230 1229	9.90 10.00 10.2	140 137 135	1242 1240 1238	10. 20 10. 33 10. 46	156
	279 278	9 48.55 8 47.77	98 96	1220 1218	$10.1 \\ 10.2$	0 114 3 112	1228 1226	10.3 10.4	3 133 6 130	1237 1235	10.58 10.71	151 149

e, ah:	oun e		1.00			m .00					
Temperature, Degrees Fal	Pressure, Poun per Square Inch.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.	Quality.
275	46. 26 45. 52 44. 78	$\frac{32}{30} \\ 28$	1184 1183 1181	9.62 9.74 9.86	46 44 42	1192 1190 1189	9.83 9.95 10.07	60 58 56	1199 1198 1196	10.04 10.15 10.28	74 72 70
272	44.06 43.35 42.64	$\frac{26}{24}$ $\frac{22}{22}$	1180 1178 1177	9.98 10.10 10.23	41 39 37	1188 1187 1185	10.20 10.33 10.47	54 52 50	1195 1193 1192	10. 40 10. 54 10. 67	68 66 64
269	$41.95 \\ 41.26 \\ 40.58$	$\frac{21}{19}$	1176 1175 1173	10.36 10.50 10.64	35 33 31	1184 1182 1181	10.60 10.73 10.87	49 47 45	1191 1190 1188	10, 80 10, 94 11, 08	62 60 58
266	$39.91 \\ 39.26 \\ 38.60$	15 13 11	1172 1170 1169	10.76 10.90 11.05	29 27 25	1179 1178 1177	11.00 11.15 11.30	43 41 39	1187 1186 1184	11.22 11.37 11.52	56 54 52
264 263 262	37.96 37.33 36.71	10 8 6	1168 1167 1165	11. 19 11. 33 11. 48	$\begin{array}{c} 23 \\ 21 \\ 20 \\ \end{array}$	$1175 \\ 1174 \\ 1173$	11.45 11.59 11.74	37 35 33	1183 1181 1180	11.67 11.81 11.96	50 49 47
260	36.09 35.48 34.88	$\begin{array}{c} 4 \\ 2 \\ 0 \end{array}$	1164 1162 1161	11. 63 11. 78 11. 93	18 16 14	$\begin{array}{c} 1172 \\ 1170 \\ 1169 \end{array}$	11.89 12.04 12.20	31 29 27	1178 1177 1176	12. 12 12. 27 12. 45	45 43 41
258 257 256	34.29 33.71 33.14	$\begin{array}{c} 9992 \\ 9982 \\ 9972 \end{array}$	1159, 9 $1158, 6$ $1157, 3$	12.17	12 10 8	1167 1166 1164	$\substack{12.36\\12.52\\12.69}$	25 23 21	1174 1173 1172	12.60 12.78 12.96	39 37 35
254	32.57 32.01 31.46	9960 9949 9938	1156.0 1154.6 1153.4	12.74	6 4 2	1163 1161 1160	12 .85 13.02 13.20	20 18 16	$^{1171}_{1169}_{1168}$	13, 14 13, 30 13, 49	33 31 29
251	30.92 30.38 29.86	9928 9918 9907	1152.1 1150.8 1149.5	13, 35	9993	1159 1157.8 1156.5		14 12 10	1167 1165 1164	13, 66 13, 85 14, 05	27 25 23
248	$\begin{vmatrix} 29.34 \\ 28.82 \\ 28.32 \end{vmatrix}$	9896 9885 9875	1148.2 1146.8 1145.5	13, 77 13, 98 14, 19	9971 9960 9950	1155.2 1153.9 1152.6	13.87 14.08 14.30	S. 6	1162 1161 1160	14 25 14 45 14 64	21 19 17
245	27.82 27.33 26.85		1144.2 1142.9 1141.6	14, 63	9928	ł .	14.52 14.74 14.99	2 0 9992	1158 1157 1155. 7	14.84 15.04 15.10	15 13 12
243 242 241	$ \begin{array}{c} 26.37 \\ 25.90 \\ 25.44 \end{array} $	9832 9822 9811	1140.3 1139.0 1137.7	15, 35	9896	1146.0	15. 23 15. 47 15. 72	9971	1154 4 1153 0 1151 7	15.58	10 8 6
239	24.98 24.53 24.09	9790	1136.3 1135.0 1133.6	16, 10	9864	1142.0	15 .97 16 .23 16. 49	9938	1150.3 1149.0 1147.6	16 - 35	4 2 0
236	23.66 23.23 22.80	9759	1132.3 1131.0 1129.7	16.91	9832	1139.3 1138.0 1136.0	16.76 17.04 17.31	9916 9905 9894	1146,3 1144,9 1143,5	16.89 17.17 17.44	9989 9979 9967
233	22.39 21.98 21.57	9737 9726 9715	1128.3 1127.0 1125.6	17.47 17.76 18.05	9810 9799 9788	1133.5	17.60 17.89 18.19	9872	1140.8	17, 73 18, 03 18, 32	9945

ture,	Poun uare	-	-	1.12		1	1.10	-e-		1.01	·e		±	
Temperature, Degrees Fah	Pressure, Poun per Square	I Inch.	Qualitý.	Heat Contents	Specific Volume.	Quality.	Heat Contents.	Specific Volume.	Quality.	Heat Con-	Specific Volume.	Quality.	Heat Contents.	Specific Volume.
276 275 274	46.2 45.5 44.7	26 52 78	92 90 88	1216 1214 1213	10.48 10.60 10.74	107 105 103	$1223 \\ 1222 \\ 1220$	10.72 10.86 11.00	$126 \\ 123 \\ 121$	1233 1231 1229	10.97 11.10 11.24	144 141 139	1241 1239 1238	11.20 11.34 11.49
272	44.0 43.3 42.6	35	86 83 81	$\begin{array}{c} 1212 \\ 1210 \\ 1208 \end{array}$	10.87 11.00 11.15	101 99 96	$\begin{array}{c} 1219 \\ 1218 \\ 1216 \end{array}$	11.12 11.26 11.40	119 116 114	1228 1226 1225	11.39 11.51 11.66	137 134 132	1237 1235 1234	11.63 11.77 11.91
270 269 268	41.9 41.2 40.5	05 26 58	79 77 75	$\begin{array}{c} 1207 \\ 1206 \\ 1204 \end{array}$	11.29 11.43 11.57	94 92 90	1214 1213 1212	11.54 11.69 11.84	112 109 107	1224 1222 1220	11.80 11.94 12.10	124	1232 1231 1229	12.06 12.20 12.36
267 266 265	39.9 39.2 38.6	26 30	73 71 69	$^{1203}_{1202}_{1200}$	11.72 11.87 12.03	88 86 83	1210 1209 1207	11.99 12.14 12.30	105 102 100	1219 1217 1216	12.25 12.40 12.56	122 120 117	1227 1226 1224	12.52 12.68 12.84
264 263 262	37. 9 37. 3 36. 7	96 33 71	67 65 62	1199 1197 1195	12.19 12.34 12.50	81 79 77	1206 1204 1203	12.45 12.60 12.77	98 95 93	1214 1212 1211	12.71 12.88 13.04	110	1223 1222 1220	13.00 13.15 13.32
261 260 259	36.6 35.4 34.8	09 48 88	60 58 56	1194 1193 1191	12.67 12.84 13.00	75 73 70	1202 1200 1198	12.94 13.10 13.28	91 88 86	1210 1208 1207	13.20 13.38 13.55	108 105 103	1218 1217 1215	13.49 13.66 13.84
258 257 256	34. 33. 33.	29 71 14	54 52 50	1190 1189 1187	13.18 13.36 13.54	68 66 64	1197 1196 1194	13.45 13.62 13.80	84 81 79	1205 1203 1202	13.73 13.90 14.09	96	1214 1212 1211	14.01 14.20 14.38
255 254 253	32. 32. 31.	57 01 46	48 46 44	1186 1184 1183	13.70 13.90 14.09	62 60 58	1193 1192 1190	13.99 14.17 14.35	74	1201 1199 1197	14. 28 14. 46 14. 6	6 91	1209 1208 1206	14. 56 14. 57 14. 94
251	30. 30. 29.	38	$\frac{42}{40}$	1182 1180 1178	14. 28 14. 46 14. 66	55 53 51	1188 1187 1186	14.54 14.73 14.93	70 68 65	1196 1195 1193	14.83 15.03 15.2	86 84 4 81	1204 1203 1201	15. 12 15. 33 15. 54
249 248 247	29. 328. 28.	34 82 32	35 33 31	1177 1176 1174	14.86 15.05 15.27	47	1184 1183 1182	15. 12 15. 33 15. 54	63 61 59	1191 1190 1189	15.4 15.6 15.8	79 77 6 74	1200 1199 1197	15.75 15.95 16.18
246 246 246		82 33 85	29 27 25	1173 1172 1170	15.48 15.69 15.90	43 41 39	1180 1179 1177	15.75 15.95 16.18	57 54 52	1188 1186 1184	16.0 16.3 16.5	0 70	1195 1194 1192	16.39 16.60 16.84
243 243 243	26. 25. 125.	37 90 44	$\frac{23}{21}$ $\frac{19}{19}$	1169 1167 1166	16.11 16.33 16.55	36 34 32	1175 1174 1173	16.40 16.62 16.88	2 48	1183 1181 1180	16.7 16.9 17.2	8 62 60	1191 1189 1188	17.07 17.30 17.54
240 233 233	24. 9 24. 8 24.	98 53 09	17 15 13	1165 1163 1162	16.78 17.00 17.2	28	1171 1170 1169	17.08 17.33 17.5	2 42	1179 1177 1175	17.4 17.7 17.9	5 58 0 56 5 53	1186 1185 1183	17.80 18.04 18.30
23	7 23. 6 23. 5 22.	23	11 9 7	1160 1159 1158	17.48 17.7 17.9	3 24 1 22 7 20	1167 1166 1165	17.8 18.0 18.3	6 35	1174 1173 1172	18. 2 18. 4 18. 7	6 49	1182 1180 1178	18.55 18.80 19.08
23 23 23	4 22. 3 21. 2 21.	39 98 57	5 3 1	1156 1155 1153	18. 2 18. 4 18. 7	1 18 9 16 5 14	1163 1162 1160	18.59 18.8 19.1	9 31 5 29 2 27	1170 1169 1168	18.9 19.2 19.5	9 44 4 42 0 40	1177 1176 1174	19.35 19.62 19.90
23	1 21.	.18	0.9995	1151.	9 18.9	0 12	1159	19.4	0 25	1166	19.7	7 37	1172	20.18

re, Fahr	Pouniare		1.00			1.00							
Temperature, Degrees Fab	Pressure, Pour per Square Inch.	Quality.	Heat Contents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Contents.	Specific Volume.
227	20.02 19.64 19.28	9673 9662 9651	1120.2 1118.9 1117.6	19.60	9744 9734 9723	1127.1 1125.8 1124.4	19.75	9816 9805 9795	1134.0 1132.7 1131.3	19.56 19.90 20.25	9888 9877 9866	1140.8 1139.5 1138.1	20.04
225 224 223	18.91 18.56 18.21	9640 9630 9620	1116.3 1114.9 1113.6	20.63	9712 9701 9691	1123.1 1121.7 1120.4	20.43 20.78 21.14	9783 9773 9762	1129.9 1128.5 1127.2	20.93	9855 9844 9833	1136.8 1135.4 1134.0	21.09
221	17.86 17.52 17.19	9609 9600 9589	1112.2 1110.9 1109.5	21.33 21.70 22.08	9680 9670 9660	1119.0 1117.7 1116.3	21.86	9751 9741 9731	1125.8 1124.5 1123.1	$21.65 \\ 22.03 \\ 22.41$	$9822 \\ 9812 \\ 9801$	1132.6 1131.3 1129.9	22.19
218	16.86 16.53 16.21	9578 9566 9556	1108. 1 1106. 7 1105. 4	22.86	9648 9637 9626	1114.9 1113.5 1112.1	22.64 23.03 23.43	9719 9707 9696	1121.7 1120.3 1118.9	23.20	9790 9778 9767	1128. 5 1127. 0 1125. 6	23.37
215	15.90 15.59 15.29	9545 9535 9524	1104.0 1102.7 1101.3	23.66 24.08 24.51	9615 9605 9594	1110.7 1109.4 1108.0	23.84 24.25 24.69	9686 9675 9664	1117.5 1116.2 1114.8	24. 01 24. 43 24. 86	9756 9745 9734	1124.3 1122.9 1121.5	24.61
212	14.99 14.70 14.41	9514 9503 9492	1100.0 1098.6 1097.3	25.33	$\begin{array}{c} 9583 \\ 9573 \\ 9562 \end{array}$	1106.7 1105.3 1103.9	25.52	$\begin{array}{c} 9653 \\ 9642 \\ 9631 \end{array}$	1113. 4 1112. 0 1110. 6	25.30 25.71 26.11	$\begin{array}{c} 9723 \\ 9711 \\ 9700 \end{array}$	1120. 1 1118. 7 1117. 3	25. 48 25. 89 26. 30
209	14.12 13.84 13.57	9482 9471 9460	1095. 9 1094. 4 1093. 1	26.67	9551 9540 9529	1102.5 1101.1 1099.8	26.39 26.86 27.35	9620 9609 9598	1109.2 1107.8 1106.4	27.06	9689 9678 9667	1115.9 1114.5 1113.1	26.77 27.25 27.74
206	13.29 13.03 12.77	9449 9439 9428	1091.7 1090.3 1088.9	28.16	9518 9507 9496	1098.4 1097.0 1095.6	[28, 36]	9587 9576 9565	1105.0 1103.6 1102.2	28.56	9656 9644 9633	1111.7 1110.3 1108.9	28. 25 28. 77 29. 29
203	12.51 12.25 12.01	9417 9407 9397	1087. 6 1086. 2 1084. 9	29. 18 29. 72 30. 26	9486 9475 9464	1094.2 1092.8 1091.5	29.40 29.93 30.48	9554 9543 9532	1100.8 1099.4 1098.1	30.15	$9622 \\ 9611 \\ 9600$	1107.5 1106.1 1104.7	29.82 30.36 30.91
200	11.76 11.52 11.28	9387 9376 9365	1083.5 1082.1 1080.7	31.39	9455 9444 9433	1090.1 1088.7 1087.3	31.05 31.62 32.20	9522 9511 9500	1096.7 1095.3 1093.8	31. 27 31. 84 32. 43	9590 9579 9568	1103.3 1101.9 1100.4	31.49 32.07 32.66
197	11.05 10.82 10.60	9355 9343 9332	1079.3 1077.8 1076.4	33.17	9422 9410 9399	1085.9 1084.4 1083.0	33.41	9490 9478 9466	1092.5 1091.0 1089.5	33.65	9557 9545 9533	1099.1 1097.5 1096.1	33.88
195 194 193	10.38 10.16 9.95	9322 9311 9301	1075.1 1073.7 1072.3	34.44 35.08 35.75	9389 9378 9368	1081.6 1080.2 1078.8	34.68 35.34 36.01	9456 9445 9434	1088.2 1086.7 1085.4	$34.93 \\ 35.59 \\ 36.26$	$\begin{array}{c} 9523 \\ 9511 \\ 9501 \end{array}$	1094.7 1093.3 1091.9	35.18 35.84 36.52
192 191 190	9.53	9290 9279 9269	1070.9 1069.5 1068.1	37.13	9357 9345 9335	1077.4 1076.0 1074.6	37.39	9423 9412 9401	1083.9 1082.5 1081.1	37.66	9489 9478 9467	1090.4 1089.0 1087.6	37.92
189 188 187	8.94	9259 9248 9237	1066.8 1065.3 1063.9	38.57 39.31 40.07	9325 9313 9303	1073.2 1071.8 1070.4	38.85 39.59 40.36	9391 9379 9369	1079.7 1078.3 1076.9		9457 9445 9434	1086.2 1084.7 1083.3	39.40 40.15 40.93
186 185 184	8.37	9226 9216 9205	1062.5 1061.1 1059.7	41.66	9292 9281 9270	1069.0 1067.6 1066.1	41.95	9357 9347 9335	1075.4 1074.0 1072.6	42.25	9423 941 2 9401	1081.9 1080.5 1079.0	42.54
183	8.01	9194	1058.3	43.31	9259	1064.7	43.62	9325	1071.2	43.93	9390	1077.6	44. 23

-	222	2 2 2	2:	2 2	2 2 2	$\frac{2}{2}$	- 1	1	- {		- 1	4 3	6	2	3	. 8
Heat Con- tents.	168 167 166	164 163 161	159 158 157	155 154 153	151 150 148	$\frac{147}{45.6}$	42.7 41.5 39.8	138.4 136.9 135.4	134. 132. 131.	129. 128. 126.	125. 123. 122.	120. 119. 118.	116. 115. 113.	112. 110. 109.	107. 106. 104.	103. 101. 1100.
	1 1	1 1	1	1:	1:			- 1	- 1	- (- 1]	3	7	2	9
Quality.	31 29 27	25 23 20	18 16 14	12 10 8	$\begin{array}{c} 6 \\ 4 \\ 2 \end{array}$	0 9989 9978	9966 9954 9942	9930 9919 9907	9895 9883 9872	9861 9850 9838	9826 9814 9802	9790 9778 9767	9755 9743 9732	9721 9709 9697	9685 9674 9662	9650 9639 9627
	1	2 4 .6	31	37	71 14 58		35 34 34	91	- 1	36	- 1		72 46	99 78	43 29	. 04
Specific	0.6 0.9 1.2	1.8 21.8 22.	22. 4 22. 8 23. 3	23. 23. 24.	24. 25. 25.		27. 27. 28.	29.					38. 39.	40 41	43 44	46
	2	240404	2	312	5 2 1 2 7 2		0 6 1	8	1	. 2			. 5 . 1	. 7	. 8 . 3	. 4
Heat Con- tents.	1161 1160 1158	1157 1155 1154	1153 1151 1150	1149 147. 145.	144. 143. 141.	140. 138. 137.	136. 134. 133.	131. 130. 128.	127.125.124.	123 121 120	1118 1117 1115	1114 1112 1111	1110 1108 1107	1105 1104 1102	1101 1099 1098	1096 1095 1093
				1	1111		1111	1					5	3	6	4
Quality.	18 16 14	12 10 8	$\begin{array}{c} 6 \\ 4 \\ 2 \end{array}$	0 9989 9977	9966 9955 9943	9931 9920 9908	9897 9885 9873	9862 9850 9839	9827 9815 9804	9794 9782 9770	9759 9746 9735	9724 9712 9701	9689 9677 9666	965 964 963	9620 9600 959	958 957 956
votume.	21 52 82	39	51	71	96		15 64 14	18	24 79 35	.52	. 74 . 36 . 01	. 67 . 34 . 03	. 4 5 . 19	. 95 . 71 . 50	. 13	. 85 . 73
Specific	20. 20. 20.	21.	22.	23.	24.		27. 27. 28.	29.	30 30 31	32	33 34 35	35 36 37	38	39 40 41	43 43	1 44 0 45 5 46
		0	9	6	4		. 3 . 9 . 5	. 6	. 7 . 3 . 9	. 0	1. 2 1. 7 1. 2	. 6 . 3	2. (). (9. 2 7. 7 3. 3	3.4 1.9	0. 4 9. 0 7
Heat Con- tents.	1155 1153 1151	150. 149. 147.	146. 144. 143.	142. 140. 139.	137. 136. 135.	133. 132. 130.	129 127 126	$125 \\ 123 \\ 122$	120 119 117	116 115 113	1112 1110 1109	1107 1106 1104	1103 1102 1100	1099 1097 1096	1094 1093 1093	1090 1089 108
	-1	' 1	l 1) 1	3 1 3 1		3 1	2	9 7 6	4	2 9 8	7 5 4	100	39 77 36	13)9
Quality.	6 4 1	999 998 997	996 995 994	993 991 990	989 988 987	986 985 983	982 981 980	979 978 977	973 974 973	97: 97 97:	96 96 96	96 96 96	96 96 96	95 95 95	95 95 95	95
aurnio A	19	89 24 60	96 35 74	54	36 78 22	08	45	45 97 49	03 58 13	72 30 89	.50 .12 .76	. 78 . 78	. 48 . 19 . 92	. 67 . 43 . 21	. 01 . 84 . 68	.42
Specific	20.	20. 21. 21.	21. 22. 22.	23.	$\begin{array}{c} 24. \\ 24. \\ 25. \end{array}$	26.	27.	28. 28. 29.	30. 30. 31.	31 32 32	33 34 34	36	37 38 38	39 40 41	42 42 43	445
	4 2	629	5 1 7	8	0 6 2	4	. 2	. 4 . 9 . 5	. 1 . 7 . 3	. 9 . 4 . 0	. 6 . 1 . 6	. 4	. 0 5. 5 1. 1	2.7	3. 3 3. 9 5. 4	2. €
Heat Con- tents.	47. 46. 45.	43. 42. 40.	39. 38. 36.	35. 33. 32.	31. 29. 28.	.26. 25. 24.	122. 121. 119.	118. 116. 115.	114 112 111	109 108 107	$105 \\ 104 \\ 102$	101 099 098	097 095 094	092 091 089	088 086 085	.084 .082
	11	11 11 11	11 11 11	11	11 11 11	11	1:	1:	1111	1 1 1	1111	1	11111	1111]	. 11
Quality.	949	926 915 904	893 883 872	860 848 837)826)815)803	9792 9781 9770	9759 9747 9736	9724 9713 9702	9690 9679 9668	9658 9647 9635	9624 9612 9601	9590 9578 9567	9556 9544 9533	9523 9511 9500	9488 9477 9466	9455 9444
Tucu.	4	6	6 2 9	3	9	70	34	03	25	76 52 28	82	16	74 53 33	13 94 75	56 37 19	01 84 67
per Squa	9.6	8.5	7.8 7.5 7.1	6.5	5.5	4.7	13.8	13.0	12.:	11. 11. 11.	10.	10. 10. 9.	9. 9. 9.	8.	8. 8. 8.	8. 7.
Degrees	28 2 27 1 26 1	25 1 24 1 23 1	22 1 221 1 220 1	219 1 218 1 217 1	216 215 214	213 212 211	210 209 208	207 206 205	204 203 202	201 200 199	198 197 196	195 194 193	192 191 190	189 188 187	186 185 184	183 182
	- 1															

l di	Quality. Heat Contents. Specific Volume.	9356 1073.2 46.91 1071.7 47.84 1070.3 48.79	$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	9290 1064.5 52.86 9279 1063.1 53.94 9268 1061.6 55.04	9256 1060.1 56.16 9245 1058.6 57.32 9234 1057.2 58.52	9223 1055.7 59.74 9212 1054.3 60.99 9201 1052.8 62.26	9190 1051.3 63.57 9179 1049.9 64.91 9167 1048.4 66.28	9156 1046. 9 67. 69 9146 1045. 5 69. 15 9135 1044. 0 70. 62	9124 1042.5 72.14 9113 1041.0 73.70 9102 1039.6 75.31	9091 1038. 1 76. 96 9079 1036. 6 78. 64 9068 1035. 1 80. 36	9057 1033. 6 82. 13 9046 1032. 1 83. 96 9035 1030. 6 85. 82	9024 1029. 1 87. 75 9012 1027. 6 89. 71 9002 1026. 2 91. 73	8990 1024. 6 93.77 8979 1023. 2 95. 90 8968 1021. 6 98. 11	8957 1020. 1 100. 3 8945 1018. 6 102. 6	8935 1017.1 105.0	8924 1015.6 107.5 8913 1014.1 110.0 8902 1012.6 112.6	8924 1015.6 107.5
1 4 1 4 1	Heat Contents. Specific Volume.	1066.8 46.59 1065.4 47.51 1063.9 48.46	1062.5 49.44 1061.0 50.44 1059.6 51.45	1058.2 1056.7 1055.3 52.50 53.57 54.67	1053.8 1052.3 1050.9 56.93 58.12	1048.0 60.58	1043.6 64.47	1039.3 68.68	1034.8 73.21	1030.4 78.11	i 1026.0 83.39	1023.0 87.16 2 1021.5 89.1 2 1020.1 91.1	1020.1 91.1	1018.6 93.14 1017.1 95.20	0 1018.6 93.14 0 1017.1 95.20 8 1015.6 97.40 7 1014.1 99.6	0 1018.6 93.1 ⁴ 0 1017.1 95.2 ⁴ 8 1015.6 97.4 ⁴ 7 1014.1 99.6 ⁴ 6 1012.6 101.9 6 1011.1 104.3 7 1009.6 106.7 7 1008.1 109.3	0 1018.6 93.1-1 0 1017.1 95.2:1 8 1015.6 97.4:4 7 1014.1 99.6: 6 1012.6 101.9 5 1011.1 104.3 5 1009.6 106.7 4 1008.1 109.3 3 1006.6 111.9 2 1005.1 114.5 1 1003.6 117.1
	Quality.	9281	9248	9215		9149	9116	9085	9062 9051 9041	9030 9018 9007	8997 8985 8974	8964	1 8952	8952 8942 2 8930 2 8920	1 8952 0 8942 2 8930 2 8920 1 8908	1 8952 0 8942 2 8930 2 8920 1 8908	1 8952 0 8942 2 8930 2 8920 1 8908 9 8897 8886 8875 8865 8843 8832
	Specific Volume.	46.26 47.18 48.12	49.09 50.09 51.09	52.13 53.20 54.29	55.39 56.54 57.72	58.92 60.16 61.41	62.70 64.03 65.38	68.21	72.71	77.58	82.83	i	88.5	88.5 90.50 92.50 94.60	88.5 90.5 92.5 94.6 96.8	88.55 90.50 92.55 94.65 96.8 98.99	88.55 90.56 92.55 94.65 96.8 1 98.99 101.2 1 103.6 1 106.0
	Heat Contents.	1060.4 1059.0 1057.6	1056. 1 1054. 7 1053. 3	1051.8 1050.4 1049.0	1047.5 1046.1 1044.6	1043.2 1041.7 1040.3	1038.8 1037.4 1035.9	1034.5 1033.1 1031.6	1030. 1 1028. 7 1027. 2	1025 · 8 1024 · 3 1022 · 8	1021.4 1019.9 1018.4		1015.4	1015.4 1014.0 1012.5 1011.0	1015.4 1014.0 1012.8 1011.0 1009.8 1008.1	1015.4 1014.0 1012.8 1011.0 1009.8 1008.1 1005.1 1003.0 1002.1	1015.4 1014.6 1012.8 1011.6 1009.8 1008.1 1008.1 1003.1 1003.1 1003.1 1000.6 1000.1
	Quality.		9195 9184 9173	9162 9152 9141	9130 9119 9108	9097 9086 9076	9065 9054 9043	9032 9023 9012	9001 8990 8979	5 8957	8 8936 7 8925 0 8914		1 8892	1 8892 9 8881 9 8870 8 8860	8892 9 8881 9 8870 8 8860 5 8849	1 8892 9 8881 9 8870 8 8860 5 8849 2 8838 8827 8816 8806 8795	1 8892 9 8881 9 8870 8 8860 5 8849 2 8838 8827 8816 8806 8795
	Specific Volume.	45.94 46.85 47.78	48.75 49.74 50.74	51.77 52.83 53.91	55.00 56.14 57.32	58.52 59.75 60.99	62.27 63.59 64.93	66.32 67.74 69.19	70.68 72.21 73.79	75.41 77.05 78.74	80.48 82.27 84.10	04.10	85.99	85.99 87.91 89.89 91.89 93.98	85.99 87.91 89.89 91.89 93.98 96.18	85.99 87.91 89.89 91.89 93.98 96.18 98.32	85. 99 87. 91 89. 89 91. 89 93. 98 96. 15 98. 33 100. 6 102. 9
1.00	Heat Con- tents.	1054.0 1052.6 1051.2	1049.8 1048.3 1046.9	1045.5 1044.1 1042.7	1041.2 1039.8 1038.3	1036.9 1035.5 1034.0	1032.6 1031.1 1029.7	1028.3 1026.9 1025.4	1023.9 1022.5 1021.1	1019.6 1018.1 1016.7	1015.2 1013.8 1012.3	1012.3	1	1010.8 1009.4 1007.9	1010.8 1009.4 1007.9 1006.4 1005.0 1003.8	1010.8 1009.4 1007.9 1006.4 1005.0 1003.8 1002.0 1000.8 999.1	1010.8 1009.4 1007.9 1006.4 1005.0 1003.5 1002.0 1000.5 1999.1 997.6 998.1 994.6
	Quality.	9162 9152 9141	9131 9120 9109	9099 9088 9077	9066 9056 9045	9034 9024 9013	9002 8991 8981	8961	8928	8896	1 8864	8853	8853 6 8843	9 8853 6 8843 5 8832 6 8821 9 8810 3 8800	9 8853 6 8843 5 8832 6 8821 9 8810 8 8800 8 789 8 8778 8 8767	9 8853 6 8843 5 8832 6 8821 9 8810 9 8800 0 8789 8 8767 8757 3 8747 7 8736	9 8853 6 8843 5 8832 6 8821 9 8810 9 88767 8 8767 9 8757 3 8747 7 8736 4 8725 2 8715 2 8704
o I	Pressure, Pound per Square Inch.	7.50 7.34 7.17	7.01 6.86 6.70	6.55 6.41 6.26	6.12 5.98 5.84	5.71 5.58 5.45	5.32 5.20 5.08	4.960 4.844 04.729	4.617 34.508 74.400	4. 295 4. 191 4. 090	3.991 23.894	$\frac{3.799}{13.799}$	1 3. 799 0 3. 706 9 3. 615 8 3. 526	1 3.799	1 3. 799 0 3. 706 9 3. 615 8 3. 526 7 3. 439 6 3. 353	1 3. 799 0 3. 706 9 3. 615 8 3. 526 7 3. 439 6 3. 353 5 3. 270 4 3. 188 3 3. 108	1 3. 799 0 3. 706 9 3. 615 8 3. 526 7 3. 439 6 3. 353 5 3. 270 4 3. 188 3 3. 108 2 3. 029 1 2. 953 0 2. 873
9.8	Temperature, Degrees Fahr		177 176	174 173	171 170	168 167 166	165 164	161	158	158	159	159	155 155	155 156 149 149 149 141 141	152 153 154 144 144 144 144 144 144 144	15: 15: 15: 14: 14: 14: 14: 14: 14: 14: 14: 14: 14	15% 151 144 144 144 144 144 144 144 144 13
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5.84 5.71 5.58 5.45 5.32 5.20 5.08 4.960 4.844 4.729 4.617 4.500 4.295 4.4191 4.090 3.991 3.894	9421 1079. 9410 1078. 9399 1076. 9388 1075. 9365 1072. 9354 1069. 9383 1069. 9384 1066. 9308 10664. 9297 1063. 9208 1059. 9252 1057. 9241 1056. 9230 1054. 9218 1053. 9218 1053. 9218 1054. 9218 1053. 9218 1054. 9218 1054. 9218 1053. 9174 1047. 9163 1045. 9118 1039. 9152 1044. 9141 1042. 9141 1042. 9141 1042. 9141 1042. 9141 1042. 9141 1042. 9141 1042. 9163 1041.	1 48.17 9 49.13 9 49.13 9 7 49.13 9 7 51.14 9 8 52.16 9 8 53.22 9 9 55.42 9 9 55.42 9 14 56.54 9 9 57.71 9 5 58.92 9 16 60.15 9 16 62 9 17 69.62 9 18 68.15 9 18 68.15 9 18 68.15 9 18 74.20 9 18 77.48 9 18 77.4	9486 108 9486 108 9475 108 9486 108 94463 108 94429 107 94406 107 94406 107 94395 107 94383 107 94383 107 94383 107 94383 107	36.0 36.1	70. 08 71. 58 73. 12 74. 70 76. 33 78. 00 79. 70 81. 44 83. 24 85. 08	9539 9528 9516 9504 9493 9445 9470 9459 9446 9435 9423 9412 9300 9389 9377 9389 9377 9392 9297 9297 9286 9228	1.74 -uo (1092. 4 1090. 9 1089. 4 1085. 0 1083. 5 1082. 0 1077. 5 1077. 6 1077. 6 1077. 1 1068. 6 1067. 1 1068. 5 1069. 5 1055. 0 1055. 5 1055. 0 1055. 5 105	80.22 81.98	9532 9512 9510 9498 9486 9475 9463 9451 9440 9394 9382 9371 9359 9348 9312 9312 9301 9229	1.75 1098.7 1098.7 1099.8 1092.8 1092.8 1092.8 1088.8 1088.8 1088.8 1088.8 1089.8 1077.8 1076.3 1074.8 1076.3 1076.2 1062.7 1064.2 1062.7 1064.2 1062.7 1064.2 1065.6 1055.6 1055.6 1055.6 1055.6 1055.6	50. 14 51. 15 52. 19 53. 23 54. 31 55. 42 56. 55 57. 70 62. 66 63. 96 65. 29 66. 67 71. 02 72. 54 74. 09 75. 69 77. 34 79. 04 80. 75 82. 55 84. 34 86. 21
5.98 5.84	9308 9297 1063.	57.71 9 58.92 9	0372 107 0360 106	1.2 9.8	58.10 59.32	9435 9423	1077.5 1076.0	1	9498 9486	1083.8 1082.3	58.89 60.12
57 5.58 56 5.45	9263 1059.	61.41 9	339 106 326 106	6.8 5.3	61.82 63.11	9300 9389	1073.1 1071.6	62. 24 63. 53	9463 9451	1079.3 1077.8	62.66
65 5.32 64 5.20 63 5.08	9241 1056. 1 9230 1054. 0	65.35 9: 66.73 9:	292 106	0.8	65.79 67.18	9366 9354	1068. 6 1067. 1	67.63	9428 9416	1074.8 1073.3	66.67
61 4.844 60 4.729	9208 9197 1050.	7 69.62 95 71.10 95	259 105	6.4	70.08 71.58	9332 9321	1064. 1 1062. 6	70.55 72.06	9394 9382	1070.3 1068.8	71.02
59 4.617 58 4.508 57 4.400	9174 1047. 5 9163 1045. 5	74. 20 92 75. 82 92	236 105 224 105		- 1	9297 9286	1059.5 1058.1	75.20 76.83	9359 9348	1065.7	75.69
56 4. 295 55 4. 191 54 4. 090	9141 1042 .3 9129 1041 .3	80.90 91	202 104 190 104	8.9 7.3	79.70 81.44	9263 9251	1055. 0 1053. 5	81.98	9324 9312	1062.7 1061.2 1059.6	80.75
53 3.991 52 3.894 51 3.799	9107 9095 1036.	86.40 91	167 104 156 104	4.3 2.8	83. 24 85. 08 86. 97	9228	1050.5	85.64	9289	1058.1 1056.6 1055.0	84. 34 86. 21 88. 12
50 3.706 49 3.615 48 3.526	9084 1035. 2 9073 1033. 3 9062 1032. 2	$\begin{bmatrix} 90.31 & 91 \\ 92.34 & 91 \end{bmatrix}$	145 104 133 1039 122 1039	9.8 8.3	90.91 92.95	9193 9182	1047.4 1045.9 1044.4	91.51	9253	1053.5 1052.0 1050.5	90. 10 92. 11 94. 18
47 3.439 46 3.353 45 3.270	9050 1030.7 9039 1029.2 9028 1027.7	96.54 90	110 1036 099 1038 087 1038	- 1	97.18 99.42	9170 9159 9147	1042.8 1041.3 1039.8	97.82	9219	1048.9 1047.4 1045.8	96. 27 98. 45 100. 7
44 3.188 43 3.108 42 3.029	9016 9005 8994 1023. 1	103.3 90	076 1032 064 1030 053 1029	$\begin{array}{c} 2.2 \\ 0.7 \\ 0.2 \\ 0.2 \end{array}$	01.7 04.0 06.4	$ \begin{array}{c c} 9136 & 1 \\ 9124 & 1 \\ 9112 & 1 \end{array} $	038.3 036.7 035.2	02.3 04.6 07.1	9195 9183 9171	1044.3 1042.7 1041.2	103.0 105.3 107.8
41 2. 953 40 2. 877 39 2. 804	8984 1021.6 8972 1020.1 8961 1018.6	110.7 90	031 1026	7.6 10 3.1 1 4.6 1	11.4	9102 1 9090 1 9078 1	033.6 032.1 030.5	09.6 12.2 14.8	9161 9149 9137	1039.7 1038.1 1036.5	110.3 112.9 115.6
37 2.662	8950 8938 8927 1014.0	118.7 89	008 1023 996 1021 985 1019	3.011 1.511 0.912	16.7 19.5 22.3	9067 9055 1 9043	$\begin{array}{c} 029.0 \\ 027.4 \\ 025.9 \\ 1 \end{array}$	17.5 20.2 23.1	9126 9114 9102	1035.0 1033.4 1031.8	118.3 121.0 123.9
35 2.526	8915 1012.5	124.4 89	74 1018	3.4 12	25.2	9032 1	024.41	26.0	9090	1030.3	26.8

re, Fal	, Pour uare												
Temperature, Degrees Fa	Pressure, F per Squa Inch.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.
131	2.333 2.272 2.212	8650 8639 8628	984.2 982.7 981.2	130.1 133.2 136.4	8708 8697 8686	990.1 988.6 987.1	134.1	8765 8754 8743	996.0 994.5 993.0	135.0	8823 8812 8801	1001.9 1000.4 998.9	135.9
129 128 127	$\begin{array}{c} 2.153 \\ 2.096 \\ 2.040 \end{array}$	8618 8607 8596	979.7 978.2 976.7	$139.8 \\ 143.2 \\ 146.7$	8675 8664 8653	985.6 984.1 982.6	144.2	$\begin{array}{c} 8732 \\ 8721 \\ 8710 \end{array}$	991.5 989.9 988.4	141.7 145.1 148.7	8790 8779 8767	997.3 995.8 994.3	142.7 146.1 149.7
125	1.985 1.932 1.880	8585 8574 8563	975. 2 973. 5 972. 2	150.4 154.2 158.0	8642 8631 8620	981.0 979.5 978.0	155.2	8699 8688 8677	986. 9 985. 4 983. 8	156.2	8756 8745 8734	992.7 991.2 989.7	157.2
123 122 121	1.829 1.779 1.730	8553 8542 8532	970.7 969.1 967.6	166.0	8609 8598 8589	976. 5 974. 9 973. 4	167.1	8666 8655 8645	982.3 980.7 979.2	$164.0 \\ 168.2 \\ 172.5$	8722 8711 8701	988.2 986.6 985.1	165.1 169.3 173.6
119	1.683 1.636 1.591	8521 8510 8500	$966.1 \\ 964.6 \\ 963.1$	179.0	8577 8566 8556	971.9 970.4 968.9	175.7 180.2 184.8	8634 8623 8612	977.7 976.2 974.7	176.8 181.3 186.0	8690 8679 8668	983.5 982.0 980.4	182.5
116	1.547 1.504 1.462	8489 8478 8467	961.6 960.0 958.5	193.1	8545 8533 8523	967.4 965.8 964.3	194.4	8601 8589 8579	973.1 971.5 970.0	195.7	8656 8645 8634	978.9 977.3 975.8	196.9 I
114 113 112	1.421 1.381 1.342	8456 8445 8435	957.0 955.5 953.9	203.3 208.6 214.1	8512 8501 8490	$\begin{array}{c} 962.7 \\ 961.2 \\ 959.7 \end{array}$	$204.6 \\ 210.0 \\ 215.5$	8567 8556 8545	968.5 967.0 965.4	206.0 211.3 216.9	8623 8611 8600	974. 2 972. 7 971. 1	207.3 212.7 218.3
110	1.304 1.266 1.230	8424 8413 8402	952.4 950.9 949.4	225.6	8479 8468 8457	958.2 956.6 955.1	227.0	8534 8523 8512	963.9 962.3 960.7	228.5	8589 8578 8566	969.6 968.8 966.4	230.0
107	1.195 1.160 1.127	8392 8380 8370	947.8 946.3 944.7	237.7 244.0 250.6	8446 8435 8424	953.5 952.0 950.4	245.6	8501 8489 8478	959.1 957.6 956.0	240.8 247.2 253.8	8555 8544 8533	964.8 967.3 961.7	242.4 248.8 255.5
104	1.094 1.062 1.031	8359 8348 8337	943.2 941.6 940.1	264.5	8413 8402 8391	948.8 947.2 945.7	266.2	8467 8456 8445	954.5 952.9 951.4	$260.8 \\ 267.9 \\ 275.2$	8522 8510 8499	960.1 958.5 957.0	269.6
101	1.000 0.971 0.942	8326 8316 8305	938.5 937.0 935.4	286.8	8380 8370 8359	944.1 942.6 941.0	288.6	8434 8424 8412	$949.8 \\ 948.2 \\ 946.6$	282.7 290.5 298.4	8488 8478 8466	955.4 953.8 952.2	284.5 292.3 300.3
99 98 97	0.914 0.887 0.860	8294 8284 8273	933. 9 932. 3 930. 8	302.9 311.4 320.1	8348 8337 8326	939.5 937.9 936.4	$304.9 \\ 313.4 \\ 322.3$	8401 8390 8379	945.0 943.4 941.9	315.4	8455 8444 8432	950.6 949.0 947.5	308.8 317.4 326.2
95	0.834 0.809 0.784	8263 8252 8241	929.3 927.8 926.2	338.5	8316 8305 8294	934.8 933.3 931.7	$331.3 \\ 340.7 \\ 350.3$	8369 8358 8347	940.4 938.8 937.2	342.8	8422 8411 8399	946.0 944.4 942.8	345.0
93 92 91	0.761 0.737 0.715	8230 8219 8208	924. 6 923. 0 921. 5	368.3	8283 8272 8261	930.1 928.5 927.0	360.3 370.7 381.4	8335 8324 8313	935.7 934.1 932.5	362.6 373.0 383.8	8388 8377 8365	941.3 939.6 938.0	375.4
89	0.693 0.671 0.650	8197 8186 8175	919.9 918.3 916.7	401.1	8250 8238 8227	925.4 923.8 922.2	403.7	8302 8291 8279	930.9 929.3 927.7	394.8 406.2 417.9	8354 8343 8331	934.8	397.3 408.8 420.6
	0.630 0.610	8165 8154	$915.2 \\ 913.6$	$424.9 \\ 437.4$	8217 8206	$920.6 \\ 919.0$	$427.6 \\ 440.1$	8269 8257	926.1 924.5	$\frac{430.3}{442.9}$	8320 8309	931.6 930.0	433.0 445.7

) 061 9 319 7 8615 967 4 314 6 8668 973.0 310.0 	8 961. 2 321. 4 8603 965. 8 322. 4 8657 971. 3 325. 4 958. 5 330. 4 8592 964. 2 332. 4 8645 969. 8 334. 5 8 957. 0 339. 8 8581 962. 6 341. 9 8634 968. 2 344. 0 8 955. 4 349. 3 8569 961. 0 351. 5 8622 966. 6 353. 7 9 953. 8 359. 2 8558 959. 4 361. 5 8611 964. 9 363. 7 8 952. 2 369. 5 8546 957. 8 371. 8 8599 963. 3 374. 0 8 950. 6 380. 1 8534 956. 1 382. 4 8587 961. 6 384. 8
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$\begin{array}{c} 7\\ 264.1\\ 1271.3\\ 8618\\ 6278.7\\ 8607\\ 968.2\\ 280.5\\ 8661\\ 973.8\\ 8627\\ 968.2\\ 280.5\\ 8661\\ 973.8\\ 822.3\\ 8715\\ 975.4\\ 274.7\\ 8726\\ 978.2\\ 8672\\ 975.4\\ 274.7\\ 8726\\ 981.0\\ 276.5\\ 981.0\\ 276.5\\ 981.0\\ 276.5\\ 981.0\\ 276.5\\ 981.0\\ 276.5\\ 981.0\\ 276.5\\ 981.0\\ 276.5\\ 981.0\\ 276.5\\ 981.0\\ 276.5\\ 981.0\\ 276.5\\ 981.0\\ 276.5\\ 981.0\\ 276.5\\ 979.4\\ 284.0\\ 976.2\\ 299.7\\ 969.0\\ 306.0\\ 8680\\ 974.6\\ 307.9\\ 976.2\\ 299.7\\ 969.0\\ 306.0\\ 8680\\ 974.6\\ 307.9\\ 976.2\\ 299.7\\ 969.0\\ 306.0\\ 8680\\ 974.6\\ 307.9\\ 976.2\\ 299.7\\ 969.0\\ 306.0\\ 8680\\ 974.6\\ 307.9\\ 976.2\\ 299.7\\ 961.2\\ 325.4\\ 966.2\\ 332.4\\ 8645\\ 969.8\\ 334.5\\ 968.2\\ 344.5\\ 969.8\\ 334.5\\ 968.2\\ 344.0\\ 961.6\\ 363.7\\ 968.2\\ 344.0\\ 966.6\\ 353.7\\ 968.2\\ 345.5\\ 969.8\\ 334.5\\ 969.8\\ 335.7\\ 968.2\\ 346.6\\ 353.7\\ 968.2\\ 346.6\\ 353.7\\ 968.2\\ 346.6\\ 353.7\\ 968.2\\ 346.6\\ 353.7\\ 968.2\\ 346.6\\ 368.2\\ 966.6\\ 353.7\\ 968.3\\ 337.0\\ 8506.9\\ 953.8\\ 359.2\\ 8566.9\\ 957.8\\ 371.8\\ 8599.9\\ 963.3\\ 374.0\\ 966.6\\ 353.7\\ 964.9\\ 363.3\\ 374.0\\ 966.6\\ 363.4\\ 382.4\\ 3$
	5319. 4 8550 960. 2 321. 4 8603 965. 8 323. 4 8657 971. 3 325. 4 328. 3 8539 958. 5 330. 4 8592 964. 2 332. 4 8645 969. 8 334. 5 5 337. 6 8528 957. 0 339. 8 8581 962. 6 341. 9 8634 968. 2 344. 0 3 357. 0 8505 953. 8 359. 2 8558 959. 4 361. 5 8611 964. 9 363. 7 7 367. 2 8493 952. 2 369. 5 8546 957. 8 371. 8 8599 963. 3 374. 0 1377. 7 8482 950. 6 380. 1 8534 956. 1 382. 4 8575 966. 6 384. 8

93.8 280 11 91.2 275 12 90.0 272 11 88.7 270 11 87.4 267 1 86.2 265 1 85.0 262 1 83.8 260 1 82.6 257 1 81.4 255 1 80.2 252 1 77.9 247 1 76.8 245 1 77.4 6 240 1 77.4 6 240 1 77.4 232 1 87.4 235 1 80.2 252 1 80.2 252 1 81.4 255 1 80.2 255 1 80.2 255 1 80.2 255 1 80.3 247 1 80.4 247 1 80.5 247 1 80.6 240 1 80.6 240 1 80.7 240 1 80.8 245 1 80.9 247 1 80	282 13 287 13 277 13 275 13 272 270 14 265 1 265 1 257 1 255 1 257 1 255 1 247 1 245 1 240 1 245 1 240 1 237 1 245 1 242 1 240 1 237 1 235 1 247 2 245 1 247 2 247		324 323 321 320 318 317 315 314 317 315 317 317 317 318 319 317 318 319 319 319 319 319 319 319 319 319 319	oglobal de	235 232 229 227 224 222	1330 1328 1327 1325 1325 1322 1321 1318 1316 1315 1313 1311 1310 1308 1307 1308 1307 1308 1309 1298 1298 1298 1298 1298 1298 1298 129	outplox of the control of the contro	242 239	1325 1324 1322 1321 1318 1316 1314 1311 1311 1309 1308 1307 1305 1303 1302 1300 1298 1297 1293	7. 910 A. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1. 1.	298 295 292 290 287 284 3 281 275 272 270 267 2 264 4 261	Heat Columbia 1321 1320 1318 1317 1315 1313 1310 1308 1306 1305 1303 1302 1300 1308	sumploA 8.966 9.17 9.27 9.37 9.48 9.59 9.70 9.80 9.92 10.03 10.15 10.27 10.452
307 306 305 304 303 302	74.6 73.5 72.4 71.4 8 70.3 2 69.3	240 237 235 232 230 227	1298 1296 1295 1293 1292 1290	7.99 8.08 8.17 8.26	261 258 255 253 250 247	1307 1305 1304 1302 1301 1299	8. 16 8. 25 8. 34 8. 44 8. 54 8. 64	285 282 279 277 274 271	1318 1316 1314 1313 1311 1309	8. 45 8. 55 8. 64 8. 74 8. 84	298 295	1321 1320	8.96 9.06
305 304 303 302 301	72. 4 71. 4 70. 3 69. 3 68. 2	235 232 230 227 225	1295 1293 1292 1290 1289	8. 26 8. 35 8. 45 8. 55	250 247 245	1304 1302 1301 1299 1298	8. 44 8. 54 8. 64 8. 74	277 274 271 269	1314 1313 1311 1309 1308	8.55 8.64 8.74 8.84 8.95	298 295 292	1321 1320 1318	8.96 9.06 9.17
298 298 297 298 298	66. 2 65. 2 64. 3 63. 3 62. 3	220 217 214 212 209	1286 1284 1282 1281 1279	8.74 8.85 8.95 9.05 9.15	240 237 235 232 229	1295 1293 1292 1290 1288	8.94 9.04 9.14 9.25 9.35	258 255 252	1303 1302 1300 1298 1297	9. 27 9. 38 9. 49 9. 50 9. 70	284 281 278 275 275	1313 1312 1310 1308 1306	9.48 9.59 9.70 9.80
29: 29: 29: 29:	3 60.5 2 59.5 1 58.6 0 57.7 9 56.8	204 202 199 197	1278 1276 1275 1273 1272 1270	9. 20 9. 37 9. 49 9. 60 9. 70 9. 81	222	1285 1284	9.68	247 244 242 239 236	1295 1293 1292	9.80	270 267 2 264 4 261 5 258	1303 1302 1300 1298	10. 15 10. 27 10. 40 10. 52
28 28	8 56.0 7 55.1 6 54.2 5 53.4 4 52.6 3 51.7	189	1269 1267 1266 1264 1262 1260	9. 93 10. 05 10. 17 10. 29 10. 41 10. 53	209 206 203 1 201	1277 1276 1274 1272 1271 1269	10. 14 10. 20 10. 40 10. 52 10. 64 10. 77	231 228 225 223	1288 1286 1284 1282 1281 1279	10. 3 10. 5 10. 6 10. 7 10. 8 11. 0	252 3 250 5 247 8 244	1297 1295 1294 1292 1290 1288	10.64 10.77 10.90 11.03 11.16 11.30
28 28	2 50.9 1 50.1 0 49.3	177 174	1259 1257 1256	10.66 10.79	6 196 193	1268 1266 1265	10.90 11.00 11.10	217 215 212	1278 1276 1275	11.1 11.2 11.4	0 232	1287 1285 1283 1282	11.44 11.57 11.70

ure, Fah Poun are		1.80			1.81			1.82			1.83	
Temperature, Degrees Fah Pressure, Poun per Square	Quality.	Heat Con-	Specific Volume.	Quality.	Heat Con-	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.
324 95. 1 323 93. 8 322 92. 5												
321 91.2 320 90.0 319 88.7						·						
318 87.4 317 86.2 316 85.0												
315 83.8 314 82.6 313 81.4												
312 80.2 311 79.1 310 77.9			• • • • • • • • • • • • • • • • • • • •									
309 76.8 308 75.7 307 74.6												•••
306 73.5 305 72.4 304 71.4										•		•••
303 70.3 302 69.3 301 68.2												···
300 67. 2 299 66. 2 298 65. 2									:::			
297 64.3 296 63.3 295 62.3							• • • • • • • • • • • • • • • • • • • •					···
294 61. 4 293 60. 5 292 59. 5	298 295 292	1318 1316 1314	10. 19 10. 30 10. 41	•••						•••	•••	
291 58.6 290 57.7 289 56.8	289 286 283	1312 1311 1309	10.53 10.65 10.77	•••			•••		:::	•••	···	
288 56.0 287 55.1 286 54.2	280 277 274	1307 1306 1304	10.90 11.03 11.15	298	1314	11.43	•••			•••	•••	
285 53. 4 284 52. 6 283 51. 7	271 269 266 263	1302 1301 1299 1298	11. 28 11. 41 11. 55 11. 68	295 292 289	1313 1311 1309 1307	11.56 11.69 11.82						
282 50.9 281 50.1 280 49.33 279 48.55	260 257	1296 1294 1292	11. 81 11. 95 12. 10	286 283 280 277	1306 1304 1302	12. 09 12. 23 12. 38				•••	•••	

e, ahr	ound		1.76			1.11								
Temperature, Degrees Fahr.	Pressure, Pound per Square Inch.	Quality.	Heat Con- tents	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume,	Quality.	Heat Contents.	Specific Volume.	
275	46.26 45.52 44.78	162 159 157	1250 1248 1247	11.46 11.60 11.74	180 178 175	1258 1257 1255	11.70 11.85 12.00	201 198 196	1268 1266 1265	11.96 12.11 12.26	$\begin{array}{c} 221 \\ 218 \\ 215 \end{array}$	$\begin{array}{c} 1277 \\ 1275 \\ 1273 \end{array}$	12.27 12.41 12.57	
272	44.06 43.35 42.64	154 152 149	1245 1244 1242	11.88 12.02 12.17	173 170 167	$^{1254}_{1252}_{1250}$	12.16 12.30 12.45	193 190 188	$^{1263}_{1261}_{1260}$	12.40 12.57 12.73	$\frac{212}{210} \\ 207$	1272 1270 1269	12.71 12.88 13.03	
269	41.95 41.26 40.58	147 144 141	1241 1239 1237	12.33 12.49 12.63	$165 \\ 162 \\ 160$	$\begin{array}{c} 1249 \\ 1247 \\ 1246 \end{array}$	12.60 12.76 12.92	185 182 180	1258 1257 1255	12.88 13.04 13.20	$204 \\ 201 \\ 198$	1267 1265 1264	13.19 13.34 13.50	
266	39.91 39.26 38.60	139 137 134	1235 1234 1232	12 .80 12 .95 13.11	157 155 152	$\begin{array}{c} 1244 \\ 1243 \\ 1241 \end{array}$	13. 09 13. 25 13. 42	$177 \\ 174 \\ 172$	1253 1252 1251	13.37 13.54 13.71	195 193 190	1262 1261 1259	13.67 13.84 14.00	
264 263 262	37.96 37.33 36.71	$^{132}_{129}_{127}$	1231 1229 1228	13. 27 13. 44 13. 61	150 147 145	1240 1238 1237	13.59 13.76 13.93	169 166 163	1249 1247 1245	13.89 14.06 14.24	187 184 181	1257 1255 1253	14. 19 14. 37 14. 55	
261 260 259	36.09 35.48 34.88	$124 \\ 122 \\ 119$	1226 1225 1223	13.78 13.95 14.15	$\frac{142}{139}$ 137	1235 1233 1232	14.10 14.28 14.47	161 158 155	$\begin{array}{c} 1244 \\ 1242 \\ 1240 \end{array}$	14.41 14.60 14.79	178 176 173	1252 1250 1249	14.72 14.91 15.10	
257	34. 29 33. 71 33. 14	117 114 112	1222 1220 1219	14.33 14.51 14.70	$134 \\ 132 \\ 129$	1230 1229 1227	14.66 14.83 15.03	153 150 147	1239 1237 1236	14.99 15.17 15.38	170 167 165	1247 1245 1244	15.30 15.51 15.71	
254	32.57 32.01 31.46	109 107 104	1217 1216 1214	14.89 15.09 15.29	$^{127}_{124}_{122}$	1226 1224 1222	15. 22 15. 42 15. 62	144 142 139	1234 1232 1231	15.58 15.78 15.99	162 159 156	1242 1240 1239	15.91 16.13 16.34	
252 251 250	30.92 30.38 29.86	102 99 97	1212 1210 1209	15. 49 15. 68 15. 89	119 117 114	1220 1219 1217	15.82 16.01 16.23	136 134 131	1229 1228 1226	16.19 16.40 16.61	154 151 148	1237 1235 1234	16.56 16.77 16.99	
248	29.34 28.82 28.32	95 92 90	1208 1206 1205	16.10 16.31 16.52	$\frac{112}{109}$ $\frac{107}{107}$	1216 1214 1213	16.45 16.67 16.90	128 126 123	1224 1223 1221	16.83 17.05 19.27	145 143 140	1232 1231 1229	17.21 17.45 17.68	
245	27.82 27.33 26.85	87 85 82	1203 1202 1200	16.75 16.98 17.20	104 102 99	1211 1210 1208	17.12 17.36 17.59	120 118 115	1219 1218 1216	17.50 17.74 17.97	137 134 132	1227 1225 1224	17.91 18.15 18.40	
243 242 241	26.37 25.90 25.44	80 77 75	1198 1196 1195	17.44 17.69 17.91	96 94 91	1206 1205 1203	17.83 18.07 18.31	112 110 107	1214 1213 1211	18.21 18.46 18.71	129 126 124	1222 1220 1219	18.64 18.99 19.15	
239	24. 98 24. 53 24. 09	73 70 68	1194 1192 1191	18.16 18.40 18.66	89 86 84	1202 1200 1199	18.57 18.83 19.10	105 102 99	1210 1208 1206	18.96 19.23 19.50	121 119 116	1217 1216 1214	19.40 19.68 19.94	
236	23. 66 23. 23 22. 80	66 63 61	1189 1187 1186	18.93 19.20 19.46	81 79 76	1197 1195 1193	19.35 19.62 19.90	97 94 92	1205 1203 1202	19.77 20.04 20.32	113 111 108	1212 1211 1209	20.20 20.50 20.78	
234 233 232	22.39 21.98 21.57	59 56 54	1185 1183 1182	19.73 20.00 20.29	74 72 69	1192 1191 1189	20.19 20.48 20.75	89 87 84	1200 1199 1197	20.60 20.90 21.20	106 103 100	1208 1206 1204	21.06 21.35 21.65	
231	21.18 20.78	52 50	1180 1170	20.59	67 64	1188	21.03 21.34	82 79	1195	21.50 21.80	98 95	1203 1201	$\frac{21.95}{22.27}$	

 $21.20 \\ 21.50$

 $\bar{2}\bar{1}.80$

22.10

20.77 21.05 21.34

21.63

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192

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 $1243 \\ 1241$

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1238

re. Fahr.	ounds re		1.80			1.81			1.82			1.83	
Temperature, Degrees Fahr.	Pressure, Pounds per Square Inch.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Contents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Contents.	Specific Volume,
275	46.26 45.52 44.78	245 242 239	1287 1286 1284	12.54 12.69 12.84	267 264 261	1297 1295 1293	12.81 12.98 13.13	293 289 286	1308 1306 1304	13.11 13.27 13.44	• • • • • • • • • • • • • • • • • • • •		
272	$44.06 \\ 43.35 \\ 42.64$	236 233 230	1282 1280 1279	13.00 13.15 13.30	258 255 252	1292 1290 1288	13.29 13.45 13.61	283 280 277	1302 1301 1299	13.60 13.77 13.93	 299	13.08	 14. 25
269	41.95 41.26 40.58	$227 \\ 224 \\ 221$	$\begin{array}{c} 1277 \\ 1275 \\ 1274 \end{array}$	13.48 13.64 13.81	249 246 243	1287 1285 1283	13.78 13.94 14.11	273 270 267	1297 1295 1293	14.10 14.28 14.46	296 293 289	1306 1305 1302	14.43 14.60 14.78
266	39.91	218	1272	13.99	239	1281	14.30	263	1291	14. 62	286	1301	14.96
	39.26	215	1270	14.16	236	1279	14.49	260	1290	14. 81	282	1299	15.15
	38.60	212	1268	14.34	233	1277	14.65	257	1288	15. 00	279	1297	15.34
263	37.96	209	1267	14.51	230	1276	14.82	254	1286	15. 20	276	1295	15.54
	37.33	206	1265	14.70	227	1274	15.01	250	1284	15. 39	272	1293	15.73
	36.71	203	1263	14.89	224	1272	15.20	247	1282	15. 59	269	1291	15.92
260	36.09	200	1262	15.08	221	1271	15. 40	244	1281	15.79	266	1290	16.13
	35.48	197	1260	15.27	217	1269	15. 61	241	1279	15.98	262	1288	16.33
	34.88	194	1258	15.47	214	1267	15. 80	237	1277	16.19	259	1286	16.54
257	34. 29	192	1257	15.67	211	1265	16.00	234	1275	16.40	255	1284	16.75
	33. 71	189	1255	15.87	208	1263	16.23	231	1273	16.60	252	1282	16.96
	33. 14	186	1253	16.08	205	1262	16.45	228	1272	16.81	249	1280	17.19
254	32.57	183	1252	16.30	202	1260	16.67	225	1270	17.03	245	1278	17.40
	32.01	180	1250	16.50	199	1258	16.89	221	1268	17.26	242	1277	17.64
	31.46	177	1248	16.71	196	1256	17.10	218	1266	17.49	239	1275	17.87
251	30.92	174	1246	16.94	193	1255	17.32	215	1264	17.71	235	1273	18.10
	30.38	171	1245	17.16	190	1253	17.55	212	1263	17.95	232	1271	18.35
	29.86	168	1243	17.38	187	1251	17.78	209	1261	18.19	229	1269	18.60
248	29.34	165	1241	17.60	184	1250	18. 02	205	1259	18.42	226	1268	18.84
	28.82	162	1239	17.85	181	1248	18. 25	202	1257	18.68	222	1266	19.09
	28.32	159	1238	18.09	178	1246	18. 50	199	1255	18.92	219	1264	19.34
245	27.82	156	1236	18.32	175	1244	18.75	196	1254	19.19	216	1262	19.60
	27.33	153	1234	18.56	172	1243	19.00	193	1252	19.44	212	1260	19.85
	26.85	151	1233	18.81	169	1241	19.25	190	1250	19.70	209	1259	20.11
242	26.37	148	1231	19.08	166	1240	19.50	187	1249	19.95	206	1257	20.39
	25.90	145	1230	19.31	163	1238	19.77	184	1247	20.21	202	1255	20.65
	25.44	142	1228	19.59	160	1236	20.02	181	1245	20.50	199	1253	20.93

 $\begin{array}{c} 158 \\ 155 \end{array}$

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19.85 20.11

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20.66 149

 $1226 \\ 1224$

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240 24. 98 239 24. 53

238 24.09

237 23.66

 $\frac{1235}{1233}$

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20.30 20.58

20.85

21.15168

177 174

171

re, Fah	oun	Name and Address of the Owner, where the Owner, which is the Own	±.10		page of the specific						-	1	
Temperature, Degrees Fah	Pressure, Pound per Square Inch.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Hear Con- tents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.
1 227	20.02 19.64 19.28	45 43 41	1174	21.50 21.80 22.13	59 57 55	1183 1181 1180	$\begin{array}{c} 21.95 \\ 22.29 \\ 22.60 \end{array}$	74 72 69	1190 1189 1187	22.44 22.76 23.09	90 87 85	1198 1196 1195	22.90 23.24 23.58
224	18. 91 18. 56 18. 21	38 36 34	1170	22.47 22.80 23.14	52 50 48	1178 1177 1176	22. 93 23. 27 23. 60	67 65 62	1186 1185 1183	23, 41 23, 75 24, 10	82 80 77	1193 1192 1190	$23,90 \\ 24,25 \\ 24,60$
221	17.86 17.52 17.19	$\frac{32}{30} \\ 27$	1166	23.50 23.84 24.20	45 43 41	1174 1172 1171	23.95 24.31 24.67	60 57 55	1182 1180 1178	24, 45 24, 80 25, 18	75 72 69	1189 1187 1185	24.95 25.31 25.69
218	16. 86 16. 53 16. 21	$\frac{25}{23}$	1161	$24.55 \\ 24.93 \\ 25.30$	$\frac{39}{36}$	1170 1168 1166	25.05 25.41 25.80	52 50 48	1176 1175 1174	25, 55 25, 92 26, 30	67 64 62	1184 1182 1181	26.05 26.44 26.84
1 215	15.90 15.59 15.29	19 17 15	1157	25.68 26.05 26.45	$\frac{32}{30} \\ 28$	1165 1164 1163	26, 20 26, 60 27, 00	45 43 41	1172 1171 1169	26.70 27.10 27.50	59 57 54	1179 1178 1176	27. 25 27. 67 28. 10
212	14.99 14.70 14.41	$^{12}_{10}_{8}$	1152	26.85 27.29 27.70	25 23 21	1160 1159 1158	27.40 27.85 28.30	38 36 34	1167 1166 1165	27, 90 28, 35 28, 79	52 50 47	1174 1173 1171	28.52 28.95 29.40
209	14.12 13.84 13.57	$\begin{array}{c} 6 \\ 4 \\ 2 \end{array}$	1149	28.14 28.60 29.05	19 17 15	1156 1155 1154	28.71 29.17 29.63	32 29 27	1163 1161 1160	29, 23 29, 70 30, 20	45 42 40	1170 1168 1167	29.85 30.30 30.78
206	13. 29 13. 03 12. 77	9999 9987 9975	1145. 1 1143. 6 1142. 1	29, 26 29, 79 30, 33	$^{12}_{10}_{8}$	1152 1150 1149	30.10 30.55 31.05	25 22 20	1159 1157 1155	30 . 70 31 . 05 31 . 60	38 35 33	1166 1164 1162	$31.25 \\ 31.72 \\ 32.20$
203	$\begin{array}{c} 12.51 \\ 12.25 \\ 12.01 \end{array}$	9963 9951 9940	1140.6 1139.2 1137.8	$30.88 \\ 31.44 \\ 32.01$	6 4 2	1147 1146 1145	$ \begin{array}{r} 31.50 \\ 32.00 \\ 32.55 \end{array} $	18 16 14	1154 1153 1151	32.10 32.60 33.15	31 28 26	1161 1159 1158	32.70 33.20 33.75
200	11.76 11.52 11.28	9929 9917 9905	1136.3 1134.8 1133.4	33.20	9997 9985 9973	1142.9 1141.4 1139.9	33.43	11 9 7	1149 1148 1146	33.70 34.20 34.75	24 22 19	1156 1155 1153	34.30 34.85 35.40
197	11.05 10.82 10.60	9894 9881 9869	1131.9 1130.4 1128.9	34, 44 35, 08 35, 73	9961 9948 9936	1138.5 1136.9 1135.4	35, 32	5 3 0	1145 1144 1142	35.30 35.90 36.50	17 15 13	1152 1150 1148	36.00 36.60 37.20
	10.38 10.16 9.95	9857 9845 9834	1127. 4 1125. 9 1124. 5	37.10	9924 9912 9900	1134.0 1132.5 1131.0	37, 35	9991 9979 9967	1139.0	36, 91 37, 60 38, 31	10 8 6	1147 1145 1144	37.80 38.40 39.05
192 191 190	9.53	9822 9810 9798	1123.0 1121.5 1120.1	39.25	9888 9876 9864	1129.5 1128.0 1126.6	39.51	9955 9942 9930	1134.7	39.04 39.78 40.55	4 1 9997	1143 1141 1139.6	$ \begin{array}{r} 39.70 \\ 40.30 \\ \hline 40.82 \end{array} $
189 188 187	8.94	9787 9774 9763	1118.6 1117.1 1115.7	41.55	9853 9840 9829	1123.6	41.05 41.83 42.64	9919 9906 9894	1130.1	41.32 42.11 42.92	9985 9972 9960	11136. 5	41.60 42.39 43.21
186 186 184	8.37	9751 9739 9727	1114.2 1112.7 1111.2				43, 47 44, 32 45, 19		11125 (43.76 44.61 145.49	9947 9935 9923	1133.8 1132.0 1130.8	44.05 44.91 45.79

		1.80	(e)		1.81	- i		1,82			1.83	1 6	
Pressure, Pour per Square Inch.	Quality.	Heat Contents.	Specific Volume.	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Con-	Specific Volume.	Quality.	Heat Con-	Specific Volume,	
20. 02 19. 64 19. 28	106 104 101	1206 1205 1203	23.40 23.74 24.09	123 120 118	1214 1212 1211	23.94 24.27 24.61	141 138 135	1222 1221 1219	24.48 24.80 25.15	158 155 152	1230 1228 1227	25.00 25.38 25.74	
18.91 18.56 18.21	98 96 93	1201 1200 1198	24. 43 24. 80 25. 15	115 112 109	1209 1208 1206	24.97 25.34 25.72	$132 \\ 129 \\ 127$	1217 1216 1214	25.50 25.88 26.25	149 146 143	1225 1223 1222	26. 10 26. 49 26. 85	
17.86 17.52 17.19	90 88 85	1196 1195 1193	25.51 25.88 26.26	107 104 101	1205 1203 1200	26.10 26.47 26.86	124 121 118	1213 1211 1209	26. 64 27. 04 27. 44	140 137 134	1220 1218 1216	27. 25 27. 65 28. 05	-
16.86 16.53 16.21	83 80 78	1192 1190 1189	26.65 27.05 27.45	98 96 93	1199 1198 1196	27.25 27.67 28.09	115 112 110	1207 1205 1204	27.85 28.27 28.69	$131 \\ 128 \\ 126$	1215 1213 1212	28.45 28.88 29.30	
15.90 15.59 15.29	75 72 70	1187 1185 1184	27.85 28.29 28.70	90 88 85	1194 1193 1191	28.50 28.91 29.35	107 104 101	1202 1201 1199	29.10 29.53 29.97	$123 \\ 120 \\ 117$	1210 1208 1206	29.74 30.19 30.64	
14.99 14.70 14.41	67 65 62	1182 1181 1179	29.14 29.58 30.02	82 80 77	1189 1188 1186	29.80 30.24 30.70	98 96 93	1197 1196 1194	30.44 30.90 31.35	114 111 109	1205 1203 1202	31.10 31.55 32.05	
14.12 13.84 13.57	60 57 55	1178 1176 1175	30.48 30.95 31.40	74 72 69	1184 1183 1181	31.15 31.65 32.10	90 87 85	1192 1190 1189	31.85 32.35 32.85	106 103 100	1200 1198 1197	32.55 33.05 33.55	<u> </u>
13.29 13.03 12.77	52 50 47	1173 1171 1169	$\begin{array}{c} 31.90 \\ 32.40 \\ 32.90 \end{array}$	$\frac{66}{64}$	1179 1178 1176	32.60 33.10 33.60	82 79 77	1187 1186 1184	33.35 33.90 34.40	97 94 91	1195 1193 1191	34.05 34.60 35.10	
$12.51 \\ 12.25 \\ 12.01$	45 43 40	1168 1167 1166	33.40 33.95 34.50	59 56 54	1175 1173 1172	34. 10 34. 65 35. 20	74 71 69	1182 1181 1179	34.90 35.45 36.00	89 86 83	1190 1188 1187	35.60 36.15 36.70	
11.76 11.52 11.28	38 35 33	1165 1162 1160	35.05 35.60 36.15	51 49 46	1170 1169 1167	35.75 36.32 36.90	66 64 61	1178 1176 1174	36.55 37.10 37.65	80 78 75	1185 1183 1182	37. 30 37. 85 38. 45	
11.05 10.82 10.60	30 28 26	1158 1157 1156	36.75 37.35 37.95	44 41 39	1166 1164 1162	37. 49 38. 05 38. 64	58 56 53	1173 1171 1169	38. 25 38. 90 39. 50	72 69 67	1180 1178 1177	39. 05 39. 65 40. 30	
10.38 10.16 9.95	23 21 19	1154 1153 1151	38.57 39.20 39.85	36 34 31	1160 1159 1157	39.25 39.90 40.55	50 48 45	1168 1166 1164	40.14 40.77 41.47	64 61 59	1175 1173 1172	40.90 41.60 42.30	
9.74 9.53 9.33	16 14 12	1149 1148 1147	40.50 41.15 41.82	29 26 24	1156 1154 1153	41.23 41.90 42.62	43 40 38	1163 1161 1160	42.08 42.80 43.54	56 54 51	1170 1169 1167	43.00 43.70 44.40	*
9.13 8.94 8.75	9 7 5	1145 1143 1142	42.48 43.20 43.90	22 19 17	1151 1149 1148	43.35 44.05 44.80	35 33 30	1158 1157 1155	44.25 45.00 45.75	48 46 43	1166 1164 1162	45.20 45.95 46.70	
8.56 8.37 8.19	$\frac{2}{0}$		44.65 45.35 46.09	14 12 10	1146 1145 1143	45.50 46.25 47.05	28 25 23	1154 1152 1150	46.50 47.25 48.05	41 38 36	1161 1159 1157	47.50 48.30 49.10	
8 N1	0076	1125 1	17 00	7	1141	17 95	20	1118	48 00	33	1155	49 90	

15 9314 1058. 0 92. 71 9374 1064. 1 93. 31 9434 1070. 2 93. 91 9494 1076. 3 $94.\overline{5}$	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$\begin{array}{c} 1071.9 \\ 1070.4 \\ 77.85 \\ 9470 \\ 1076.6 \\ 1076.6 \\ 78.36 \\ 9532 \\ 1082.7 \\ 78.86 \\ 9593 \\ 1082.7 \\ 78.86 \\ 9593 \\ 1088.9 \\ 77.19 \\ 9605 \\ 1090.4 \\ 77.68 \\ 9593 \\ 1088.9 \\ 77.37 \\ 1088.9 \\ 79.37 \\ 1088.9 \\ 79.55 \\ 9488 \\ 1071.9 \\ 83.60 \\ 9495 \\ 1071.9 \\ 83.60 \\ 9495 \\ 1078.0 \\ 84.14 \\ 9556 \\ 1084.2 \\ 84.68 \\ 1064.2 \\ 84.89 \\ 9422 \\ 1071.9 \\ 83.60 \\ 9495 \\ 1071.0 \\ 84.14 \\ 9556 \\ 1084.2 \\ 84.68 \\ 1082.7 \\ 86.54 \\ 1081.2 \\ 84.68 \\ 1082.7 \\ 86.54 \\ 1081.2 \\ 84.68 \\ 1082.7 \\ 86.54 \\ 1082.3 \\ 1082.7 \\ 86.54 \\ 1082.3 \\ $
	26 9302 1056.5 94.79 9362 1062.6 95.40 9422 1068.7 96.01 9482 1074.8 96.62 39 9290 1055.0 96.89 9350 1061.0 97.52 9410 1067.1 98.14 9470 1073.1 98.77 53 9278 1053.4 99.09 9338 1059.5 99.73 9398 1065.5 100.4 9458 1071.6 101.0 9266 1051.8 101.4 9326 1057.9 102.0 9385 1063.9 102.7 9445 1070.0 103.3

Temperature, Degrees Fal	Pressure, Pour per Square Inch.	.ty.	Con- ts.	fie ume.	ty.	Con-	Specific Volume.	ty.	Heat Con- tents.	Specific Volume.	ity.	Heat Con- tents.	Specific Volume.
Temp	Pressu per Incl	Quality.	Heat Con- tents.	Specific Volume.	Quality.	Heat Contents.	Speci Vol	Quality	Heat ten	Speci	Quality	Heat	Speci
170	7.50 7.34 7.17	9939 9926 9914	1130.7 1129.2 1127.7	49.83 50.81 51.82		1137 1135. 6 1134. 1	50.33 51.14 52.16	13 10 8	1144 1142 1140	51.35 52.20 53.20	25 23 20	1150 1149 1147	52.40 53.30 54.30
176	7.01 6.86 6.70	9902 9889 9877	1126.2 1124.6 1123.0	52.87 53.93 55.01	9966 9953 9940	1132.5 1130.9 1129.4	53.21 54.28 55.37	5 3 0	1139 1137 1136	54. 20 55. 19 56. 10	18 15 13	1146 1144 1142	55.20 56.10 57.10
173	6.55 6.41 6.26	9864 9852 9840	1121.5 1120.0 1118.4	56.13 57.27 58.44	9916	1127.9 1126.3 1124.8	56.49 57.64 58.81	9992 9979 9967	1134.2 1132.6 1131.1	56.85 58.01 59.19	10 8 6	1140 1139 1138	58.10 59.20 60.20
170	6.12 5.98 5.84	9827 9814 9802	1116.8 1115.3 1113.8	60.85	9877	1123.1 1121.6 1120.0		1	1129.5 1127.9 1126.3	61.63	1_1_	$\begin{array}{ c c c }\hline 1136 \\ 1134 \\ \hline 1132.6 \\ \hline \end{array}$	61.30 62.40 63.31
167	5.71 5.58 5.45	9789 9777 9765	1112.2 1110.6 1109.1	64.73	9852 9840 9827	1118.5 1116.9 1115.3	65.15	9915 9902 9890	1124. 8 1123. 2 1121. 6	65.56	9966	1131.0 1129.4 1127.9	65.98 67.35
168 168 168	5.32 5.20 5.08	9752 9740 9727	1107.5 1106.0 1104.4	68.88	9815 9802 9789	1113.8 1112.2 1110.6	69.32	9877 9864 9852	1120.0 1118.4 1116.9	69.76 71.2	9927 9914	1	71.68
16:	$\begin{array}{c} 4.960 \\ 4.844 \\ 4.725 \end{array}$	9704	1102.8 1101.3 1099.7	71.83 73.30 74.93	9777 9766 9753	1109.0 1107.5 1105.9	73.83	9839 9828 9815	1115.3 1113.7 1112.1	75.8	9877	1118.3	74.77
15	9 4.61 8 4.50 7 4.40	9666	1098.2 1096.6 1095.1	76.53 78.1 79.8	3 9740 8 9728 8 9716	1104.4 1102.8 1101.5	78.68 80.39	9789 9777	1110.8 1108.9 1107.4	979.1	9838	1115. 1113.	79.6 81.4
15	6 4. 29 5 4. 19 4 4. 09	1 9629	1093. 1091. 1090.	83.4	3 9703 0 9690 2 9677	1099. 1098. 1096.	0 83.93	9764 9751 9738	1105.8 1104.5 1102.	82.6 284.4 686.3	$ \begin{array}{c c} 6 & 9812 \\ 0 & 9799 \end{array} $	1110. 1108.	3 84.9 7 86.8
15 15 15	3 3.99 2 3.89 1 3.79	1 9605 4 9592 9 9579	1088. 1087. 1085.	1 89.0	9 9665 2 9653 9 9640	1094. 1093. 1091.	87.6 89.5 6 91.5	9726 9713 9700	1101.0 1099.4 1097.	$ \begin{array}{c c} 0 & 88.2 \\ 4 & 90.1 \\ 8 & 92.1 \end{array} $	5 9774	1105.	$ \begin{array}{c c} 5 & 90.7 \\ 9 & 92.7 \\ \end{array} $
15 14 14	0 3.70 9 3.61 8 3.52	6 9567 5 9554 6 9542	1084. 1082. 1080.	4 95.1	3 9628 1 9615 4 9602	1090. 1088. 1086.	5 95.7	0 9675	1096. 1094. 1093.	2 94.2 6 96.3 0 98.4	0 9748 0 9738 6 9723	5 1100. 3 1099.	6 96.9 1 99.0
14 14 14	3.43 6 3.35 5 3.27	9530 9518 9505	1079. 1077. 1076.	2 99.3 7 101.6 0 104.0	9590 9577 9564	1085. 1083. 1082.	3 100.0 7 102.3 1 104.6	9650 9637 9624	1088.	3 100. 8 102. 1 105.	3 968	7 1095. 4 1094.	8 103.6
14 14 14	3. 18 3. 10 2. 3. 02	9493 9480 9468	1072.	5 106.3 8 108.7 3 111.2	9552 9539 9527	1078.	5 107.0 9 109.4 3 111.9	9599	1084.	5 107. 9 110. 3 112.	1 965	8 1090. 5 1089.	6 108.3 9 110.8 3 113.3
14	2.98 2.87 39 2.80	77 9444	L 1068.	7 113.9 0 116.5 5 119.5	9503	1074.	7 114.6 0 117.3 4 120.1	9562	1080. 1078.	7 115. 0 118. 4 120	0 962 8 960	1 1086 8 1084	7 116. 0 118. 4 121.
13	38 2.73 37 2.66 36 2.59	62 9406	i 1063.	9 122. 2 124. 6 127.	9465	1070. 1069. 1067.	8 122.8 2 125.7 6 128.6	9537 9523 9511		8 123 1 126 5 129	6 959 5 958 4 956	2 1081	. 8 124. . 1 127. . 5 130.
13	3 5 2. 5	26 938	1060.	0 130.	9440	1066.	0 131.7		3 1071. 1070	9 132	. 5 955 7 954	$\begin{array}{c c} 7 & 1077 \\ 3 & 1076 \end{array}$. 9 133. 2 136.

ıture,	S La	, Fou juare		l è	ne.	participant is not	ģ			-1	E.e.	***	ė	j.
Temperature,	außact I	per Squ Inch.	Quality.	Heat Con- tents.	Specific Volume	Quality.	Hest Can-	Zaria de la companya		4 1 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2		Quality.	Heat Con- tents.	Specific Volume.
13	1 2	. 333 . 272 . 212	9113 9101 9089	1031.5 1029.9 1028.3	140.3	9170 9159 9147	$1037.4 \\ 1035.8 \\ 1034.2$		9228 9216 9204	1043 3 1041 7 1040 1	142.1	9286 9274 9262	1049. 2 1047. 6 1046. 0	143 C
12	8 2	. 153 . 096 . 040	9077 9065 9053	1026.8 1025.2 1023.6	150.8	9135 9123 9111	1032.7 1031.1 1029.5	151.8	9192 9180 9168	1038 5 1036 9 1035 3	152/8	9250 9237 9225	1044.4 1042.8 1041.2	153.7
12	5 1	. 985 . 932 . 880	9041 9030 9018	1022. 0 1020. 5 1018. 8	162.4	9099 9086 9074	1027 9 1026 3 1024 7	163 4	9156 9143 9131	1033 7 1032 2 1030 5	164 4	9213 9200 9188	1039, 6 1038, 0 1036, 3	165.4
12	2 1	. 829 . 779 . 730	9006 8994 8983	1017.3 1015.6 1014.0	174.7	9062 9050 9040	1023 1 1021 4 1019 9	175 S	9119 9107 9096	1029 0 1027 3 1025 7	172 6 176 9 181 5	9176 9163 9152	1034, 8 1033, 1 1031, 5	178.0
11	9 1	. 683 . 636 . 591	8971 8959 8948	1012.5 1010.9 1009.3	188.4	9027 9015 9004	1018.3 1016.7 1015.1	189 6	9054 9071 9060	Iugo 9	190 S 195 7	9140 9127 9116	1029, 9 1028, 3 1026, 6	187. 2 191. 9 196. 9
111	6 1	. 547 . 504 . 462	8936 8923 8912	1007.7 1006.1 1004.5		8991 8979 8968	1013.5 1011.8 1010.2	204 5	9047 9005 9023	1019 2 1017 5 1015 9	200 7 205 8 211 1	9103 9090 9079	1025.0 1023.3 1021.7	207.1
11:	3 1.	. 421 . 381 . 342	8900 8888 8876	1002.9 1001.3 999.7	219.5°	8955 8943 8931	1008 6 1007 0 1005 4	220 9	9014 8998 8986	1014 3 1012 7 1011 1	216 6 222 3 228 1	9066 9054 9042	1020. 1 1018. 4 1016. 8	223.6
110) [. 304 . 266 . 230	8864 8852 8840	998.1 996.4 994.8	237.3	8907	1003 S 1002 I 1000 S	238 N	8970 8962 8950	1007 S 1007 S 1001 2	240 3.	9029 9017 9004	1015.2 1013.5 1011.9	241.7
10	7 1.	. 195 . 160 . 127	8829 8816 8805	993.2 991.6 989.9	95A 7	8883 8871 8859	998.9 997.3 995.6	258 3	8938 8925 8913	1004 S 1002 S 1001 2		8992 8980 8968	1010.2 1008.6 1006.9	261.5
104	L 1.	. 094 . 062 . 031	8793 8781 8769	988.3 986.7 985.1	270 8 278 2 285 8	8847 8835 8823	993 0 992 3 990 7		8901 8889 8877	900 6 907 9 106 3	281 6.	8956 8943 8931	1005.3 1003.6 1002.0	283.3
101	.]0.	.000 .971 .942	8757 8746 8734	983.4 981.8 980.2	301.6	8811 8800 8787		295 3 303 4 311 7	8865 8854 8841	994 7 993 0 991 3	305 3	8919 8907 8894	1000-3 998-6 996-9	307.1
98	B)0.	. 914 . 887 . 860	8722 8710 8698	978.6 976.9 975.3	327.4	8775 8763 8751	984. 1 982. 5 980. 9	329 4	8829 8817 8805	unu 7 unu u unu 4	331 4	8882 8870 8858	995, 3 993, 6 992, 0	333.4
96 95 94	0. 0. 0.	834 809 784	8687 8675 8663	973. 7 972. 1 970. 4	355.9	8740 8728 8716	979 3 977 7 976 0	358 0.	8793 8781 8769	1984 N 1983 2 1981 5	350 3 360 2 370 4	8846 8834 8822	990.4 988.8 987.1	362.4
92	0.	761 737 715	8651 8639 8627	968.8 967.2 965.5	387. I	8704 8692 8680	974 4 972 7 971 0	378 6 389 5 400 7	8757 8744 8732	979 9 978 2 978 5	380 9 391 8 403 2	8809 8797 8785	985.4 983.7 982.0	394.2
89	0.	693 671 650	8615 8603 8591	963.84 962.24 960.54	109.7 121.6 133.7	8668 8656 8643	969, 3 967, 7 966, 0	424 1	8720 8708 8695	974 8	414.7 426.7	8772 8760 8747	980.3 978.6 976.9	429.2
87	0.	630	8580	958.94	46.5	8632	964.4	449 2	KOK4	969 8	451 9	8736	975.3	454 R

	Specific	14	15 15 16	163 163 173	178 182 187	191 196 201	206 212 217	223 229 235	241 247 254	267	290	306 314 323	332 341 350	360 371 381	392 403 415	439	465
1.83	Heat Con- tents.	1072.9 1071.3 1069.6	1068.0 1066.3 1064.7	1063.0 1061.4 1059.7	1058. 1 1056. 3 1054. 7	1053.0 1051.4 1049.7	1048.0 1046.3 1044.7	1043.0 1040.4 1039.7	1038. 0 1036. 3 1034. 7	1032.9 1031.2 1029.5	$027.8 \\ 026.1 \\ 024.5$.022.8 .021.1 .019.3	017.6 015.9 013.3	012.6 010.9 009.2	007.5 005.8 004.1	002.3 000.6 998.8	997.1
	Quality.	9518 9505 9492	9479 9466 9454	9441 9428 9415	9402 9389 9378	9365 9352 9339	9326 9313 9301	9288 9275 9262	9249 9237 9223	9198	9159	9134 9122 9109	9096 9083 9070	9059 9046 9033	9020 9007 8994	8981 8968 8955	8943
	Specific Volume.	142.3 145.7 149.2	156.6	1644 168.5 172.7	176.9 181.3 186.0	190.6 195.5 200.5	205.6 210.9 216.3	227 7	239.9 246.2 252.7	259.4 266.3 273.4	80.8 88.5 96.3	04.4 12.7 21.2	30. 2 39. 4 48. 9	58.8 68.9 89.3	90.1 01.3 12.8	36.9	62.7
1 .82	Heat Con- tents.	1067. 0 1065. 4 1063. 7	1062. 1 1060. 4 1058. 8	1057. 1 1055. 5 1053. 8	1052. 2 1050. 5 1048. 9	1047. 2 1045. 6 1044. 0	1042.3 1040.6 1039.0	1037.3 1035.6 1033.9	1032.3 1030.6 1028.9	1027. 2 1025. 6 1023. 9	1022. 2 1020. 5 1018. 8	1017. 1 3 1015. 4 3 1013. 7 3	1012. 0 1010. 3 1008. 7	1007. 1 1005. 4 1003. 7	1001.9 1000.2 998.5	996.8 4 995.1 4 993.4 4	991.74
	Quality.	9460 9447 9435	9422 9409 9396	9384 9371 9358	9345 9333 9321	9309 9296 9283	9271 9257 9245	9219	9194 9182 9169	9156 9143 9131	9118 9105 9093	9080 9068 9055	9043 1 9030 1 9017 1	9005 8993 1 8980	8967 8955 8942	8916	8891
1.81	Heat Contents. Specific Volume.	1061.1 141.4 1059.4 144.8 1057.8 148.2	1056. 2 152. 0 1054. 6 155. 6 1053. 0 159. 4	1051.3 163.4 1049.7 167.5 1048.0 171.6	046. 4 175. 8 044. 7 180. 2 043. 1 184. 8	041. 5 189. 5 039. 9 194. 3 038. 2 199. 3	036. 5 204. 4 034. 8 209. 6 033. 2 215. 0	031.5 220.6 029.9 226.4 028.2 232.2	026. 6 238. 4 024. 9 244. 7 023. 3 251. 2	$\begin{array}{c} 021.6 \\ 019.9 \\ 018.2 \\ 271.7 \end{array}$	016.5 279.2 014.8 286.7 013.2 294.6	011.5 302.6 009.8 310.8 008.1 319.3	006. 5 328. 3 004. 8 337. 4 003. 2 346. 8	001. 5 356. 7 999. 8 366. 7 998. 1 377. 1	994.7 398.9	989.6 434.3	86.2460.0
	Quality.	9402 9389 9377	9364 9352 9339	9314	9289 9276 9265	9240	9202 1	9164 []	9127 1	9102 9089 1 9076	9064 9051 9039	9026 9015 9002	8989 8977 8964	8952 8940 8927	8915 8902 8889	8864 1	8839
	Specific Volume.	140.5 143.9 147.3	151.1 154.7 158.4	166.4l	179.1 183.7	188.3 193.1 198.1	203.1 208.3 213.7	219.3 225.0 230.9	237.0 243.2 249.7	256.3 263.1 270.1	277.5 285.0 292.8	10 00	35.4	64.5	85.5 96.5 08.0	19.7 31.8 44.2	57.3 70.7
1.80	Heat Con- tents.	1055.2 1053.5 1051.9	1050.3 1048.7 1047.1	1045.4 1043.8 1042.2	1040.6 1038.9 1037.3	1035.7 1034.1 1032.4	1030.8 1029.1 1027.5	1025.8 1024.2 1022.5	1020.9 1019.2 1017.6	1015.9 1014.3 1012.6	1010.9 1009.2 1007.6	1005.9 1004.2 1002.5	1001.93 999.23 997.63	996.03 994.33 992.63	990.9 989.2 987.5	985.8 984.1 982.4	980.74
	Quality.	9344 9332 9319	9307 9295 9282	9270 9257 9245	9232 9220 9209	9196 9184 9171	9159 9146 9134	9122 9109 9097	9084 9072 9059	9047 9034 9022	9010 8997 8985	8961	8936 8923 8911	8899 8887 887 4	8862 8850 8837	8825 8812 8799	8787 8775
oun	Pressure, Poun- per Square Inch.	2.333 2.272 2.212	2.153 2.096 2.040	1.985 1.932 1.880	1.829 1.779 1.730	1.683 1.636 1.591	1.547 1.504 1.462	1.421 1.381 1.342	1.304 1.266 1.230	1. 195 1. 160 1. 127	1.094 1.062 1.031	0.971	0.887	0.809	0.737	0.671). 630). 610
re, Fahi	Temperature, Degrees Fab	132 131 130	128	125	122	119	116	1113	111 110 109	107	104	101	99 98 97	96 95 94	99	89	87 86

		0	1	2	3	4	5	6	7	8	9
	1.0	0.0000	0.00995	0.01980	0.02956	0.03922	0.04879	0.05827	0.06766	0.07696	0.08618
	1.1 1.2 1.3	$\begin{array}{c} 0.09531 \\ 0.1823 \\ 0.2624 \end{array}$	$\begin{array}{c} 0.1044 \\ 0.1906 \\ 0.2700 \end{array}$			0.2151		0.2311	0. 1570 0. 2390 0. 3148	$egin{array}{c} 0.1655 \ 0.2469 \ 0.3221 \end{array}$	0. 1739 0. 2546 0. 3293
	1.4 1.5 1.6	0.3365 0.4055 0.4700	$\begin{array}{c} 0.3436 \\ 0.4121 \\ 0.4762 \end{array}$	0.4187	0.4253	$0.4318 \pm$	0.4382	0.4447	$\begin{array}{c} 0.3853 \\ 0.4511 \\ 0.5128 \end{array}$	$\begin{array}{c} 0.3920 \\ 0.4574 \\ 0.5188 \end{array}$	0.3988 0.4637 0.5247
	1.7 1.8 1.9	0.5306 0.5878 0.6418	0.5933	0.5988	0.6043	0.6098^{-5}	0.6152%	0 6206	0.6259	0, 5766 0, 6313 0, 6831	$\begin{array}{c} 0.5822 \\ 0.6366 \\ 0.6881 \end{array}$
	2.0	0.6931	0.6981	0.7031	0.7080	0.7129	0,7178	0.7227	0.7275	0.7324	0.7372
	2.1 2.2 2.3	0.7884	0.7930	0.7975	0.8020%	0.8065%	$0.8109 \pm$	0.8154 \pm	0.8198	0.7793 0.8242 0.8671	$egin{array}{c} 0.7839 \ 0.8286 \ 0.8713 \end{array}$
	2.4 2.5 2.6	0.9163	0.9203	0.9243 - 0	0.9282 (0.9322 (1.9361 (3 35400 (9439	0.9478	0.9123 0.9517 0.9895
ı	2.7 2.8 2.9	1.0296	1.0332	1.0367	1.0403	1.0438 4	1.0473	0508	0543	1.0578	1.0260 1.0613 1.0953
	3.0	1.0986	1.1019	1.1053	1.1086	$\mathfrak{l}_{\parallel}^{+}$ erri.	. 1151 - 1	1.1184	1.1217	1.1249	1.1282
1	3.1 3.2 3.3	1.1632	1.1663 1	1.1694 1	1.1725 - 1	1.1756 - 1	. 1787 -1	1817 [1	. 1848	1.1878	1.1600 1.1909 1.2208
		1.2528	1.2556	1.2585 1	.2613 1	.2641 - 1	.2669 - 1	, 2098 1	. 2726	. 2754	1.2499 1.2782 1.3056
H	3.8	1.3350	1.3376 1	. 3403 [1	.3429 [1	, 3455 1	.34×1 1	3507 1	. 3533 1	. 3558	1,3324 1,3584 1,3838
ŀ	1.0	1.3863	1.3888	. 3913 1	. 3938 1	$,3962\left[1\right.$.3987 1	4012 1	4036	. 4061	1.4085
14	.2	1.4351 [1	1.4375 1	. 4398 [1	. 4422 1	4446 1	4469 1	4493 1	. 4516 1	. 4540	. 4327 . 4563 . 4793
4	.5	1.5041 1	.5063 1	.5085 1	.5107 1	5129 1	5151 1	5173 1	5195 1	.5217 1	. 5019 . 5239 . 5454
4	.8	1.5686 1	.5707 1	.5728 1	.5748 1	5769 1	5581 1 5790 1 5994 1	5810 1	5x31 1	. 5851 1	. 5665 . 5872 . 6074
8	.0	1.6094 1	. 6114 1	. 6134 1	6154 1	6174 1	6194 1	6214 1	. 6233 1	. 6253 1	. 6273
5	.2	1.6487 1	.6506 1	. 6525 1	6544 1	6563 1.	6582 1	6601 1	.6620 1	. 6639 1	. 6467 . 6658 . 6845
5	.5	1.7047 1	$\begin{array}{c ccccccccccccccccccccccccccccccccccc$. 6901 1 . 7884 1 . 7263 1	$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	6938 1 7120 1		6974 1 7156 1		.7011 1 .7192 1	.7029 .7210

NAPERIAN LOGARITHMS.

1	0	1	2	3	4	5	6	7	8	9
	1.7405 1.7579 1.7750	1.7422 1.7596 1.7766	1.7440 1.7613 1.7783	1.7457 1.7630 1.7800	1.7475 1.7647 1.7817	1.7492 1.7664 1.7834	1.7509 1.7681 1.7851	1.7527 1.7699 1.7867	1.7544 1.7716 1.7884	1.7561 1.7733 1.7901
	1.7918	1.7934	1.7951	1.7967	1.7984	1.8001	1.8017	1.8034	1.8050	1.8066
1	1.8083 1.8245 1.8405	1.8099 1.8262 1.8421	1.8116 1.8278 1.8437	1.8132 1.8294 1.8453	1.8148 1.8310 1.8469	1.8165 1.8326 1.8485	1.8181 1.8342 1.8500	1.8197 1.8358 1.8516	1.8213 1.8374 1.8532	1.8229 1.8390 1.8547
	1.8563 1.8718 1.8871	1.8579 1.8733 1.8886	1.8594 1.8749 1.8901	1.8610 1.8764 1.8916	1.8625 1.8779 1.8931		1.8656 1.8810 1.8961	1.8672 1.8825 1.8976	1.8687 1.8840 1.8991	1.8703 1.8856 1.9006
	1.9021 1.9169 1.9315	1.9036 1.9184 1.9330	1.9051 1.9199 1.9344	1.9066 1.9213 1.9359	1.9081 1.9228 1.9373	1.9242	1.9110 1.9257 1.9402	1.9125 1.9272 1.9416	$\substack{1.9140\\1.9286\\1.9430}$	1.9155 1.9301 1.9445
	1.9459	1.9473	1.9488	1.9502	1.9516	1.9530	1.9544	1.9559	1.9573	1.9587
	1.9601 1.9741 1.9879	1.9615 1.9755 1.9892	1.9629 1.9769 1.9906	1.9643 1.9782 1.9920	1.9657 1.9796 1.9933	1.9810	1.9685 1.9824 1.9961	1.9699 1.9838 1.9974	1.9713 1.9851 1.9988	1.9727 1.9865 2.0001
15	2. 0015 2. 0149 2. 0281	$egin{array}{c} 2.0028 \ 2.0162 \ 2.0295 \ \end{array}$	2.0176	2.0055 2.0189 2.0321	2.0202	2.0215	2.0096 2.0229 2.0360	2.0242	2.0122 2.0255 2.0386	2.0136 2.0268 2.0399
12	2. 0412 2. 0541 2. 0668	2.0425 2.0554 2.0681	2.0567	2 0580	2.0592	2.0605	2.0618	2.0631	2.0516 2.0643 2.0769	2.0528 2.0656 2.0782
5	2.0794	2.0807	2.0819	2.0832	2.0844	2.0857	2.0869	2.0881	2.0894	2.0906
2		2.1054	2.1066	2.1078	2.1090	2.1102	2.1114	2.1126	2. 1017 2. 1138 2. 1258	2.1029 2.1150 2.1270
19		2.1412	2.1424	2.1436	2.1448	2.1459	2.1471	2.1483	2.1377 2.1494 2.1610	2.1389 2.1506 2.1622
2	2.1748	2.1759	2.1770	2.1782	2.1793	2.1804	2.1815	2.1827	$egin{array}{ccc} 2.1725 \ 2.1838 \ 2.1950 \ \end{array}$	2.1736 2.1849 2.1961
2	2. 1972	2.1983	2.1994	2.2006	2.2017	2. 2028	2. 2039	2.2050	2.2061	2.2072
2	2.2192	2.2203	2. 2214	2. 2225	2.2235	2. 2246	2.2257	2.2268	2.2170 2.2279 2.2386	2.2181 2.2289 2.2396
222	2. 2513	2.2523	2. 2534	2. 2544	2. 2555	2. 2565	2.2576	2.2586	2. 2492 2. 2597 2. 2701	2.2502 2.2607 2.2711
12	. 2824	2. 2834	2. 2844	2. 2854	$2.2865 \mid :$	2.2875	2. 2885	2.2895	2. 2803 2. 2905 2. 3006	2.2814 2.2915 2.3016
2	3026									

									,										
											1		Pr	ры	tion	ial]	Par	ta.	
Nat. Nos.	0	1	2	3	4	5	6	7	8	: 9 : :		L 2	3	4	5	6	7	8	9
11	0000 0414 0792	0453	0492	0128 0531 0899	0569	0607	0253 0645 1004	0682 1038	0719	0374 0755 1106	:	1 8	10	15	19 17	$\frac{23}{21}$	26 24	$\frac{30}{28}$	34
13	1139 1461	1173	1206	1239 1553			1335 1644			1430 1732		8 6		13 12	16 15	19 18	23 21	$\frac{26}{24}$	29 27
16 17 18	1761 2041 2304 2553 2788	2068 2330 2577	$2095 \\ 2355 \\ 2601$	1847 2122 2380 2625 2856	$2148 \\ 2405 \\ 2648$	2672		2227 2480 2718	2253 2504	2014 2279 2529 2765 2989		65554	8 7 7	11 10 9	13 12 12	16 15 14	18 17 16	22 21 20 19 18	2:
	3010 3222 3424 3617 3802	3032 3243 3444 3636	3054 3263 3464 3655	3075 3284 3483 3674 3856	3096 3304 3502 3692	3118 3324 3522 3711	3139 33 4 5	3160 3365 3560 3747	3181 3385 3579	3201 3404 3598 3784	1 4 4 4 4	4 4 4 4	6 6	8 8 8 7	11 10 10 9	13 12 12 11	15 14 14 13	17 16 15	13
25 26 27 28 29	3979 4150 4314 4472 4624	3997 4166 4330 4487	4014 4183 4346 4502	4031 4200 4362 4518 4669	4048 4216 4378 4533	4065 4232	4082 4249 4409 4564	4099 4265 4425 4579	4116	4133 4298 4456 4609	000000	3 3 3 3	5 5 5	7 7 6 6 6	9 8 8 8 7	10 10 9	12 11 11	14 13 13 12 12	18
30 31 32 33 34	4771 4914 5051 5185 5315	4928 5065 5198	4942 5079 5211	4814 4955 5092 5224 5353	4969 5105 5237	4843 4983 5119 5250 5378	4997 5132 5263	5011 5145 5276	$\frac{5159}{5280}$	5038 5172	1	3 3 3 3	4		7 7 7 6 6	9 8 8 8	10 9 9	11 11 11 10 10	1:
38	5441 5563 5682 5798 5911	5575 5694 5809	5587 5705 5821	5478 5599 5717 5832 5944	5611 5729 5843	5502 5623 5740 5855 5966	5635 5752 5866	5647 5763 5877	5539 5658 5775 5888 5999	5670 5786 5899	1	24 24 24 24 24	3	5 5 5	6 6 6 5	7 7 7 7 7	8 8 8		
41 42 43	6021 6128 6232 6335 6435	6138 6243 6345	6149 6253 6355	6053 6160 6263 6365 6464	6170 6274 6375		6191	6201 6304 6405	6107 6212 6314 6415 6513	6222 6325 6425	1	24 24 24 24 24	3	4 4 4	5 5 5 5 5	6 6 6 6	7 7 7	- 8 - 8 - 8	9
45 46 47 48 49	6532 6628 6721 6812 6902	6637 6730 6821	6646 6739 6830	6561 6656 6749 6839 6928	6665 6758 6848 6937	6675 6767 6857 6946	6590 6684 6776 6866 6955	6693 6785 6875 6964	6702 6794 6884 6972	6893 6893	1	22222	3 3 3 3	4 4	5 5 5 4 4	6 6 5 5 5	7 6 6	7 7 7	
50 51 52 53 54	6990 7076 7160 7243 7324	7084 7168 7251	7093 7177 7259	7016 7101 7185 7267 7348	7024 7110 7193 7275	7118 7202 7284	7042 7126 7210 7292 7372	7050 7135 7218 7300	$7226 \\ 7308$		1	2 2 2 2 2	3 2 2	3	4 4 4 4 4	5 5 5 5 5	6 6 6	7 7 6	

7435 7443 7451

7412 7419 7427

Nat.

Nos.

 9547 9552 9557

9595 9600 9605

9643 9647 9652

9689 9694 9699

9736 9741 9745

9782 9786 9791

9827 9832 9836

9872 9877 9881

9917 9921 9926

		100 1220 1202	1 700 1 700 1 717 1	, , , , ,	0 1	J	J	•
7482	7490 7497 7505	7513 7520 7528	7536 7543 7551	1 2 2	3 4	5	5	6
7559	7566 7574 7582	7589 7597 7604	7612 7619 7627	1 2 2	3 4	5	5	6
7634	7642 7649 7657	7664 7672 7679	7686 7694 7701	112	3 4	4	5	6
7709	7716 7723 7731	7738 7745 7752	7760 7767 7774	112	3 4	.4	5	6
			1 1 1				_	-
7782	7789 7796 7803	7810 7818 7825	7832 7839 7846	112	3 4	4	5	6
7853	7860 7868 7875	7882 7889 7896	7903 7910 7917	112	3 4	4	5	6
7924	7931 7938 7945	7952 7959 7966	7973 7980 7987	112	3 3	4	5	6
7993	8000 8007 8014	8021 8028 8035	8041 8048 8055	112	3 3	4	5	5
8062	8069 8075 8082	8089 8096 8102	8109 8116 8122	1 1 2	3 3	4	5	5
	7482 7559 7634 7709 7782 7853 7924 7993	$ \begin{array}{c cccc} 7482 & 7490 & 7497 & 7505 \\ 7559 & 7566 & 7574 & 7582 \\ 7634 & 7642 & 7649 & 7657 \\ 7709 & 7716 & 7723 & 7731 \\ 7782 & 7789 & 7796 & 7803 \\ 7853 & 7860 & 7868 & 7875 \\ 7924 & 7931 & 7938 & 7945 \\ 7993 & 8000 & 8007 & 8014 \\ \end{array} $	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$					

LOGARITHMS.

7459 7466 7474

'n

Proportional Parts.

2 2 7 7

7853	7860	7868	7875	7882	7889	7896	7903	7910	7917	1	1	2	3	4	4	5
7924	7931	7938	7945	7952	7959	7966	7973	7980	7987	1	1	2	3	3	4	5
7993	8000	8007	8014	8021	8028	8035	8041	8048	8055	1	1	2	3	3	4	5
8062	8069	8075	8082	8089	8096	8102	8109	8116	8122	1	1	2	3	3	4	5
								<u> </u>							-	
8129	8136	8142	8149	8156	8162	8169	8176	8182	8189	1	1	2	3	3	4	5
8195	8202	8209	8215	8222	8228	8235	8241	8248	8254	1	1	2	3	3	4	5
8261	8267	8274	8280	8287	8293	8299	8306	8312	8319	1	1	2	3	3	4	5
8325	8331	8338	8344	8351	8357	8363	8370	8376	8382	1	1	2	3	3	4	4
8388	8395	8401	8407	8414	8420	8426	8432	8439	8445	1	1	2	2	3	4	4
	1															
8451	8457	8463	8470	8476	8482	8488	8494	8500	8506	1	1	2	2	3	4	4
10-10	1	~=~=	0 204	11 0-0-	0 = 10	0 2 40	11 0 = = =	0 201	0 - 0 -		-	•	١ ۵	•	4	

J + U U	0202	0200	0220	11 022		0,0200	- 11	~	~~~	0201		-	_		•	-	•	•	
3261	8267	8274	8280	828	37 829	3 8299		8306	8312	8319	1	1	2	3	3	4	5	5	
3325	8331	8338	8344	83	835	7 8363	11	8370	8376	8382	1	1	2	3	3	4	4	5	
3388	8395	8401	8407	84	4 842	0 8426	Ш	8432	8439	8445	1	1	2	2	3	4	4	5	
				11	-		- 11			Į						- 1			
3451	8457	8463	8470	847	6 848	2 8488	Ш	8494	8500	8506	1	1	2	2	3	4	4	5	
3513			8531	853	7 854	3 8549	- 11	8555	8561	8567	1	1	2	2	3	4	4	5	
3573	8579	8585	8591	859	7 860	3 8609	-	8615	8621	8627	1	1	2	2	3	4	4	5	
3633			8651	86	7 866	3 8669	Ш	8675	8681	8686	1	1	2	2	3	4	4	5	
3692			8710	87	6 872	2 8727		8733	8739	8745	1	1	2	2	3	4	4	5	
		0.01					_ -				_					_			_
3751	8756	8762	8768	877	4 877	9 8785	- -	8791	8797	8802	1	1	2	2	3	3	4	5	
2000			8825			7 8849				8850	ī	î	5	9	2	2	Ã	Ē	

70	8451	8457	8463	8470	8476	8482	8488	8494	8500	8506	1	1	2	2	3	4	4	5	
71	8513	8519	8525	8531	8537	8543	8549	8555	8561	8567	1	1	2	2	3	4	4	5	
72	8573	8579	8585	8591	8597	8603	8609	8615	8621	8627	1	1	2	2	3	4	4	5	
73	8633	8639	8645	8651	8657	8663	8669	8675	8681	8686	1	1	2	2	3	4	4	5	
74	8692	8698	8704	8710	8716	8722	8727	8733	8739	8745	1	1	2	2	3	4	4	5	
																			_
75	8751	8756	8762	8768	8774	8779	8785	8791	8797	8802	1	1	2	2	3	3	4	5	
76	8808	8814	8820	8825	8831	8837	8842	8848	8854	8859	1	1	2	2	3	3	4	5	
77	8865	8871	8876	8882	8887	8893	8899	8904	8910	8915	1	1	2	2	3	3	4	· 4	
78	8921	8927	8932	8938	8943	8949	8954	8960	8965	8971	1	1	2	2	3	3	4	4	

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